

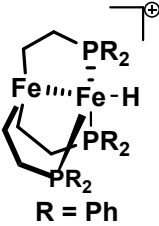
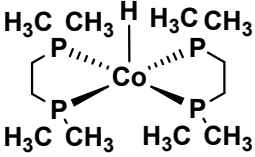
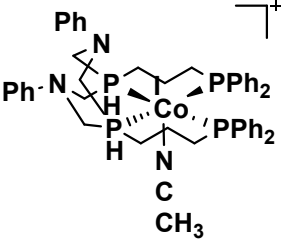
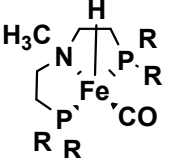
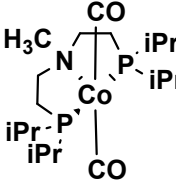
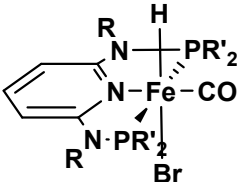
Supporting Information

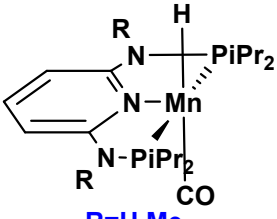
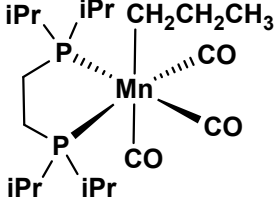
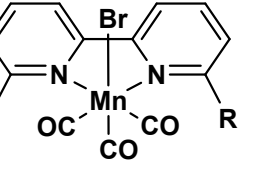
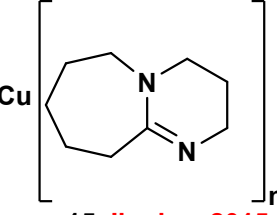
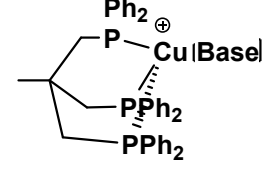
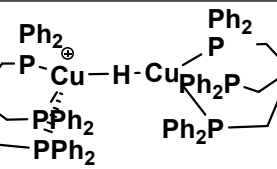
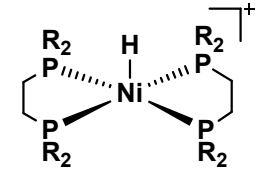
Recent developments in first-row transition metal complex-catalyzed CO₂ hydrogenation

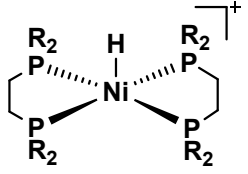
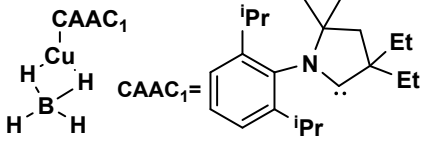
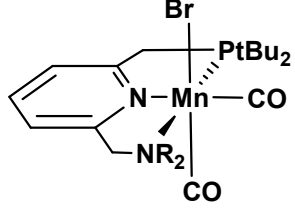
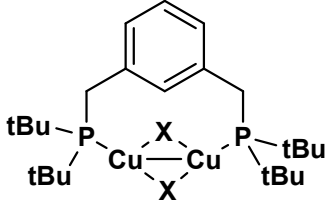
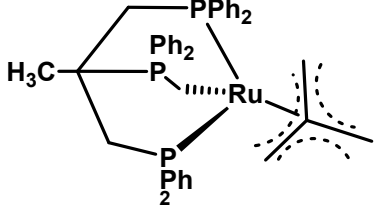
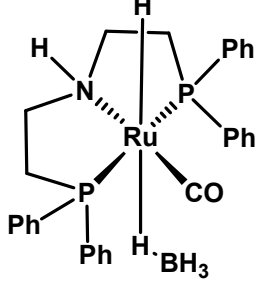
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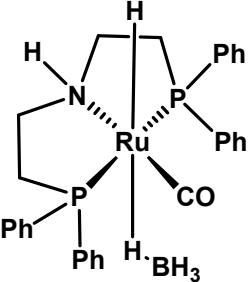
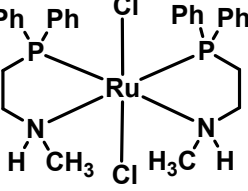
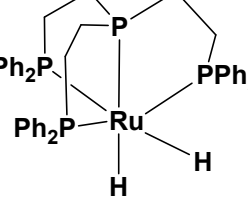
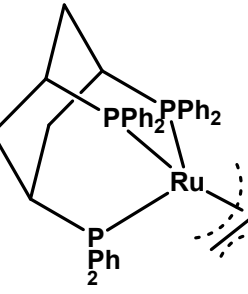
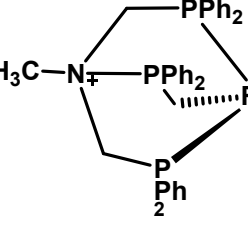
Table S1. The structure, reaction conditions, and catalytic performance of different CO₂ hydrogenation catalysts.

