

Supporting Information

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Metal-induced microporous aminosilica creates a highly permeable gas-separation membrane

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Supporting Information

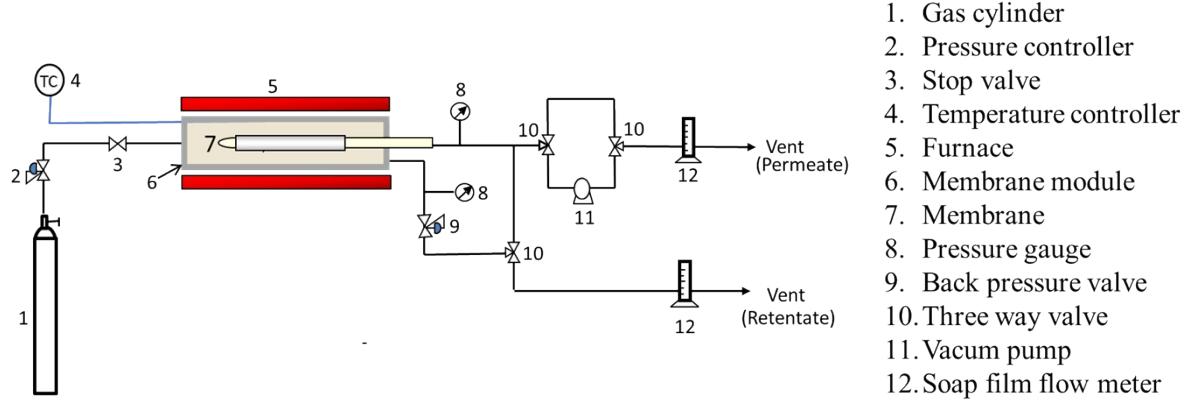


Fig. S1. Set-up single gas permeation equipment

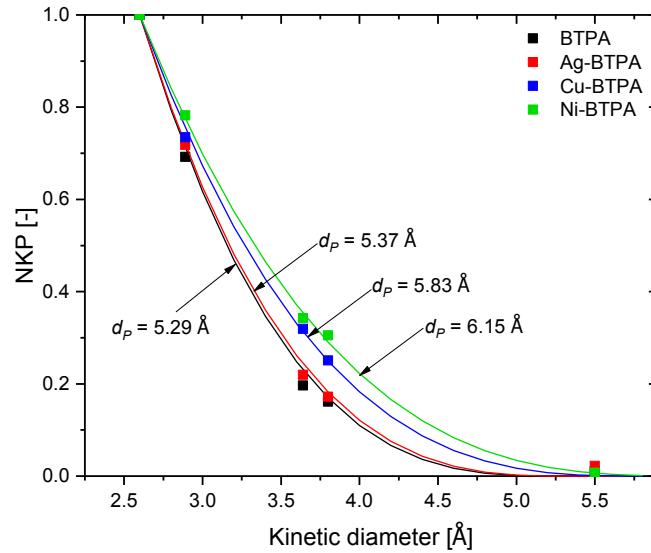


Fig. S2. Pore size prediction based on the NKP method of BTPA and metal-doped BTPA with different metals at 200 °C

