

Supporting Information for
“Jacket temperature regulation allowing well-defined non-adiabatic lab-scale solution free radical polymerization of acrylates”

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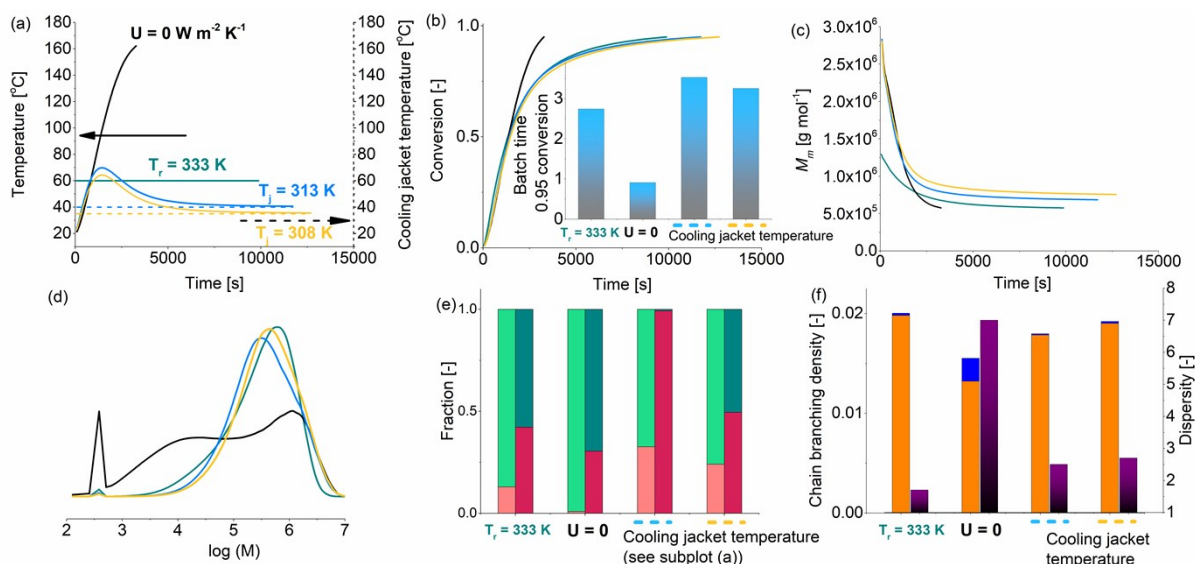


Figure S1. Comparing adiabatic and non-adiabatic reactor operations for solution free radical polymerization (FRP) of *n*-butyl acrylate (*n*BuA) with $[n\text{BuA}]_0 = 3.3 \text{ mol L}^{-1}$ and $T_{r,0} = 298 \text{ K}$ but applying the zeroth order initiation case with AIBN. Evolution of (a) reactor temperature (left axis) and jacket temperature (T_{jacket} ; right axis) as a function of time, (b) monomer conversion as a function of time as well the final batch time for 0.9 (monomer) conversion, (c) mass average molar mass M_n as a function of time and (d) molar mass distribution (MMD) ($w(\log M)$) format at a monomer conversion of 0.90; (e) fractions of macromonomer and dead polymer at a monomer conversion of 0.90 with light- green/red number fraction and dark-green/red: mass fraction, (f) left axis: orange and blue: short and long chain branching density at a monomer conversion of 0.90, (f) right axis in dark-purple dispersity at 0.90 monomer conversion; blue: $T_{\text{jacket}} = 313 \text{ K}$, yellow: $T_{\text{jacket}} = 308 \text{ K}$, black: adiabatic operation with U in Equation (1) equal to 0 instead of $100 \text{ W m}^{-2} \text{ K}^{-1}$ (the dimension of U is omitted in the figure), dark-cyan: isothermal (theoretical) at 313 K ; Arrhenius parameter in Table 1.

