

Supplementary Information for

Matrix Effects on the Performance and Mechanism of Hg Removal from Groundwater by MoS₂ Nanosheets

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Materials

All chemicals used in this study were of analytical grade or higher. Sodium sulfate (Na_2SO_4) and sodium bicarbonate (NaHCO_3) were obtained from Linfeng Chemical Reagent Technology (Shanghai, China). Mercury nitrate ($\text{Hg}(\text{NO}_3)_2 \cdot \text{H}_2\text{O}$) was purchased from Macklin Chemical Reagent Technology (Shanghai, China). Calcium chloride anhydrous (CaCl_2) and sodium chloride (NaCl) were obtained from Guoyao Chemical Reagent Corporation (Shanghai, China).

Sorption kinetic and isotherm models

The commonly used pseudo-first-order (**Eq. (1)**) and pseudo-second-order (**Eq. (2)**) kinetic models were employed to evaluate the controlling of kinetic mechanism of adsorption process, and the relative model equations are presented in the following:¹

$$\ln(q_e - q_t) = \ln q_e - K_1 t \quad (1)$$

$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{t}{q_e} \quad (2)$$

where q_t and q_e (mg/g) represent the Hg uptake at time t (h) and equilibrium, respectively; K_1 and K_2 are pseudo-first-order and pseudo-second-order sorption rate constants, respectively.

The isotherm data was fitted with the classical Langmuir (**Eq. (3)**) model and Freundlich model (**Eq. (4)**):

$$q_e = \frac{q_m K_L C_e}{1 + K_L C_e} \quad (3)$$

$$q_e = K_F C_e^{\frac{1}{n}} \quad (4)$$

where q_e (mg/g) and C_e (mg/L) are the equilibrium Hg uptake and the equilibrium Hg concentration, q_m (mg/g) is the monolayer maximum sorption capacity, and K_L (L/mg) is the Langmuir affinity constant. K_F is the Freundlich affinity coefficient [(mg/g)/(mg/L)ⁿ], and n is the exponential coefficient.

Desorption tests

Before leaching tests, the Hg-laden MoS₂ and AC samples were prepared by adding 20 mg/L Hg(II) with either 8 mg/L MoS₂ nanosheets or 1.67 g/L activated carbon. The Hg removal efficiency by MoS₂ nanosheets and AC were above 97%, indicating nearly complete anchoring of Hg ions by MoS₂ and AC. Desorption tests were performed by monitoring the Hg release from Hg-laden MoS₂ and AC samples in 20 mL simulated groundwater, 20 mL acid solution (0.23 mM H₂SO₄ and 0.17 mM HNO₃), or 20 mL 1 mM EDTA solution. The mixture of solution of H₂SO₄ and HNO₃ was prepared at a mass ratio of 2:1 in DI water (pH = 3.2±0.1) to simulate the condition in which the samples are exposed to acidic rain (HJ/T 299-2007, China).² In all cases, the vials were sealed and continuously mixed on an end-over-end rotator at 60 rpm at room temperature (25±1 °C) for 1 d, 2 d, 4 d, and 7 d. The samples were filtered through the 0.22 μm PTFE filters and analyzed for Hg concentrations in the filtrates.

Table S1. Pseudo-first-order and pseudo-second-order models for simulating Hg sorption kinetics and the corresponding fitting parameters.

Kinetic models	Parameters			R^2
Pseudo-first-order	K_1 (h^{-1}) 0.97±0.12	q_e (mg/g) 50.91±1.18	$h_1 = K_1 q_e$ (mg/(g•h)) 49.38	0.9698
Pseudo-second-order	K_2 (g/(mg•h)) 0.075±0.01	q_e (mg/g) 1250±0.63	$h_2 = K_2 q_e^2$ (mg/(g•h)) 117187.5	0.9999

Table S2. Regression parameters of sorption isotherm data of Hg(II) onto MoS₂ nanosheets by Langmuir and Freundlich models.