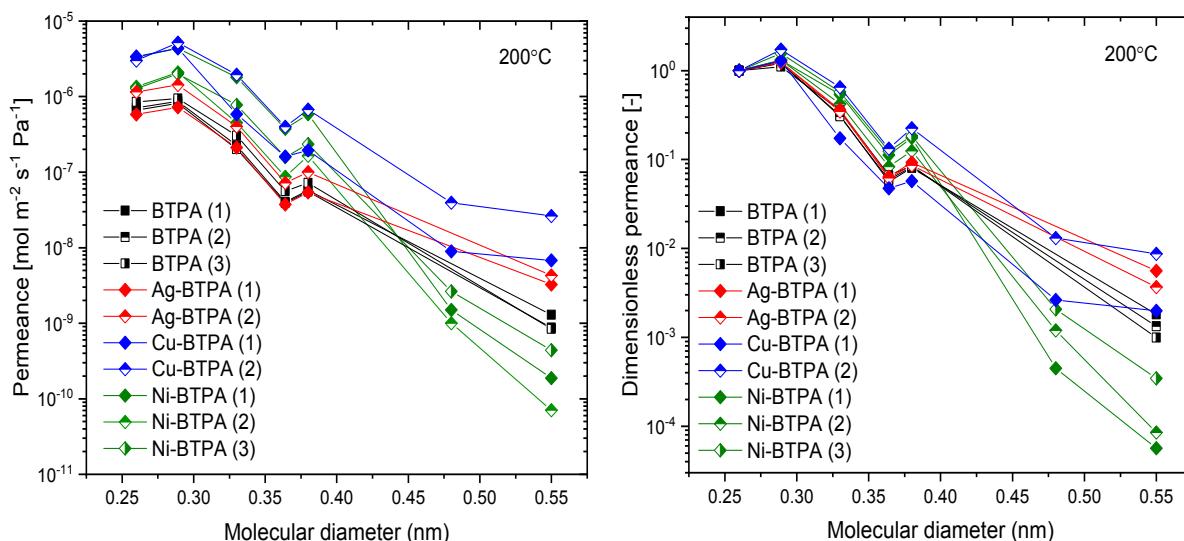


Fig. S3. Reproducible data of single gas permeance for Ni-BTPA as a function of kinetic diameter size of gases measured at 200 °C

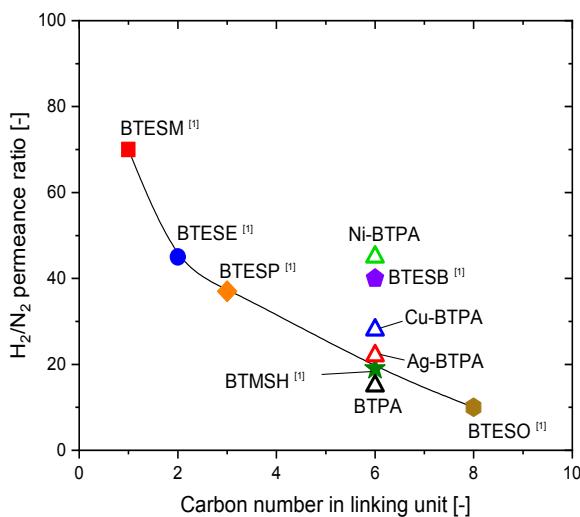


Fig. S4. permeance ratio of H_2/N_2 as a function of carbon number in linking unit of bi-silyl structure

Fig. S4. reveals that there has been a gradual decrease in the H_2/N_2 permeance ratio by increasing the number of carbon molecules between the bi-silyl bridges that gives rise to a higher flexibility in the linking unit [1]. BTPA has a structure that is similar to that of BTMSH (six carbon atoms in linking unit) and shows a H_2/N_2 permeance ratio of 15, which corresponds to the small pore size of the membranes. By contrast, after the addition of metal doping into the BTPA structure, a higher permeance ratio was achieved, which equates to an increase in membrane connectivity and in the rigidity of the linking unit via amine-metal interactions. The linking unit structure transforms from flexible into rigid with increases in the metal affinity.

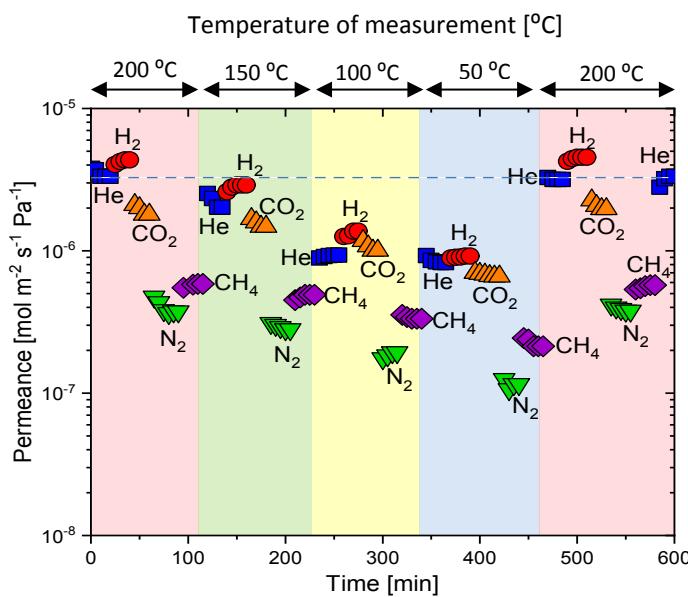


Fig. S5. Effective time courses for Ni-BTPA single-gas permeation performance at different operation temperature (200 °C → 150 °C → 100 °C → 50 °C → 200 °C)

