Electronic Supplementary Information

Bayesian based reaction optimization for complex continuous gas-liquid-solid reactions

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Table of contents

1. Analysis method

2. Sample chromatographs for the hydrogenation

3. Reaction pathways for the hydrogenation

4. Optimization routes of OVAT, Bayesian And modified Bayesian optimization for the hydrogenation

1. Analysis method

The sample is analyzed offline utilizing gas chromatography (Agilent, GC-8860) with an FID detector and an Agilent HP-5 column (length: 30 m, diameter: 0.32 mm, film thickness: 0.25 μ m). The samples are diluted with methanol (molar ratio: 1:5) and measured under the following conditions: the injection temperature, 280 °C; the column temperature, 50 ~ 110 °C, 20 °C/min, 110 ~ 150 °C, 10 °C/min, 150 °C, 4 min, 150 ~ 250 °C, 20 °C/min; the detector temperature, 280 °C. The sample volume for all analysis was 1 μ L. Based on these analytical conditions, the retention times of the reactants and products are as following: aniline: 3.6 min, nitrobenzene: 4.7 min, dichloroaniline: 5.8 min: 3,4-dichloronitrobenzene: 7.8 min; 3,4-dichloroaniline: 8.5 min: 5aminotetrahydroisoquinoline: 11.5 min, 5-aminoisoquinoline: 12.2 min, 5nitroisoquinoline: 12.5 azoxy compound (hydrogenation of 3.4min, dichloronitrobenzene): 13.3 min, azoxy compound (hydrogenation of 5nitroisoquinoline): 16.2 min.

2. Sample chromatograms for the hydrogenation

The sample chromatograms for the hydrogenation of nitrobenzene, 3,4-

chloronitrobenzene and 5-nitroisoquinoline are shown in Figure S1, Figure S2 and Figure S3 respectively.



Figure S1 The sample chromatography for the hydrogenation of nitrobenzene.



Figure S2 The sample chromatography for the hydrogenation of 3,4dichloronitrobenzene



Figure S3 The sample chromatography for the hydrogenation of 5-nitroisoquinoline

3. Reaction pathways for the hydrogenation

For the hydrogenation of 3,4-dichloronitrobenzene, the reduction of 3,4dichloronitrobenzene proceeds via the nitroso compound and hydroxylamine to 3,4dichloroaniline. Dehalogenation of the nitro raw material is possible to occur at any step during the reaction pathway, but the dehalogenation of the more electron-rich product (3,4-dichloroaniline) is commonly faster. Another pathway can accrue from condensation of these intermediates. For instance, nitroso and hydroxylamine intermediates can condense to form azoxy compounds. Besides, nitroso intermediate can also react with 3,4-dichloroaniline to form diazo compound. These compounds could be reduced to 3,4-dichloroaniline through a hydrazo intermediate, and the complex reaction pathways are depicted in Scheme S1.



Scheme S1 The reaction pathway for the hydrogenation of 3,4-dichloronitrobenzene While for the synthesis of 5-aminoisoquinoline, the over hydrogenation of pyridine may also appear during the reaction process except for the similar pathway described in the hydrogenation of 3,4-dichloronitrobenzene, and the reaction mechanism of 5nitroisoquinoline is depicted as Scheme S2.



Scheme S2 The reaction pathway for the hydrogenation of 5-nitroisoquinoline

4. Optimization routes of OVAT and Bayesian optimization for the hydrogenation

Optimization routes proposed by OVAT and Bayesian optimization of the hydrogenation of nitrobenzene, 3,4-dichloronitrobenzene and 5-nitroisoquinoline are listed in Table S1 - S6, respectively.

Experiment	Temperature	Hydrogen	Liquid flow rate	Conversion	Selectivity of	Yield of
number	/°C	pressure /MPa	/mL/min	/%	aniline /%	aniline /%
1	30.0	1.0	1.4	51.2	100.0	51.2
2	35.0	1.0	1.4	58.5	100.0	58.5
3	40.0	1.0	1.4	66.6	100.0	66.6
4	45.0	1.0	1.4	69.1	100.0	69.1
5	50.0	1.0	1.4	74.5	100.0	74.5
6	40.0	1.0	0.6	91.9	100.0	91.9
7	40.0	1.0	0.8	85.7	100.0	85.7
8	40.0	1.0	1.0	77.4	100.0	77.4
9	40.0	1.0	1.2	71.8	100.0	71.8
10	40.0	1.0	1.4	64.7	100.0	64.7
11	40.0	0.5	1.0	55.4	100.0	55.4
12	40.0	1.0	1.0	75.4	100.0	75.4
13	40.0	1.5	1.0	90.4	100.0	90.4
14	40.0	2.0	1.0	94.5	100.0	94.5
15	40.0	2.5	1.0	98.5	100.0	98.5

 Table S1 The OVAT optimization route for the hydrogenation of nitrobenzene

Reaction conditions: initial concentration: 0.2 mol/L, solvent: methanol, gas flow rate: 20 mL/min, catalyst: 0.5 wt% Pd/Al₂O₃, catalyst loading: 0.34 g (diluted by 1.36 g Al₂O₃).

