Supporting Information

Screening RAFT agents and photocatalysts to mediate PET-RAFT polymerization using a high throughput approach

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| RAFT Agent | ΔH _{stab} (kJ mol ⁻¹) | ∆H _{frag} (kJ mol⁻¹) | RSE of R [•] (kJ mol ⁻¹) |
|------------|--|-------------------------------|---|
| R1 | 59.4 | -4.4 | 41.3 |
| R2 | 59.4 | -4.4 | 59.0 |
| R3 | 59.4 | -4.4 | 54.9 |
| R4 | 86.8 | -44.3 | 41.3 |
| R5 | 41.3 | 21.0 | 59.0 |
| R6 | 47.9 | -5.5 | 31.9 |
| R7 | 45.0 | -3.2 | 59.0 |
| R8 | 90.6 | -32.7 | 59.0 |
| R9 | 90.6 | -32.7 | 31.9 |
| R10 | 90.6 | -32.7 | 31.9 |

Table S1. Enthalpy values of RAFT stability (ΔH_{stab}), the fragmentation efficiency (ΔH_{frag}), and the radical stabilization energy (RSE•) of the leaving R group radicals (kJ/mol) for the various RAFT agents.

Note: The values of ΔH_{stab} , ΔH_{frag} , and RSE of R^{\bullet} (kJ/mol) for RAFT agents were collected from the literature.^{1, 2}

The ΔH_{stab} and ΔH_{frag} of R1 are 59.4 kJ/mol and -4.4 kJ/mol, with respect to S(CH₂)₂CH₃ group. RSE of R• for the R group (CH(CH₃)COOH) of R1 = 41.3 kJ/mol.

The ΔH_{stab} and ΔH_{frag} of R2 are 59.4 kJ/mol and -4.4 kJ/mol, with respect to S(CH₂)₁₁CH₃ group. RSE of R• for the R group (C(CH₃)(CN)(CH₂)₂COOH) of R2 \approx 59.0 kJ/mol, based on C(CH₃)₂CN.

The ΔH_{stab} and ΔH_{frag} of R3 are 59.4 kJ/mol and -4.4 kJ/mol, with respect to S(CH₂)₁₁CH₃ group. The RSE of R• for the R group C(CH₃)₂COOH of R3 \approx 54.9 kJ/mol, based on C(CH₃)₂COOCH₃.

The ΔH_{stab} and ΔH_{frag} of R4 are 86.8 kJ/mol and -44.3 kJ/mol, with respect to OCH₂CH₃ group. The RSE of R• for the R group CH(CH₃)COOCH₃ of R4 = 41.3 kJ/mol.

The ΔH_{stab} and ΔH_{frag} of R5 are 41.3 kJ/mol and 21.0 kJ/mol, with respect to C₆H₅ (phenyl) group. The RSE of R• for the R group C(CH₃)(CN)(CH₂)₂COOH of R5 \approx 59.0 kJ/mol. The ΔH_{stab} and ΔH_{frag} of R6 are 50.0 kJ/mol and -3.0 kJ/mol, with respect to 3,5-dimethyl-pyrazole group. The RSE of R• for the R group CH₂CN of R6 = 31.9 kJ/mol.

The ΔH_{stab} and ΔH_{frag} of R7 are 45.0 kJ/mol and -10.0 kJ/mol, with respect to 4-chloro-3,5-dimethylpyrazole group.

The RSE of R• for the R group (C(CH₃)(CN)CH₂CH₃) of R7 \approx 59.0 kJ/mol, based on C(CH₃)₂CN.

The ΔH_{stab} and ΔH_{frag} of R8 are 90.6 kJ/mol and -32.7 kJ/mol, with respect to methyl-*N*-(pyridin-4-yl) group. The RSE of R• for the R group (C(CH₃)(CN)CH₂CH₃) of R8 \approx 59.0 kJ/mol, based on C(CH₃)₂CN.

The ΔH_{stab} and ΔH_{frag} of R9 are 90.6 kJ/mol and -32.7 kJ/mol, with respect to methyl-*N*-(pyridin-4-yl) group. The RSE of R• for the R group CH₂CN of R9 = 31.9 kJ/mol.

