Electronic Supplementary Information

Selective synthesis of furfuryl acetate over solid acid catalysts and active site exploration using Density Functional Theory

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Experimental details

Catalyst synthesis

SAPO-11 was synthesized as per the reported synthesis procedure ¹. Typically, 15 g of pseudoboehmite and 25.3 g of orthophosphoric acid were stirred with 95 mL of distilled water to which 22.3 g of triethylamine and 1.6 g of ludox AS-40 were added. The mixture was stirred for 4 h at room temperature and then was transferred to a teflon-lined stainless-steel autoclave and heated in an oven at 200 °C for 24 h. The material was filtered, washed, dried, and calcined (600 °C for 6 h) to yield SAPO-11.

Al-SBA-15 was synthesized as per the reported procedure ². In a typical synthesis, 4 g of amphiphilic triblock co-polymer poly–(ethylene glycol)–block poly–(propylene glycol)–block poly–(ethylene glycol) and 120 g of 2M HCl were homogenized in 30 g of distilled water. To this solution, 8 g of tetraethyl orthosilicate was added dropwise and stirred for 24 h at 40 °C. The gel formed was transferred to teflon lined stainless steel autoclave and placed in a preheated oven (100 °C) for 48 h. The material was filtered, washed with distilled water, dried, and calcined at 550 °C

for 24 h to yield SBA-15. SBA-15 (2 g) was subjected to post-synthetic modification by isomorphically substituting Si with Al (0.88 g of anhydrous AlCl₃). The precursors were suspended in ethanol and aged for 10 h at 80 °C and further filtered, washed with ethanol, and dried at RT. The final material was calcined at 550 °C for 5 h to yield Al-SBA-15.







Figure S1. (A) N_2 sorption isotherms of all the screened catalysts- (a) amberlyst-15, (b) Al-SBA-15, (c) ferrierite, (d) Y-Zeolite, (e) SAPO-11, (f) H-Beta (B) N_2 sorption isotherms of sulfated zirconia catalysts with varied sulfation (C) Mean pore diameter of sulfated zirconia catalysts with varied sulfation



Figure S2. Pyridine-FTIR spectra of screened catalysts



Figure S3. SEM micrographs of sulfated zirconia catalysts with different sulfation.

Catalytic activity study

Entry	Retention time	Component		
1	4.4	Acetic acid		
2	6.7-6.8	Furfuryl acetate		
3	7.5	2,2'-difurfurylmethane		
4	8.4	Furfuryl alcohol		
5	11.5	Difurfuryl ether		
6	14.6-14.7	5-(furan-2-ylmethyl)furan-2-yl-aceta		
7	15.7	Difurfuryl furan		

Table S1. Components in GC analysis and their retention time

GC program: Oven: 80 °C (1 min), @ 20 °C/min to 120 °C (1min), @ 10 °C/min to 165 °C (1min), @20 °C/min to 200 °C (1min), 15 °C/min to 245 °C (15min)

Representative chromatograms



Figure S4. Effect of temperature. Reaction conditions: Catalyst- SZr(2.5M-w), catalyst concentration- 1.5wt%, reactants mole ratio- 1:10 (FA: acetic acid), reaction time- 15mins, temperature- 110 °C



Figure S5. Effect of catalyst loading. Reaction conditions: Catalyst- SZr(2.5M-w), temperature-100 °C, reactants mole ratio- 1:10 (FA: acetic acid), reaction time- 15mins, Catalyst concentration-0.37wt%



Figure S6. Catalyst screening. Reaction conditions: Catalyst- amberlyst-15, temperature- 100 °C, reactants mole ratio- 1:10 (FA: acetic acid), Catalyst concentration- 1.5wt%, reaction time- 6h

Table S2.	Performance	of	different	screened	catalysts	for	FA	esterification	reaction	with
acetic acio	d									

Catalyst	FA FAc conversion Selectivi		Others selectivity (%)					Carbon Balance	FAc yield
	(%)	ty (%)	SP1	SP2	SP3	SP4	Others	(%)	(%)
Blank reaction	9.0	36.1	12.0	19.3	9.5	23.1	0.0	99	3.2
Y-Zeolite (SAR5.1)	12.9	30.7	8.6	39.6	13.5	7.6	0.0	98	4.0

H-Beta (SAR25)	14.4	31.3	3.9	20.4	14.3	21.8	8.3	98	4.5
SAPO-11	16.9	29.9	3.4	17.8	8.6	31.4	8.8	98	5.1
Al-SBA-15 (SAR35)	17.0	36.8	19.9	15.0	22.0	6.2	0.0	98	6.3
Ferrierite (SAR20)	16.8	38.5	5.6	13.7	9.1	25.9	7.2	98	6.5
Sulfated zirconia	28.2	46.7	13.5	10.3	12.5	12.4	4.6	99	13.2
Amberlyst-15	42.6	42.6	6.1	8.2	7.3	5.9	30.0	98	18.1

SP1- 2,2'-difurfurylmethane, SP2- difurfuryl ether, SP3- 5-(furan-2-ylmethyl)furan-2-yl-acetate, SP4- Difurfuryl furan

Catalyst screening. Reaction conditions: catalyst concentration - 1.5wt%, temperature- 70 °C, reaction time- 4 h, mole ratio- 1:10 (FA: acetic acid).

Table S3 Acidity of the fresh and spent SZr(2.5M-w) catalyst for comparison

Catalyst	Acidity (mmol g ⁻¹) from NH ₃ TPD						
Catalyst	Weak	Moderate	Strong	Total			
SZr(2.5M-w)	0.01	0.09	0.13	0.23			
SZr (2.5M-w)-Used	0.01	0.06	0.13	0.20			

Plausible reaction mechanism

Table S4. Hammett acidity values of solid acid catalysts used in this study

S.No.	Catalysts	T _m (K) from NH ₃ -TPD	1/T _m	Но
1	Sulfated Zirconia	-	-	-14.5
2	H_2SO_4	-	-	-11.9
3	Y-Zeolite (SAR 5.1)	488	0.002049	-10.4
4	Ferrierite (SAR20)	441	0.002268	-8.4

5	Al-SBA-15 (SAR35)	440	0.002273	-8.3
6	H-Beta (SAR25)	435	0.002299	-8.1
7	SAPO-11	388	0.002577	-5.6
8	Amberlyst-15	-	-	-2.2

Note: Catalysts 1,2 and 8 are from references ^{3,4}. Catalysts 3-7, Hammett acidity values were determined using the formula $H_0 = a+b (1/T_m)$ where a and b are empirical constants specific for aluminosilicate catalysts and T_m is temperature peak maximum obtained from NH₃-TPD profile as given in references ^{5,6}

Table S5. Three trials to find the repeatability of the experiments

Trial	FA Conversion (%)	FAc selectivity (%)	FAc Yield (%)
1	83.3	85.1	70.9
2	83.0	85.8	71.2
3	83.8	85.0	71.2

Reaction conditions: Catalyst- SZr, catalyst concentration- 1.5wt%, temperature- 100 °C, reactants mole ratio- 1:10 (FA: acetic acid), reaction time- 6 h. The calculated % error for the data $< \pm 1$ %

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