

Mechanistic Insight into Low Temperature SCR by Ceria-Manganese Mixed Oxide Phases Incorporated into Zeolites

Supporting Information

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Table S1. Textural properties obtained through N₂ physisorption

Sample	BET surface area (m ² g ⁻¹)		Pore volume (cm ³ g ⁻¹)	
	Total	Micropore	Total	Micropore
H-SSZ-13	729	667	0.30	0.25
Ce _{0.7} Mn _{0.3} O _x /H-SSZ-13	552	509	0.28	0.19
Ce _{0.7} Mn _{0.3} O _x	28	n/a	0.54	n/a

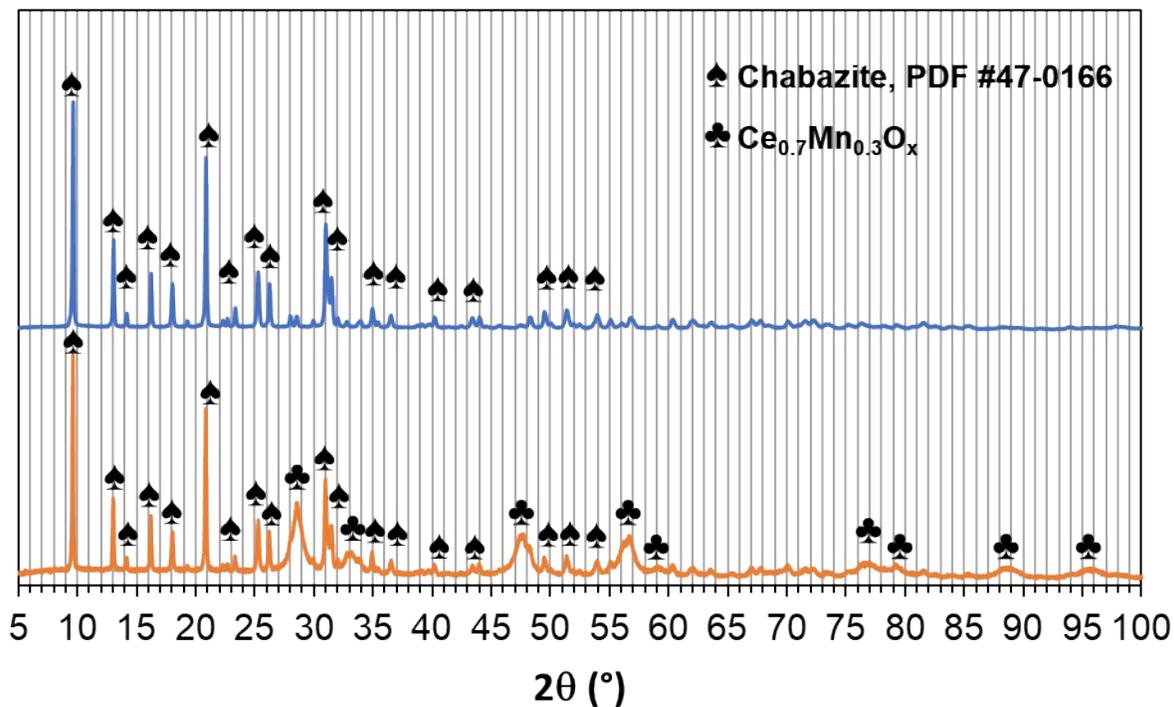


Figure S1. Experimental XRD pattern of H-SSZ-13 (top) and $\text{Ce}_{0.7}\text{Mn}_{0.3}\text{O}_x/\text{H-SSZ-13}$ (bottom).