Experiment	Temperature	Hydrogen	Liquid flow rate	Conversion	Selectivity of	Yield of
number	/°C	pressure /MPa	/mL/min	/%	aniline /%	aniline /%
1	30.0	1.0	1.0	68.1	100.0	68.1
2	40.0	1.0	1.0	75.4	100.0	75.4
3	50.0	1.0	1.0	85.5	100.0	85.5
4	40.0	0.5	1.0	55.4	100.0	55.4
5	40.0	2.5	1.0	98.5	100.0	98.5
6	40.0	1.0	0.6	91.9	100.0	91.9
7	40.0	1.0	1.6	61.0	100.0	61.0
8	44.8	2.5	0.6	99.8	99.1	98.9
9	35.1	2.5	0.6	99.7	100.0	99.7

 Table S2 Bayesian optimization route for the hydrogenation of nitrobenzene

Reaction conditions: initial concentration: 0.2 mol/L, solvent: methanol, gas flow rate: 20 mL/min, catalyst: 0.5 wt% Pd/Al₂O₃, catalyst loading: 0.34 g (diluted by 1.36 g Al₂O₃).

	Experiment	Temperature/	Hydrogen	Liquid flow rate	Conversion	Selectivity of	Yield of
	number	°C	pressure /MPa	/mL/min	/%	aniline /%	aniline /%
	1	40.0	1.0	1.0	77.4	100.0	77.4
Initial	2	44.0	1.0	1.0	92.2	100.0	92.2
simplex	3	40.0	1.5	1.0	90.4	100.0	90.4
	4	40.0	1.0	1.2	71.8	100.0	71.8
Lecal	5	42.7	1.3	0.8	99.1	100.0	99.1
	6	44.1	1.4	0.6	99.6	100.0	99.6
optimization	7	45.4	1.6	0.7	99.7	100.0	99.7

Table S3 The proposed Bayesian based optimization route for the hydrogenation of nitrobenzene

Reaction conditions: initial concentration: 0.2 mol/L, solvent: methanol, gas flow rate: 20 mL/min, catalyst: 0.5 wt% Pd/Al₂O₃, catalyst loading: 0.34 g (diluted by 1.36 g Al₂O₃).

Experiment	Temperature	Hydrogen	Liquid flow rate	Conversion	Selectivity	Yield of 3,4-
number	/°C	pressure /MPa	/mL/min	/%	/%	dichloroaniline /%
1	40.0	2.0	0.30	74.7	92.0	68.7
2	50.0	2.0	0.30	96.1	94.6	90.9
3	60.0	2.0	0.30	100.0	94.9	94.9
4	70.0	2.0	0.30	100.0	97.4	96.4
5	80.0	2.0	0.30	100.0	93.0	93.0
6	60.0	2.0	0.20	100.0	96.7	96.7
7	60.0	2.0	0.25	100.0	98.6	98.6
8	60.0	2.0	0.30	94.3	96.8	91.3
9	60.0	2.0	0.35	69.8	96.1	67.1
10	60.0	2.0	0.40	56.4	92.2	52.0
11	60.0	1.0	0.30	89.8	93.3	83.8
12	60.0	1.5	0.30	90.7	93.9	85.2
13	60.0	2.0	0.30	96.5	98.1	94.7
14	60.0	2.5	0.30	97.4	98.0	95.5
15	60.0	3.0	0.30	100.0	96.8	96.8

Table S4 The OVAT optimization route for the hydrogenation of 3,4-dichloronitrobenzene

Reaction conditions: initial concentration: 0.39 mol/L, solvent: methanol, gas flow rate: 20 mL/min, catalyst: 20 wt% Ni/SiO₂, catalyst loading:

1.88 g.