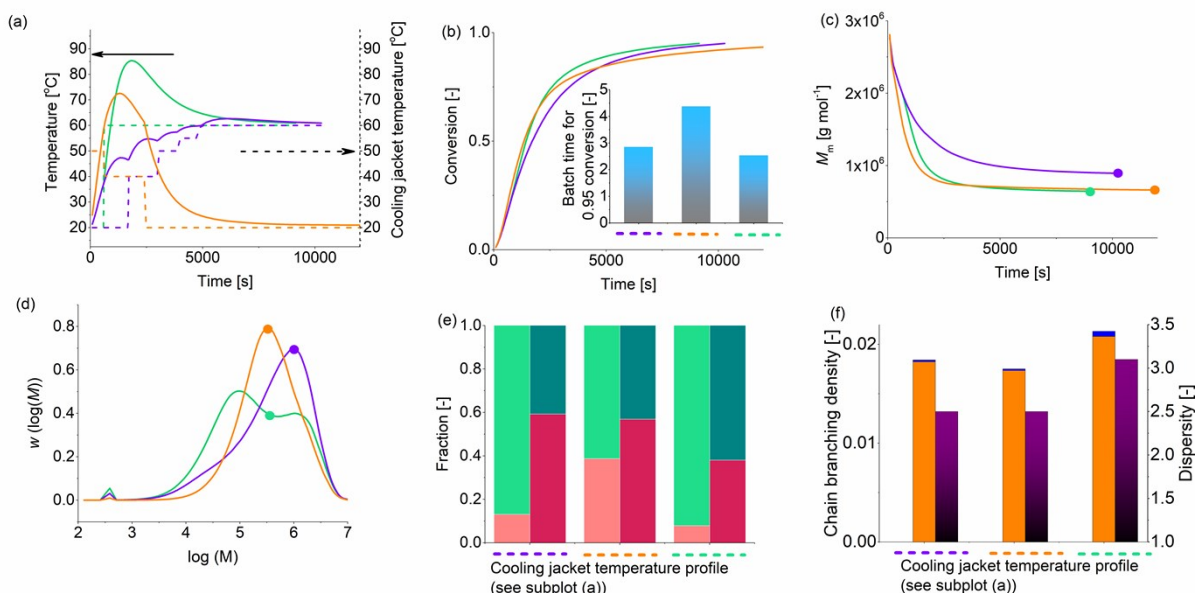


Figure S2. Same outline as in Supplementary Figure S1 considering three non-adiabatic cases with stepwise jacket temperature (T_{jacket}) control; orange: $T_{\text{jacket}} = 323, 313, 293 \text{ K}$, green: $T_{\text{jacket}} = 293, 333 \text{ K}$, violet $T_{\text{jacket}} = 293, 313, 323, 328, 333 \text{ K}$.