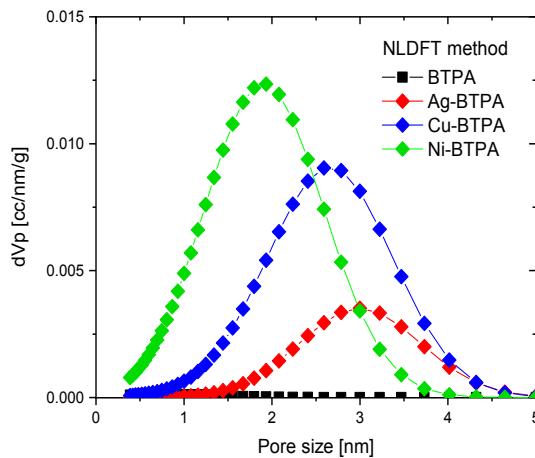


Fig. S6 NLDFT pore size distribution of amorphous aminosilica and metal-doped powder

According to the pore size distribution data in Fig. S6, as affinity for the metal-dopant increased, the pore size distribution narrowed as evident by a decrease in the full width at half maximum (FWHM) value in the NLDFT curve when fitted with a Gaussian function. In this case, the Ni-BTPA showed the most uniform pore size distribution while the BTPA and Ag-BTPA with highly maintained flexible amorphous material showed typically negligible and broad pore size distributions, respectively.

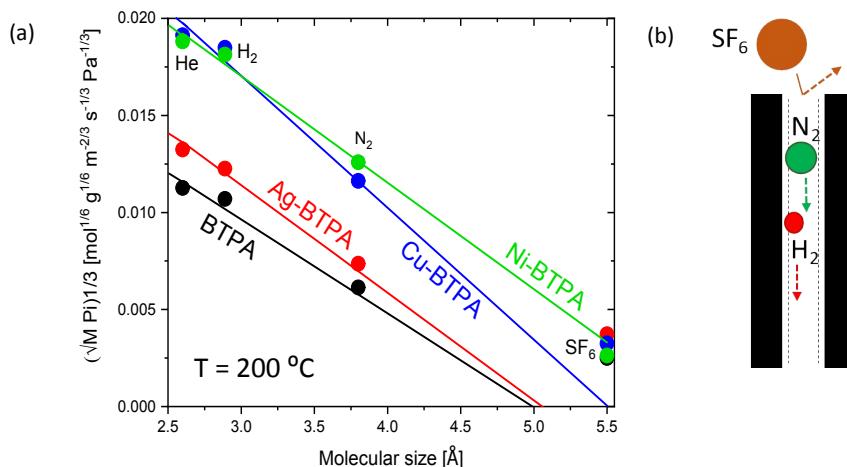


Fig. S7 The correlation of $(\sqrt{M_i} P_i)^{1/3}$ as a function of molecular size of permeating gases (points and lines are experimental and theoretically calculated, respectively) (a), and schematic gas transport for different gases in a cylindrical pore of Ni-BTPA (b).

The pore size of metal-doped BTPA-derived membranes was estimated by using modified-GT models, as shown in Eq. (1), where the functions of $(\sqrt{M_i} P_i)^{1/3}$ for different permeating gases were plotted as the sizes of the permeating gases (d_i). As shown in Fig. S7(a), experimental permeation reveals that the membrane pore size was enlarged on the order of Ni-BTPA (6.10 nm) > Cu-BTPA (5.51 nm) > Ag-BTPA (5.06 nm) > BTPA (4.89 nm). Fig. S7(b) presents a schematic illustration of gas transport within cylindrically shaped pores of Ni-BTPA. H₂ and N₂ were accepted within the Ni-BTPA pores, whereas a large gas such as SF₆ was rejected by the repulsive forces between neighboring membrane pore walls. H₂ as a smaller molecule tends to perform at a higher level of potential energy compared with that of N₂. On this occasion, the micropore diffusion rate was determined by the slower passage rate of N₂ through the membrane pore wall [5]. As reported for most microporous organosilica membranes, the gas separation factor is typically at a moderate level for H₂/N₂ separation with a relatively high rate of permeation

