

# Gas adsorption in the topologically disordered Fe-BTC framework

## SUPPLEMENTARY INFORMATION

*Adam F. Sapnik,<sup>1</sup> Christopher W. Ashling,<sup>1</sup> Lauren K. Macreadie,<sup>2,3</sup> Seok J. Lee,<sup>2</sup>  
Timothy Johnson,<sup>4</sup> Shane G. Telfer<sup>2</sup> and Thomas D. Bennett<sup>1\*</sup>*

1. Department of Materials Science and Metallurgy, University of Cambridge, Cambridge, CB3 0FS, United Kingdom.
2. MacDiarmid Institute for Advanced Materials and Nanotechnology, Institute of Fundamental Sciences, Massey University, Palmerston North, New Zealand.
3. School of Chemistry, University of Sydney, Sydney, NSW, 2006, Australia.
4. Johnson Matthey Technology Centre, Blount's Court, Sonning Common, RG4 9NH, United Kingdom.

\* To whom correspondence should be addressed; E-mail: tdb35@cam.ac.uk

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## Supplementary Methods

### Surface Area Analysis

Brunauer–Emmett–Teller (BET) surface areas were calculated from N<sub>2</sub> adsorption isotherms at 77 K according to the following procedure.<sup>1</sup> The isotherm region where  $v(1 - P/P_0)$  increases versus  $P/P_0$ , where  $v$  is the amount of N<sub>2</sub>, was identified. Within this isotherm region, sequential data points that led to a positive intercept in the plot of  $\frac{(P/P_0)}{v(1-P/P_0)}$  against  $P/P_0$  were found. This plot yields a slope  $a$  and a positive intercept  $b$ . The BET surface area was then calculated according to the following equation:

$$A_{\text{BET}} = v_m \times \frac{1}{22400} \times \sigma_0 \times N_A \times 10^{-20}, \quad (1)$$

where  $N_A$  is Avogadro's constant and  $\sigma_0$  is the cross-sectional area of a N<sub>2</sub> molecule, which is 16.2 Å<sup>2</sup>.

### Non-Local Density Functional Theory Analysis

Pore size distributions were extracted from the N<sub>2</sub> adsorption isotherms at 77 K using a non-local density functional theory (NL-DFT) approach.<sup>2</sup> Within NL-DFT, classical fluid density functional theory is used to construct adsorption isotherms in ideal pore geometries and then solve the adsorption integral equation. The main limitation of NL-DFT as applied here is the absence of a specific kernel designed for MOFs.<sup>3</sup> Instead, kernels for activated carbons are often used given the majority of accessible surface within a MOF is organic in nature – that is the 1,3,5-benznetricabolate anion in the case of MIL-100 and Fe-BTC.<sup>4,5</sup> Furthermore, while the use of NL-DFT methods on amorphous MOFs has proven valuable, it cannot be scrutinised with the same quantitative level of detail as for crystalline systems.<sup>3</sup> NL-DFT methods have also been reported to underestimate the pore dimensions, compared to the expected van der Waals dimensions.<sup>6,7</sup> Pore size distributions were calculated within the SAIEUS software employing a *carbon–N<sub>2</sub>, 2D heterogenous* kernel and a regularisation parameter ( $\lambda$ ) of 1.75.<sup>8</sup>

### Virial Analysis

Isosteric heat of adsorption,  $Q_{\text{st}}$ , values were calculated from adsorption isotherms measured at 273 and 293 K for CO<sub>2</sub>, CH<sub>4</sub> and C<sub>3</sub>H<sub>6</sub>.<sup>9</sup> The isotherms were fit via global optimisation to the virial equation:

$$\ln P = \ln N + \frac{1}{T} \sum_{i=0}^m a_i N^i + \sum_{i=0}^n b_i N^i, \quad (2)$$

where  $P$  is pressure,  $N$  is the amount of gas adsorbed,  $a$  and  $b$  are the virial coefficients,  $m$  and  $n$  are the number of coefficients required to model the isotherm.  $Q_{\text{st}}$  values were then derived using the parameters obtained from the virial fits using the following equation:

$$Q_{\text{st}} = -R \sum_{i=0}^m a_i N^i. \quad (3)$$

The heat of adsorption at near-zero coverage were approximated using the following equation:

$$Q_{\text{st}}^0 \approx -R \times a_0. \quad (4)$$

## Ideal Adsorbed Solution Theory Analysis

Thermodynamic gas selectivities for equimolar mixtures of CO<sub>2</sub>/N<sub>2</sub>, CH<sub>4</sub>/N<sub>2</sub> and CO<sub>2</sub>/CH<sub>4</sub> at 273 K were calculated using ideal adsorbed solution theory (IAST) in the IAST++ software package.<sup>10,11</sup> The pure-component isotherms of CO<sub>2</sub>, N<sub>2</sub> and CH<sub>4</sub> for both MIL-100 and Fe-BTC were first fit to either a dual-site Langmuir-Freundlich [Eq. 5], Langmuir-Freundlich [Eq. 6], dual-site Langmuir [Eq. 7] or Langmuir [Eq. 8] model:

$$\text{DSLF} \quad n(P) = q_1 \frac{(k_1 P)^{n_1}}{1 + (k_1 P)^{n_1}} + q_2 \frac{(k_2 P)^{n_2}}{1 + (k_2 P)^{n_2}} \quad (5)$$

$$\text{LF} \quad n(P) = q \frac{(kP)^n}{1 + (kP)^n} \quad (6)$$

$$\text{DSL} \quad n(P) = q_1 \frac{k_1 P}{1 + k_1 P} + q_2 \frac{k_2 P}{1 + k_2 P} \quad (7)$$

