

## Electronic Supplementary Information

### Efficient and selective removal of $\text{Pb}^{2+}$ from aqueous solution by using a $\text{O}^-$ functionalized metal-organic framework

Wen Jiang,<sup>a,‡</sup> Cai-Xia Yu,<sup>a,‡,\*</sup> Ming-Xuan Yu,<sup>a</sup> Jing Ding,<sup>a</sup> Jian-Guo Song,<sup>a</sup> Xue-Qin Sun<sup>a</sup> and Lei-Lei Liu<sup>a,\*</sup>

<sup>a</sup> School of Environmental and Material Engineering, Yantai University, Yantai 264005, P. R. China

<sup>‡</sup> The first two authors contributed equally.

\* To whom correspondence should be addressed. E-mail addresses: liuleileimail@163.com (L.-L. Liu).

## Experimental Section

**General Procedure.** Ligand H<sub>2</sub>ADB was prepared according to the literature method.<sup>1</sup> All other chemicals and reagents were obtained from commercial sources and used as received. Powder X-ray diffraction (PXRD) was performed using a PANalytical X'Pert PRO MPD system (PW3040/60). Thermal analysis was performed with a Netzsch STA-449F3 thermogravimetric analyzer at a heating rate of 10 °C min<sup>-1</sup> and a flow rate of 20 cm<sup>3</sup> min<sup>-1</sup> (N<sub>2</sub>). Fourier transform infrared (FT-IR) spectra were recorded on an IR Prestige-21. The FT-IR samples were prepared by blending compound with KBr and compressing the mixture to obtain transparent sheets. X-ray photoelectron spectroscopy (XPS) was performed on a Thermo Escalab 250 spectrometer with monochromated Al<sub>Kα</sub> excitation. The zeta potential was determined using dynamic light scattering (DLS) on Malvern Instruments Nanosizer-ZS90.

**X-ray crystal structure determination.** Single X-ray diffraction intensities of crystal were collected on a CCD diffractometer at 296 K. All diffractometers were equipped with a graphite monochromated Mo-Kα radiation ( $\lambda = 0.71073$ ). The structure was solved by direct method and expanded with Fourier technique. All calculations were performed with SHELXL-97 package. All H atoms in **Pr-MOF** were placed in geometrically idealized positions and constrained to ride on their parent atoms. The crystal data for **Pr-MOF** was summarized as follows: C<sub>25</sub>H<sub>21</sub>N<sub>4</sub>O<sub>8.5</sub>Pr, Mr = 654.36, monoclinic, space group *P2<sub>1</sub>/n*, *a* = 16.455(3) Å, *b* = 8.7878(18) Å, *c* = 20.761(4) Å,  $\alpha = 90^\circ$ ,  $\beta = 93.15(3)^\circ$ ,  $\gamma = 90^\circ$ , *V* = 2997.6(10) Å<sup>3</sup>, *Z* = 4, *D<sub>c</sub>* = 1.468 g cm<sup>-3</sup>, *F*(000) = 1320.0 and  $\mu = 1.678$  mm<sup>-1</sup>, 29334 reflections collected, 5276 unique (*R*<sub>int</sub> = 0.0532). *R*<sub>1</sub> = 0.0358, *wR*<sub>2</sub> = 0.0887 and *S* = 1.064.

**Adsorption experiments.** The adsorption kinetics data were fitted with different kinetic models, pseudo first-order model, pseudo-second-order, expressed as follows:

$$\ln(q_e - q_t) = \ln q_e - k_1 t \quad (1)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (2)$$

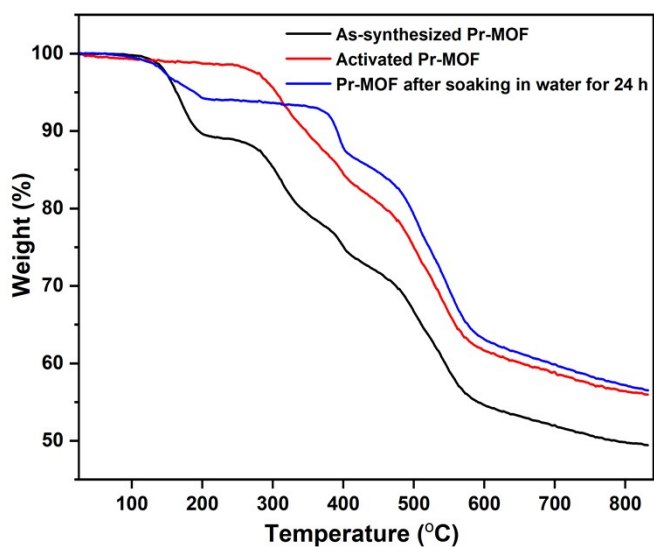
where *q<sub>t</sub>* (mg g<sup>-1</sup>) and *q<sub>e</sub>* (mg g<sup>-1</sup>) are the adsorption capacity at any time *t* (min) and at equilibrium; *k<sub>1</sub>* (min<sup>-1</sup>) and *k<sub>2</sub>* (g mg<sup>-1</sup> min<sup>-1</sup>) are kinetic rate constants for the pseudo-first-order and pseudo-second-order models, respectively.