Water bodies	Adsorption isotherm	Parameters		R^2
Groundwater	Langmuir	q_m (mg/g) 6288	b (L/mg) 1.82	0.9801
	Freundlich	K_F , (mg/g)/(mg/L) ⁿ 3494.11	n 0.23	0.9145
DI Water	Langmuir	q_m (mg/g) 4042.85	b (L/mg) 0.41	0.9592
	Freundlich	K_F , (mg/g)/(mg/L) ⁿ 1893.86	n 0.21	0.9883

Table S3. Comparison of the Hg removal capacities of different materials.

Adsorbent	Material Type	Capacity (mg/g)	Reference
Other Materials	FeS	3086.4	3
	Indium-modified ZVI	220.9	4
	Biochar	57.8	5
	SnS ₂	185.83	6
	GO	255.1	6
	SGO/Fe-Mn	233.17	7
	Multilayered Ti ₃ C ₂ Ox Mxene	4806	8
MoS ₂ -based Materials	d-MoS ₂ /Fe ₃ O ₄	425.5	9
	MoS ₂ -HNR	~1991	10
	Petal-like MoS ₂	289	11
	□P-PVDF/MoS ₂	578	12
	MoS ₂ /MMT	1836	13
	2D-MoS ₂	6288	Our work

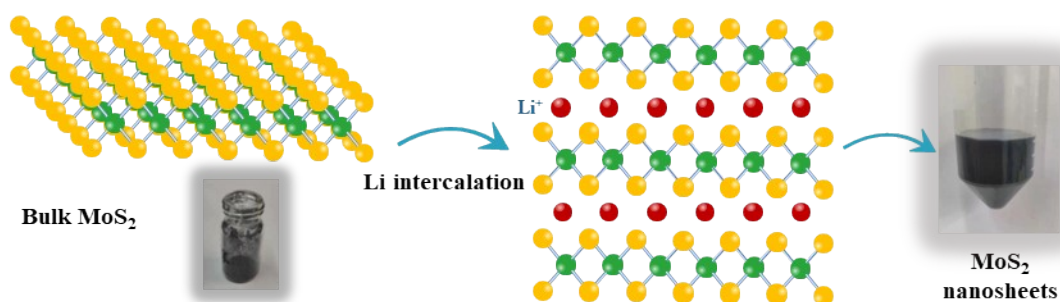


Figure S1. Schematic illustration of the chemical exfoliation of bulk MoS₂.

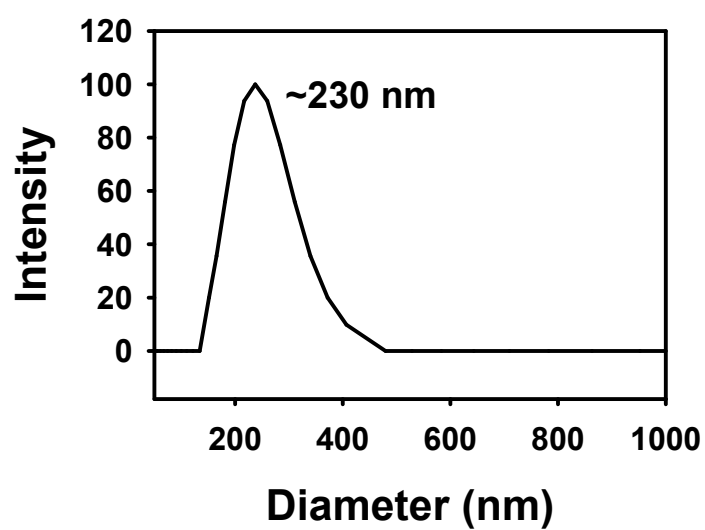


Figure S2. Particle size distribution of as-exfoliated MoS₂ nanosheets measured by dynamic light scattering.