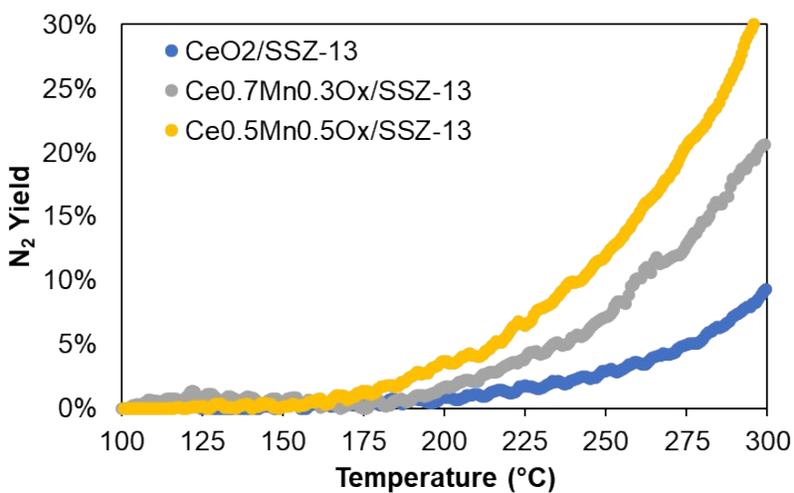


Figure S2. N_2 yield as a function of temperature during NH_3 -SCR over $\text{Ce}_x\text{Mn}_{1-x}\text{O}_y/\text{H-SSZ-13}$ composite catalyst. Reaction conditions: $[\text{NO}] = 325$ ppm; $[\text{NO}_2] = 6$ ppm; $[\text{NH}_3] = 330$ ppm; $[\text{O}_2] = 15\%$; $[\text{N}_2] = \text{balance}$; flow rate = 1.5 SLM; GHSV = $1.7 \times 10^6 \text{ h}^{-1}$.

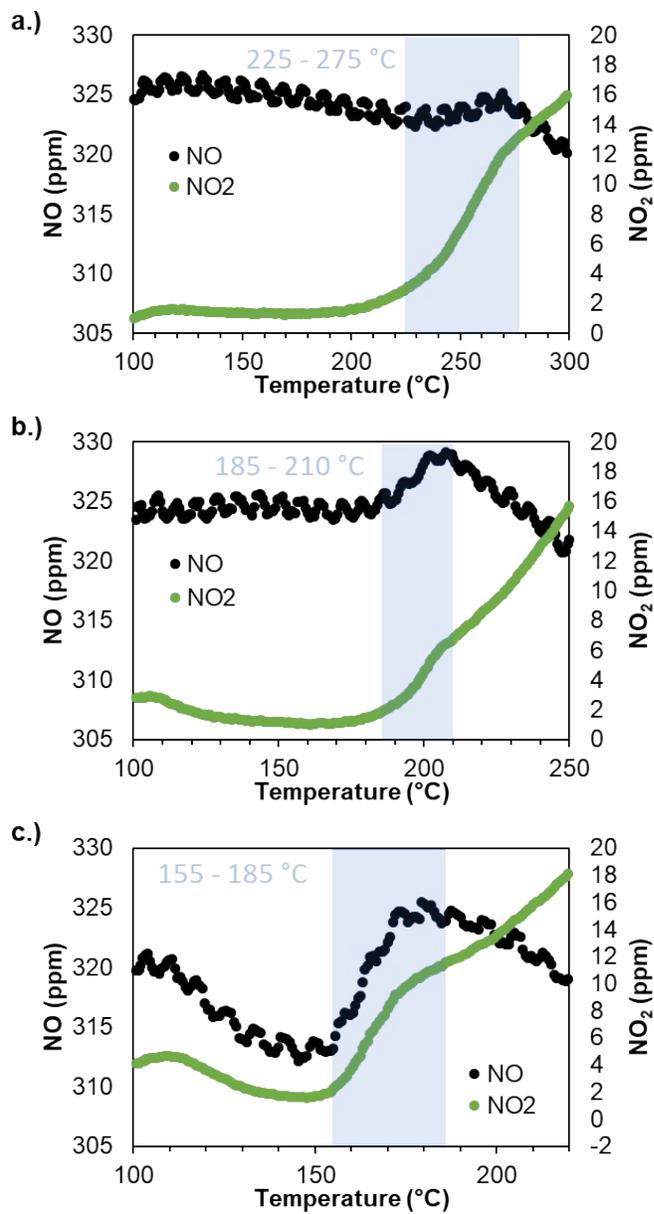


Figure S3. NO and NO₂ concentration profile at the reactor outlet over (a) CeO₂/H-SSZ-13, (b) Ce_{0.7}Mn_{0.3}O_y/H-SSZ-13, (c) Ce_{0.5}Mn_{0.5}O_y/H-SSZ-13 during NO oxidation with pre-adsorbed NH₃. Reaction conditions: [NO] = 325 ppm; [NO₂] = 6 ppm; [O₂] = 15 %; [N₂] = balance; F = 1.5 SLM; GHSV = 1.7e+6 h⁻¹.