that relates to a thin topmost layer [5-7]. More importantly, the $(\sqrt{M_i} P_i)^{1/3}$ of most gases has been the best fit for Ni-BTPA membranes, which indicate that Ni-BTPA consist of uniform pores. On the other hand, other metal-doped BTPA showed points that deviated from the calculated lines, which indicated that the pore sizes were not uniform.

$$(\sqrt{M_i} P_i)^{1/3} = \left(\frac{k_0}{\sqrt{RT}} \exp\left(-\frac{E_{p,i}}{RT}\right) \right)^{1/3} (d_0 - d_i) \quad (1)$$

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Table S1. Summary of He/N₂ and He/SF₆ permeance ratio at 200 °C for different types of organosilica membranes

Membrane material	He/N ₂ [-]	He/SF ₆ [-]	Ref.
BTESE 6	5.62	1660	
BTESE 6	4.83	133	
BTESE 6	4.14	431	
BTESE 6	5.05	256	
BTESE 60	8.31	4710	
BTESE 60	6.43	7190	
BTESE 60	7.63	220	
BTESE 90	12.5	6310	
BTESE 90	6.99	155	
BTESE 120	25.5	9810	
BTESE 120	21.2	129	
BTESE 120	55.6	296	
BTESE 120	46.3	218	
BTESE 120	30.4	344	
BTESE 120	32.5	632	[5]
BTESE 120	33.1	4170	
BTESE 120	12.2	351	
BTESE 120	15.2	1000	
BTESE 120	11.9	4250	
BTESE 120	18.2	5600	
BTESE 120	25.9	9170	
BTESE 120	7.25	14300	
BTESE 120	10.2	42900	
BTESE 120	45.6	33500	
BTESE 120	21.8	865	
BTESE 120	25	14200	
BTESE 240	39.7	9350	
BTESE 240	28.4	40600	
BTESB	88	2600	[6]
BTESA	10	3300	[7]
BTPA	12	553	
BTPA	12	753	
BTPA	12	1010	
Ag-BTPA	11	178	
Ag-BTPA	12	272	This work
Cu-BTPA	17	502	
Cu-BTPA	4	115	
Ni-BTPA	9	17694	
Ni-BTPA	8	19148	

Table S2. Permeation data from different types of membranes for H₂/N₂ separation reported in the reference

