Supporting Information: Influence of heat transfer and wetting angle on condensable fluid flow through nanoporous anodic alumina membranes

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S3 Permeance versus relative upstream pressure for a pore size of 18 nm. Contact angles of 0°, 10°, 30°, 60°, and 80°, boundary condition $T_1 - T_2 = 0.7(T_1 - T_{2,\text{adiabatic}})$. Flow of (a) isobutane and (b) freon 142b. S-4

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S5 Permeance versus relative upstream pressure for a pore size of 60 nm. Contact angles of 0°, 10°, 30°, 60°, and 80°, boundary condition $T_1 - T_2 = 0.7(T_1 - T_{2,\text{adiabatic}})$. Flow of (a) isobutane and (b) freon 142b. S-5

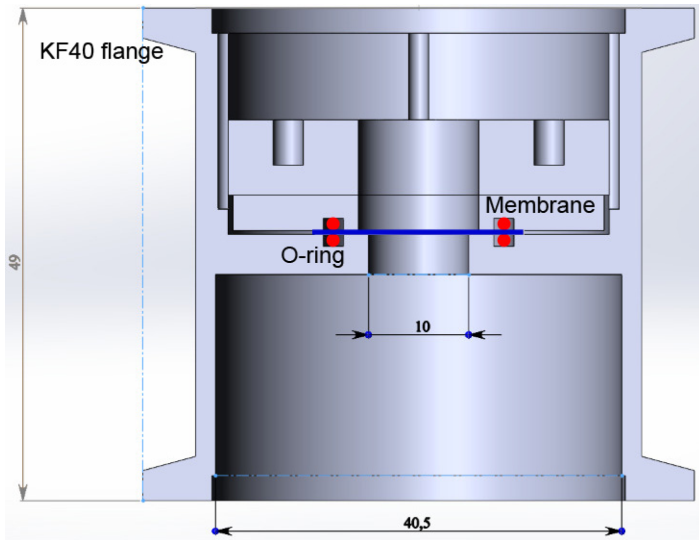

Figure S1: Experimental cell.

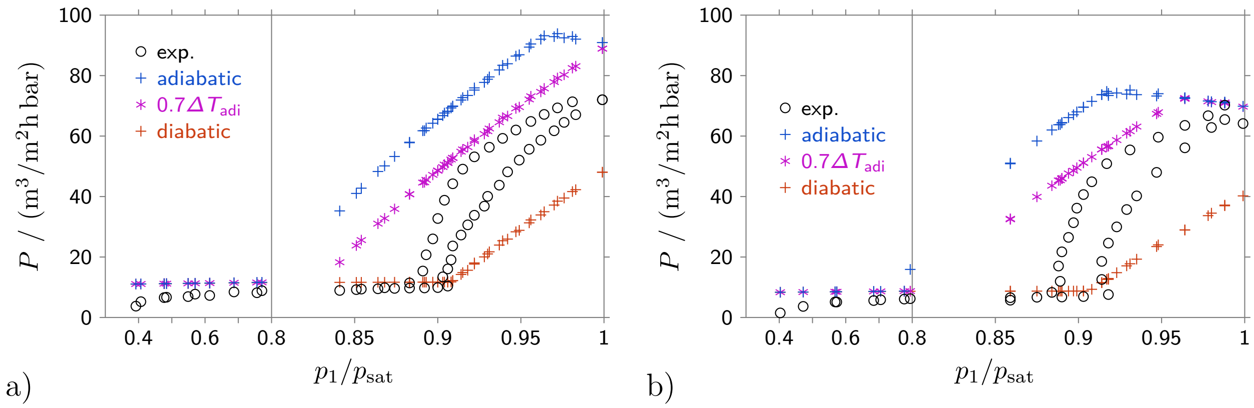

Figure S2: Permeance versus relative upstream pressure for a pore size of 18 nm. Contact angle of 0° and boundary conditions: adiabatic, diabatic, $T_1 - T_2 = 0.7(T_1 - T_{2,\text{adiabatic}})$. Flow of (a) isobutane and (b) freon 142b.

