Supplementary Information

Redox-catalysis flow electrode desalination in an organic solvent

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Figure S1. Three-electrode CV of I^-/I^{3-} solution with Pt counter and Ag/AgCl reference in acetonitrile or water medium



Figure S2. The desalination performance at different current densities from Figure 1: (a) 1 mA cm⁻²; (b) 3 mA cm⁻²; (c) 5 mA cm⁻²; (d) 7 mA cm⁻². The initial salt feed: 12000 ppm salt. Electrolyte: 50 mM NaI/30 mM I₂ and 500 mM TBAP in 5 ml acetonitrile; salt feed: 12000 ppm in 3 mL. The red solid lines represent the conductivity of the brine stream while the blue solid lines the conductivity of the desalinated stream.



Figure S3. The desalination performance of different CNTs content with the ratio of 0 wt% (a), 1 wt% (b), 3 wt% (c). The initial salt feed: 12000 ppm salt, current density: 5 mA cm⁻²; The initial salt feed: 12000 ppm salt. Electrolyte: 50 mM NaI/30 mM I₂ and 500 mM TBAP in 5 ml acetonitrile; salt feed: 12000 ppm in 3 mL; Current density: 5 mA cm⁻². The red solid lines represent the conductivity of the brine stream while the blue solid lines the conductivity of the desalinated stream.



Figure S4. SEM images of multi wall carbon nanotubes, before (a) and after (b) the desalination test. The current density: 5 mA cm^{-2} .



Figure S5. Membrane images before (a) and after (b) the desalination test.



Figure S6. The LSV curve of two-electrode architecture in organic redox flow electrode. Device structure: end plate | graphite paper as current collector | redox couples/carbon flow chamber || redox couples/carbon flow chamber | graphite paper as the current collector | end plate (The symbols of | and || detonate the compartment separation and membrane, respectively.) The redox couples/carbon flow chamber material with the dimension of 17 mm length, 4 mm width, 5 mm thickness. The active area is 68 mm² totally.



Figure S7. Nyquist plots of organic redox flow electrodes measured by two-electrode configuration, redox couples with 0, 1, 3 wt % CNTs measured under the zero-bias with the frequency range between 100 kHz to 10 mHz at a sinusoidal amplitude of 10 mV.



Figure S8. The relationship between carbon nanotubes content and viscosity.



Figure S9. The desalination performance at different current densities: (a) 2 mA cm⁻²; (b) 5 mA cm⁻²; (c) 8 mA cm⁻²; (d) 11 mA cm⁻²; (e) 13 mA cm⁻². The initial salt feed: 12000 ppm salt in 3 mL; CNTs content: 3 wt%; Electrolyte: 50 mM NaI/ 30mM I₂ and 500 mM TBAP in 5 ml acetonitrile. The red solid lines represent the conductivity of the brine stream while the blue solid lines the conductivity of the desalinated stream.



Figure S10 The comparison of desalination performance with/without the addition of the redox couples. The constant current density: 5 mA cm⁻².



Figure S11. The comparison plot of salt removal rate vs consumption extracted from Table S1.



Figure S12. Results of multi-cycle test of the current desalination system with 3 % CNTs and 50 mM NaI /30 mM I₂ at the current density of 5 mA cm⁻² without the replacement of electrode materials and membranes.



Figure S13. The organic redox flow desalination driven by solar light at zero bias (short circuit): (a) 0 wt% CNT; (b) 1wt% CNT; (c) 3 wt% CNT; (d) the overlapping curves of 0, 1, 3 wt% CNT. The initial salt feed: 6000 ppm in 3 mL.

Electrode materials	Carbon content	Salt feed (ppm)	Operation voltage or current	Salt removal rate (µg s ⁻¹ cm ⁻²)	Energy consumption (kJ mole ⁻¹)	Ref.
Porous carbon	10 %	1170	3.84 mA cm ⁻²	0.22	109.1	1
YP-50F activated carbon	13%	10000	3.0 mA cm ⁻²	1.31	126.4	2
Modified AC	10 %	1000	1.43 mA cm ⁻²	0.41	70.7	3
Activated carbon	5%	200	1.2 V	0.17	-	4
		1100		0.67		
		5900		3.17		
		14200		3.67		
		35000		5.67		
Activated carbon	10%	5800	1.2 V	0.31	-	5
	15%			0.42		
	20%			0.67		
Activated						
carbon-N and	35%	35000	1.2 V	~33.13	-	6
Activated carbon-S						
Carbon black	2.5%	1000	1.2 V		~125	7
Activated carbon, carbon black	5%	5800	1.2 V	0.86	-	8
Activated carbon, carbon black	10%	2000	1.15 mA cm-2	0.76		
				0.71	-	9
				0.68		
Activated carbon, carbon black	5.72%	10000	2.8 V	1.83	-	10
CNTs suspension	7.41 %	11688	1.6 V	0.82	270.0	11
Activated carbon, and FCNTs	5.25%	35000	1.2 V	33.43	-	12

Supplementary Table S1. Comparison of FCDI energy consumption and salt removal rate

V^{2+}/V^{3+}						
Activated carbon				0.226	192.89	
(AC)	7.41%	3000	0.43 mA cm ⁻²	0.235	168.66	
AC and V ²⁺ /V ³⁺				0.237	103.26	13
AC, V ²⁺ /V ³⁺ and 0.5% CNTs				0.24	77.99	
AC, V ²⁺ /V ³⁺ and 1% CNTs				0.25	72.62	
Activated carbon, carbon black, ferri- /ferrocyanide	10 %	9000	0.47 mA cm ⁻²	0.16	40.95	14
			1.42 mA cm ⁻²	0.63	52.2	
			2.38mA cm ⁻²	1.33	98.07	
			3.33mA cm ⁻²	1.72	135.0	
			4.28 mA cm ⁻²	2.7	160.0	
		1170	0.4 mA cm ⁻²	0.27	177.0	15
TE-3 activated			0.52 mA cm ⁻²	0.3	263.5	
carbon beads	8.3 %		0.6 mA cm ⁻²	0.33	345.6	
			0.8 mA cm ⁻²	0.39	456.0	
			0.573 mA cm ⁻²	0.3	97.3	
DARCO, and Noritactivated charcoal	2000	10 %	1.146 mA cm ⁻²	0.63	142.8	16
			1.719 mA cm ⁻²	0.91	187.0	
			2.292 mA cm ⁻²	1.12	233.7	
			2.865 mA cm ⁻²	1.27	289.9	
			3.438 mA cm ⁻²	1.5	329.5	
			4.011 mA cm ⁻²	1.78	362.7	
DARCO,and Noritactivated charcoal	1000	10 %	0.909 mA cm ⁻²	1.12	35.79	17
			1.818 mA cm ⁻²	2.30	162.61	
			2 mA cm ⁻²	1.08	66.08	
NaI/I ₂ and 3% CNTs	3%	12000	5 mA cm ⁻²	2.77	113.84	This work
			8 mA cm ⁻²	4.37	185.13	
			11 mA cm ⁻²	6.08	238.07	
			13 mA cm ⁻²	6.80	373.07	

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