# Charged droplets-driven fast formation of nickel-iron (oxy)hydroxide with rich oxygen defects for boosting overall water splitting

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# **Experimental Procedures**

Synthesis of *E-NiFeOOH by electrospray ionization*: Firstly, nickel foam is cleaned by ultrasonic in acetone, hydrochloric acid (3 M) and DI water for 10 min to remove nickel oxide layer and containments, respectively and dried under ambient condition. Then, 0.1 M FeCl<sub>3</sub>·6H<sub>2</sub>O was dissolved in DI water as a precursor. Then this solution was injected into a fused silica capillary (50  $\mu$ m inner diameter and 150  $\mu$ m outer diameter) by a 500  $\mu$ L syringe (Hamilton) and a syringe pump (Harvard Apparatus) at a rate of 10  $\mu$ L/min for 20, 30, 40, 60 min (named as E-NiFeOOH-x min, x represents the electrospray time). The 8.5 ± 0.5 kV is applied between the needle and the glass on the lifts as a receiver which 1 x 1 cm<sup>2</sup> nickel foam placed on with a distance of 4 ± 0.3 cm to form a multi-jet mode to ensure the uniform distribution of charged droplets. During this spraying process, the charged microdroplets diminish in size by a series of solvent evaporation and coulomb fission. The smaller the droplet, the faster the reaction will be accelerated. Thousands of small droplets promote the entire reaction at the confined and charged solid-liquid interface. The electrodes were also rinsed with DI water after the reaction.

*Synthesis of I-NiFeOOH by corrosion engineering*: The fabrication of NiFeOOH by corrosion engineering only needs to immerse  $1 \times 1 \text{ cm}^2$  Ni foam into 1.5 mL (0.1 M) FeCl<sub>3</sub>·6H<sub>2</sub>O (named as I-NiFeOOH) for the same time compared with E-NiFeOOH. It is worth noting that the E-NiFeOOH and I-NiFeOOH were washed several times with DI water to end the spontaneous redox reaction on the surface.

Synthesis of Pt/C/NF and RuO<sub>2</sub>/NF: Pt/C and RuO<sub>2</sub> catalysts are loaded on the Ni foams to fabricate Pt/C/NF and RuO<sub>2</sub>/NF. Briefly, a homogenous ink was obtained by dispersing the commercial 7 mg Pt/C or RuO<sub>2</sub> catalysts in the mixture of 200  $\mu$ L water and 5  $\mu$ L Nafion by ultrasonic treatment. And then, all the ink was dropped on the Ni

foam to ensure that the loading mass of Pt/C and RuO<sub>2</sub> were both 2.5 mg/cm<sup>2</sup>.

*Material Characterization*: The morphology of NiFeOOH samples was observed using field emission scanning electron microscopy (FE-SEM, Hitachi S-4800, Zeiss-Gmini500) and transmission electron microscopy (TEM, FEI Tecnai F-20 operated at 200 kV). In addition, the high-resolution transmission electron microscope (HRTEM) equipped with energy dispersive X-ray (EDX) spectroscopic analysis (TEM, FEI Tecnai F-20 operated at 200 kV) was employed to give more detailed morphologies. The valence state, surface chemical state, and compositions were explored by X-ray photoelectron spectroscopy (XPS, Thermo Fisher Scientific K-Alpha). XRD patterns were analyzed on an X-ray diffractometer (Rigaku, RINT2500) with a Cu Kα radiation source. EPR measurement was done by Bruker EMX-10/12 under 100 K conditions.

*Electrocatalytic Performance Characterization*: The overall water splitting measurements were performed through an electrochemical work station (CHI 660E, Shanghai Chenhua) with a typical three-electrode system: different NiFeOOH samples as work electrodes, graphite rod as a counter electrode and mercury oxide (Hg/HgO) as a reference electrode, 1 M KOH solution as alkaline electrolyte. The HER and OER polarization curves were measured at a scan rate of 5 mV/s. All potentials reported were calibrated to the reversible hydrogen electrode (RHE) by  $E_{RHE} = E_{SCE} + 0.098 \text{ V} + 0.059$  $\times$  pH, and all LSV curves were corrected for an ohmic drop (85%) to evaluate the true activity of the electrocatalysts. The electrochemical impedance spectroscopy was obtained in a 1 M KOH solution at 0.1 V from  $10^5 - 10^{-1}$  Hz with an AC voltage amplitude of 5 mV to measure the system resistance. The electrochemical surface area (ECSA) of different samples were gauged by the C<sub>dl</sub>, and CV with a different scan rate (20 mV/s, 20 mV/s, 40 mV/s, 80 mV/s, 160 mV/s) was employed to calculate the values of  $C_{dl}$ . The ECSA-normalized LSV curves are calculated by ECSA =  $C_{dl}/C_s$ . A specific capacitance (Cs) value  $Cs = 0.040 \text{ mF/cm}^2$ . Moreover, all the presented curves were in their steady-state after several cycles.