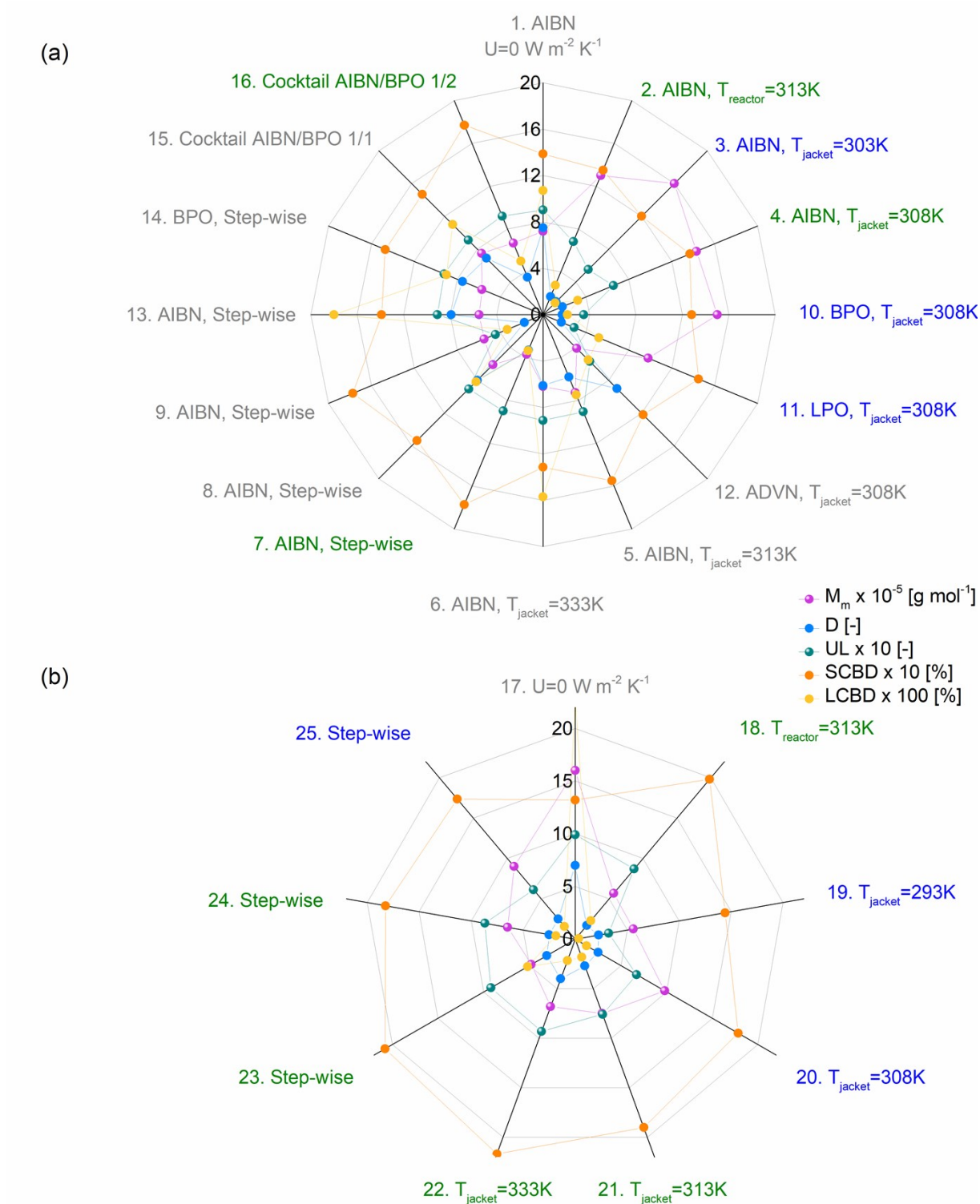


Figure S3. Radar charts with absolute data (normalized in Figure 11).