The ΔH_{stab} and ΔH_{frag} of R10 are 90.6 kJ/mol and -32.7 kJ/mol, with respect to methyl-*N*-(phenyl) group. The RSE of R• for the R group CH₂CN of R10 = 31.9 kJ/mol.

| Table S2. | PET-RAFT p | olymerization of | f DMA mediate | d with ZnTF | PP (C1) as j | photocatalyst | conducted |
|-------------|----------------|------------------|----------------------|--------------------|---------------------|---------------|-----------|
| directly in | 96-well plates | 5. | | | | | |

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | <i>M</i> _w / <i>M</i> _n ^c |
|------|-----------------------|---|--|--|
| R1 | 96 | 9 800 | 9 700 | 1.18 |
| R2 | 94 | 9 700 | 11 900 | 1.09 |
| R3 | 91 | 9 400 | 9 300 | 1.19 |
| R4 | 86 | 8 800 | 9 200 | 1.42 |
| R5 | - | - | - | - |
| R6 | 94 | 9 600 | 10 800 | 1.16 |
| R7 | 90 | 9 200 | 9 400 | 1.15 |
| R8 | 28 | 3 100 | 10 100 | 1.65 |
| R8* | 67 | 6 900 | 8 100 | 1.33 |
| R9 | 83 | 8 500 | 11 500 | 1.55 |
| R9* | 93 | 9 500 | 12 100 | 1.28 |
| R10 | 12 | 1 400 | 14 900 | 1.68 |

Table S3. PET-RAFT polymerization of **DMA** mediated with **Cl-ZnTPP** (C2) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| R1 | 96 | 9 800 | 9 400 | 1.16 |
| R2 | 95 | 9 900 | 11 400 | 1.15 |
| R3 | 82 | 8 500 | 8 900 | 1.17 |
| R4 | 71 | 7 400 | 8 100 | 1.46 |
| R5 | - | - | - | - |
| R6 | 93 | 9 500 | 9 600 | 1.16 |
| R7 | 89 | 9 200 | 12 300 | 1.17 |
| R8 | 26 | 2 900 | 9 900 | 1.70 |
| R8* | 78 | 8 000 | 10 000 | 1.11 |
| R9 | 82 | 8 400 | 11 500 | 1.41 |
| R9* | 94 | 9 600 | 13 000 | 1.11 |
| R10 | 18 | 2 100 | 15 700 | 1.58 |

Table S4. PET-RAFT polymerization of **DMA** mediated with **F-ZnTPP (C3)** as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| R1 | 53 | 5 500 | 6 000 | 1.09 |
| R2 | 78 | 8 200 | 8 400 | 1.19 |
| R3 | 63 | 6 600 | 6 700 | 1.18 |
| R4 | 54 | 5 600 | 6 300 | 1.50 |
| R5 | - | - | - | - |
| R6 | 71 | 7 300 | 9 000 | 1.13 |
| R7 | 93 | 9 500 | 18 600 | 1.34 |
| R8 | 48 | 5 000 | 8 800 | 1.68 |
| R8* | 87 | 8 900 | 11 600 | 1.23 |
| R9 | 86 | 8 800 | 13 600 | 1.49 |
| R9* | 98 | 10 000 | 13 100 | 1.10 |
| R10 | 22 | 2 400 | 16 700 | 1.65 |

Table S5. PET-RAFT polymerization of **DMA** mediated with **Zn-TCPP (C4)** as photocatalyst conducted directly in 96-well plates.

| RAFT | αª (%) | $M_{n, { m th}}{}^{ m b}$ (g/mol) | M _{n,GPC} ^c (g/mol) | <i>M</i> _w / <i>M</i> _n ^c |
|------|-----------|-----------------------------------|--|--|
| R1 | 98 | 10 000 | 10 400 | 1.07 |
| R2 | 93 | 9 700 | 9 400 | 1.17 |
| R3 | 92 | 9 500 | 10 500 | 1.07 |
| R4 | 51 | 5 300 | 6 300 | 1.46 |
| R5 | - | - | - | - |
| R6 | 63 | 6 500 | 6 700 | 1.09 |
| R7 | 51 | 5 300 | 4 900 | 1.16 |
| R8 | 21 | 2 300 | 4 400 | 1.41 |
| R8* | 86 | 8 800 | 14 100 | 1.19 |
| R9 | 89 | 9 100 | 9 400 | 1.44 |
| R9* | 95 | 9 700 | 16 200 | 1.14 |
| R10 | 16 | 1 800 | 16 100 | 2.17 |

| Table S6. PET-RAFT polymerization of BzA mediated with ZnTPP (C1) as photocatalyst c | onducted |
|--|----------|
| directly in 96-well plates. | |

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | <i>M</i> _w / <i>M</i> _n ^c |
|------|-----------------------|---|--|--|
| R1 | 95 | 15 700 | 11 300 | 1.14 |
| R2 | 91 | 15 200 | 12 600 | 1.08 |
| R3 | 88 | 14 700 | 10 200 | 1.16 |
| R4 | 47 | 7 900 | 15 600 | 1.65 |
| R5 | - | - | - | - |
| R6 | 86 | 14 200 | 11 200 | 1.26 |
| R7 | 59 | 9 900 | 7 600 | 1.13 |
| R8 | 24 | 4 100 | 11 300 | 1.73 |
| R8* | 72 | 11 900 | 11 100 | 1.34 |
| R9 | 16 | 2 800 | 33 400 | 2.27 |
| R9* | 81 | 13 400 | 28 900 | 1.54 |
| R10 | 9 | 1 700 | 59 900 | 2.61 |

