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	GHSV	T(°C)	P(Mpa)	CO₂ Conv (%)	CO sel	Hydrocarbon selectivity (%)		
Catalysts	(mLh <sup>-1</sup> g <sub>cat</sub> <sup>-1</sup> )					$CH_4$	C <sub>2-4</sub>	C <sub>5+</sub>
Na–Fe <sub>3</sub> O <sub>4</sub> / HZSM-5 <sup>1</sup>	4000	320	3.0	34.0	14.0	8.0	18.0	74.0
In <sub>2</sub> O <sub>3</sub> / HZSM-5 <sup>2</sup>	9000	340	3.0	19.0	48.0	1.0	27.6	71.4
FeNa(1.18) <sup>3</sup>	2000	320	3.0	40.5	13.5	15.8	54.1	30.1
Fe-MOF- derived <sup>4</sup>	3600	400	3.0	46.1	17.5	32.3	26.9	40.8
10K13Fe <sub>2</sub> Co 100ZrO <sub>2</sub> <sup>5</sup>	7200	400	3.0	42.3	21.9	25.7	34.0	18.4
$Na-Fe_3O_4^6$	4000	320	3.0	34.0	14.0	12.0	48.0	40.0
FeK/Al <sub>2</sub> O <sub>3</sub> <sup>7</sup>	1800	400	3.0	53.5	17.0	20.0	37.0	26.0
5Mn–Na/Fe <sup>8</sup>	2040	320	3.0	39.3	9.0	8.9	31.2	59.9
K- ZnFe <sub>2</sub> O <sub>4</sub> 9	12000	320	2.0	47.1	8.7	14.8	39.1	46.1
FeAlOx-5 <sup>10</sup>	4000	330	3.5	36.8	7.2	12.1	30.1	57.8
Our work	12000	320	3.0	57.75	9.06	8.13	18.13	73.8

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		Distribution of element (%)								
Catalyst	k	<								
	а*	b*	Fe	Со	Ni	Cu	Zn			
Fe-Fe	0.805	0.805	63.5							
Co-Fe	0.696	0.816	40.4	18.4						
Ni-Fe	0.342	0.885	33.4		15.0					
Cu-Fe	0.0438	0.812	35.2			16.3				
Zn-Fe	0.0242	0.833	32.0				15.2			

Table S2. Catalys	st components	(Same K conten	t in each catalyst)
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a: K content before K supplementation

b: K content after K supplementation

Note: The data in this table were measured by ICP

Catalyst CO <sub>2</sub> conversion	<u> </u>	S <sub>C</sub> o	FTY <sup>a</sup>	STY <sup>b</sup>	Selectivity (C-%, CO-free)			_	
	conversion		(µmol <sub>co2</sub> •g-1 Fe∙s <sup>-1</sup> )	(mmol·g-1 Fe·h <sup>-1</sup> )	$CH_4$	C= 2- 4	C0 2- 4	C <sub>5+</sub>	0/P <sup>c</sup>
Fe-Fe	34.67	26.53	11.94	20.29	17.59	41.09	6.66	34.68	6.17
Co-Fe	46.03	15.48	28.66	36.12	23.54	40.05	6.84	29.59	5.86
Ni-Fe	36.63	28.28	23.41	9.18	65.36	15.53	11.31	7.81	1.37
Cu-Fe	32.93	38.96	17.10	2.59	25.77	40.23	8.29	25.74	4.85
Zn-Fe	50.67	12.04	41.45	105.44	11.64	22.28	3.94	62.15	5.65
a: FTY: Iron time yield to hydrocarbons									

**Table S3** Comparison of performances of the catalyst (Reaction condition: T: 320 °C, P: 3 MPa,  $H_2 / CO_2 / N_2$ : 18/6/6, GHSV: 12000 mL.g-1 cat. h<sup>-1</sup>, TOS: 8 h, same K content).

b: STY: The space time yield (STY) from  $C_{5+}$  hydrocarbons

c: Olefin to paraffin ratio of C<sub>2</sub>-C<sub>4</sub> hydrocarbons



Fig S1.  $N_2$  adsorption-desorption isotherms of different iron-based catalysts.



Fig S2 HR-TEM of fresh samples.



Fig S3 Special SEM images and corresponding element composition mapping of different spinel-like catalysts.



Fig S4 HR-TEM of spent catalysts.

## Reference

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