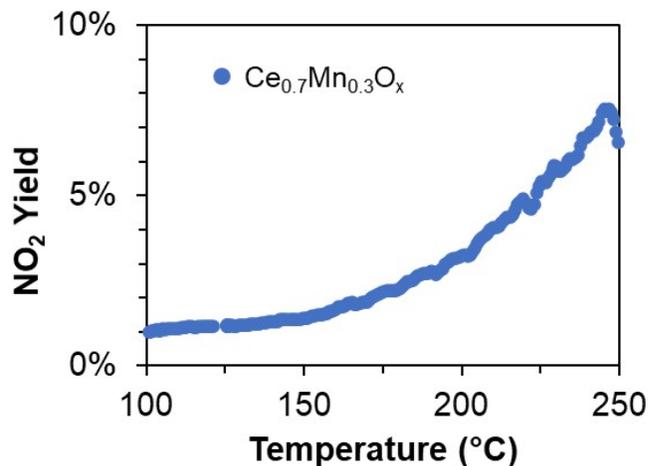


Figure S4. NO oxidation activity over bulk Ce_{0.7}Mn_{0.3}O_y with pre-adsorbed NH₃. No curvature change is observed, unlike the mixed oxide supported on zeolite. Reaction conditions: [NO] = 325 ppm; [NO₂] = 6 ppm; [O₂] = 15 %; [N₂] = balance; F = 1.5 SLM; GHSV = 4.6e6 h⁻¹.