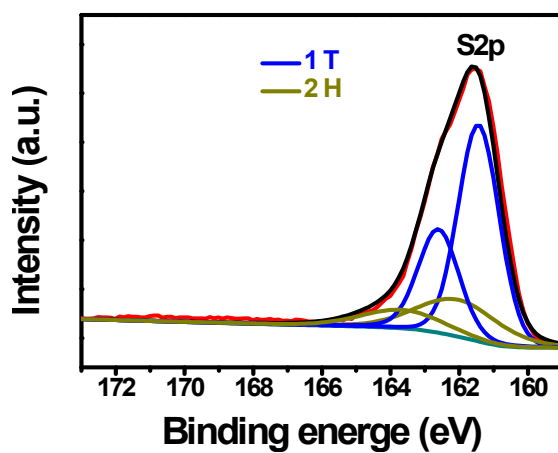


Figure S3. XPS S 2p spectra of as-prepared MoS₂ nanosheets.

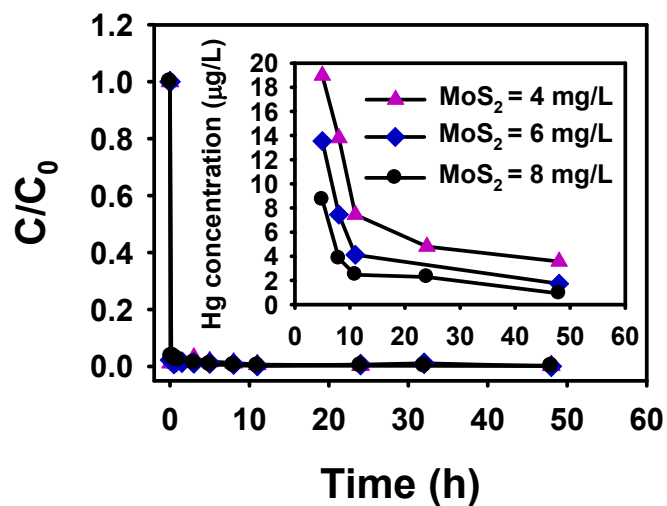


Figure S4. Hg uptake kinetics by MoS₂ nanosheets in groundwater.

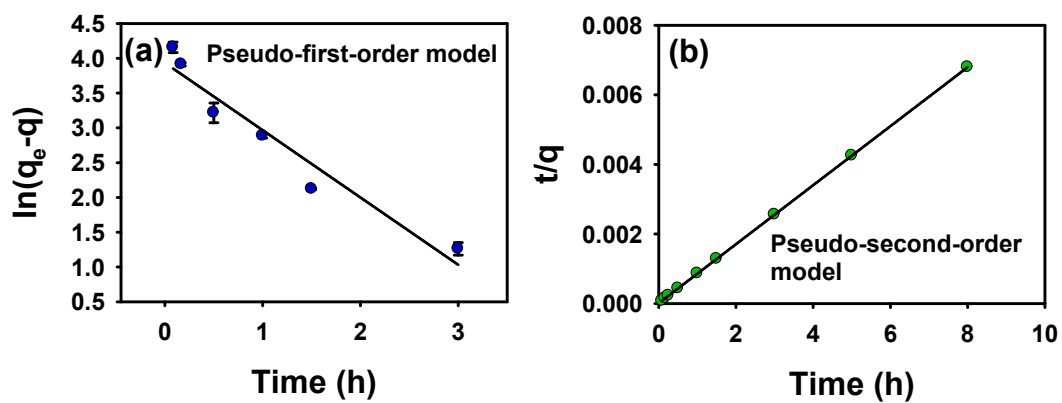


Figure S5. Hg uptake kinetics by MoS₂ nanosheets fitted with (a) pseudo-first-order model and (b) pseudo-second-order model.

