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Supporting information

Controlling the Distribution of Aluminum in a Cu-Zeolite Catalyst by Seed-Assisted Synthesis to Improve its NH₃-SCR Activity

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mol/mol %	KFI parent	KFI-SA1	KFI-SA2	KFI-SA3
Si	27.53	27.10	29.29	25.79
Al	5.64	5.66	6.06	5.20
K	0.19	0.35	0.34	0.29
Si/Al	4.88	4.79	4.83	4.96

Table S1. The composition of NH₄-KFI obtained by SEM-EDX.

	Cu-KFI parent	Cu-KFI -SA1	Cu-KFI-SA2	Cu-KFI-SA3
K (wt%)	0.24	0.33	0.27	0.30
Cu/Al (mol/mol)	0.20	0.20	0.20	0.20

Table S2. The composition of Cu-KFI obtained by ICP-AES.

	Si/Al _f ratio					
	Parent	SA1	SA2	SA3	Average	
NH ₄ -KFI	4.38	4.57	4.42	4.28	4.41 (±0.10)	
Cu-KFI	6.01	5.41	5.64	5.77	5.71 (±0.22)	
Cu-KFI HTA	7.35	7.53	7.37	7.37	7.41 (±0.07)	

Table S3. The Si/Al_f ratio of NH_4-KFI, Cu-KFI and Cu-KFI HTA.



Fig. S1. The XRD profiles of (a) NH₄-KFI and (b) Cu-KFI.



Fig. S2. The Ar-BET isotherms of the Cu-KFI.



Fig. S3. ²⁷Al-NMR spectra of the (a) NH₄-KFI and (b) Cu-KFI.



Fig. S4. The NH₃-TPD profiles of the (a) NH₄-KFI and (b) Cu-KFI.



Fig. S5. The result of cobalt ions titration for measuring the amount of paired Al sites in the parent and seed added Cu-KFI.



Fig. S6. (a) The EPR spectra and (b) H_2 -TPR profiles of Cu-KFI with different loadings.



Fig. S7. The EPR spectra of Cu-KFI at room temperature.



Fig. S8. The ²⁹Si and ²⁷Al-NMR spectra of hydrothermally aged Cu-KFI catalysts.



Fig. S9. (a) The H₂-TPR and (b) SCR activity of hydrothermally aged Cu-KFI catalysts.



Fig. S10. The SEM image of the hydrothermally aged (a) Cu-KFI parent, (b) Cu-KFI-SA1 (c) SA2, and (d) SA3.



Fig. S11. The correlation between the SCR rates in the reaction and peak consumption rates of Lewis NH₃ during DRIFT analysis.



Fig. S12. The NO and NH₃ concentration profiles during the simulated SCR protocol at 200 °C. The (a) Cu-KFI parent and (b) Cu-KFI seed #2 catalysts were pretreated under 20% O_2 /He for 30 min, and fully saturated by 350 ppm NH₃. After confirming the steady-state concentration at bypass, the 500 ppm NO and 350 ppm NH₃ were introduced into the catalysts to reduce the Cu ions (gray box). After purging with He, the reduced catalysts were oxidized with O_2 (sky blue box). Then, the NO was introduced to consume the all adsorbed NH₃.



Fig. S13. The DRIFTS peak profiles of Brønsted acid NH_4^+ and Lewis acid NH_3 in the Cu-KFI parent during the simulated SCR reaction protocol.

In oxidation process (100-140 min), the Brønsted acid NH_4^+ slightly decreased at initial. The amount of consumed NH_4^+ was quantified combining the DRIFT and NH_3 -TPD results in Figure S4. The amount of Brønsted acid sites of Cu-KFI parent is 1.34 mmol/g, which is obtained by deconvoluting the desorption profile in Figure S4. This would correspond to the intensity of B acid NH_4^+ at 40 min in the DRIFT profile. Therefore, we could estimate the decreased amount of B acid sites at 100 min by following equation.

Consumed $NH_4^+ = \frac{Decreased intensity at 100 min}{Intensity at 40 min} \times amount of NH_4^+ on Cu-KFI parent in NH_3-TPD$



Fig. S14. NH₃ oxidation of Cu-KFI parent under 500 ppm NH₃, 10% O₂ and N₂ balance (GHSV = 240,000 h⁻¹).