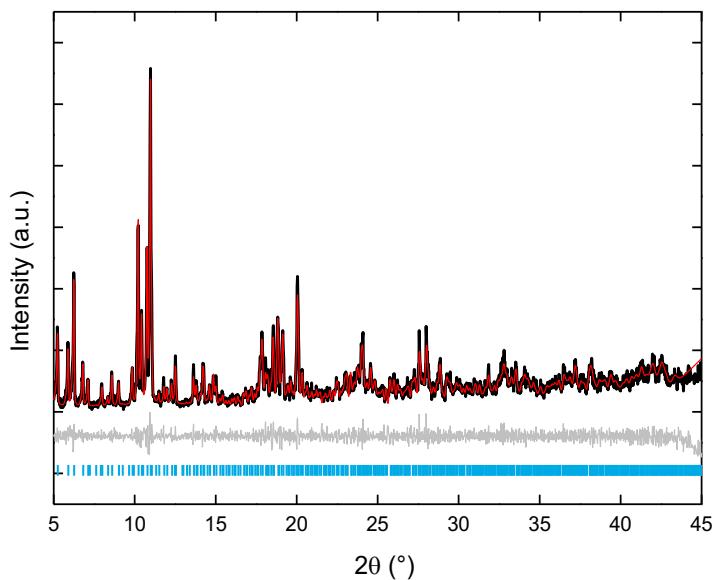
$$\text{L} \quad n(P) = q \frac{kP}{1 + kP} \quad (8)$$

$n(P)$  is the number of moles of gas adsorbed on the surface when in equilibrium with a pure gas phase as a function of its pressure  $P$ . These parameters were used afterwards to carry out IAST calculations. The selectivity,  $S_{a/b}$ , was calculated using the following equation:

$$S_{a/b} = \frac{X_a Y_b}{X_b Y_a} \quad (9)$$

$X$  is the mole fraction in the adsorbed phase and  $Y$  is the mole fraction in the gas phase.

## Pawley Refinement of MIL-100



**Figure S1** Experimental data (black), calculated diffraction pattern (red), difference function (grey) and symmetry-allowed reflections (blue tick marks). Symmetry-allowed reflections were calculated from the reported crystallographic information file in Ref. 12. Data reproduced from Ref. 13.

**Table S1** Crystallographic data from Pawley refinement of MIL-100.

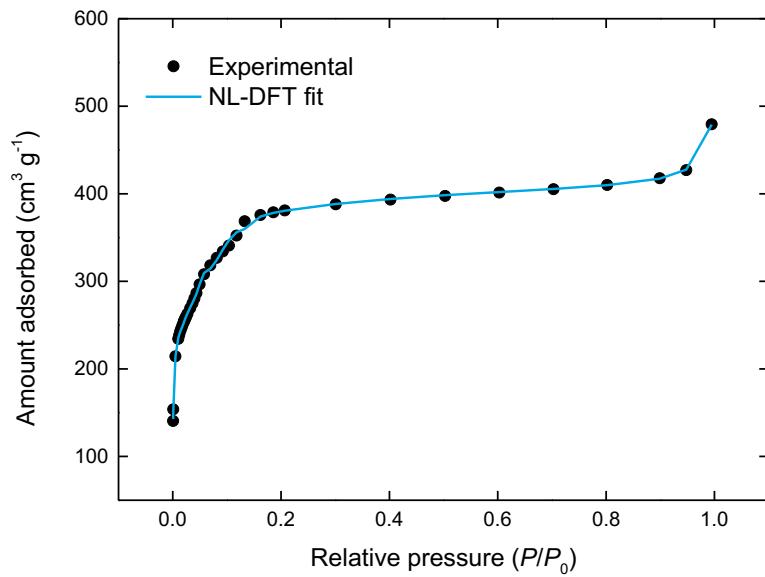
$R_{wp} = 9.48$	Experimental	Reported [12]
$a = b = c$	73.25(3)	73.340(1)
$\alpha = \beta = \gamma$	90	90

## BET Analysis Parameters – Nitrogen

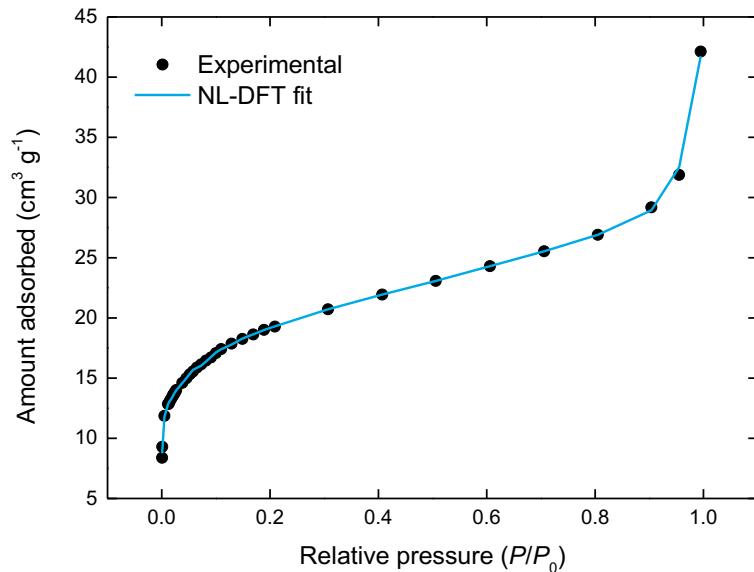
**Table S2** Refinement parameters obtained from BET analysis of N<sub>2</sub> adsorption isotherms at 77 K.

	MIL-100	Fe-BTC
Slope	0.00294	0.0636
Intercept	0.0000308	0.000260
Correlation coefficient	0.999711	0.999887
C constant	96.301	245.661
Surface area (m <sup>2</sup> g <sup>-1</sup> )	1465.627	68.170