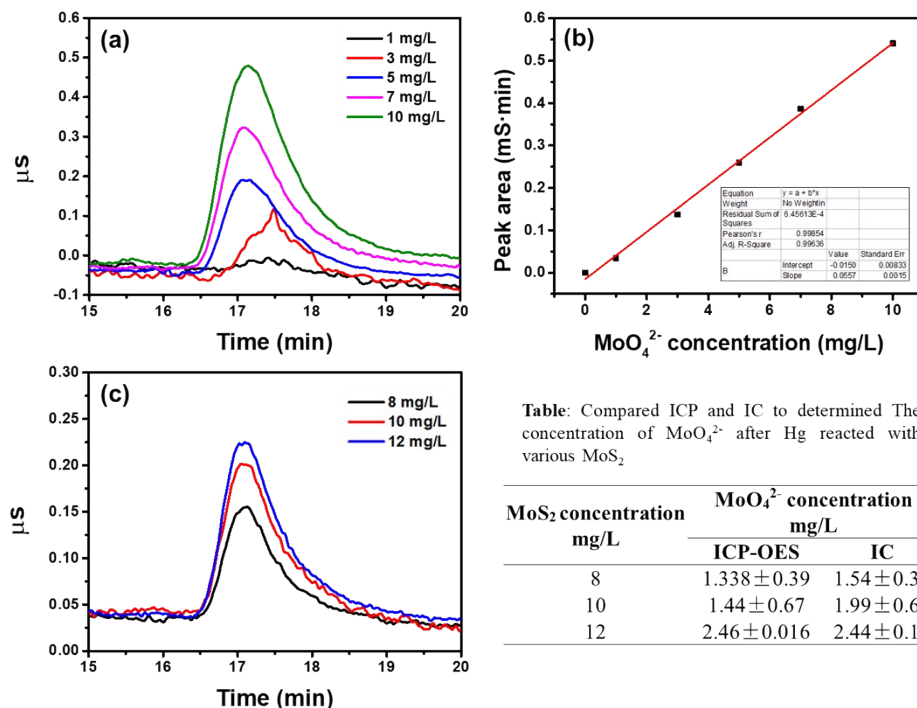


Figure S6. Determination of MoO_4^{2-} in solution by Ion Chromatography. (a) Chromatograms of different concentration of MoO_4^{2-} by the addition of sodium molybdate. (b) Linear relationship between MoO_4^{2-} concentration and peak area. (c) Ion Chromatograms of soluble Mo species after the reactions of Hg with MoS_2 at various concentrations. The concentrations of MoO_4^{2-} determined by ICP-OES and IC exhibited a good agreement (the inserted table).

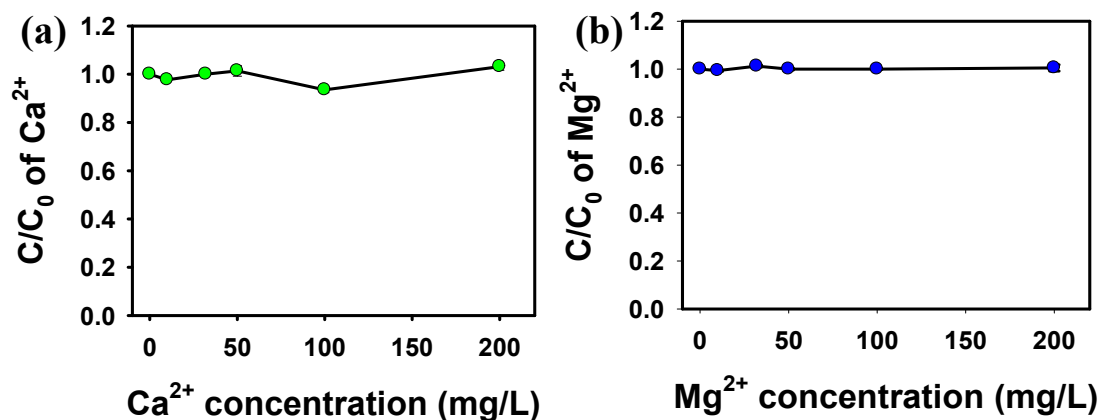


Figure S7. The ratios of the remaining to the initial concentrations of Ca^{2+} (a) and Mg^{2+} (b) in the presence of MoS_2 nanosheets.