Table S7. PET-RAFT polymerization of BzA mediated with Cl-ZnTPP (C2) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| R1 | 92 | 15 200 | 10 800 | 1.13 |
| R2 | 86 | 14 300 | 11 800 | 1.13 |
| R3 | 92 | 15 300 | 10 600 | 1.11 |
| R4 | 39 | 6 600 | 14 700 | 1.58 |
| R5 | - | - | - | - |
| R6 | 85 | 14 100 | 11 100 | 1.24 |
| R7 | 77 | 12 800 | 9 700 | 1.08 |
| R8 | 19 | 3 300 | 3 900 | 1.40 |
| R8* | 63 | 10 500 | 10 900 | 1.33 |
| R9 | 13 | 2 400 | 30 900 | 2.42 |
| R9* | 82 | 13 500 | 24 400 | 1.46 |
| R10 | 17 | 4 700 | 84 400 | 1.84 |

Table S8. PET-RAFT polymerization of BzA mediated with F-ZnTPP (C3) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| R1 | 27 | 4 600 | 4 500 | 1.20 |
| R2 | 58 | 9 600 | 9 200 | 1.15 |
| R3 | 50 | 8 300 | 7 400 | 1.13 |
| R4 | 49 | 8 200 | 15 900 | 1.51 |
| R5 | - | - | - | - |
| R6 | 56 | 9 300 | 11 400 | 1.30 |
| R7 | 86 | 14 200 | 13 700 | 1.11 |
| R8 | 15 | 2 700 | 3 700 | 1.84 |
| R8* | 85 | 14 000 | 15 000 | 1.19 |
| R9 | 16 | 2 800 | 32 400 | 2.28 |
| R9* | 89 | 14 700 | 24 600 | 1.46 |
| R10 | 12 | 2 200 | 77 300 | 2.10 |

Table S9. PET-RAFT polymerization of **BzA** mediated with **Zn-TCPP (C4)** as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| R1 | 85 | 14 000 | 11 000 | 1.11 |
| R2 | 88 | 14 500 | 11 900 | 1.10 |
| R3 | 87 | 14 300 | 11 100 | 1.09 |
| R4 | 43 | 7 200 | 14 600 | 1.68 |
| R5 | - | - | - | - |
| R6 | 88 | 14 500 | 13 500 | 1.11 |
| R7 | 72 | 11 900 | 10 900 | 1.29 |
| R8 | 32 | 5 400 | 5 500 | 1.52 |
| R8* | 78 | 12 900 | 15 600 | 1.18 |
| R9 | 11 | 2 000 | 29 200 | 2.43 |
| R9* | 84 | 13 900 | 22 400 | 1.39 |
| R10 | 17 | 3 000 | 128 800 | 1.87 |

Table S10. PET-RAFT polymerization of **BzMA** mediated with **ZnTPP (C1)** as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| R1 | 66 | 11 900 | 15 400 | 1.79 |
| R2 | 71 | 12 800 | 12 600 | 1.26 |
| R3 | 62 | 11 200 | 14 100 | 1.75 |
| R4 | 14 | 2 700 | 211 900 | 2.27 |
| R5 | 25 | 4 600 | 5 200 | 1.21 |
| R6 | 31 | 5 700 | 49 600 | 1.97 |
| R7 | 49 | 8 900 | 17 500 | 1.66 |
| R8 | 18 | 3 400 | 11 600 | 1.49 |
| R8* | 65 | 11 700 | 17 200 | 1.33 |
| R9 | 5 | 1 200 | 107 800 | 1.73 |
| R9* | 41 | 7 500 | 25 600 | 1.48 |
| R10 | 6 | 1 300 | 182 100 | 2.10 |

| RAFT | α ^a (%) | M _{n,th} ^b (g/mol) | M _{n,GPC} c (g/mol) | <i>M_w/M_n^c</i> |
|------|-----------------------|---|---------------------------------|--|
| R1 | 56 | 10 100 | 21 900 | 1.70 |
| R2 | 67 | 12 200 | 11 900 | 1.31 |
| R3 | 55 | 9 900 | 41 700 | 1.64 |
| R4 | 19 | 3 600 | 296 900 | 1.72 |
| R5 | 23 | 4 300 | 4 900 | 1.22 |
| R6 | 24 | 4 500 | 232 800 | 1.82 |
| R7 | 47 | 8 500 | 19 600 | 1.44 |
| R8 | 13 | 2 500 | 9 400 | 1.47 |
| R8* | 61 | 11 000 | 27 800 | 1.54 |
| R9 | 8 | 1 600 | 28 400 | 2.29 |
| R9* | 44 | 8 000 | 65 200 | 1.76 |
| R10 | 7 | 1 500 | 54 200 | 2.66 |