## Non-Local Density Functional Theory Analysis

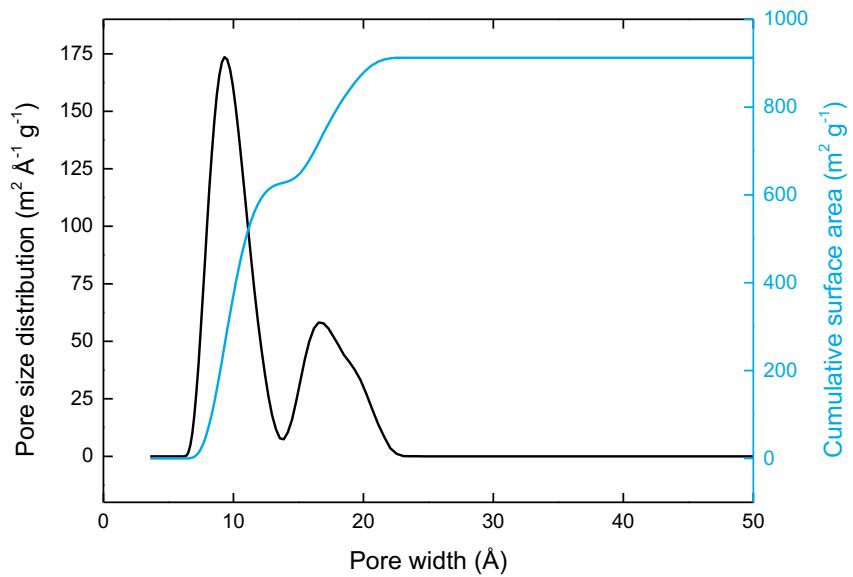


**Figure S2** Experimental N<sub>2</sub> adsorption isotherm for MIL-100 (black circles) at 77 K and the NL-DFT fit (blue line).

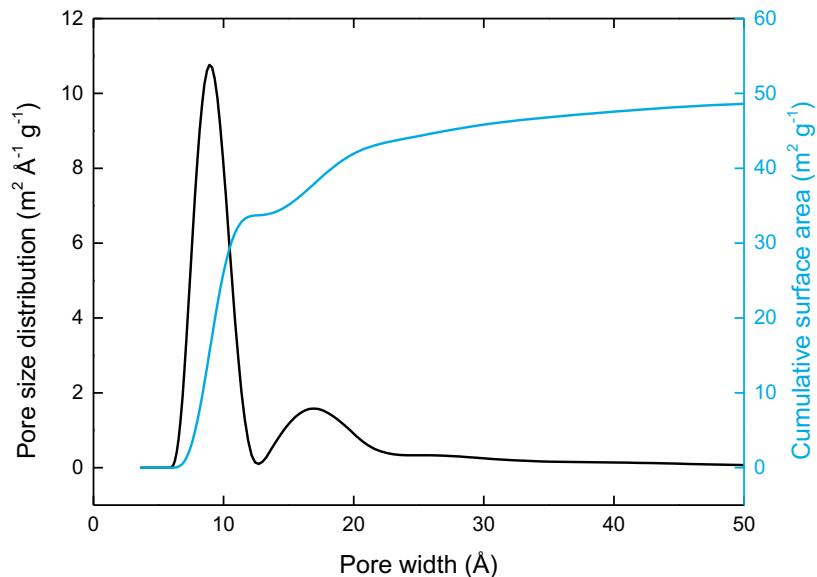


**Figure S3** Experimental N<sub>2</sub> adsorption isotherm for Fe-BTC (black circles) at 77 K and the NL-DFT fit (blue line).

## Pore Size Distributions



**Figure S4** Pore size distribution (black) and cumulative surface area (blue) for MIL-100 from NL-DFT analysis.



**Figure S5** Pore size distribution (black) and cumulative surface area (blue) for Fe-BTC from NL-DFT analysis.

## Nitrogen Isotherms

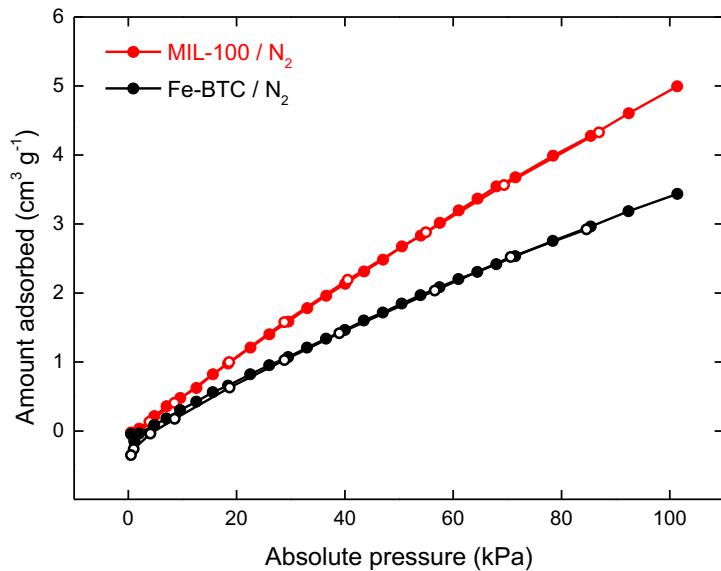


Figure S6 N<sub>2</sub> adsorption (closed) and desorption (open) isotherms at 273 K for MIL-100 (red) and Fe-BTC (black).

## Adsorbate Properties

Table S3 Properties of the adsorbate molecules used in this study, values taken from Ref. 14.

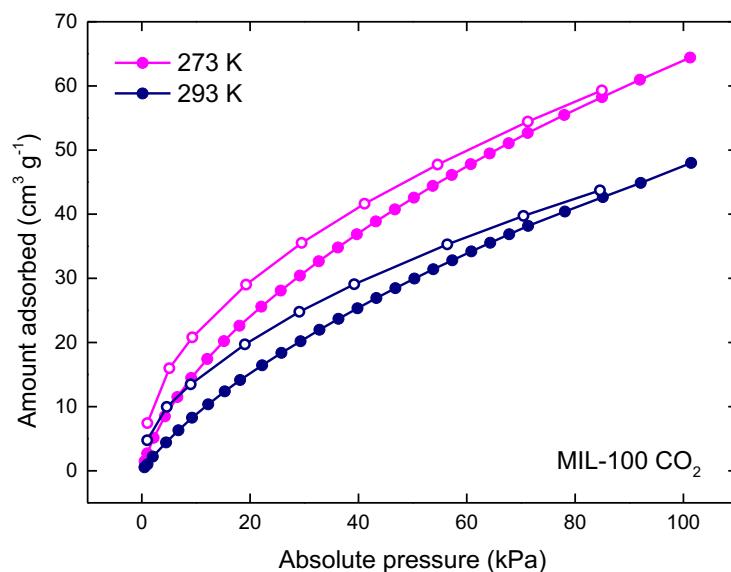
	Molecular dimensions (Å)	Polarizability ( $\times 10^{25} / \text{cm}^3$ )	Dipole Moment ( $\times 10^{18} / \text{esu cm}$ )	Quadrupole moment ( $\times 10^{26} / \text{esu cm}^2$ )
N <sub>2</sub>	3.64–3.80	17.403	0	1.52
Xe	4.047	40.44	0	0
Ar	3.542	16.411	0	0
H <sub>2</sub>	2.827–2.89	8.042	0	0.662
CO <sub>2</sub>	3.3	29.11	0	4.30
CH <sub>4</sub>	3.758	25.93	0	0
C <sub>2</sub> H <sub>4</sub>	4.163	42.52	0	1.50
C <sub>2</sub> H <sub>6</sub>	4.443	44.3–44.7	0	0.65
C <sub>3</sub> H <sub>6</sub>	4.678	62.6	0.366	0
C <sub>3</sub> H <sub>8</sub>	4.30–5.118	62.9–63.7	0.084	0