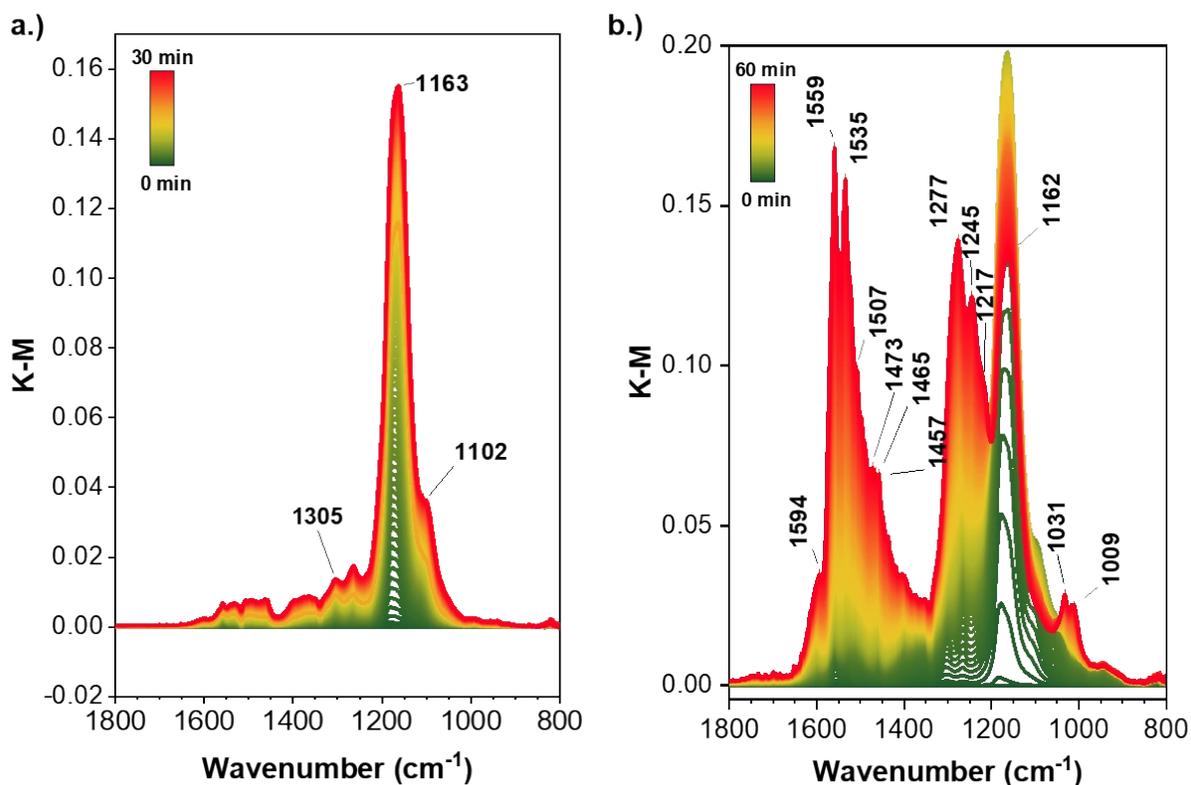


Figure S5. DRIFTS recorded during exposure of Ce_{0.7}Mn_{0.3}O_x bulk oxide to a.) NO and b.) NO + O₂ at 150 °C. The catalyst was pre-treated with 2% O₂ at 500 °C for 15 min, followed by He purge for 45 min at 500 °C prior to each measurement. Conditions: [NO] = 350 ppm; [O₂] = 2%; F = 100 mL min⁻¹. For (a), the bands

at 1163 cm^{-1} and 1305 cm^{-1} were attributed to symmetric nitrites. The band at 1102 cm^{-1} was attributed to hyponitrites.¹