The Langmuir and Freundlich isotherm model were employed to simulate the adsorption isotherm data and can be described as:

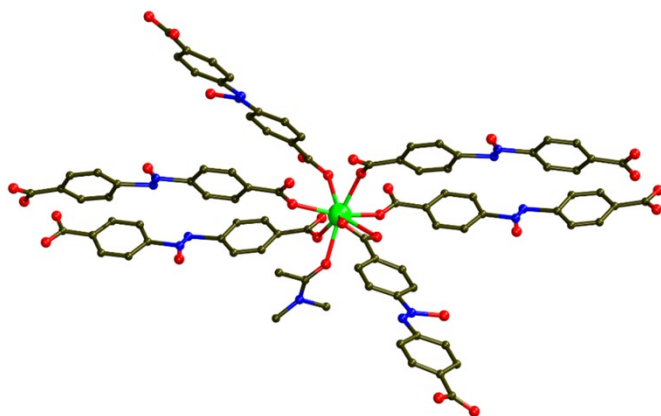
$$\frac{C_e}{q_e} = \frac{C_e}{q_m} + \frac{1}{q_m K_L} \quad (3)$$

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e \quad (4)$$

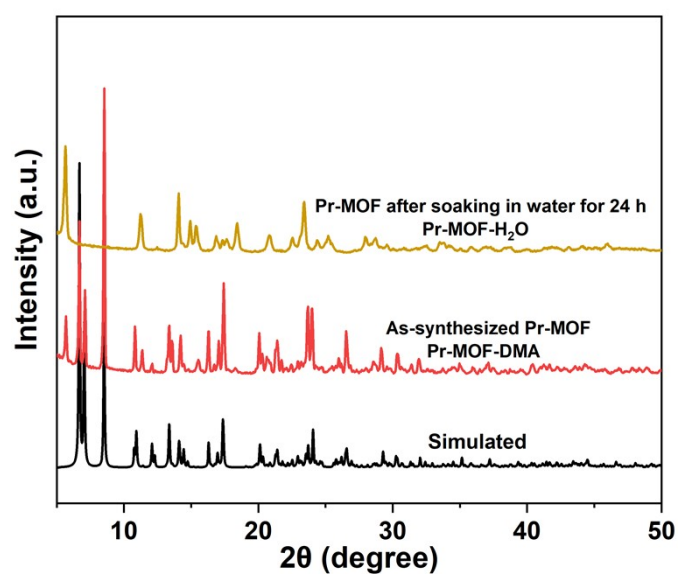
where  $q_e$  (mg g<sup>-1</sup>) is the adsorption amounts at equilibrium and  $C_e$  (mg L<sup>-1</sup>) is the equilibrium concentration of Pb(II).  $q_m$  (mg g<sup>-1</sup>) is the maximum amount or the saturated adsorption amount.  $K_L$  (L mg<sup>-1</sup>) is the Langmuir constant, quantitatively reflecting the affinity of binding sites to energy of adsorption.  $K_F$  ((mg g<sup>-1</sup>)/(L mg<sup>-1</sup>)<sup>1/n</sup>) is the Freundlich constant which indicates the adsorption capacity and  $n$  is an empirical parameter related to the intensity of adsorption. The Langmuir model assumes that the solid surface active sites can be occupied only by one layer of adsorbates and there is no interaction between the adsorbate molecules. On the contrary, the Freundlich model is based on a heterogeneous adsorption.



