

# One-pot transformation of furfural into $\gamma$ -valerolactone catalyzed by hierarchical Hf-Al-USY zeolite with balanced Lewis and Brønsted acid sites

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**Initial reaction rate:** In the present study, the initial reaction rate  $k_1$  for the target reaction was defined as moles of formed product divided by gram of catalyst per reaction time (conversion not exceeding 30%), as shown below.

For the reduction of FA to FOL,  $k_1$  ( $\text{molh}^{-1}\text{g}^{-1}$ ) =  
$$\frac{\text{moles of FOL formed}}{\text{amount of catalyst} \times \text{reaction time}}$$

For FOL conversion to IPL,  $k_2$  ( $\text{molh}^{-1}\text{g}^{-1}$ ) =

$$\frac{\text{moles of IPL formed}}{\text{amount of catalyst} \times \text{reaction time}} = \frac{\text{moles of GVL formed}}{\text{amount of catalyst} \times \text{reaction time}} \quad \text{For IPL lactonization to GVL, } k_3 \quad (\text{molh}^{-1}\text{g}^{-1}) =$$

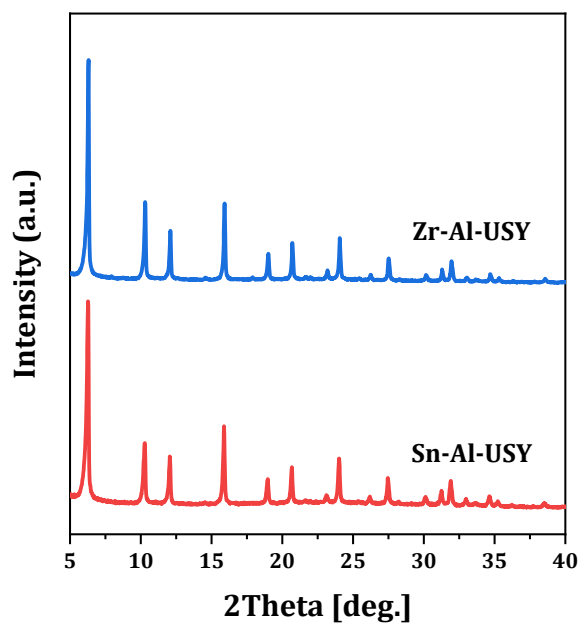


Fig. S1 XRD patterns of Sn-Al-USY and Zr-Al-USY.

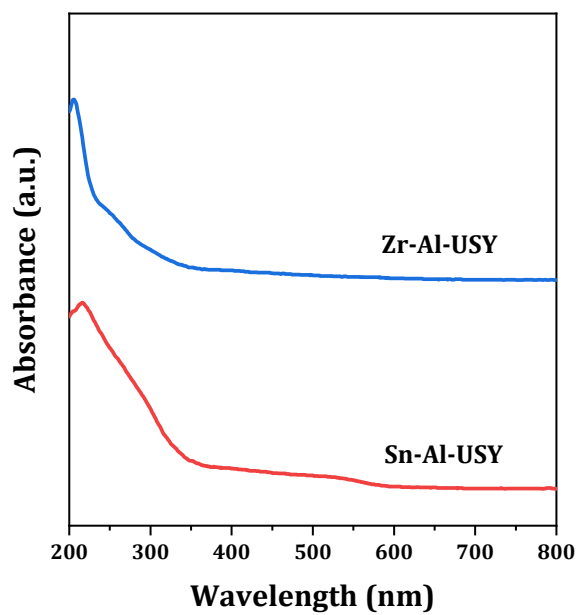
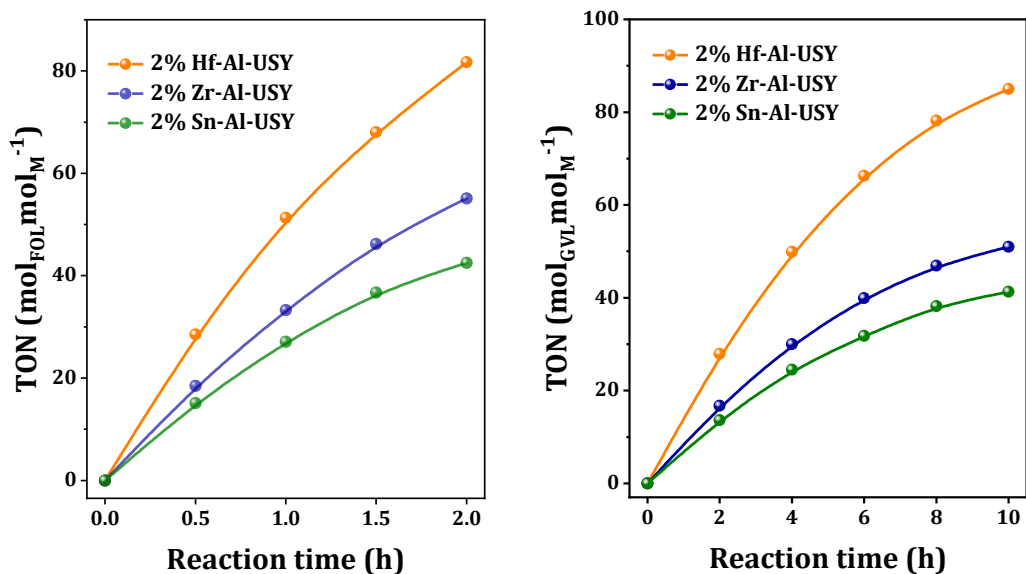
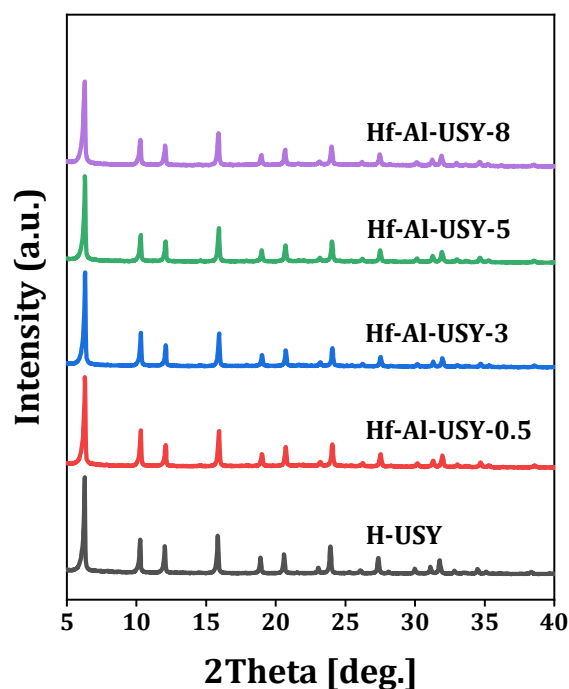