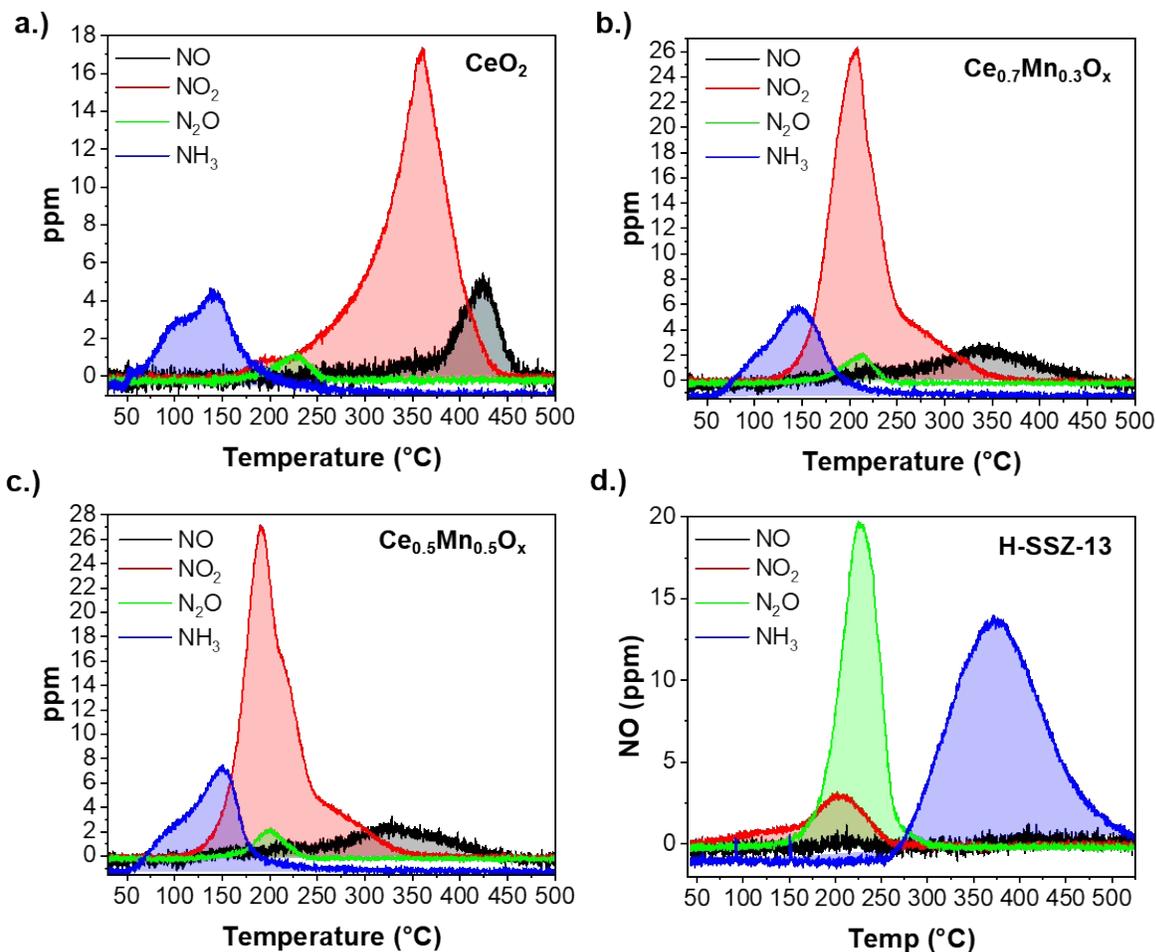


Figure S6. Ammonium nitrate decomposition products observed during heating in N_2 over bulk oxide catalysts. The shaded areas represent the integrated areas used in [Figure 3a](#). The NO evolved in (a-c) is a thermodynamic effect derived from NO_2 dissociation to NO and O_2 . For (a), the temperature that NO_2 evolved likely reflects the ability of the ceria surface to store NO_x as opposed to the temperature at which ammonium nitrate decomposes.² From panel (a) we assume that in the absence of NO_x storage, the NO_2 desorption leading edge would have been around $175\text{ }^\circ\text{C}$, about $40\text{-}50\text{ }^\circ\text{C}$ higher than for the Mn-based catalysts. Conditions: $[\text{NH}_4\text{NO}_3] = 15\text{ wt. } \%$; $\beta = 10\text{ }^\circ\text{C min}^{-1}$; $F = 1\text{ SLM}$.