## BET Analysis Parameters – Carbon Dioxide

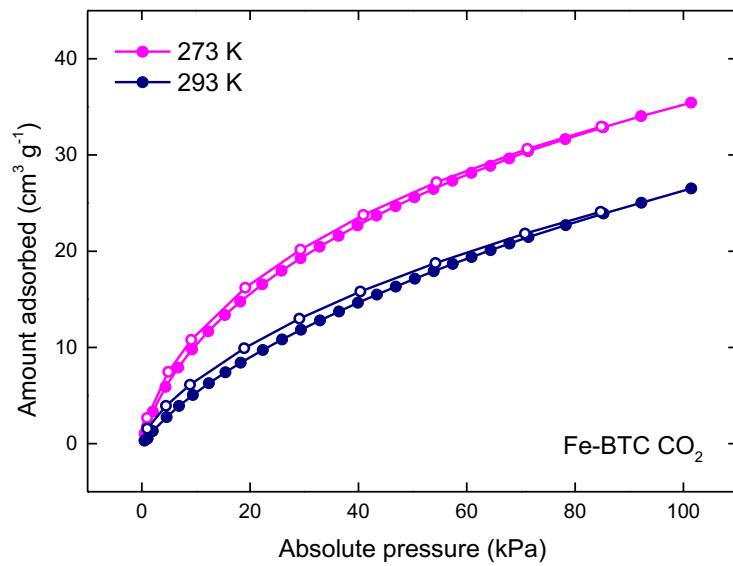
**Table S4** Refinement parameters obtained from BET analysis of CO<sub>2</sub> adsorption isotherms at 273 K.

	<b>MIL-100</b>	<b>Fe-BTC</b>
Slope	0.0321	0.0545
Intercept	0.00391	0.00518
Correlation coefficient	0.999849	0.999621
C constant	9.210	11.508
Surface area (m <sup>2</sup> g <sup>-1</sup> )	126.725	76.585

## Carbon Dioxide Isotherms

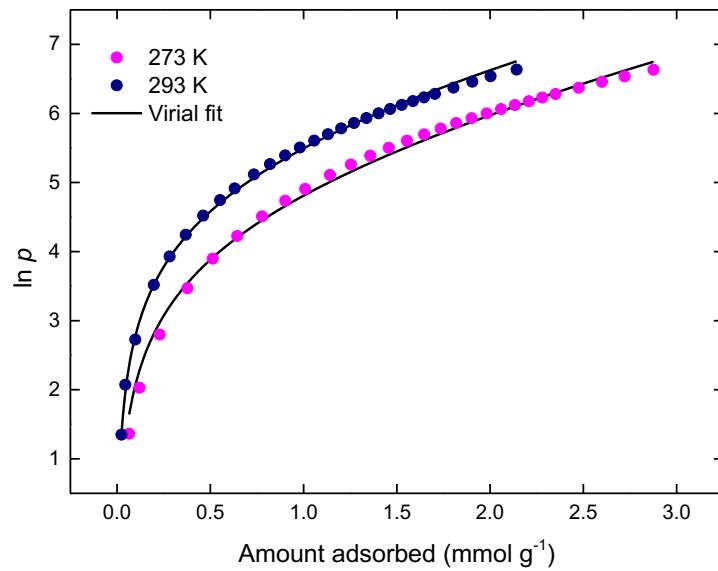


**Figure S7** Adsorption (closed) and desorption (open) isotherms of CO<sub>2</sub> for MIL-100 at 273 (pink) and 293 K (navy).

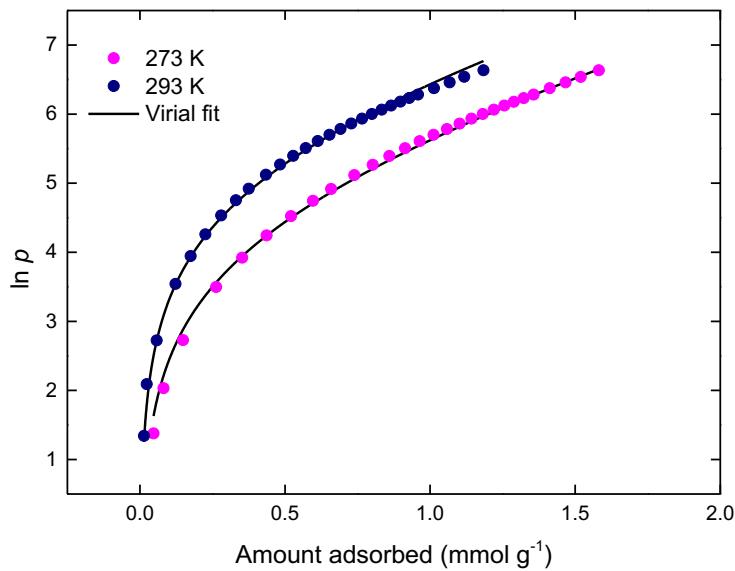


**Figure S8** Adsorption (closed) and desorption (open) isotherms of CO<sub>2</sub> for Fe-BTC at 273 (pink) and 293 K (navy).