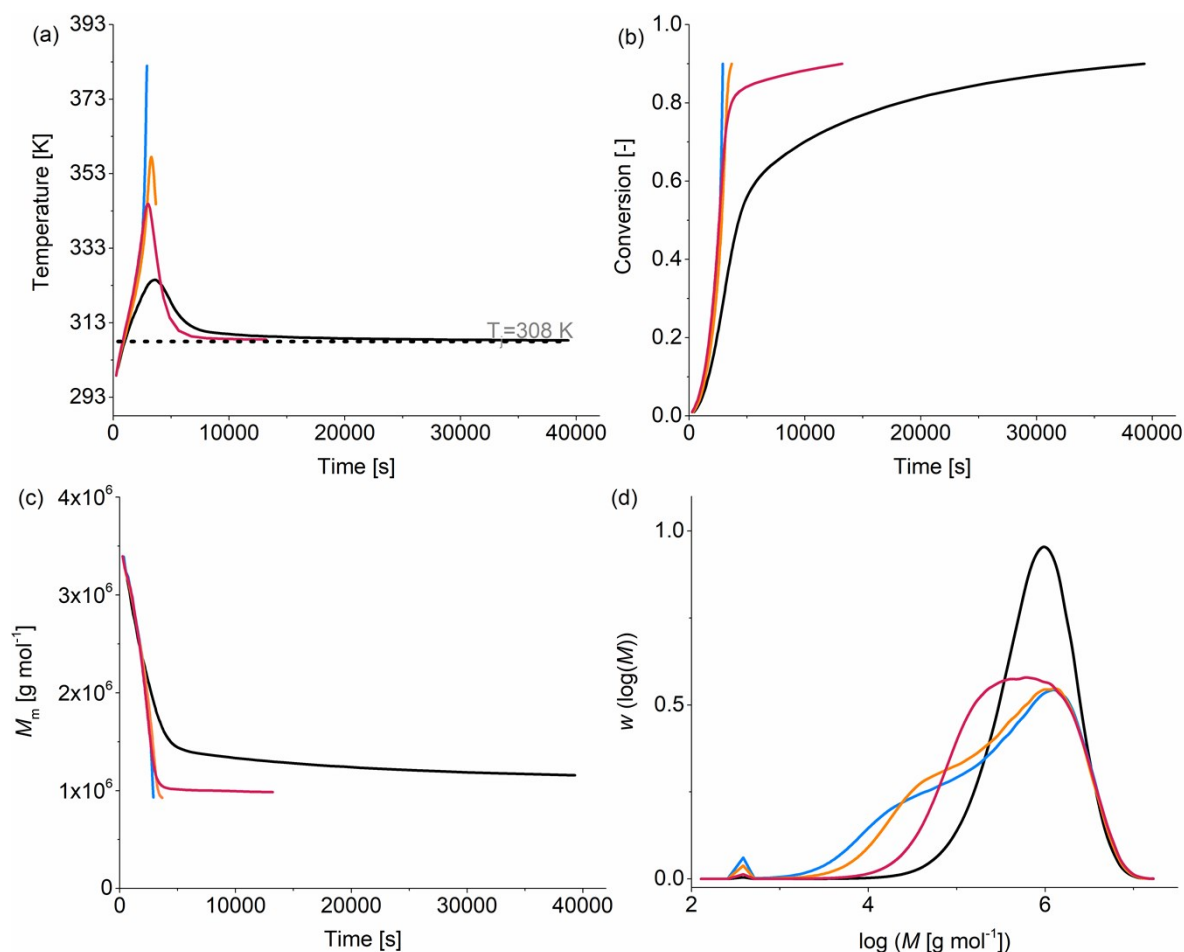


Figure S4: Influence of under/overestimated activation energies for backbiting and β -scission (while also varying pre-exponential factors) on the predicted: (a) reactor temperature, (b) monomer conversion, (c) mass average molar mass M_m as a function of time, and (d) log-molar mass distribution (MMD) at 0.9 monomer conversion; flat jacket temperature $T_{\text{jacket}} = 308$ K. All rate coefficients equal to the reference values listed in Table 1, except for: orange: $E_a^{\text{backbiting}} = 34.7$ kJ mol⁻¹, $A^{\text{backbiting}} = 1.6 \times 10^8$ s⁻¹ provided by Barth *et al.*¹ blue: $E_a^{\text{backbiting}} = 31.7$ kJ mol⁻¹, $A^{\text{backbiting}} = 4.48 \times 10^7$ s⁻¹ provided by Nikitin *et al.*² dark-red: $E_a^{\text{backbiting}} = 55.0$ kJ mol⁻¹, $A^{\text{backbiting}} = 2.8 \times 10^{11}$ s⁻¹ provided theoretically by Cuccato *et al.*³; black: reference values; $[M]_0 = 3.3$ mol L⁻¹; $[AIBN]_0 = 3 \times 10^{-3}$ mol L⁻¹ and $T_{r,0} = 298$ K; $U = 100$ W m⁻² K⁻¹.

References:

1. J. Barth, M. Buback, P. Hesse and T. Sergeeva, *Macromolecules*, 2010, **43**, 4023-4031.
2. A. N. Nikitin, R. A. Hutchinson, M. Buback and P. Hesse, *Macromolecules*, 2007, **40**, 8631-8641.
3. D. Cuccato, E. Mavrouidakis, M. Dossi and D. Moscatelli, *Macromolecular Theory and Simulations*, 2013, **22**, 127-135.