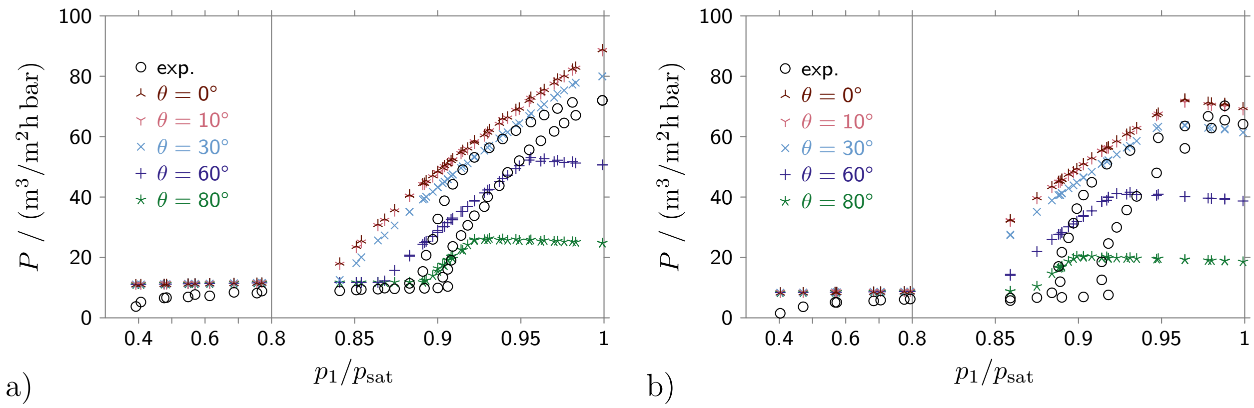

Figure S3: Permeance versus relative upstream pressure for a pore size of 18 nm. Contact angles of 0°, 10°, 30°, 60°, and 80°, boundary condition $T_1 - T_2 = 0.7(T_1 - T_{2,\text{adiabatic}})$. Flow of (a) isobutane and (b) freon 142b.

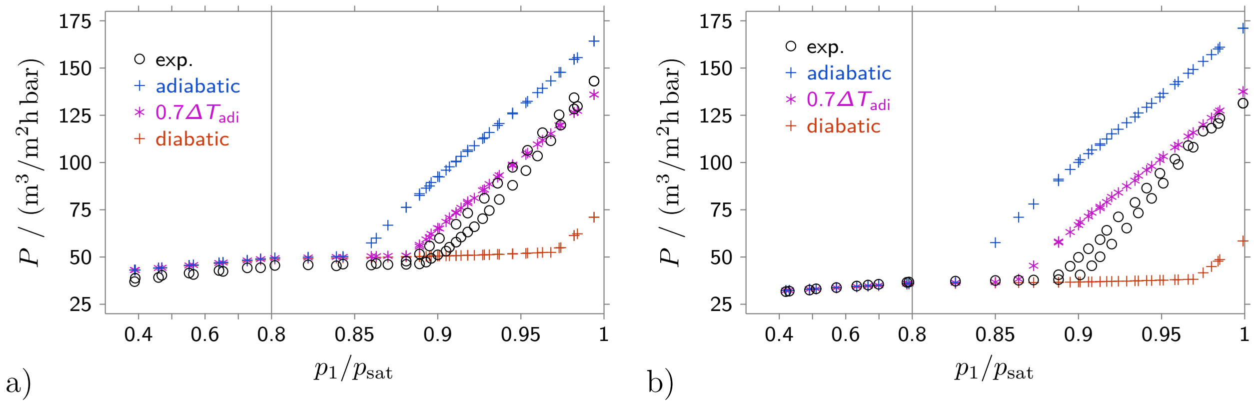

Figure S4: Permeance versus relative upstream pressure for a pore size of 60 nm. Contact angle of 0° and boundary conditions: adiabatic, diabatic, $T_1 - T_2 = 0.7(T_1 - T_{2,\mathrm{adiabatic}})$. Flow of (a) isobutane and (b) freon 142b.

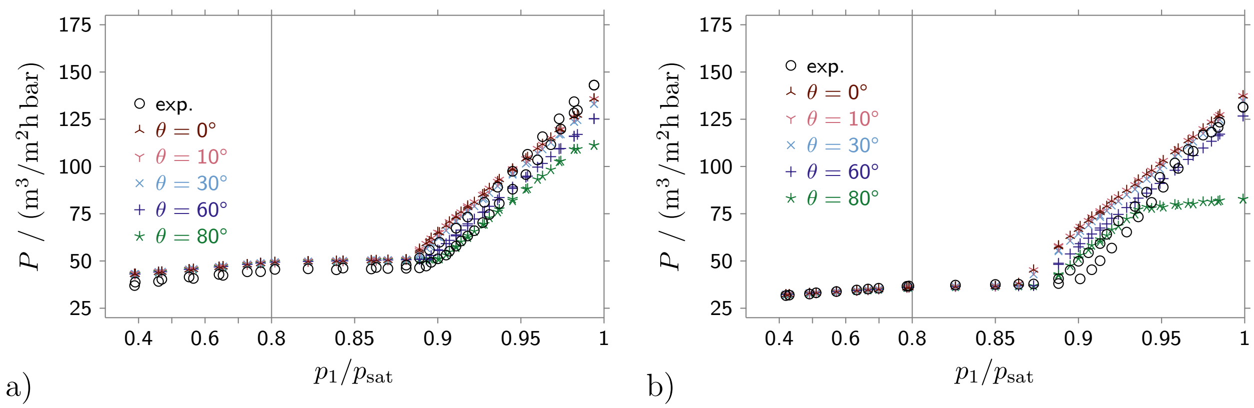

Figure S5: Permeance versus relative upstream pressure for a pore size of 60 nm. Contact angles of 0°, 10°, 30°, 60°, and 80°, boundary condition $T_1 - T_2 = 0.7(T_1 - T_{2,\mathrm{adiabatic}})$. Flow of (a) isobutane and (b) freon 142b.