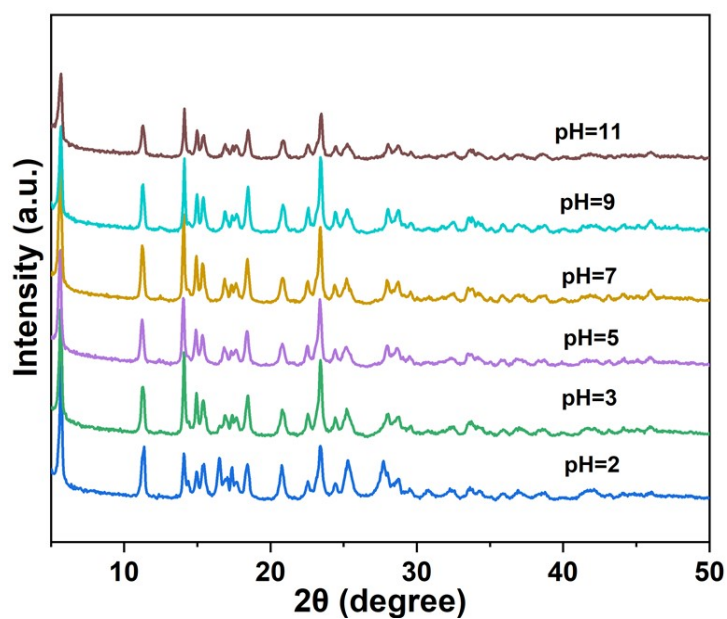
**Figure S1.** TGA curves of the as-synthesized **Pr-MOF**, activated **Pr-MOF** and **Pr-MOF** after soaking in water for 24 h.



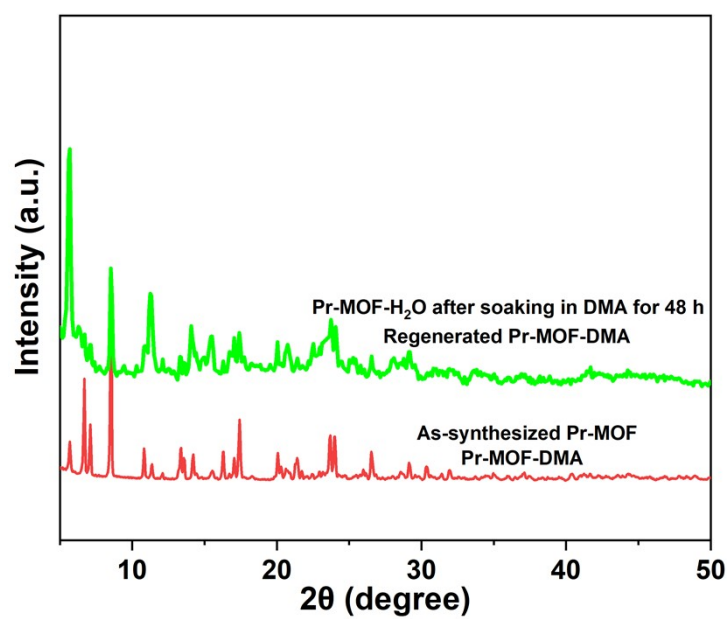
**Figure S2.** Coordination environment of Pr(III) atom in **Pr-MOF**.



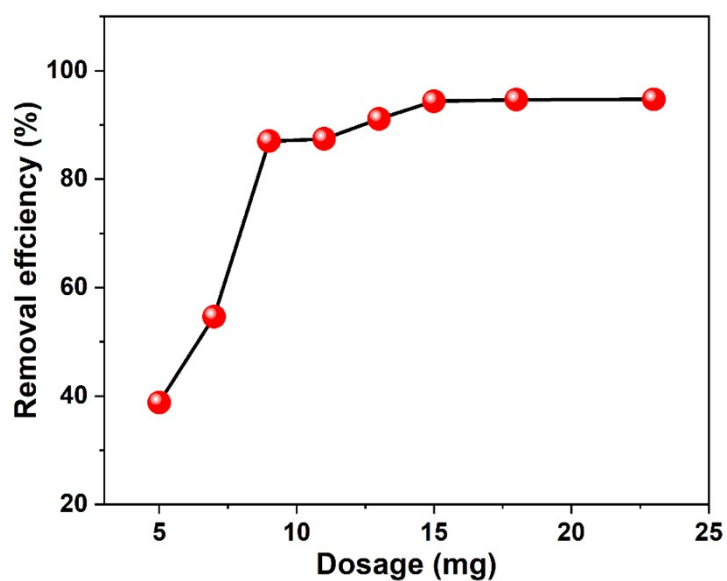
**Figure S3.** PXRD patterns of the simulated, as-synthesized **Pr-MOF** and **Pr-MOF** after soaking in water for 24 h.