 Table S11. PET-RAFT polymerization of BzMA mediated with Cl-ZnTPP (C2) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} b (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|------|-----------------------|--------------------------------|---------------------------------|---|
| R1 | 13 | 2500 | 57100 | 3.28 |
| R2 | 59 | 10600 | 11200 | 1.82 |
| R3 | 31 | 5700 | 24000 | 1.83 |
| R4 | 11 | 2200 | 50100 | 2.43 |
| R5 | 43 | 7800 | 9200 | 1.36 |
| R6 | 32 | 8000 | 31900 | 2.03 |
| R7 | 52 | 9400 | 15700 | 1.71 |
| R8 | 6 | 1300 | 23900 | 2.76 |
| R8* | 67 | 12100 | 18300 | 1.42 |
| R9 | 5 | 1100 | 62400 | 1.92 |
| R9* | 61 | 11000 | 55000 | 1.83 |
| R10 | 8 | 1600 | 66800 | 2.95 |

Table S12. PET-RAFT polymerization of BzMA mediated with F-ZnTPP (C3) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ⁵ (g/mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|--------------------------------|--|---|
| R1 | 33 | 6 100 | 40 100 | 2.31 |
| R2 | 55 | 10 100 | 9 000 | 1.29 |
| R3 | 38 | 7 000 | 26 600 | 1.93 |
| R4 | 18 | 3 400 | 198 100 | 2.28 |
| R5 | 17 | 3 200 | 3 600 | 1.20 |
| R6 | 21 | 3 900 | 104 600 | 2.22 |
| R7 | 42 | 7 600 | 15 800 | 1.63 |
| R8 | 8 | 1 600 | 81 300 | 2.57 |
| R8* | 72 | 13 000 | 22 100 | 1.40 |
| R9 | 4 | 900 | 136 600 | 2.13 |
| R9* | 49 | 8 900 | 27 600 | 1.87 |
| R10 | 9 | 1 800 | 233 700 | 2.08 |

Table S13. PET-RAFT polymerization of **BzMA** mediated with **Zn-TCPP (C4)** as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|---------------------------------|---|
| R1 | 65 | 9 500 | 21 400 | 1.81 |
| R2 | 75 | 11 100 | 24 200 | 1.28 |
| R3 | 74 | 10 900 | 24 400 | 1.41 |
| R4 | 37 | 5 500 | 112 400 | 1.70 |
| R5 | 21 | 3 200 | 11 700 | 1.11 |
| R6 | 56 | 8 200 | 96 700 | 1.85 |
| R7 | 69 | 10 100 | 27 100 | 1.12 |
| R8 | 22 | 3 300 | 12 200 | 1.36 |
| R8* | 68 | 9 900 | 25 600 | 1.15 |
| R9 | 35 | 5 200 | 13 200 | 1.46 |
| R9* | 62 | 9 100 | 75 800 | 1.56 |
| R10 | 29 | 4 400 | 140 600 | 1.65 |

Table S14. PET-RAFT polymerization of **HPMA** mediated with **ZnTPP** (C1) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|---------------------------------|---|
| R1 | 62 | 9 100 | 36 600 | 1.93 |
| R2 | 70 | 10 400 | 20 600 | 1.56 |
| R3 | 73 | 10 900 | 22 300 | 1.41 |
| R4 | 33 | 5 000 | 127 600 | 1.54 |
| R5 | 15 | 2 400 | 7 200 | 1.10 |
| R6 | 67 | 9 800 | 79 900 | 1.70 |
| R7 | 75 | 11 000 | 29 600 | 1.14 |
| R8 | 20 | 3 100 | 11 500 | 1.29 |
| R8* | 67 | 9 800 | 24 600 | 1.14 |
| R9 | 33 | 4 900 | 14 300 | 1.43 |
| R9* | 60 | 8 800 | 87 700 | 1.54 |
| R10 | 27 | 4 100 | 168 200 | 1.56 |

Table S15. PET-RAFT polymerization of **HPMA** mediated with **Cl-ZnTPP** (C2) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | $M_{n,\mathrm{th}}{}^\mathrm{b}$ (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|------|-----------------------|--|---------------------------------|---|
| R1 | 31 | 4 700 | 16 900 | 1.57 |
| R2 | 51 | 7 700 | 20 700 | 1.45 |
| R3 | 54 | 8 200 | 18 000 | 1.36 |
| R4 | 23 | 3 500 | 22 900 | 1.70 |
| R5 | 19 | 3 000 | 9 400 | 1.08 |
| R6 | 76 | 11 100 | 26 800 | 1.64 |
| R7 | 57 | 8 400 | 28 300 | 1.44 |
| R8 | 24 | 3 700 | 11 000 | 1.36 |
| R8* | 80 | 11 700 | 33 900 | 1.44 |
| R9 | 19 | 3 000 | 13 100 | 1.51 |
| R9* | 72 | 10 500 | 27 800 | 1.42 |
| R10 | 18 | 2 800 | 29 300 | 1.88 |