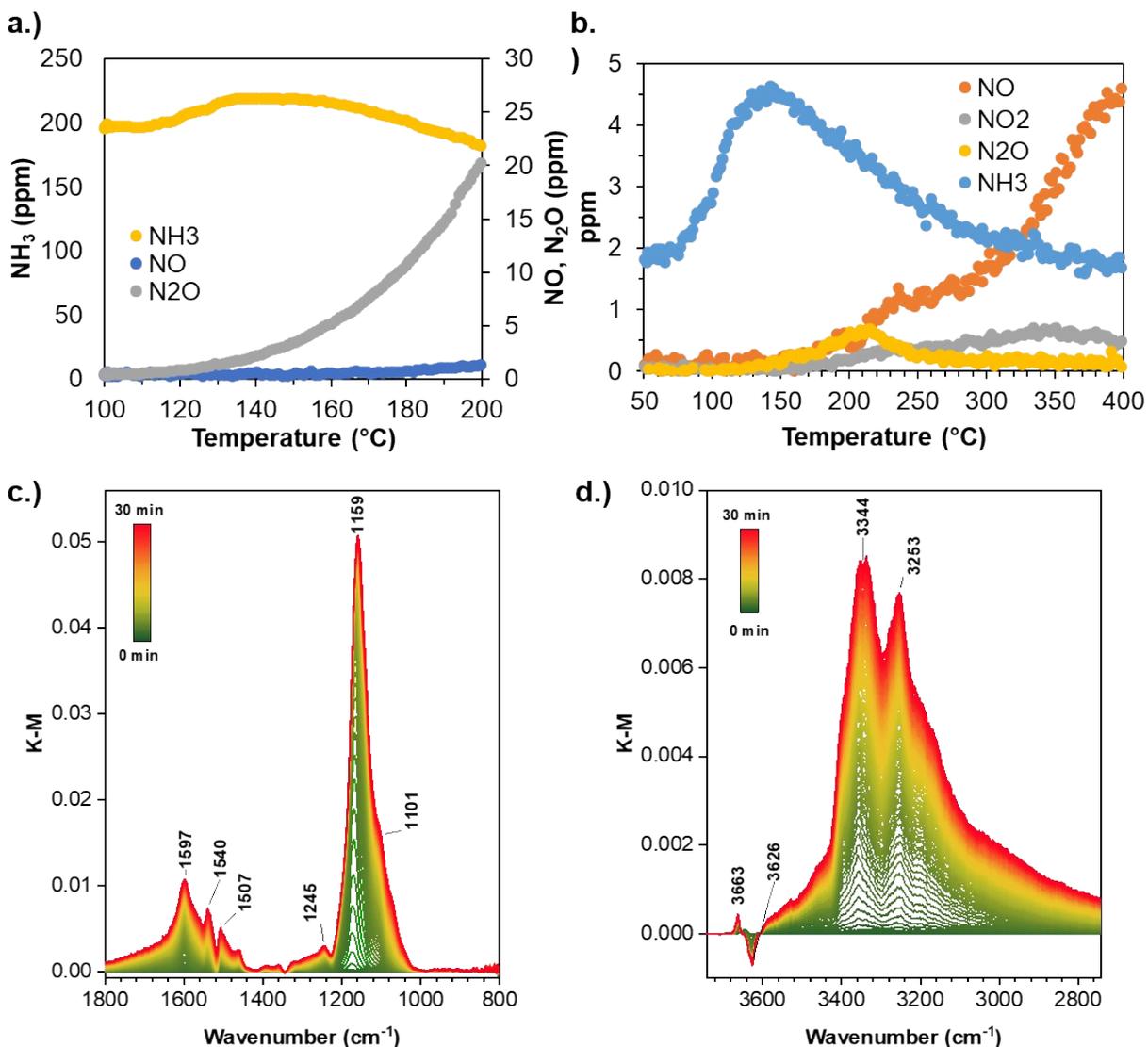


Figure S7. a.) Light-off profile obtained by flowing NH₃ over bulk Ce_{0.7}Mn_{0.3}O_y. Conditions: [NH₃] = 200 ppm; [N₂] = balance; β = 5 °C min⁻¹; F = 1 SLM. b.) NH₃ temperature programmed desorption (TPD) over bulk Ce_{0.7}Mn_{0.3}O_y. The catalyst was heated to 500 °C in 15 % O₂ for 0.5 h, followed by cooling under He, admittance of 350 ppm NH₃ for 0.5 h at 50 °C, and heating at 10 °C min⁻¹ under 1 SLM N₂. c.) DRIFTS recorded during exposure of bulk Ce_{0.7}Mn_{0.3}O_x to NH₃ at 150 °C in the 1800-800 cm⁻¹ region. The bands at 1159 cm⁻¹ and 1597 cm⁻¹ were attributed, in part, to NH₃ adsorbed at Lewis acid.³ The other labelled bands were attributed to NO_x species. The shoulder at 1101 cm⁻¹ suggests the presence of hyponitrite.¹ d.) DRIFTS recorded during exposure of bulk Ce_{0.7}Mn_{0.3}O_x to NH₃ at 150 °C in the 3730-2750 cm⁻¹ region. The bands spanning 3350-3250 cm⁻¹ are attributed to adsorbed NH₃.