Membrane type	Membrane material	H ₂ permeance [mol m ⁻² s ⁻¹ Pa ⁻¹]	$\frac{P_{H_2}}{P_{N_2}}$	Ref.
Aminosilica membranes	BTPA	8.63×10^{-7}	15	
	BTPA	9.41×10^{-7}	13	
	BTPA	8.10×10^{-7}	14	
	Ag-BTPA	1.43×10^{-6}	20	
	Ag-BTPA	1.10×10^{-6}	16	
	Cu-BTPA	4.36×10^{-6}	27	This work
	Cu-BTPA	8.63×10^{-7}	21	
	Cu-BTPA	4.45×10^{-6}	12	
	Ni-BTPA	2.10×10^{-6}	24	
	Ni-BTPA	2.01×10^{-6}	13	
	Ni-BTPA	4.45×10^{-6}	13	
Silica membranes (sol-gel)	TEOS (Tetraethylorthosilicate)	1.00×10^{-7}	31	[8]
	Co-TEOS	4.00×10^{-6}	730	[9]
	Fe/Co-TEOS	8.00×10^{-8}	11	[10]
	BTESE (1,2-bis(triethoxysilyl)ethane)	1.00×10^{-5}	20	[11]
	Zr-BTESE	1.80×10^{-7}	100	[12]
	TEOS	5.00×10^{-6}	300	[13]
	Ni-TEOS	6.30×10^{-8}	502	[14]
	Ni-TEOS	2.05×10^{-7}	400	[15]
	PCS (polycarbosilane) non-crosslinked	1.00×10^{-9} 6.00×10^{-9}	190 20	
	C-PCS (crosslinked polycarbosilane)	1.00×10^{-9} 3.00×10^{-9}	150 90	
Silica membranes (CVD)	PCS oxidized	5.00×10^{-9} 8.00×10^{-9}	800 200	[16]
	PS-dispersed PCS	2.00×10^{-8} 3.00×10^{-8}	200 100	
	TMOS (Tetramethoxysilane)	8.50×10^{-8}	1200	[17]
	Zr-TEOS	7.30×10^{-8}	25	[18]
	BTESA	2.68×10^{-6}	10	[7]
Porous silica based membranes	BTESE	9.50×10^{-7}	22	[19]
	BTESE-400 °C - 0.5 °C - 180min	2.90×10^{-7}	32	
	BTESE-600 °C - 0.5 °C - 180min	1.62×10^{-8}	4	
	BTESE-600 °C - 10 °C - 180min	1.70×10^{-8}	9	[20]
	BTESE-600 °C - 0.5 °C - 5min	4.61×10^{-8}	15	
	BTESEEthyl	1.27×10^{-7}	22	[7]
	BTESA	3.20×10^{-6}	12	[6]
	BTESAB	2.68×10^{-6}	10	[6]
	TEOS	2.00×10^{-6}	70	[9]
	TEOS	7.00×10^{-9}	23	[21]

Polymeric membranes	Poly(trimethylsilylpropyne)	5.41×10^{-6}	2	[24]
	Poly(tert-butyl acetylene)	3.85×10^{-7}	115	[25]
	Isotactic PMMA	4.32×10^{-10}	921	[26]
	Atactic PMMA	1.51×10^{-9}	385	[26]
	Syndiotactic PMMA	1.57×10^{-9}	362	[26]
	Poly[4-bis(trimethylsilyl-methyl styrene)]	1.61×10^{-7}	400	[24]
	Polybenzoxazinone imide (PBOI-2 Cu ⁺)	1.24×10^{-9}	960	[27]
	Polyimide (1,1-6FDA-DIA)	1.05×10^{-8}	165	[28]
	Polyimide (NTDA-BAPHFDS(H))	1.74×10^{-8}	141	[29]
	Poly(amide-imide)	2.41×10^{-8}	103	[30]
	PIM-7	2.88×10^{-7}	21	[31]
	PIM-1	1.00×10^{-7}	14	[31]
	Poly(trimethylsilylpropyne-cophenylpropyne)	1.34×10^{-7}	3	[32]
	Poly(trimethylsilylpropyne)	6.70×10^{-8}	3	[32]
Zolite membranes	PEI (Polyetherimide)	1.29×10^{-7}	2	
	PF (Phenol formaldehyde)	1.71×10^{-8}	32	
	PPESKPoly-(phthalazinone sulfone ketone)	2.54×10^{-7}	39	
		3.95×10^{-8}	174	
		3.40×10^{-7}	73	
	TMSPO (Trimethylsilyl-polyphenylene oxide)	6.17×10^{-7}	149	[33]
	PR (Phenolic resin)	1.73×10^{-8}	29	
	PPO 15 PVP (Poly phenylene oxide)	3.75×10^{-7}	165	
	SAPO-34	1.75×10^{-7}	4	[34]
	Zeolite	2.00×10^{-8}	53	[34]
MOF membranes	Zeolite-β	4.00×10^{-7}	67	[35]
	H-MFI + CCD	2.50×10^{-8}	140	[36]
	AM-2	4.50×10^{-9}	45	[37]
	AM-2	4.40×10^{-8}	40	[38]
	MFI + CVD	3.96×10^{-7}	63	[39]
	LTA	5.00×10^{-7}	5	[40]
	LTA	3.00×10^{-7}	4	[41]
	FAU	4.00×10^{-7}	6	[42]
	LTA	8.10×10^{-7}	7	[43]
	ZIF-8/ TiO ₂ disk	6.04×10^{-8}	12	[44]
CUBTC	ZIF-8/ α-Al ₂ O ₃ disk	2.35×10^{-7}	12	[45]
	ZIF-22/ APTES-modified TiO ₂ disk	1.60×10^{-7}	6	[46]
	ZIF-90/ APTES-modified TiO ₂ disk	2.48×10^{-7}	12	[47]
	ZIF-95/ APTES-modified α-Al ₂ O ₃ disk	2.16×10^{-7}	10	[48]
	ZIF-8/ ZnO activated α-Al ₂ O ₃ tubes	6.39×10^{-7}	8	[49]
	ZIF-8/ Organic ligand modified α-Al ₂ O ₃ disk	1.73×10^{-7}	12	[46]
	ZIF-94	4.20×10^{-9}	136	[50]
	ZIF-8	3.40×10^{-8}	2	[51]
	ZIF-8	3.40×10^{-8}	7	[52]
	CUBTC	1.58×10^{-6}	4	[53]

