

### Electronic Supplementary Information

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**Table S1.** Empirical correlations to calculate H<sub>2</sub>, CO, CO<sub>2</sub> and CH<sub>4</sub> yields during pyrolysis.

Gas (vol %)	Empirical equation
Hydrogen	$0.04694T_p - 16.96286$
Carbon monoxide	$0.0371T_p + 19.961$
Carbon dioxide	$0.000143(T_p)^2 - 0.27808T_p + 139.948$
Methane	$-9 \times 10^{-5}(T_p)^2 + 0.1221T_p - 25.206$

\* T<sub>p</sub> = Pyrolysis temperature in degree Celsius

**Table S2.** Carbon balance with variable temperature from 800 to 1600 °C (at 30 wt % SS).

Temperature (°C)	Total input C (kg/h) (RDF = 7 kg/h and SS = 3 kg/h)	Output C in syngas (kg/h)	Output solid residual C (kg/h)	Total output C (kg/h)
800	4.9669	2.9237	2.0420	4.9657
1000	4.9669	3.1318	1.8350	4.9668
1200	4.9669	3.1409	1.8260	4.9669
1400	4.9669	3.1396	1.8260	4.9656
1600	4.9669	3.1397	1.8270	4.9667

**Table S3.** Carbon balance with variable sewage sludge concentration from 0 to 100 wt. % (at 1200 °C).

<b>Sewage sludge concentration (wt %)</b>	<b>Total input C (kg/h)</b>	<b>Output C in syngas (kg/h)</b>	<b>Output solid residual C (kg/h)</b>	<b>Total output C (kg/h)</b>
0	6.2170	2.6916	3.5250	6.2166
30	4.9669	3.1409	1.8260	4.9669
50	4.1335	2.9236	1.2010	4.1246
70	3.3001	2.2614	1.0380	3.2994
100	2.0500	2.0497	0.0000	2.0497