Table S16. PET-RAFT polymerization of **HPMA** mediated with **F-ZnTPP (C3)** as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|--|---|
| | 42 | 6 300 | 25 700 | 1.97 |
| R2 | 51 | 7 700 | 18 900 | 1.63 |
| R3 | 46 | 7 000 | 16 600 | 1.46 |
| R4 | 18 | 2 800 | 18 900 | 1.54 |
| R5 | 22 | 3 400 | 11 600 | 1.12 |
| R6 | 74 | 10 800 | 28 700 | 1.68 |
| R7 | 81 | 11 800 | 36 700 | 1.45 |
| R8 | 19 | 3 000 | 11 100 | 1.36 |
| R8* | 69 | 10 100 | 25 900 | 1.15 |
| R9 | 31 | 4 700 | 13 700 | 1.40 |
| R9* | 65 | 9 500 | 49 600 | 1.53 |
| R10 | 15 | 2 400 | 23 900 | 1.48 |

Table S17. PET-RAFT polymerization of **HPMA** mediated with **Zn-TCPP** (C4) as photocatalyst conducted directly in 96-well plates.

Table S18. PET-RAFT polymerization of BzMA mediated with ZnTPP (C1) as photocatalyst conducted in glass cuvettes in the absence and presence of oxygen.

| RAFT | αª (%) | M _{n,th} ^b (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|-----------------|-----------|---|---------------------------------|---|
| R2 ^d | 72 | 13 100 | 12 800 | 1.25 |
| R2 ^e | 77 | 14 000 | 13 500 | 1.16 |

| Catalyst | α ^a (%) | M _{n,th} ⁵ (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c | Time (min) |
|----------|-----------------------|--------------------------------|---------------------------------|---|------------|
| C1 | 27 | 2 900 | 2 600 | 1.12 | 15 |
| C1 | 52 | 5 400 | 5 900 | 1.08 | 30 |
| C1 | 71 | 7 300 | 8 000 | 1.08 | 60 |
| C1 | 91 | 9 300 | 9 900 | 1.06 | 120 |
| C2 | 17 | 1 900 | 1 700 | 1.11 | 15 |
| C2 | 42 | 4 400 | 4 400 | 1.07 | 30 |
| C2 | 62 | 6 400 | 6 700 | 1.08 | 60 |
| C2 | 84 | 8 600 | 10 100 | 1.06 | 120 |
| C3 | - | - | - | - | 15 |
| C3 | - | - | - | - | 30 |
| C3 | 7 | 900 | 1 800 | 1.14 | 60 |
| C3 | 19 | 2 100 | 2 300 | 1.17 | 120 |
| C4 | 11 | 1 300 | 1 200 | 1.04 | 15 |
| C4 | 38 | 4 000 | 3 400 | 1.09 | 30 |
| C4 | 55 | 5 700 | 6 100 | 1.07 | 60 |
| C4 | 78 | 8 100 | 11 000 | 1.10 | 120 |

Table S19. Polymerization kinetics of **BTPA (R1)** mediated by PET-RAFT polymerization of **DMA** conducted directly in 96-well plates using four different catalysts.

| Catalyst | α ^a (%) | M _{n,th} ⁵ (g/mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c | Time (min) |
|----------|-----------------------|--------------------------------|--|---|------------|
| C1 | 21 | 2 300 | 2 100 | 1.15 | 15 |
| C1 | 39 | 4 100 | 4 600 | 1.13 | 30 |
| C1 | 63 | 6 500 | 6 700 | 1.08 | 60 |
| C1 | 87 | 8 900 | 10 800 | 1.06 | 120 |
| C2 | 16 | 1 800 | 1 800 | 1.11 | 15 |
| C2 | 30 | 3 200 | 3 500 | 1.12 | 30 |
| C2 | 49 | 5 100 | 6 700 | 1.09 | 60 |
| C2 | 72 | 7 400 | 9 700 | 1.08 | 120 |
| C3 | 8 | 1 000 | 1 700 | 1.13 | 15 |
| C3 | 18 | 2 000 | 2 900 | 1.19 | 30 |
| C3 | 37 | 3 900 | 4 900 | 1.14 | 60 |
| C3 | 60 | 6 200 | 7 900 | 1.15 | 120 |
| C4 | 5 | 700 | - | - | 15 |
| C4 | 10 | 1 200 | - | - | 30 |
| C4 | 15 | 1 700 | 2 200 | 1.12 | 60 |
| C4 | 29 | 3 100 | 3 800 | 1.14 | 120 |

Table S20. Polymerization kinetics of **DTC1 (R6)** mediated by PET-RAFT polymerization of **DMA** conducted directly in 96-well plates using four different catalysts.