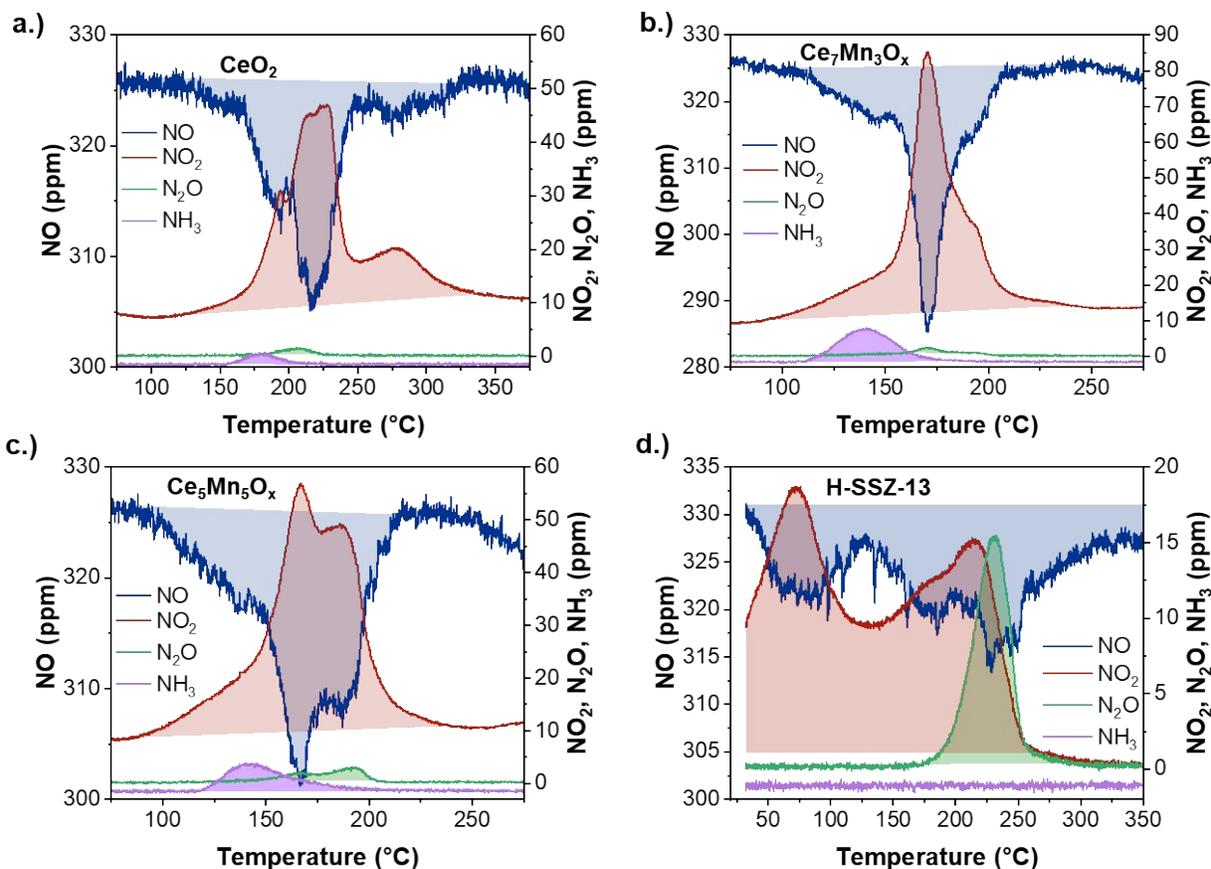


Figure S8. Temperature programmed surface reaction between NO and NH₄NO₃ over bulk oxide catalysts. The shaded areas represent the integrated areas used in Figure 3b. Conditions: [NH₄NO₃] = 15 wt. %; [NO] = 325 ppm; β = 10 °C min⁻¹; F = 1 SLM.