#### **Computational Method**

Spin-polarized density functional theory (DFT) calculations were conducted by Vienna Ab-initio Simulation Package (VASP)<sup>[1,2]</sup>, using the projected augmented wave (PAW)<sup>[3]</sup> method. The Perdew-Burke-Ernzerhof (PBE) functional was used to treat the exchange-correlation interaction<sup>[4]</sup>. The Grimme's D3-type of the semiempirical approach was applied to account for the dispersion interaction<sup>[5]</sup>. The Hubbard-U correction method (DFT + U) was adopted for accurately describing Ni/Fe 3d orbitals with U set to 4.0/6.4 eV. The cut-off energy was set to be 450 eV and the convergence threshold was set to  $10^{-4}$  and 0.02 eV/Å for energy and force, respectively. The NiFe-LDH was modelled by a  $3 \times 3$  slab and a ~15 Å vacuum layer was applied to prevent the interaction between periodical images. For the NiFe-LDH surface model, 1/4 Ni sites on surface were replaced with Fe atoms.

In the alkaline conditions, the OER involves a four proton–coupled electron transfer (PCET) process, which can be expressed as follows

$$* + OH^{-} \rightarrow OH^{*} + e^{-}$$

$$OH^{*} + OH^{-} \rightarrow O^{*} + H_{2}O + e^{-}$$

$$O^{*} + OH^{-} \rightarrow OOH^{*} + e^{-}$$

$$OOH^{*} + OH^{-} \rightarrow O_{2} + H_{2}O + e^{-}$$

where \* donates the active site, and OH\*, O\* and OOH\* are OER intermediates. Based on the computational hydrogen electrode (CHE) model [6], the Gibbs free energies for all intermediates during OER were calculated via the equation

$$\Delta G = \Delta E + \Delta E_{\text{ZPE}} - T\Delta S - neU$$

where  $\Delta E$  is the adsorption energy of the adsorbed intermediates, and  $\Delta E_{ZPE}$  and  $\Delta S$  are the difference in the zero-point energy and the change in entropy before and after adsorption, respectively. *U* is the applied potential.

According to the definition, the theoretical overpotential  $(\eta)$  is defined as

$$\eta = \max(\Delta G)/e - 1.23 \text{ V}$$

# **Supporting Figures and Tables**



**Figure S1**. a) The corrosion engineering reaction in bulk  $FeCl_3$  aqueous; b) The corrosion engineering reaction mediated by positive charged droplets.



**Figure S2**. a-b) SEM images of the E-NiFeOOH prepared using negative droplets (20 min). c) SEM images of NiFeOOH prepared in the FeCl<sub>3</sub> bulk aqurous (20 min). d) SEM images of E-NiFeOOH prepared using positive droplets (20 min).



**Figure S3**. SEM images of the E-NiFeOOH with different reaction time (a-10 min, b-20 min and c-60 min).



**Figure S4**. Digital pictures of Ni foam, I-NiFeOOH and E-NiFeOOH with  $1 \times 1 \text{ cm}^2$  area (from left to right).



Figure S5. AFM image and the corresponding height profiles of E-NiFeOOH nanosheets.



Figure S6. a) XRD profiles of E-NiFeOOH. b) XPS survey of I-NiFeOOH and E-NiFeOOH.



**Figure S7**. a-b) Polarization curves and corresponding Tafel plots of the Ni foam, E-NiFeOOH-20, 30, 40 min and Pt/C/NF electrodes for HER. c) Long-term stability tests and stability measurements of E-NiFeOOH-30 min. d) Comparison of recent representative works of NiFe-based HER electrocatalysts at 10 mA/cm<sup>2</sup> (Table S2).



**Figure S8**. a-b) Polarization curves and corresponding Tafel plots of I-NiFeOOH and E-NiFeOOH for HER. c) Comparison of current density of Ni foam, I-NiFeOOH,

Pt/C/NF and E-NiFeOOH at the overpotential of 300 mV. d-e) Polarization curves and corresponding Tafel plots of I-NiFeOOH and E-NiFeOOH for OER. f) Comparison of current density of Ni foam, I-NiFeOOH, RuO<sub>2</sub>/NF and E-NiFeOOH at the overpotential of 300 mV.



Figure S9. The concept scheme of charged droplets mediated corrosion engineering.