Fig. S2 UV-vis spectra of Sn-Al-USY and Zr-Al-USY.



**Fig. S3** Time-dependent conversion of FA (left chart) and LA (right chart) over 2% Hf-Al-USY, 2% Zr-Al-USY and 2% Sn-Al-USY zeolites. Reaction conditions: 1 mmol substrate, 5 mL solvent, 100 mg catalyst, 1.0 MPa N<sub>2</sub>; 373 K for FA conversion and 423 K for LA conversion, respectively.



**Fig. S4** XRD patterns of Hf-Al-USY zeolites prepared from different acid treatment time.

All the samples exhibited identical diffraction peaks with comparable intensity, indicating the framework integrity of USY framework during the post-synthesis procedures. Such a result can be explained by the fact that calcination of parent H-USY at a high temperature, i.e. 1073 K, can effectively improve its framework stability against destruction when treating with nitric acid aqueous solution.

**Table S1** Physicochemical properties of zeolite samples under study.

Sample	Surface area ( $\text{m}^2 \text{g}^{-1}$ )			Pore volume ( $\text{cm}^3 \text{g}^{-1}$ )		
	$S_{\text{BET}}$	$S_{\text{micro}}^{\text{a}}$	$S_{\text{meso}}$	$V_{\text{total}}$	$V_{\text{micro}}^{\text{b}}$	$V_{\text{meso}}$
H-USY	835	740	95	0.40	0.29	0.11
DeAl-USY	985	772	213	0.54	0.30	0.24
Hf-Al-USY-0.5 <sup>c</sup>	928	758	170	0.49	0.29	0.20
Hf-Al-USY-1 <sup>c</sup>	975	769	206	0.53	0.30	0.23
Hf-Al-USY-3 <sup>c</sup>	941	723	218	0.54	0.29	0.25
Hf-Al-USY-5 <sup>c</sup>	935	715	220	0.56	0.28	0.28
Hf-Al-USY-8 <sup>c</sup>	948	703	245	0.56	0.26	0.30
Sn-Al-USY	979	769	210	0.52	0.29	0.23
Zr-Al-USY	982	775	207	0.53	0.29	0.24

Hf-Al-USY-R <sup>d</sup>	763	628	135	0.45	0.27	0.18
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<sup>a</sup> The specific surface area was obtained by the BET method. <sup>b</sup> Calculated from the *t*-plot ( $t = [13.99/(0.034 - \log(p/p_0))]^{0.5}$ ) at a relative pressure  $p/p_0$  of 0.55-0.8. <sup>c</sup> Parent H-USY was treated with nitric acid solution at 358 K for *n* h ( $n = 0.5, 1, 3, 5, 8$ ). <sup>d</sup> Hf-Al-USY-R indicated reused Hf-Al-USY sample.