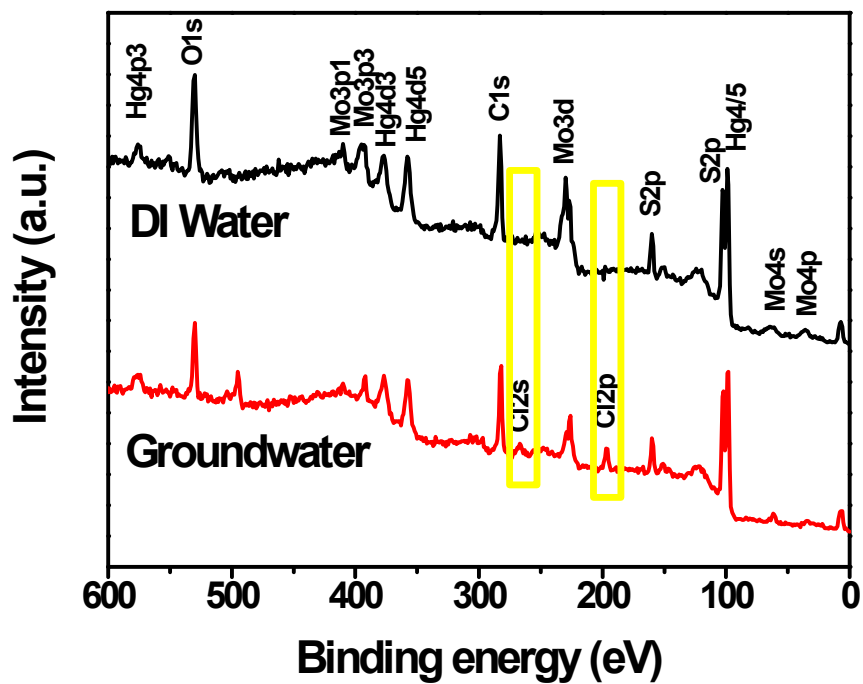


Figure S8. The XPS survey scan spectra of Hg-laden MoS₂ formed in DI water and Groundwater.

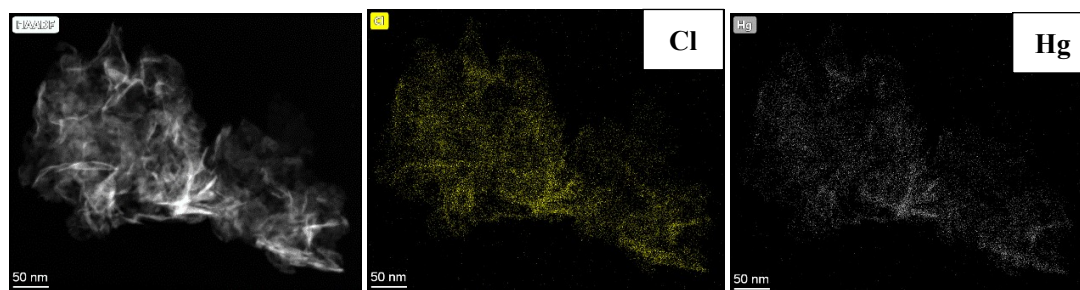


Figure S9. TEM images and EDS-mapping of Hg-laden MoS₂ nanosheets in groundwater.

