## **Supporting Information**

## Oxygen Evolution Catalysts under Proton Exchange Membrane Conditions in a Conventional Three Electrode Cell vs. Electrolyser Device: A Comparison Study and a 3D-Printed Electrolyser for Academic Labs

Michelle P. Browne<sup>ab#</sup>, James Dodwell<sup>c#</sup>, Filip Novotny<sup>a</sup>, Sonia Jaśkaniec<sup>b</sup>, Paul R. Shearing<sup>c</sup>, Valeria Nicolosi<sup>bd</sup>, Dan J.L. Brett<sup>c</sup> and Martin Pumera<sup>aefg</sup>

#joint first authorship

<sup>a</sup>Center for Advanced Functional Nanorobots, Department of Inorganic Chemistry, University of Chemistry and Technology Prague, Technicka 5, 166 28 Prague 6, Czech Republic

<sup>b</sup> Centre for Research on Adaptive Nanostructures and Nanodevices (CRANN), Advanced Materials and BioEngineering Research (AMBER) Centre and School of Chemistry, Trinity College Dublin, Ireland.

<sup>c</sup> Electrochemical Innovation Lab, Department of Chemical Engineering, University College London, London, WC1E 7JE, United Kingdom

<sup>d</sup> I-Form Research Center, Trinity College Dublin, Dublin, Ireland.

<sup>e</sup> Department of Medical Research, China Medical University Hospital, China Medical University, No. 91 Hsueh-Shih Road, Taichung, Taiwan

<sup>f</sup> Department of Chemical and Biomolecular Engineering, Yonsei University, 50 Yonsei-ro, Seodaemun-gu, Seoul 03722, Korea

<sup>g</sup> Future Energy and Innovation Laboratory, Central European Institute of Technology, Brno University of Technology, Purkyňova 656/123, Brno, CZ-616 00, Czech Republic

Author for correspondence: M.Pumera, pumera.research@gmail.com

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**Figure S1. A.** Adams metal oxide powder suspensions **and B-F.** Crystallography open database XRD references used to help assign crystal structure to materials in Figure 1.



Figure S2. Typical CCM preparation for device studies



Figure S3. LSV of RuO<sub>2</sub> on GC repeats in a conventional three electrode cell



Figure S4. LSV of Co<sub>3</sub>O<sub>4</sub> on GC repeats in a conventional three electrode cell



Figure S5. LSV of MnO<sub>x</sub> on GC repeats in a conventional three electrode cell



Figure S6. LSV of NiO on GC repeats in a conventional three electrode cell



Figure S7. LSV of  $Fe_2O_3$  on GC repeats in a conventional three electrode cell



Figure S8. Cell design of the 3D-printed compartment which is half of the overall PEM device.



Figure S9. Chronopotentiometry tests for the three- and two-electrode devices at a current density of 10  $mA cm^{-2}$  using a IrO<sub>2</sub>/Pt CCM.

To experimentally confirm that the response recorded from a two-electrode electrolyser device can be used to evaluate catalysts for the OER similar to the integrated three electrode electrolyser device, a  $IrO_2/Pt$  CCM was tested in a PEEK two- and three-electrode electrolyser device at a current density of 10 mA cm<sup>-2</sup> for 2 hours.

In **Figure S9**, the silver and red lines represent the potential (V vs. RHE) response of the cathode and anode reactions, respectively, and the black line is representative of the overall cell response in a three-electrode cell electrolyser device. This indicates that at a current density of 10 mA cm<sup>-2</sup>, the anodic reaction contributes all of the overall cell voltage. Furthermore, in a two-electrode electrolyser cell the overall cell potential is equal to that in the three-electrode cell device at the same current density. Thus, the overall potential in a two-electrode cell (with Pt/C cathode) can also be rationalised as the potential associated with the anodic reaction in a three-electrode cell, i.e. the OER. To this end, the utilisation of the 3D-printed electrolysers manufactured in this study are capable of evaluating OER catalysts at low current densities (i.e. 10 mA cm<sup>-2</sup>) and, thus, would be a cheap alternative to purchasing expensive and more complex electrolyser devices from commercial sources, **See SI Table 2**.<sup>1</sup>

**Note:** The cell resistance must be checked before conducting water splitting measurements to ensure the cell has been assembled correctly.



Figure S10. Nyquist plot of PEEK and 3D-printed cells conducted using an IrO<sub>2</sub>/Pt CCM.

Table S1: Cost of additional electrolyser parts for the PEEK and 3D-printed electrodes

Additional electrolyser parts	Estimated cost (£)
Piston	83
Mesh	3
Sinter	17

Electrolyser	Active area	Manufactured	Cost of electrolyser (£)	Reference
Commercial	5 cm <sup>2</sup>	Machined	3640.35	1
PEEK	5 cm <sup>2</sup>	Machined	274	This study
PET	5 cm <sup>2</sup>	3D-printed	0.83	This study
Co-P	5 cm <sup>2</sup>	3D-printed	1.66	This study
LTPR	5 cm <sup>2</sup>	3D-printed	19.62	This study
HTPR	5 cm <sup>2</sup>	3D-printed	26.28	This study

Table S2: Cost comparison of commercial, PEEK and 3D-printed electrolysers

1. F. C. Store, Electrolyzer Hardware - Square, <u>https://www.fuelcellstore.com/hydrogen-</u> equipment/hydrogen-production-electrolyzers/electrolyzer-hardware-test-cell-square).