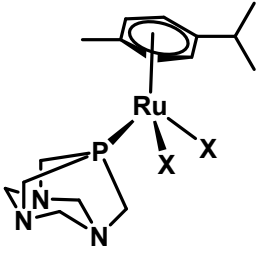
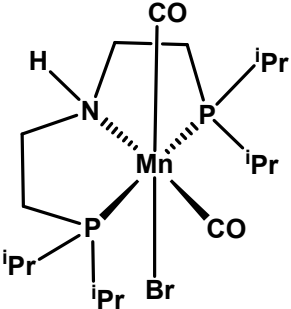
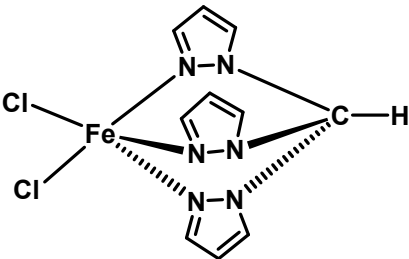
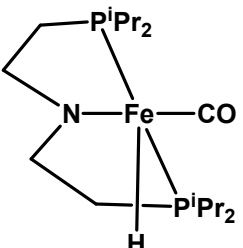
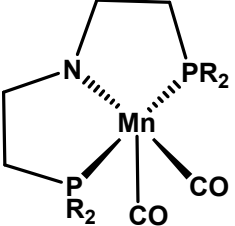
Catalyst (ref)	Pressure (CO ₂ :H ₂)	TON	TOF(h ⁻¹)	Solvent	Temperature	additives
<p>1. Reek, 2016</p>	50 bar (1:1)	685	-	DMSO	100°C	DBU
<p>2. Li, 2016</p>	5.0 MPa (1:1)	10,000	13,000	H ₂ O	40°C	-----
<p>3. Himeda, 2017</p>	0.1 MPa	14700	167	H ₂ O	25°C	-----
<p>4. Huang, 2018</p>	P _(CO₂) = 200 psi P _(H₂) = 400 psi	33000	13,000	THF/H ₂ O	110°C	-----
<p>5. Himeda, 2020</p>	0.1 MPa (1:1)	---	198	H ₂ O	25°C	-----

 <p>6. Beller 2012</p>	$P_{(H_2)} = 60 \text{ bar}$	>7500	750	Methanol	>100°C	NEt ₃
 <p>7. Linehan, 2013</p>	20 atm(1:1)	9400	74000	THF	21°C	Verkade's base
 <p>8. Linehan, 2017</p>	1.7 atm (1:1)	-	150(20)	acetonitrile	25°C	^t BuTMG
 <p>9. Hazari, Bernskoeter, 2015</p>	69 atm (1:1)	[tertiary amine = 60,000], [secondary amine = 9000]	-	THF	80°C	LiOTf, DBU
 <p>10. Bernskoeter, 2016</p>	1000 psi(1:1)	29000	5700	THF	45°C	LiOTf, DBU
 <p>11. Gonsalvi, 2016</p>	$P_{(H_2)} = 90 \text{ bar}$	1964 (for R=H), 1036 (for R=Me)	-	H ₂ O: THF (4:1)	80°C	NaOH, DBU