	ZIF-8		2.01×10^{-5}	9	[54]
	CUBTC		2.01×10^{-6}	5	[55]
	ZIF-7		2.00×10^{-9}	35	[56]
Mixed-matrix membrane	6FDA-durene	ZIF-71	1.52×10^{-6}	7	[57]
	PIM-1	Fumed-silica	7.20×10^{-8}	4	[58]
	PIM-1	ZIF-8	1.94×10^{-6}	15	[59]
	PIM-1	Silicalite-1MFI	3.00×10^{-7}	11	[60]
	PDMS41	CNT	2.65×10^{-8}	4	[61]
	Pebaxs	GO	2.79×10^{-9}	8	[62]
	Polyether	diamine	4.65×10^{-9}	9	[63]
	PEO	Silica	7.42×10^{-8}	4	[64]
	PEG	Silica	2.83×10^{-8}	4	[65]
	PTMSP	Fumed silica	5.48×10^{-8}	3	[66]
	PTMSP	TiO ₂	1.92×10^{-7}	3	[66]
	PTMSP	Trimethylsilylglucose	7.95×10^{-8}	11	[67]
	PMP	Fumed silica	4.78×10^{-8}	4	[68]
	PMP	TiO ₂	1.86×10^{-7}	4	[68]
	Teflon	AF	1.19×10^{-6}	5	[69]

Table S3. Permeation data from different types of membranes for N₂/SF₆ separation reported in the reference

Membrane type	Membrane material	Temperature [°C]	N ₂ permeance [mol m ⁻² s ⁻¹ Pa ⁻¹]	$\frac{P_{N_2}}{P_{SF_6}}$ [-]	Ref.
Aminosilica membranes	BTPA	200	5.63×10^{-8}	67	
	BTPA	200	3.92×10^{-8}	45	
	BTPA	200	4.04×10^{-8}	31	
	Ag-BTPA	200	4.07×10^{-8}	14	
	Ag-BTPA	200	7.18×10^{-8}	17	This work
	Cu-BTPA	200	3.76×10^{-7}	131	
	Cu-BTPA	200	5.55×10^{-7}	90	
	Ni-BTPA	200	1.65×10^{-7}	1223	
	Ni-BTPA	200	3.75×10^{-7}	1900	
	Ni-BTPA	200	2.55×10^{-7}	1041	
Polymeric membranes	3-aminopropyl trimethoxysilane (APrTMOS)	-	9.98×10^{-9}	11	[70]
	Poly(1-trimethylsilyl-1-propyne)	0	2.58×10^{-6}	3.3	[71]
	Poly(1-trimethylsilyl-1-propyne)	0	2.81×10^{-7}	0.4	[71]
	Poly(4-methyl-1-pentene)	40	3.41×10^{-9}	194	[72]
	Poly(4-methyl-1-pentene)	40	3.45×10^{-9}	242	[72]
	Polydimethylsiloxane	25	1.07×10^{-7}	1	[73]
	Polyimide	-	1.00×10^{-7}	46	[74]
	Polyether block amide (PEBAX)	25	3.08×10^{-9}	3	[73]
	Polycarbonate (Standard-PC)	50	1.91×10^{-9}	2	[75]
	Polyethersulfone	25	5.06×10^{-9}	6	[76]