| Catalyst | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} ^c (g/mol) | M _w /M _n ^c | Time (min) |
|----------|-----------------------|---|--|---|------------|
| C1 | 8 | 1 000 | - | - | 15 |
| C1 | 10 | 1 200 | - | - | 30 |
| C1 | 42 | 4 500 | 6 100 | 1.10 | 60 |
| C1 | 74 | 7 600 | 10 200 | 1.06 | 120 |
| C2 | 4 | 700 | - | - | 15 |
| C2 | 8 | 1 100 | - | - | 30 |
| C2 | 36 | 3 900 | 6 800 | 1.12 | 60 |
| C2 | 63 | 6 500 | 9 400 | 1.11 | 120 |
| C3 | 19 | 2 100 | 7 000 | 1.11 | 15 |
| C3 | 41 | 4 300 | 12 600 | 1.22 | 30 |
| C3 | 67 | 6 900 | 16 900 | 1.25 | 60 |
| C3 | 85 | 8 700 | 18 100 | 1.36 | 120 |
| C4 | 2 | 500 | - | - | 15 |
| C4 | 5 | 800 | - | - | 30 |
| C4 | 9 | 1 200 | - | - | 60 |
| C4 | 17 | 2 000 | 1 900 | 1.10 | 120 |

Table S21. Polymerization kinetics of **DTC2 (R7)** mediated by PET-RAFT polymerization of **DMA** conducted directly in 96-well plates using four different catalysts.

Table S22. Apparent propagation rate (min⁻¹) measured for PET-RAFT polymerization of **DMA** mediated by ZnTPP (**C1**), Cl-ZnTPP (**C2**), F-ZnTPP (**C3**) and Zn-TCPP (**C4**) under green LED light ($\lambda_{max} = 530$ nm, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]₀ = 1.0 M) with reaction time of 2 h.

| | | K _p ^{app} (min⁻¹) |
|----|----|---------------------------------------|
| | R1 | 1.94 × 10 ⁻² |
| C1 | R6 | 1.71 × 10 ⁻² |
| | R7 | 1.26 × 10 ⁻² |
| | R1 | 1.52×10^{-2} |
| C2 | R6 | 1.04×10^{-2} |
| | R7 | 0.95 × 10 ⁻² |
| | R1 | 0.21×10^{-2} |
| C3 | R6 | 0.80×10^{-2} |
| | R7 | 1.59 × 10 ⁻² |
| | R1 | 1.27×10^{-2} |
| C4 | R6 | 0.27×10^{-2} |
| | R7 | 0.16 × 10 ⁻² |

| RAFT | α ^a (%) | M _{n,th} ^b (g∕mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|---------------------------------|---|
| R1 | 13 | 1 600 | 1 300 | 1.10 |
| R2 | 21 | 2 500 | 2 100 | 1.14 |
| R3 | 35 | 3 900 | 3 200 | 1.13 |
| R4 | 24 | 2 600 | 4 900 | 1.48 |
| R5 | - | - | - | - |
| R6 | 18 | 2 100 | 1 500 | 1.12 |
| R7 | 17 | 2 000 | 1 500 | 1.11 |
| R8 | 4 | 700 | - | - |
| R9 | 28 | 3 000 | 7700 | 1.69 |
| R10 | 6 | 900 | - | - |

 Table S23. PET-RAFT polymerization of DMA mediated with FTPP (non-metalated) as photocatalyst conducted directly in 96-well plates.

| RAFT | α ^a (%) | M _{n,th} ^b (g/mol) | M _{n,GPC} c (g/mol) | M _w /M _n ^c |
|------|-----------------------|---|---------------------------------|---|
| | 35 | 3 700 | 3 000 | 1.13 |
| R2 | 30 | 3 300 | 3 100 | 1.12 |
| R3 | 56 | 6 000 | 5 700 | 1.08 |
| R4 | 43 | 4 600 | 5 400 | 1.43 |
| R5 | - | - | - | - |
| R6 | 31 | 3 400 | 3 500 | 1.18 |
| R7 | 54 | 5600 | 5900 | 1.15 |
| R8 | 12 | 1 500 | - | - |
| R9 | 34 | 3 600 | 9 400 | 1.62 |
| R10 | 9 | 1 200 | - | - |

Table S24. PET-RAFT polymerization of **DMA** mediated with **TCPP** (non-metalated) as photocatalyst conducted directly in 96-well plates.



Figure S1. The Q-band absorption spectrum of C1 (ZnTPP), C2 (Cl-ZnTPP), C3 (F-ZnTPP) and C4 (ZnTCPP) recorded in DMSO and green LED emission ($\lambda = 530$ nm).



Figure S2. Digital image of the HT-PET RAFT wellplate polymerization setup.



Figure S3. Molecular weight distributions for *N*,*N*-dimethylacrylamide (DMA) polymers prepared using PET-RAFT polymerization conducted in 96-well plates. Polymerizations were conducted for 4 hours under green LED light ($\lambda_{max} = 530 \text{ nm}$, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]_0 = 1.0 M), catalyzed by different photocatalyst where (A) ZnTPP (C1), (B) Cl-ZnTPP (C2), (C) F-ZnTPP (C3), and (D) Zn-TCPP (C4).