Experiment	Temperature	Hydrogen	Liquid flow rate	Conversion	Selectivity	Yield of 3,4-
number	/°C	pressure /MPa	/mL/min	/%	/%	dichloroaniline /%
1	40.0	2.0	0.30	74.7	92.0	68.7
2	60.0	2.0	0.30	100.0	94.9	94.9
3	80.0	2.0	0.30	100.0	93.0	93.0
4	60.0	2.0	0.20	100.0	96.7	96.7
5	60.0	2.0	0.40	56.4	92.2	52.0
6	60.0	1.0	0.30	89.8	93.3	83.8
7	60.0	3.0	0.30	100.0	96.8	96.8
8	60.0	2.5	0.20	100.0	93.6	93.6
9	59.6	2.8	0.20	100.0	92.4	92.4
10	59.5	2.2	0.20	100.0	94.3	94.3
11	53.3	1.7	0.23	99.7	98.5	98.2
12	52.3	1.5	0.25	99.5	96.6	96.1
13	75.4	2.9	0.30	100.0	83.0	83.0
14	52.8	1.4	0.34	99.3	91.6	91.0
15	52.7	1.9	0.22	100.0	98.3	98.3
16	53.2	2.3	0.40	90.8	97.4	88.4
17	59.5	1.4	0.30	99.5	97.9	97.4
18	59.0	1.7	0.34	100.0	98.0	98.0

 Table S5 Bayesian optimization route for the hydrogenation of 3,4-dichloronitrobenzene

Reaction conditions: initial concentration: 0.39 mol/L, solvent: methanol, gas flow rate: 20 mL/min, catalyst: 20 wt% Ni/SiO₂, catalyst loading: 1.88 g.

	Experiment	Temperature	Hydrogen	Liquid flow rate	Conversion	Selectivity	Yield of 3,4-
	number	/°C	pressure /MPa	/mL/min	/%	/%	dichloroaniline /%
	1	60.0	2.0	0.30	100	94.8	94.8
Initial	2	70.0	2.0	0.30	100	97.4	97.4
simplex	3	60.0	2.0	0.35	69.8	96.1	67.1
	4	60.0	2.5	0.30	100	95.5	95.5
	5	66.7	2.3	0.25	100	95.6	95.6
т 1	6	71.1	2.5	0.27	100	93.6	93.6
	7	62.8	2.1	0.29	100	94.6	94.6
optimization	8	68.3	2.4	0.28	100	92.4	92.4
	9	64.2	2.2	0.29	100	94.1	94.1
	10	40.0	1.0	0.20	73.8	95.5	70.5
C1 1 1	11	80.0	1.0	0.20	100	96.7	96.7
Global	12	80.0	3.0	0.40	100	97.3	97.3
optimization	13	80.0	3.0	0.20	100	94.7	94.7
	14	60.4	2.2	0.20	100	98.9	98.9

 Table S6 The proposed Bayesian based optimization route for the hydrogenation of 3,4-dichloronitrobenzene

15	70.5	2.5	0.22	100	99.1	99.1
16	70.7	1.8	0.40	99.8	98.4	98.2
17	67.5	2.6	0.20	100	97.9	97.9
18	80.0	2.0	0.31	100	99.1	99.1

Reaction conditions: initial concentration: 0.39 mol/L, solvent: methanol, gas flow rate: 20 mL/min, catalyst: 20 wt% Ni/SiO₂, catalyst loading: 1.88 g.

Experiment	Temperature	Hydrogen	Liquid flow rate	Gas flow rate	Conversion	Selectivity	Yield of 5-
number	/°C	pressure /MPa	/mL/min	/mL/min	/%	/%	aminoisoquinoline /%
1	40.0	2.0	0.30	20.0	98.1	99.1	97.2
2	50.0	2.0	0.30	20.0	99.0	93.5	92.6
3	60.0	2.0	0.30	20.0	99.6	87.4	87.1
4	70.0	2.0	0.30	20.0	100.0	81.6	81.6
5	80.0	2.0	0.30	20.0	100.0	76.3	76.3
6	60.0	2.0	0.20	20.0	99.6	92.4	92.1
7	60.0	2.0	0.30	20.0	99.8	93.7	93.4
8	60.0	2.0	0.40	20.0	100.0	95.3	95.3
9	60.0	2.0	0.50	20.0	100.0	96.5	96.5
10	60.0	2.0	0.60	20.0	100.0	97.6	97.6

Table S7 The OVAT optimization route for the hydrogenation of 5-nitroisoquinoline