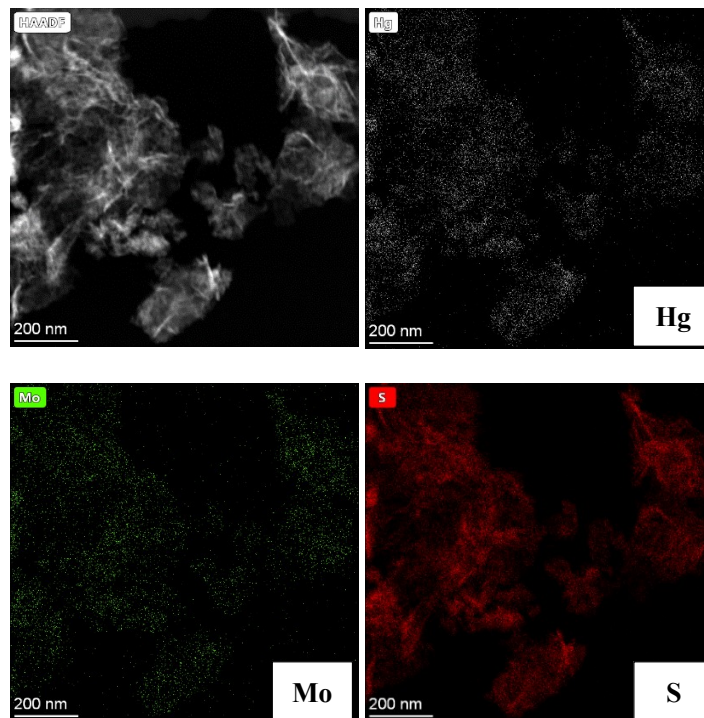


Figure S10. TEM images and EDS-mapping of Hg-laden MoS₂ nanosheets in DI water.

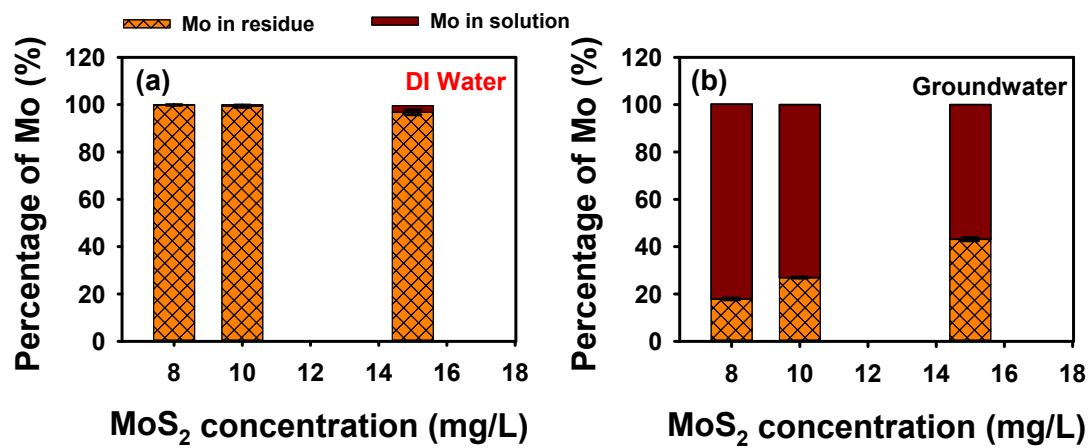


Figure S11. Mass distributions of Mo species in (a) DI water and (b) groundwater.

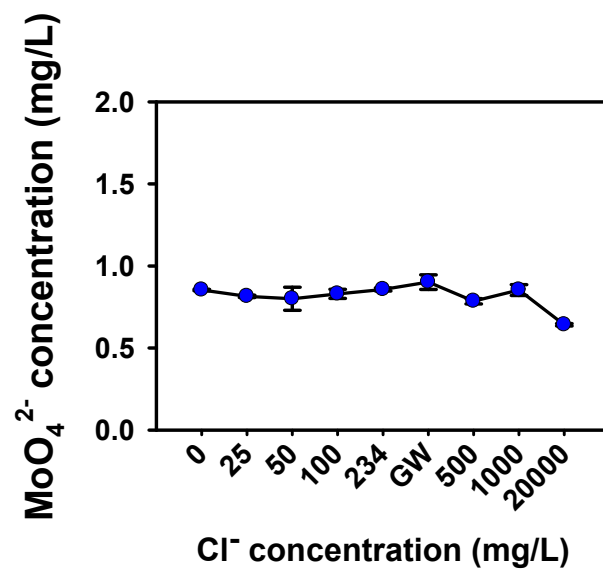


Figure S12. Oxidation of MoS₂ nanosheets in presence of Cl⁻ at various concentrations.