Figure S4. Molecular weight distributions for benzyl acrylate (BzA) polymers prepared using PET-RAFT polymerization conducted in 96-well plates. Polymerizations were conducted for 4 hours under green LED light ($\lambda_{max} = 530 \text{ nm}$, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]_0 = 1.0 M), catalyzed by different catalyst where (A) ZnTPP (C1), (B) Cl-ZnTPP (C2), (C) F-ZnTPP (C3), and (D) Zn-TCPP (C4).



Figure S5. Molecular weight distributions for benzyl methacrylate (BzMA) polymers prepared using PET-RAFT polymerization conducted in 96-well plates. Polymerizations were conducted for 4 hours under green LED light ($\lambda_{max} = 530$ nm, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]₀ = 1.0 M), catalyzed by different catalyst where (A) ZnTPP, (B) Cl-ZnTPP, (C) F-ZnTPP, and (D) Zn-TCPP.



Figure S6. Molecular weight distributions for 2-hydroxylpropyl methacrylamide (HPMA) polymers prepared using PET-RAFT polymerization conducted in 96-well plates. Polymerizations were conducted for 24 hours under green LED light ($\lambda_{max} = 530 \text{ nm}$, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]_0 = 1.0 M), catalyzed by different catalyst where (A) ZnTPP, (B) Cl-ZnTPP, (C) F-ZnTPP, and (D) Zn-TCPP.



Figure S7. Molecular weight distributions for benzyl methacrylate (BzMA) polymers prepared using PET-RAFT polymerization conducted in glass cuvettes. Polymerizations were conducted for 4 hours under green LED light ($\lambda_{max} = 530$ nm, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]₀ = 1.0 M).



Figure S8. PET-RAFT polymerization of DMA conducted in 96-well plates irradiated under green LED light ($\lambda_{max} = 530 \text{ nm}, 5.5 \text{ mW/cm}^2$) targeted at ([DMA]:[BTPA]:[Catalyst] = 100:1:0.015 and [DMA]_0 = 1.0 M) using three different RAFT agents. Evolution of the GPC derived molecular weight and dispersity with monomer conversion conducted with **BTPA** RAFT agent using (**A**) C2, (**C**) C3, (**E**) C4 catalysts. The respective molecular weight distributions at various time points for the corresponding M_n versus conversion graph using different catalysts (**B**) C2, (**D**) C3, (**F**) C4.



Figure S9. PET-RAFT polymerization of DMA conducted in 96-well plates irradiated under green LED light ($\lambda_{max} = 530 \text{ nm}, 5.5 \text{ mW/cm}^2$) targeted at ([DMA]:[DTC1]:[Catalyst] = 100:1:0.015 and [DMA]_0 = 1.0 M) using three different RAFT agents. Evolution of the GPC derived molecular weight and dispersity with monomer conversion conducted with **DTC1** RAFT agent using (**A**) C2, (**C**) C3, (**E**) C4 catalysts. The respective molecular weight distributions at various time points for the corresponding M_n versus conversion graph using different catalysts (**B**) C2, (**D**) C3, (**F**) C4.



Figure S10. PET-RAFT polymerization of DMA conducted in 96-well plates irradiated under green LED light ($\lambda_{max} = 530 \text{ nm}, 5.5 \text{ mW/cm}^2$) targeted at ([DMA]:[DTC2]:[Catalyst] = 100:1:0.015 and [DMA]_0 = 1.0 M) using three different catalysts. Evolution of the GPC derived molecular weight and dispersity with monomer conversion conducted with DTC2 RAFT agent using (A) C2, (C) C3, (E) C4 catalysts. The respective molecular weight distributions at various time points for the corresponding M_n versus conversion graph using different catalysts (B) C2, (D) C3, (F) C4.



Figure S11. Electrostatic potential (ESP) surfaces for (A) R7 (DTC2), (B) R6 (DTC1), (C) R1 (BTPA), (D) C1 (ZnTPP) and (E) C3 (F-ZnTPP) respectively, calculated at the B3LYP-GD3BJ/def2-SVP level of theory with SMD-water solvation model.



Figure S12. Molecular weight distributions for *N*,*N*-dimethylacrylamide (DMA) polymers prepared using PET-RAFT polymerization conducted in 96-well plates. Polymerizations were conducted for 4 hours under green LED light ($\lambda_{max} = 530$ nm, 5.5 mW/cm²) targeted at ([Monomer]:[RAFT]:[Catalyst] = 100:1:0.015 and [Monomer]_0 = 1.0 M), catalyzed by non-metalated catalyst (A) FTPP, (B) TCPP.