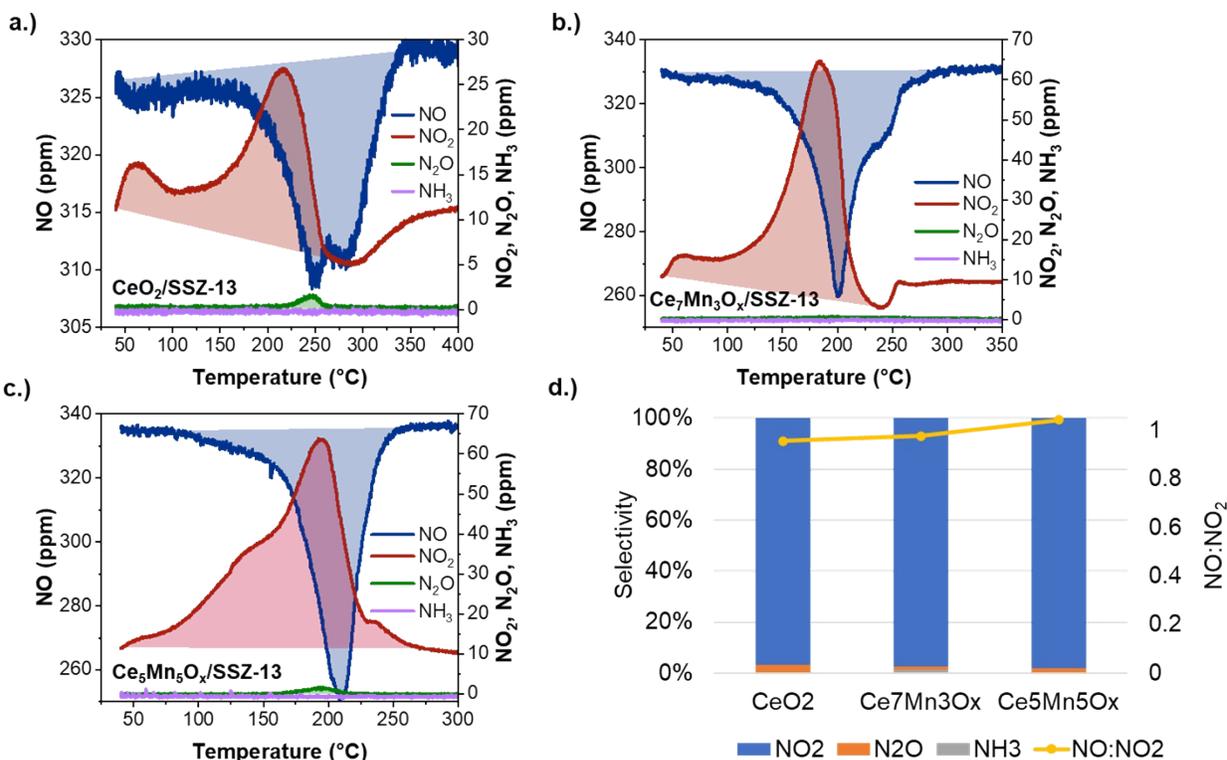


Figure S9. Temperature programmed surface reaction between NO and NH₄NO₃ over zeolite-supported mixed oxide catalysts. The shaded areas represent the integrated areas used in for the histogram in (d). Conditions: [NH₄NO₃] = 15 wt. %; [NO] = 325 ppm; β = 10 °C min⁻¹; F = 1 SLM.

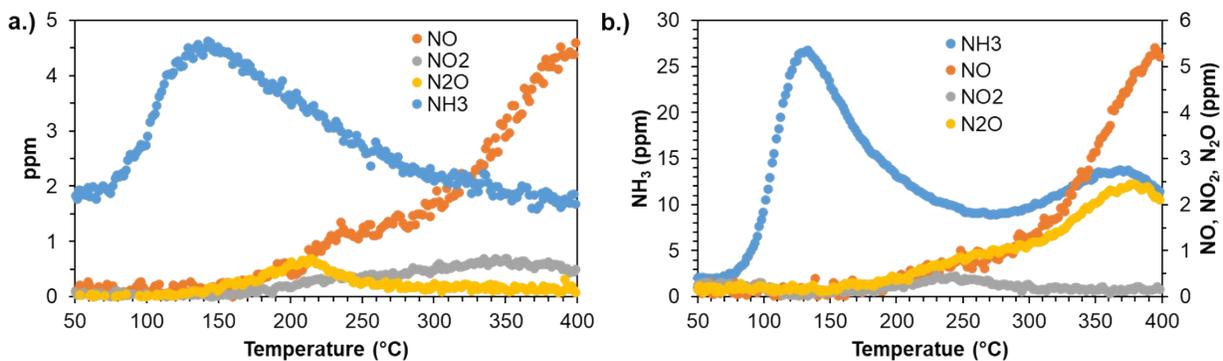


Figure S10. NH₃ temperature programmed desorption (TPD) over a.) bulk Ce_{0.7}Mn_{0.3}O_y and b.) Ce_{0.7}Mn_{0.3}O_y/SSZ-13. Both catalysts were heated to 500 °C in 15 % O₂ for 0.5 h, followed by cooling under He, admittance of 350 ppm NH₃ for 0.5 h at 50 °C, and heating at 10 °C min⁻¹ under 1 SLM N₂.

References:

1. Mihaylov, M. Y.; Ivanova, E. Z.; Vayssilov, G. N.; Hadjiivanov, K. I., Revisiting ceria-NO_x interaction: FTIR studies. *Catal. Today* **2020**, *357*, 613-620.
2. Kim, Y.; Hwang, S.; Lee, J.; Ryou, Y.; Lee, H.; Kim, C. H.; Kim, D. H., Comparison of NO_x Adsorption/Desorption Behaviors over Pd/CeO₂ and Pd/SSZ-13 as Passive NO_x Adsorbers for Cold Start Application. *Emission Contr. Sci. Technol.* **2019**, *5*, 172-182.
3. Zhang, L.; Pierce, J.; Leung, V. L.; Wang, D.; Epling, W. S., Characterization of Ceria's Interaction with NO_x and NH₃. *J. Phys. Chem. C* **2013**, *117*, 8282-8289.