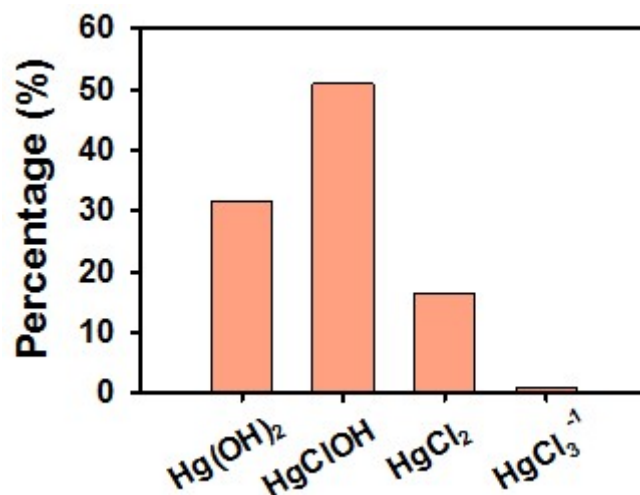


Figure S13. The percentage of Hg species in simulated groundwater using Visual MINTEQ (version 3.1) at pH = 8.0.

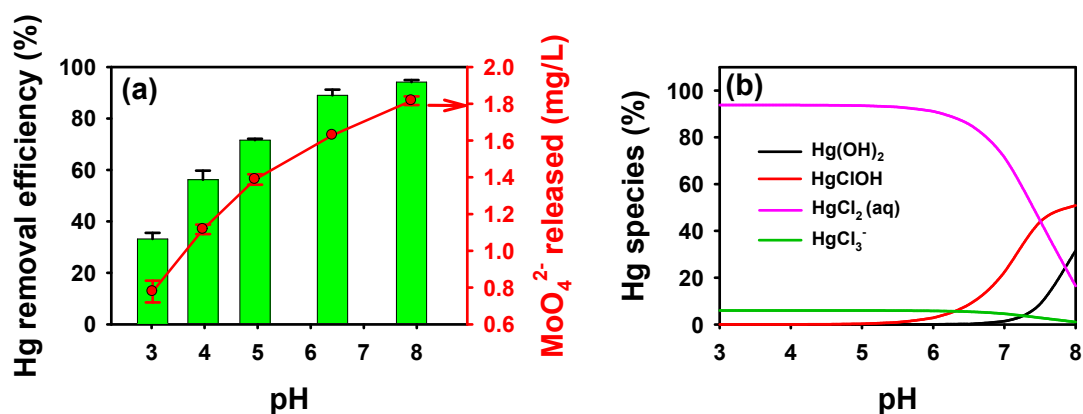


Figure S14. (a) Effects of pH on Hg removal efficiency by MoS₂, Hg = 20 mg/L, MoS₂ = 4 mg/L. (b) Hg speciation as a function of pH determined by Visual MINTEQ.

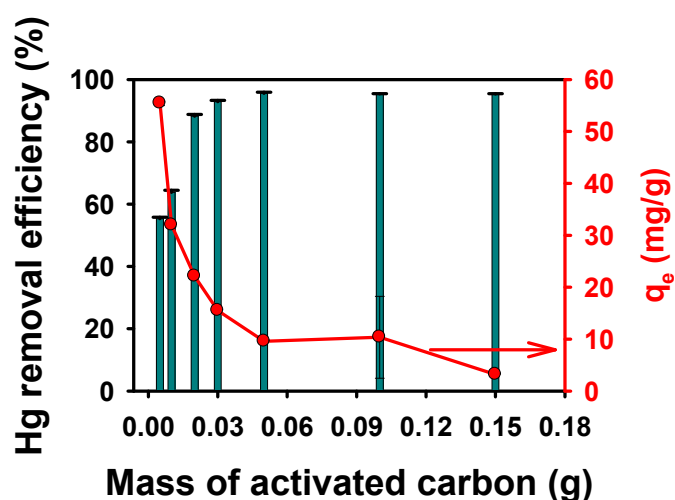


Figure S15. Hg uptake by AC in the groundwater. The mass of AC is 0–0.15 g, Hg concentration is 20 mg/L.

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