11	60.0	2.0	0.70	20.0	99.2	98.2	97.5
12	60.0	2.0	0.80	20.0	99.6	98.6	98.2
13	60.0	2.0	0.90	20.0	100.0	98.9	98.9
14	60.0	2.0	1.00	20.0	98.3	99.3	97.5
15	60.0	2.0	1.10	20.0	96.8	99.2	96.1
16	60.0	1.0	0.30	20.0	98.0	97.8	95.9
17	60.0	1.5	0.30	20.0	98.0	97.0	95.1
18	60.0	2.0	0.30	20.0	100.0	94.8	94.8
19	60.0	2.5	0.30	20.0	100.0	94.1	94.1
20	60.0	3.0	0.30	20.0	100.0	93.2	93.2
21	60.0	2.0	0.30	15.0	100.0	94.5	94.5
22	60.0	2.0	0.30	20.0	99.3	93.5	92.8
23	60.0	2.0	0.30	25.0	99.4	93.8	93.3
24	60.0	2.0	0.30	30.0	99.4	94.1	93.5

Reaction conditions: initial concentration: 0.18 mol/L, solvent: tetrahydrofuran, catalyst: 5 wt% Pt/C, catalyst loading: 0.8 g.

Table S8 Bayesian optimization route for the hydrogenation of 5-nitroisoquinoline

Experiment	Temperature	Hydrogen	Liquid flow rate	Gas flow rate	Conversion	Selectivity	Yield of 5-
number	/°C	pressure /MPa	/mL/min	/mL/min	/%	/%	aminoisoquinoline /%
1	40.0	2.0	0.30	20.0	99.3	97.9	97.2

2	60.0	2.0	0.30	20.0	100.0	93.4	93.4	
3	60.0	2.0	0.60	20.0	100.0	97.6	97.6	
4	80.0	2.0	0.30	20.0	100.0	76.3	76.3	
5	60.0	1.0	0.30	20.0	100.0	95.9	95.9	
6	60.0	3.0	0.30	20.0	100.0	93.2	93.2	
7	60.0	2.0	0.20	20.0	100.0	92.1	92.1	
8	60.0	2.0	1.20	20.0	98.3	94.7	93.1	
9	60.0	2.0	0.30	15.0	100.0	94.5	94.5	
10	60.0	2.0	0.30	30.0	100.0	93.5	93.5	
11	48.0	1.0	1.20	15.0	94.2	92.4	87.0	
12	60.0	1.5	0.70	20.0	100.0	94.8	94.8	
13	40.0	2.8	0.20	27.0	99.1	98.4	97.5	
14	47.0	1.0	1.20	30.0	97.2	92.9	90.3	
15	40.0	2.4	0.30	26.0	99.6	98.8	98.4	
16	40.0	2.9	1.10	23.0	93.6	90.2	84.4	
17	40.0	2.9	0.20	26.0	100.0	95.9	95.9	
18	41.0	2.1	0.40	27.0	100.0	96.8	96.8	
19	40.0	1.9	0.70	27.0	100.0	97.0	97.0	
20	40.0	1.2	0.20	26.0	100.0	95.3	95.3	

Reaction conditions: initial concentration: 0.18 mol/L, solvent: tetrahydrofuran, catalyst: 5 wt% Pt/C, catalyst loading: 0.8 g.

	Experiment number	Temperatur e /°C	Hydrogen pressure /MPa	Liquid flow rate /mL/min	Gas flow rate /mL/min	Conversion /%	Selectivity /%	Yield of 5- aminoisoquinoline /%
	1	60.0	2.0	0.60	20.0	100.0	97.6	97.6
Initial	2	70.0	2.0	0.60	20.0	100.0	95.2	95.2
	3	60.0	2.4	0.60	20.0	100.0	98.4	98.4
simplex	4	60.0	2.0	0.80	20.0	100.0	98.2	98.2
	5	60.0	2.0	0.60	25.0	100.0	98.5	98.5
	6	50.0	2.2	0.70	22.5	100.0	99.4	99.4
	7	40.0	2.3	0.75	23.8	99.5	99.5	99.0
Local	8	55.0	2.3	0.75	23.8	100.0	99.5	99.5
optimization	9	52.5	2.5	0.83	25.7	100.0	99.5	99.5
	10	52.5	2.5	0.53	25.7	100.0	98.2	98.2
	11	54.4	2.4	0.60	24.3	100.0	98.4	98.4
	12	40.0	1.8	0.42	15.2	99.7	99.2	98.9
Global	13	40.0	2.8	1.04	29.9	99.2	98.4	97.6
optimization	14	40.2	1.3	0.57	15.4	100.0	99.4	99.4
	15	43.2	2.7	1.17	15.1	100.0	99.3	99.3

Table S9 The proposed Bayesian based optimization route for the hydrogenation of 5-nitroisoquinoline

Reaction conditions: initial concentration: 0.18 mol/L, solvent: tetrahydrofuran, catalyst: 5 wt% Pt/C, catalyst loading: 0.8 g.