## Carbon Dioxide Virial Fits



**Figure S9** Virial fit (black lines) to the CO<sub>2</sub> adsorption data for MIL-100 at 273 (pink) and 298 K (navy).

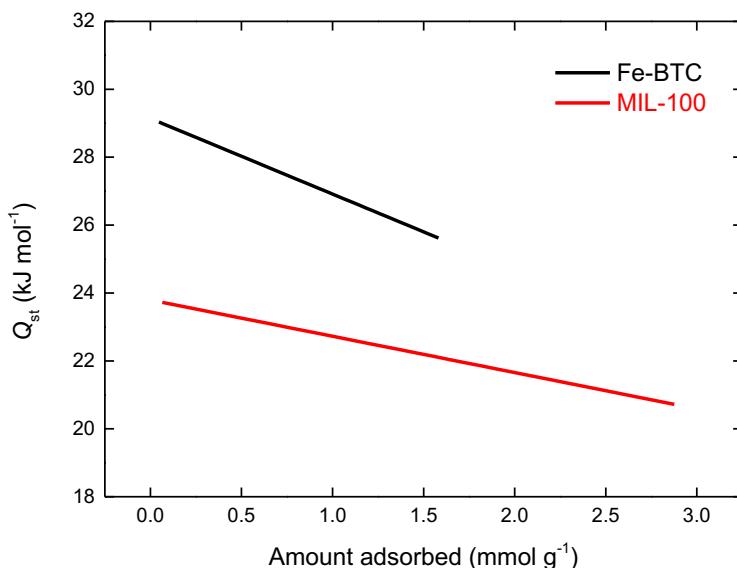


**Figure S10** Virial fit (black lines) to the CO<sub>2</sub> adsorption data for Fe-BTC at 273 (pink) and 293 K (navy).

**Table S5** Fitting parameters used for virial analysis of CO<sub>2</sub> in MIL-100 and Fe-BTC.

	MIL-100		Fe-BTC	
	Value	Uncertainty	Value	Uncertainty
$a_0$	-2861.97804	94.55277	-3504.88219	91.15603
$a_1$	128.50874	4.27335	267.70237	7.28523
$b_0$	14.82226	0.32837	17.47992	0.331527
$R^2$	0.9963		0.99672	
$\chi^2$	0.00685		0.00607	

### Carbon Dioxide $Q_{st}$ Values



**Figure S11**  $Q_{st}$  values for CO<sub>2</sub> for MIL-100 (red) and Fe-BTC (black) determined from the virial coefficients.

## Methane Isotherms

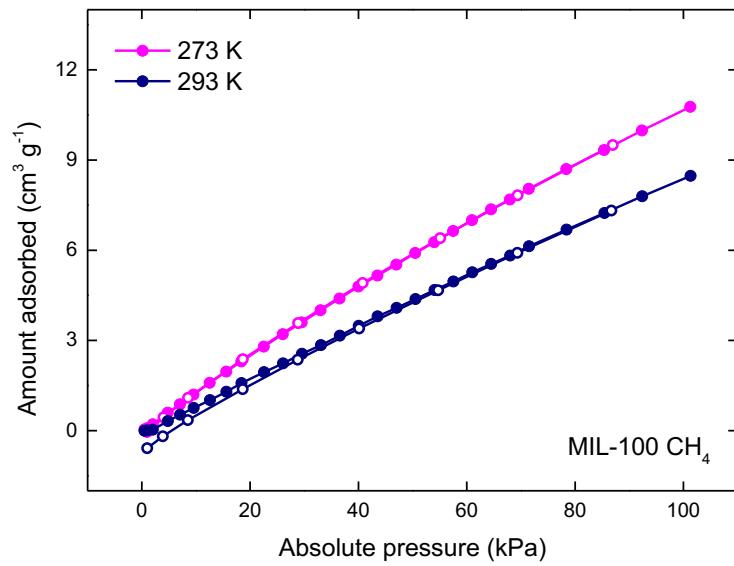


Figure S12 Adsorption (closed) and desorption (open) isotherms of CH<sub>4</sub> for MIL-100 at 273 (pink) and 293 K (navy).

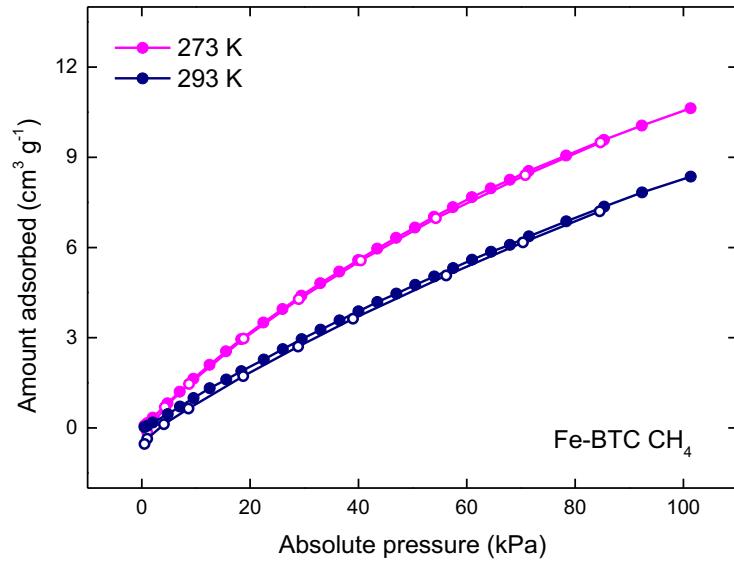


Figure S13 Adsorption (closed) and desorption (open) isotherms of CH<sub>4</sub> for Fe-BTC at 273 (pink) and 293 K (navy).