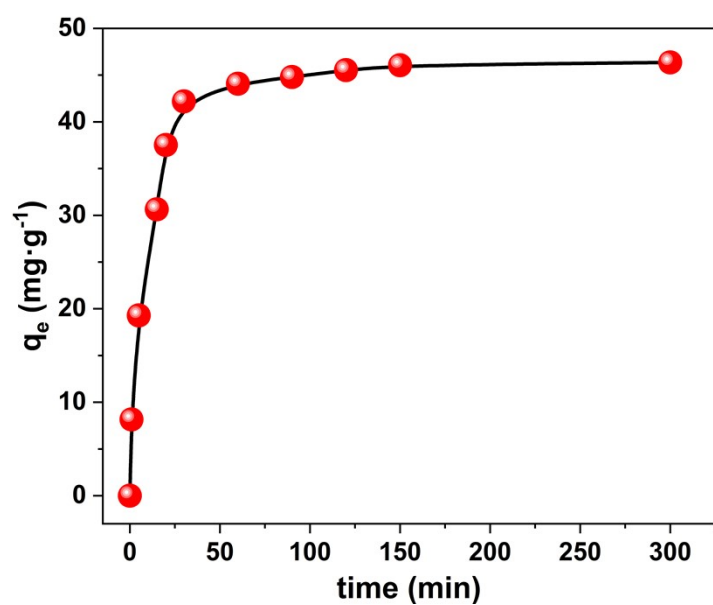
**Figure S4.** PXRD patterns of **Pr-MOF** after soaking in water (24 h) for different pH values.



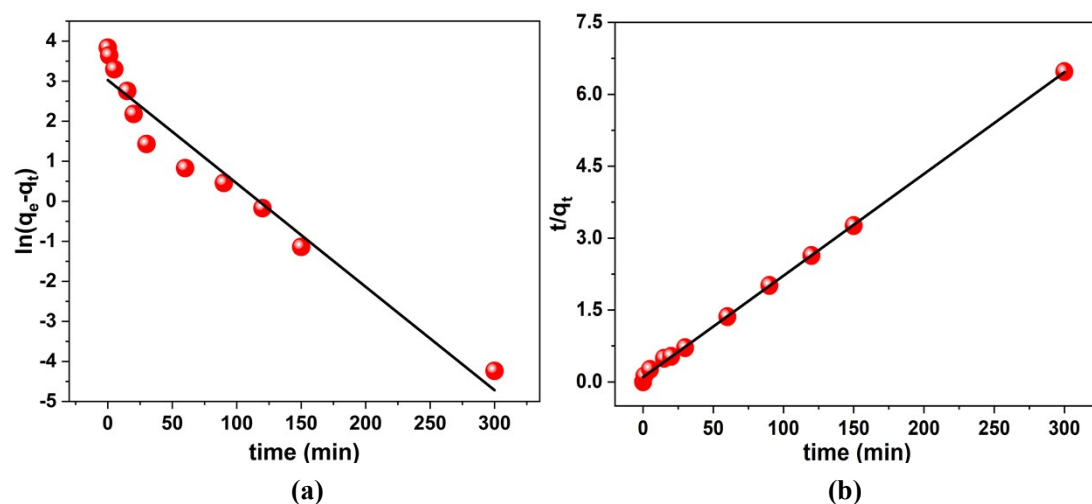
**Figure S5.** PXRD patterns of as-synthesized **Pr-MOF** and **Pr-MOF-H<sub>2</sub>O** after soaking in DMA for 48 h.