 <p>R=H, Me 12. Gonsalvi, 2017</p>	80 bar(1:1)	30,000	-	H ₂ O: THF	80°C	DBU, LiOTf
 <p>13. Gonsalvi, 2021</p>	75 bar (1:1)	~2000	-	THF	80°C	DBU, LiOTf
 <p>R=H, OH, OMe, NH₂ 14. Khusnutdinova, 2017</p>	60 bar(1:1)	>6000	-	acetonitrile	65°C	DBU
 <p>15. Ikariya, 2015</p>	20 (1:1)	167	-	1,4-dioxane	100°C	DBU
 <p>16. Appel, 2015</p>	40 (1:1)	500	25	acetonitrile	140°C	DBU
 <p>17. Appel, 2016</p>	40 atm (1:1)	-	7.5	CD ₃ CN	25°C	DBU
 <p>18. Appel, 2017</p>	34 atm(1:1)	-	4.0(5) × 10 ⁻¹	H ₂ O	80°C	NaHCO ₃

 <p>18. Appel, 2017</p>	$P_{(CO_2)} = 30 \text{ atm}$ $P_{(H_2)} = 30 \text{ atm}$	58	-	0.082 mole fraction of water in acetonitrile	22°C	[NEt ₄ HCO ₃]
 <p>19. Bertrand, 2018</p>	60 bar (1:3)	1881	-	THF	100°C	DBU, BCF
 <p>20. Milstein, 2019</p>	60 bar(1:1)	-	-	THF	110°C	KOH
 <p>X = Cl, Br, I, CN</p> <p>21. Rath, 2021</p>	1 atm (1:1)	-	10.65x10 ⁵	1,4-dioxane	80°C	DBU
 <p>22, Walter leitner, 2012</p>	10 bar/30ar	63	-	THF	140°C	EtOH
 <p>23, Sanford, 2015</p>	$P_{(H_2)} = 50 \text{ bar}$	550	-	THF	155°C	NHMe ₂ K ₃ PO ₄

 <p>24, Prakash, 2016 & 2020</p>	$P_{(H_2)} = 70 \text{ bar}$	520	-	biphasic 2-MTHF/water system	145°C	K_3PO_4
 <p>25, Wass, 2017</p>	$P_{(CO_2)} = 10 \text{ bar}$ $P_{(H_2)} = 30 \text{ bar}$	8900	4500	Toluene	100°C	NaOEt
 <p>26, Golderg, 2019</p>	In the first step $H_2 : CO_2 = 900 \text{ psi}$ And in the second step 1200 psi	430	-	1,4-dioxane/EtOH	120°C	$Sc(OTf)_3$
 <p>27, Klankarmayer, 2020</p>	$P_{(CO_2)} = 30 \text{ bar}$ $P_{(H_2)} = 90 \text{ bar}$	Upto 2100	-	EtOH	140°C	$Al(OTf)_3$
 <p>28, Wildner, 2020</p>	$P_{(CO_2)} = 15 \text{ bar}$ $P_{(H_2)} = 45 \text{ bar}$	240	23	EtOH	90°C	-

 <p>29. Rath, 2021</p>	$P_{(\text{CO}_2)} = 1 \text{ atm}$ $P_{(\text{H}_2)} = 3 \text{ atm}$	4752	-	THF	60°C	EtOH
<p>[Co(Triphos)(L)n]^{m+} Beller, 2017</p>	20 bar/70 bar	50	-	THF/EtOH	100°C	HNTf ₂
 <p>30. Prakash, 2017</p>	60 bar/60bar	36	-	THF	110°C	K ₂ CO ₃
 <p>31. Pombeiro, 2017</p>	75 atm (1:3)	2387	66	Solvent- or amine-free	80°C	K ₃ PO ₄
 <p>32. Bernskoeter, 2019</p>	100 psi/900 psi and 0/1150 psi from formamide	590	-	THF	100°C	DBU and LiOTf.
 <p>33. Leitner, 2021</p>	5 bar/160 bar	160	-	methanol and 1,4-dioxane	150°C	(Ti(O ⁱ Pr) ₄ and Sc(O ⁱ Pr) ₃)