## Methane Virial Fits

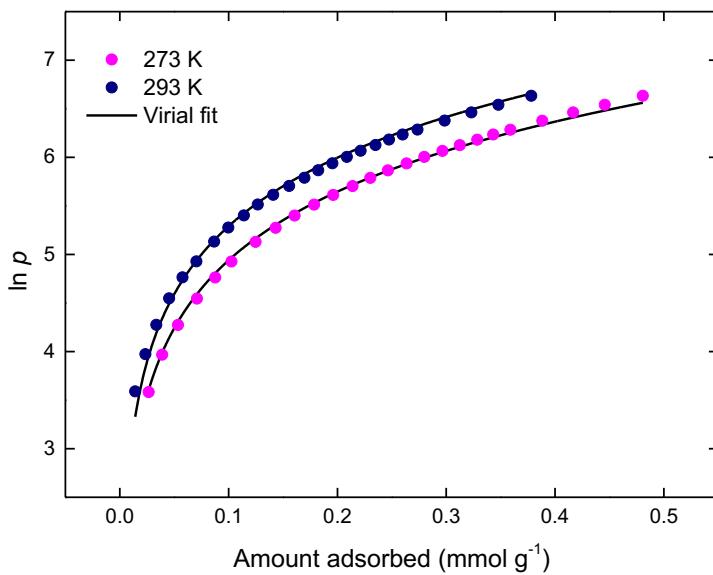


Figure S14 Virial fit (black lines) to the CH<sub>4</sub> adsorption data for MIL-100 at 273 (pink) and 293 K (navy).

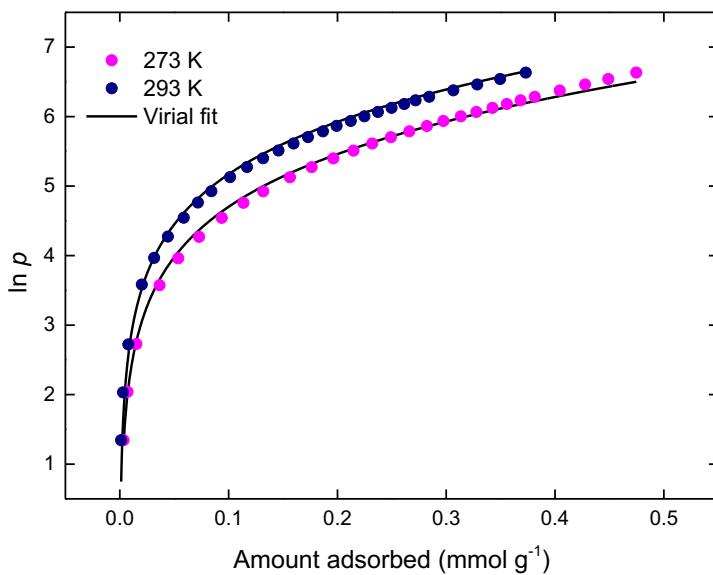


Figure S15 Virial fit (black lines) to the CH<sub>4</sub> adsorption data for Fe-BTC at 273 (pink) and 293 K (navy).

Table S6 Fitting parameters used for Virial analysis of CH<sub>4</sub> in MIL-100 and Fe-BTC. Note, the lowest pressure data (where there was minimal uptake) was excluded for MIL-100 to obtain a reasonable fit.

	MIL-100		Fe-BTC	
	Value	Uncertainty	Value	Uncertainty
$a_0$	-1406.90184	65.12101	-1893.30126	131.92175
$a_1$	37.29642	18.5466	176.35328	34.67179
$b_0$	12.38232	0.22695	13.87521	0.46047
$R^2$	0.99550		0.99247	
$\chi_v^2$	0.00302		0.01393	

## Methane $Q_{st}$ Values

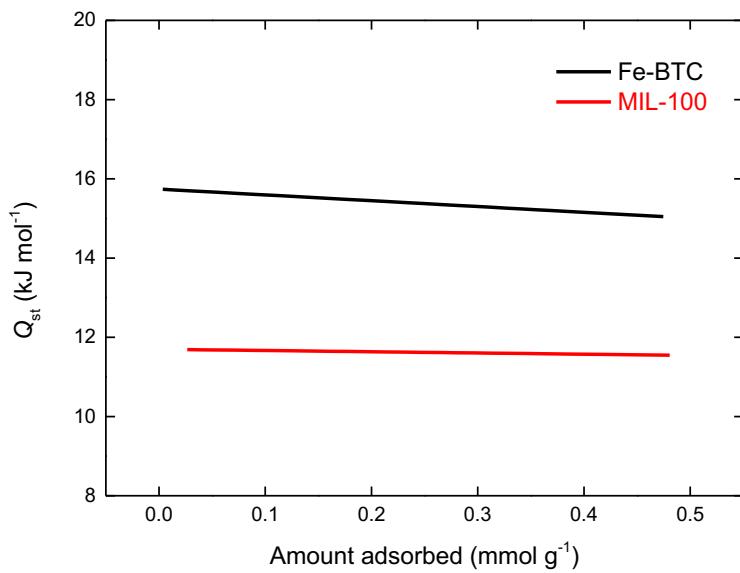


Figure S16  $Q_{st}$  values for CH<sub>4</sub> for MIL-100 (red) and Fe-BTC (black) determined from the virial coefficients.