**Figure S10.** The characterization of electrocatalysts after OER reaction a-d) SEM, TEM and HRTEM images, respectively. e-h) XRD spectra and high solution XPS spectra of Fe 2p, Ni 2p and O 2p, respectively.



**Figure S11**. a) EIS Nyquist plots of the Ni foam and E-NiFeOOH electrodes prepared using different reaction times in 1 M KOH electrolyte. b-d) Cyclic voltammetry curves of Ni foam, E-NiFeOOH and I-NiFeOOH with different rates from 20 to 160 mV/s in 1 M KOH electrolyte. e)  $C_{dl}$  values calculated by the capacitive current at 0.17 V (vs. RHE). f) ECSA-normalized LSV curves of I-NiFeOOH and E-NiFeOOH.

**Table S1**. The calculated XPS peak area of M-OH and M-O of I-NiFeOOH and E-NiFeOOH with corresponding estimated  $O_v$  density.

Samples	Oxygen-vacancy	M-O Peak Area	O <sub>v</sub> density	
	Peak Area			
I-NiFeOOH	59030.02	6479.35	9.11	
E-NiFeOOH	84241.48	4329.51	19.46	

Table	<b>S2</b> .	Comparison	of H	ER	performance	of	E-NiFeOOH-30	min	with	other
advanc	ed N	liFe-based ele	ctroca	ataly	sts in 1 M KC	)H r	nedia.			

Electrocatalysts	Electrolyte	<b>η</b> 10	Tafel slope	Reference	
		(mV)	(mV/dec)		
E-NiFeOOH	1 M KOH	145	115	This work	
Porous NiCoFe LTH	1 M KOH	200	70	ACS Energy Lett. 2016, 1, 445	
Exfoliated NiFe	1 M KOH	210	110	Adv. Mater. 2017, 29, 1700017-1700024	
LDH/defective graphene					
VOOH hollow nanosphere	1 М КОН	164	104	Angew. Chem., Int. Ed. 2017, 56, 573-577	
NiFe LDH	1 M KOH	269	/	Adv. Mater. 2018, 1706279	
Ni <sub>2</sub> P	1 M KOH	220	/	Energy Environ. Sci. 2015, 8, 2347.	
Ni <sub>3</sub> S <sub>2</sub> NSs/NF	1 M KOH	223	/	J. Am. Chem. Soc. 2015, 137, 14023-14026	
Ni/Ni(OH) <sub>2</sub> /Graphite	1 M KOH	225	/	Proc. Natl. Acad. Sci. U.S.A. 2017, 114,	
				8986–8990.	
porous NiFe-oxide	1 M KOH	197	130	ACS Appl. Mater. Interfaces 2017, 9,	
nanocubes				41906-41915	
NiFe LDH@NiCoP/NF	1 M KOH	120	88.2	Adv. Funct. Mater. 2018, 28, 1706847	
Ni <sub>12</sub> P <sub>5</sub>	1 M KOH	170	/	ACS Catal. 2017, 7, 103-109	
NiCoP/NF	1 M KOH	185	124.4	Adv. Funct. Mater. 2018, 28, 1706847	
NiFeOF HF	1 M KOH	253	96	ACS Catal. 2017, 7, 12, 8406–8412	
Cu@NiFe LDH	1 M KOH	190	/	Adv. Energy Mater. 2015, 5, 1401660	
NiCo <sub>2</sub> S <sub>4</sub> nanowire	1 M KOH	210	58.9	Adv. Funct. Mater. 2016, 26, 4661-4672	
NiFe LDH/NF	1 M KOH	210	/	Science 2014, 345, 1593-15960	
Ni nanosheets	1 M KOH	130	62	Adv. Mater. 2020, 1906915	