	Polyimide (Matrimid)	40	1.34×10^{-9}	66	[77]
	Polyimide (PA4050-P3)	25	3.35×10^{-10}	44	[78]
	Polyimide	25	3.62×10^{-8}	100	[79]
	Polyimide	25	3.68×10^{-10}	39	[80]
	Polyimide (PA4050-P3)	25	3.35×10^{-10}	44	[75]
	Polysulfone	25	1.61×10^{-9}	24	[78]
	Polysulfone	25	2.28×10^{-9}	19	[80]
	Polysulfone (MF/1008P)	25	1.61×10^{-9}	23.6	[75]
	Tetra-bromo polycarbonate	25	2.21×10^{-9}	2.5	[80]
		45	2.96×10^{-9}	45	
	Polysulfone	35	2.51×10^{-9}	31	
		25	1.62×10^{-9}	24	
		45	2.74×10^{-9}	4	
	Tetrabromopolycarbonate	35	2.42×10^{-9}	3	[75]
		25	2.18×10^{-9}	3	
		45	7.33×10^{-10}	78	
	Polyimide	35	4.72×10^{-10}	57	
		25	3.26×10^{-10}	44	
		25	8.37×10^{-10}	39	
		50	1.21×10^{-9}	62	
		75	1.64×10^{-9}	92	
	Matrimid	100	2.11×10^{-9}	110	[77]
		125	2.81×10^{-9}	115	
		150	3.55×10^{-9}	112	
		175	4.42×10^{-9}	104	
		200	5.26×10^{-9}	96	
	Poly(4-methyl-1-pentene)	30	2.53×10^{-9}	476	
	Poly(4-methyl-1-pentene)	50	4.52×10^{-9}	165	[72]
	Poly(4-methyl-1-pentene)	55	5.02×10^{-9}	95	
	Poly(4-methyl-1-pentene)	60	5.59×10^{-9}	67	
	TEOS/BTPA 400	200	3.20×10^{-8}	320	
	TEOS/BTPA 500	200	5.54×10^{-9}	55	[81]
	TEOS/BTPA 600	200	4.10×10^{-8}	2	
	PrTMOS	200	5.00×10^{-10}	110	
	PrTMOS	300	7.00×10^{-9}	240	[82]
Silica membranes	TMOS	200	1.00×10^{-11}	3	
	BTESE-acid	200	3.00×10^{-8}	333	
	BTESE-swing	200	2.00×10^{-8}	200	[83]
	BTESE-100°C	100	7.00×10^{-9}	4	
	BTESE-200°C	100	7.00×10^{-8}	88	[84]
	BTESE-300°C	100	9.00×10^{-8}	113	
	MFI-12h	25	1.40×10^{-6}	25	
	MFI-6h	25	1.50×10^{-6}	75	
	MFI-3h	25	4.40×10^{-6}	40	
Zeolite membranes	MFI/S-1 (α - Al ₂ O ₃)	25	1.40×10^{-6}	40	
	MFI/ZSM-5 (α - Al ₂ O ₃)	25	2.94×10^{-6}	41	[85]
	MFI/ZSM-5 (CTI-Al ₂ O ₃ -TiO ₂)	25	2.50×10^{-6}	35	
	MFI/ZSM-5 (Al ₂ O ₃ -TiO ₂)	25	2.50×10^{-6}	30	
	MFI/ZSM-5 (α - Al ₂ O ₃)	25	3.70×10^{-6}	40	
	MFI/ZSM-5 (α - Al ₂ O ₃)	25	5.20×10^{-6}	40	

MFI/ZSM-5 (Inocermia- α - Al_2O_3)	25	3.80×10^{-6}	50	
MFI/S-1 (Hyflux- α - Al_2O_3)	25	8.20×10^{-7}	40	
MFI/S-1 (Hyflux- α - Al_2O_3)	25	7.60×10^{-7}	30	
Chabazite 130 °C	130	1.00×10^{-8}	3	
Chabazite 145 °C	130	1.60×10^{-8}	30	[86]
Chabazite 160 °C	130	8.00×10^{-9}	20	

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