## Propene Isotherms

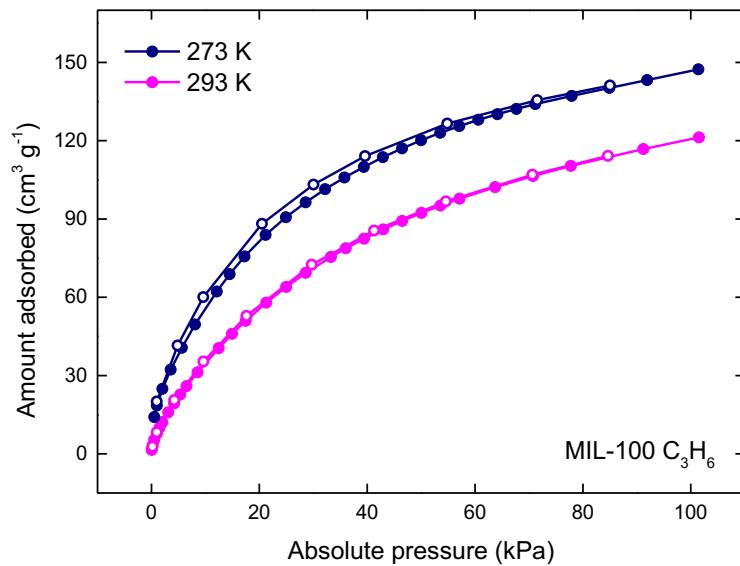
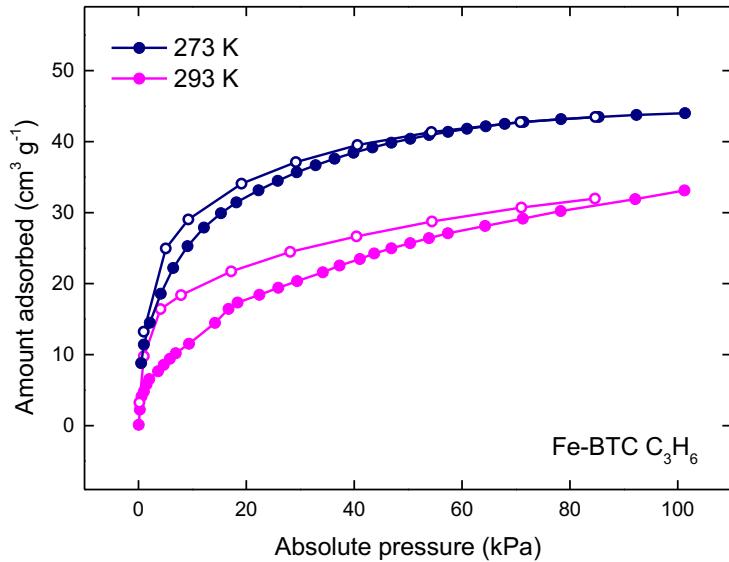
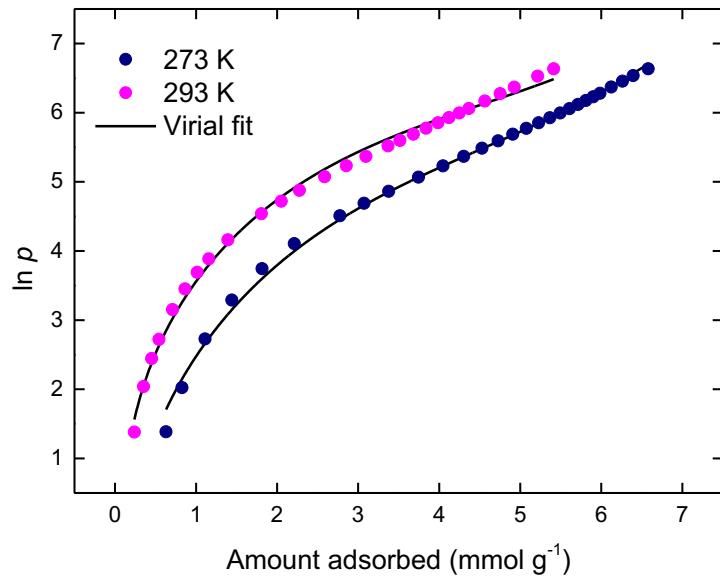


Figure S17 Adsorption (closed) and desorption (open) isotherms of C<sub>3</sub>H<sub>6</sub> for MIL-100 at 273 (navy) and 293 K (pink).



**Figure S18** Adsorption (closed) and desorption (open) isotherms of  $C_3H_6$  for Fe-BTC at 273 (navy) and 293 K (pink).

## Propene Virial Fits



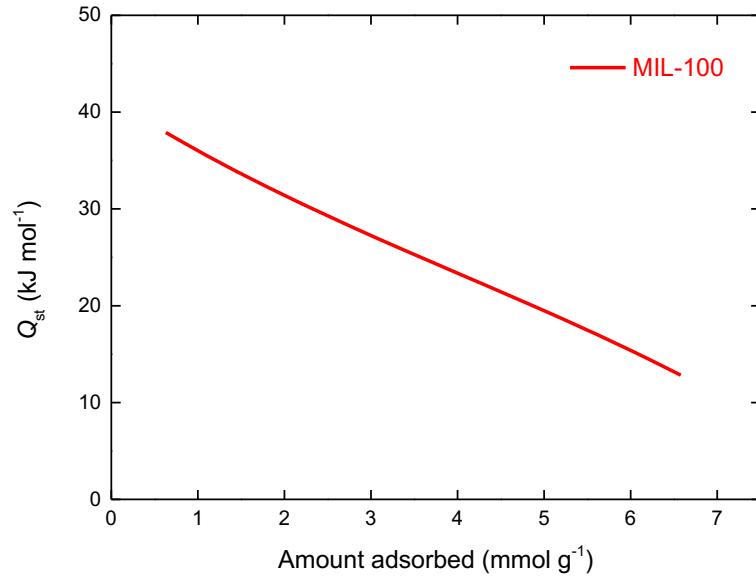
**Figure S19** Virial fit (black lines) to the  $C_3H_6$  adsorption data for MIL-100 at 273 (navy) and 293 K (pink).

**Table S7** Fitting parameters used for Virial analysis of  $C_3H_6$  in MIL-100.

	MIL-100	
	Value	Uncertainty
$a_0$	-4974.37325	251.30488
$a_1$	695.0499	75.96277
$a_2$	-57.30614	7.53744
$a_3$	4.7039	0.72963