Additional discussion on the interactions between C3 and RAFT agents

A peculiar result was observed for C3 (F-ZnTPP) and DTC2 (R7). Among all the ten RAFT agents, DTC2 (R7) exhibited the fastest polymerization kinetics in the presence of C3, almost twice the k_p^{app} of the DTC1 (R6) system and eight times the k_p^{app} of the BTPA (R1) system. The slow polymerization kinetics observed with BTPA mediated by C3 was ascribed to the highly electron withdrawing of fluorine substituents present on C3, which reduces the lowest triplet excited state (T₁) state of C3. The low T₁ state is unable to effectively activate BTPA (R1) and therefore the polymerization.³

To understand the unusual superiority of C3 over other photocatalysts to activate R7, we performed electrostatic potential (ESP) analysis for C1 (ZnTPP) and C3 (F-ZnTPP) to visualize the distribution of electrostatic potentials on their molecular surfaces. Molecular electrostatic potential maps illustrate information about the charge distribution of a molecule or electron distribution (SI, Figure S7). A region of higher-than-average electrostatic potential energy indicates the absence of negative charges, which means that there are fewer electrons in this region. In contrast, a negative electrostatic potential energy indicates rich electron domains. The presence of 20 highly electron-withdrawing -F atoms on the phenyl rings of F-ZnTPP (SI, Figure S7E) renders the middles of the four phenyl rings (site A) and the peripheral H atoms (site B) of porphyrin highly positively charged (ca. 15-16 kcal/mol). This is in stark contrast to those in ZnTPP (SI, Figure S7D) – the middles of the phenyl rings (site A) and peripheral H (site B) of porphyrin are negatively charged (electron rich). Meanwhile, we noted that DTC2 (R7) (SI, Figure S7A) has a strongly negative -CN group (site A, -27.6 kcal/mol). The presence of this negative charge on site A of DTC2 can interact with the positive sites A and B of F-ZnTPP. In addition, the electron-withdrawing effect of the -CN group is enhanced by its interaction with F-ZnTPP which affects the electron density of C-S bond, weakening the C-S bond in DTC2. Moreover, F-ZnTPP also exhibits a more positively charged Zn centre (site C, 24.6 kcal/mol) compared to ZnTPP with a much less positive Zn centre (site C, 11.6 kcal/mol). The negative dithioester-imidazole plane can also form π - π conjugation with one of the pentafluorophenyl groups.

To test this hypothesis, we optimized the geometry of the T_1 state of F-ZnTPP/DTC2 exciplex. The equilibrium geometry of the exciplex corresponds to the geometry proposed (see **Figure 5A**, middle), i.e., site **C** (Cl atom) of DTC2 binding with site **C** of F-ZnTPP, dithioester-imidazole plane stacked with the porphyrin plane and site **A** of DTC2 exhibiting electrostatic affinity with site A/B of F-ZnTPP. Subsequently, we performed climbing-image nudged elastic band (CI-NEB)⁴⁻⁶ calculations to optimize the reaction path for the activation of DTC2 via T_1 state F-ZnTPP. As shown in **Figure 5A**, the starting point of this reaction path has a C-S bond length of 1.88 Å whereas the ending point bears a C-S bond length of 3.25 Å, in which DTC2 cleaved to a dimethylcyano-carbon radical and a dithioester leaving group. Encouragingly, this reaction path exhibited an energy barrier of 13.8 kcal/mol, which is deemed sufficiently low for efficient activation of PET-RAFT polymerization.⁷

Secondly, we performed NEB calculations to optimize a reaction path for activation of DTC1 (R6) by F-ZnTPP (**Figure 5B**). Consistent with the experimental observation (lower k_p^{app} than F-ZnTPP/DTC2), the F-ZnTPP/DTC1 system bears a higher energy barrier of 25.9 kcal/mol. We attributed this difference of energy of DTC1 to DTC2 in two aspects: (i) DTC1 does not have a -Cl group capable to interact with Zn which does not decrease the C-S dissociation bond energy; (ii) the carbon radical generated by DTC1 is a cyano-carbon radical which is less stable than that of DTC2.

As for BTPA (R1), we found its equilibrium geometry possessed a negative region (site **A**, -18.8 kcal/mol) located in the carbonyl group but less negative than -CN of DTC2 and DTC1. However, unlike the strong interaction of -CN groups in DTC2 and DTC1, the interaction of the carbonyl acid group is reduced due to the adjacent methyl group due to steric hindrance, which reduces the interactions with **A** and **B** sites of F-ZnTPP. However, by rotation of the carbonyl group, we were still able to locate a low-energy configuration where the carbonyl group can interact with site **A** and **B** in F-ZnTPP. A reaction path was found for the F-ZnTPP/BTPA (**Figure 5C**) system as well which displayed a higher energy barrier of 28.0 kcal/mol than the other two systems, partly because of this weak interaction. This high energy barrier calculated by NEB is consistent with the experimental observation that the F-ZnTPP/BTPA system displayed the lowest k_p^{app} .

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