Electrocatalysts	Electrolyte	η10 (mV)	Tafel slope	Reference	
			(mV/dec)		
E-NiFeOOH	1 М КОН	215	30.7	This work	
Ni <sub>2</sub> P@NiFe-LDH	1 M KOH	205	32	Chem. Sci. 2018, 9, 1375.	
NiFe-LDH@DG <sub>10</sub>	1 M KOH	210	52	Adv. Mater. 2017, 29, 1700017.	
NiFe-LDH-V <sub>Ni</sub>	1 M KOH	229	62.9	Small 2018, 14, 1800136.	
NiFe-LDH@graphene	1 M KOH	230	42	ACS Nano 2015, 9, 1977.	
Defect NiFe-LDH	1 M KOH	236	39	Adv. Energy Mater. 2019, 9,	
				1900881.	
$Fe_{6.4}Ni_{16.1}P_{12.9}B_{4.3}O_{60.2}$	1 M KOH	249	40.3	ACS Nano 2019, 13, 12969.	
Fe <sup>2+</sup> -NiFe-LDH	1 M KOH	250	69	Angew. Chem., Int. Ed. 2018, 57,	
				9392	
Atomic layer NiFe-	1 M KOH	254	32	Adv. Energy Mater. 2018, 8,	
LDH				1703585.	
NiFe-LDH/C	1 M KOH	270	56	Angew. Chem. 2017, 129, 11411.	
NiFe-LDH	1 M KOH	280	47.6	J. Am. Chem. Soc. 2014, 136,	
				13118.	
Ultra-thin NiFe-LDH	1 M KOH	280	46	Adv. Energy Mater. 2016, 6,	
				1502585.	
NiFe-LDH	1 M KOH	280	49.4	Angew. Chem. 2018, 130, 178.	
nanoprisms					
NiFe-LDH NS	1 M KOH	300	40	Nat. Commun. 2014, 5, 4477.	
Porous NiFe oxides	1 M KOH	328	42	Adv. Sci. 2015, 2, 1500199.	
R-NiFe CPs	1 M KOH	225	27.78	Adv. Energy Mater. 2020, 2002228	
NiFeCr/NF	1 M KOH	270	36	Energy Environ. Sci., 2020	

**Table S3**. Comparison of OER performance of E-NiFeOOH-40 min with otheradvanced NiFe-based electrocatalysts in 1 M KOH media.

**Table S4.** Comparison of overall water splitting performance of E-NiFeOOH-30min/E-NiFeOOH-40minelectrodescouplewithotheradvancedNiFe-basedelectrocatalystsin 1 M KOH media.

Electrocatalysts	Electrolyte	η10 (V)	Reference	
E-NiFeOOH	1 М КОН	1.59	This work	
NiFe LDH/Mxene/NF	1 M KOH	1.51	Nano Energy, 2019, 63, 103880	
Ni/NiFe LDH	1 M KOH	1.53	J. Mater. Chem. A, 2019, 7, 21722-21729	
NiCo <sub>2</sub> S <sub>4</sub> /NF	1 M KOH	1.63	Adv. Funct. Mater. 2016, 26, 4661-4672	
Ni <sub>2</sub> P	1 M KOH	1.63	Energy Environ. Sci 2015, 8, 2347-2351	
CoP films	1 M KOH	1.63	Angew. Chem. 2015, 127, 6349-6352.	
Fe-Ni/NCNTs	1 M KOH	1.64	Angew. Chem., 2018, 57, 8921.	
NiFe/NiCo <sub>2</sub> O <sub>4</sub> /NF	1 M KOH	1.67	Adv. Funct. Mater., 2016, 26, 3515-3523	
EG/Co <sub>0.85</sub> Se/NiFe-LDH	1 M KOH	1.67	Energy Environ. Sci. 2016, 9, 478-483	
CoMnCH/NF	1 M KOH	1.68	J. Am. Chem. Soc., 2017, 139, 8320-8328	
FeCoNi/NCP	1 M KOH	1.687	ACS Catal. 2017, 7, 469-479	
PO-Ni/Ni-NCNFs	1 M KOH	1.69	Nano Energy, 2018, 51, 286.	
NiFe LDHs/NF	1 M KOH	1.7	Science 2014, 345, 1593-1596	
Co(OH) <sub>2</sub> /NCNTs/NF	1 M KOH	1.72	Nano Energy, 2018, 47, 96-104	
Ni <sub>3</sub> S <sub>2</sub>	1 M KOH	1.76	J. Am. Chem. Soc. 2015, 137, 14023-14026	
NiFe OF	1 M KOH	1.83	ACS Catal. 2017, 7, 12, 8406–8412	
Pt/C-IrO <sub>2</sub>	1 M KOH	1.7	Small 2019, 15, 1803639	

System		E (eV)	$E_{ZPE}(eV)$	TS (eV)
	*	-161.56	0	0
NiFe-	OH*	-170.20	0.31	0.03
LDH	O*	-166.08	0.05	0.06
(Ni <sub>9</sub> Fe <sub>1</sub> )	OOH*	-174.50	0.43	0.12
	*	-163.33	0	0
NiFe-	OH*	-172.43	0.29	0.09
LDH-O <sub>v</sub>	O*	-167.93	0.04	0.10
(Ni <sub>3</sub> Fe <sub>1</sub> )	OOH*	-176.97	0.41	0.17

**Table S5**. Calculated total energy E, zero-point energy E<sub>ZPE</sub>, and entropic contribution TS for all intermediates.

NiFe-LDH(Ni<sub>9</sub>Fe<sub>1</sub>):



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