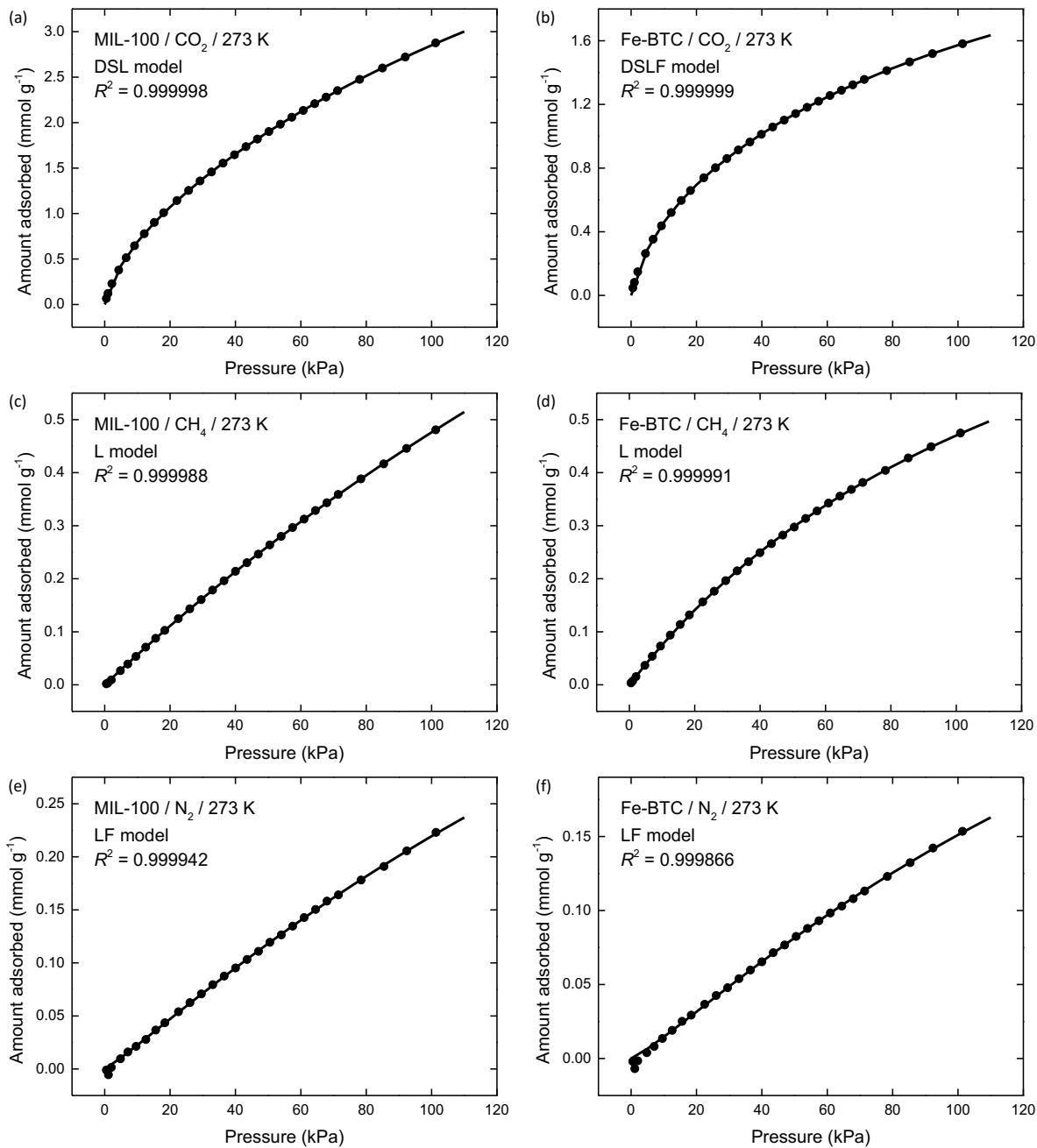
$b_0$	19.75367	0.86481
$b_1$	-1.41067	0.24428
$R^2$		0.99585
$\chi^2_v$		0.00844

### Propene $Q_{st}$ Values



**Figure S20**  $Q_{st}$  values for  $C_3H_6$  for MIL-100 determined from the virial coefficients.

## IAST Models



**Figure S21** Experimental adsorption isotherms (black circle) and corresponding fit (black line) to either the Langmuir-Freundlich (LF), dual-site Langmuir (DSL), dual-site Langmuir Freundlich (DSLF) or Langmuir (L) model.

**Table S8** Fitting parameters for the LF, DSL, DSLF and L models used to fit the experimental adsorption data for MIL-100 and Fe-BTC at 273 K

<b>Fe-BTC / N<sub>2</sub> / LF</b>	
<i>q</i> (mmol g <sup>-1</sup> )	0.485282
<i>k</i> (kPa <sup>-n</sup> )	0.00505054
<i>n</i>	1.16267
<i>R</i> <sup>2</sup>	0.999866
<b>MIL-100 / N<sub>2</sub> / LF</b>	
<i>q</i> (mmol g <sup>-1</sup> )	0.855488
<i>k</i> (kPa <sup>-n</sup> )	0.00381855
<i>n</i>	1.1054
<i>R</i> <sup>2</sup>	0.999942
<b>MIL-100 / CO<sub>2</sub> / DSL</b>	
<i>q</i> <sub>1</sub> (mmol g <sup>-1</sup> )	6.91921
<i>q</i> <sub>2</sub> (mmol g <sup>-1</sup> )	0.576341
<i>k</i> <sub>1</sub> (kPa <sup>-1</sup> )	0.00500354
<i>k</i> <sub>2</sub> (kPa <sup>-1</sup> )	0.163364
<i>R</i> <sup>2</sup>	0.999998
<b>Fe-BTC / CO<sub>2</sub> / DSLF</b>	
<i>q</i> <sub>1</sub> (mmol g <sup>-1</sup> )	1.84866
<i>q</i> <sub>2</sub> (mmol g <sup>-1</sup> )	0.852406
<i>k</i> <sub>1</sub> (kPa <sup>-n1</sup> )	0.00862247
<i>k</i> <sub>2</sub> (kPa <sup>-n2</sup> )	0.074762
<i>n</i> <sub>1</sub>	1.2241
<i>n</i> <sub>2</sub>	0.896536
<i>R</i> <sup>2</sup>	0.999999
<b>MIL-100 / CH<sub>4</sub> / L</b>	
<i>q</i> (mmol g <sup>-1</sup> )	2.66348
<i>k</i> (kPa <sup>-1</sup> )	0.00217646
<i>R</i> <sup>2</sup>	0.999988
<b>Fe-BTC / CH<sub>4</sub> / L</b>	
<i>q</i> (mmol g <sup>-1</sup> )	1.13186
<i>k</i> (kPa <sup>-1</sup> )	0.00710647
<i>R</i> <sup>2</sup>	0.999991

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