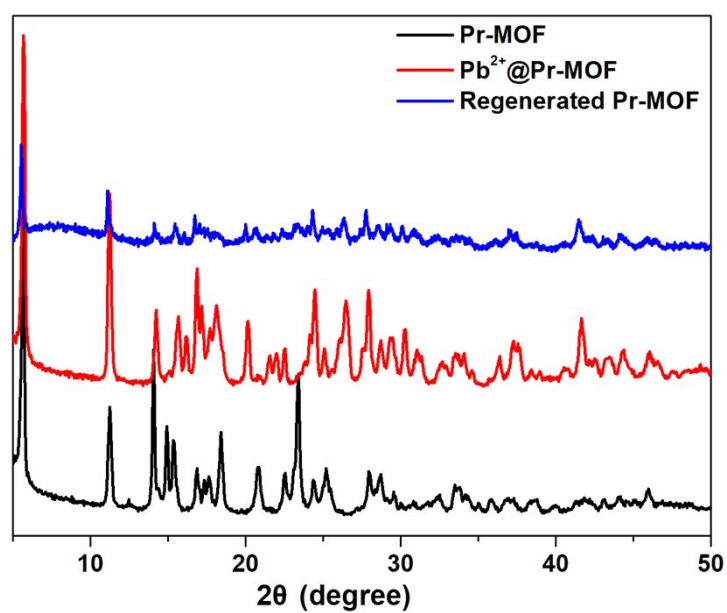
**Figure S6.** Effect of Pr-MOF dosage on the removal of  $\text{Pb}^{2+}$ .  $C_0 = 60$  ppm,  $V = 50$  mL,  $\text{pH} = 6$  and  $T = 298$  K.



**Figure S7.** Influences of adsorption time on adsorption.  $C_0 = 10$  ppm,  $m_{\text{adsorbent}} = 9$  mg,  $V = 50$  mL,  $\text{pH} = 6.0$ , and  $T = 298$  K.



**Figure S8.** (a) Pseudo-first-order kinetic model and (b) Pseudo-second-order kinetic model.



**Figure S9.** The PXRD patterns of Pr-MOF,  $Pb^{2+}@Pr-MOF$  and the recovered samples after four cycles of adsorption-desorption experiments.

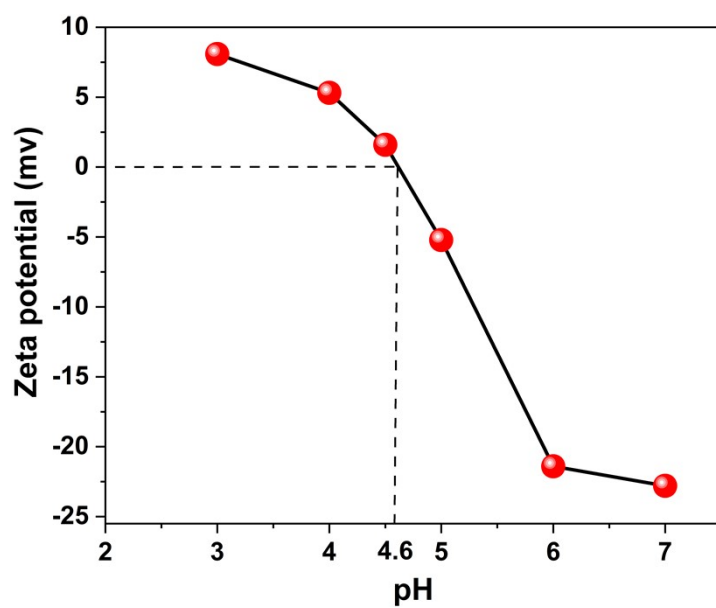


Figure S10. The effect of pH on zeta potentials of **Pr-MOF**.

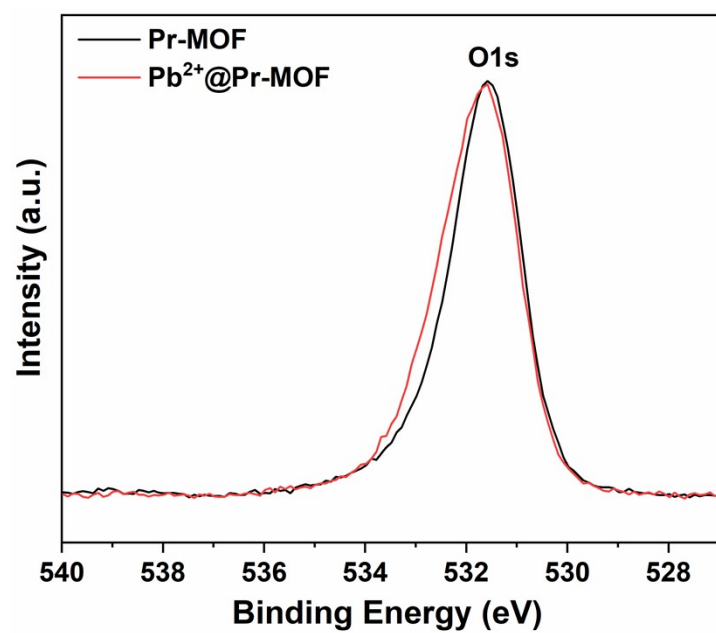
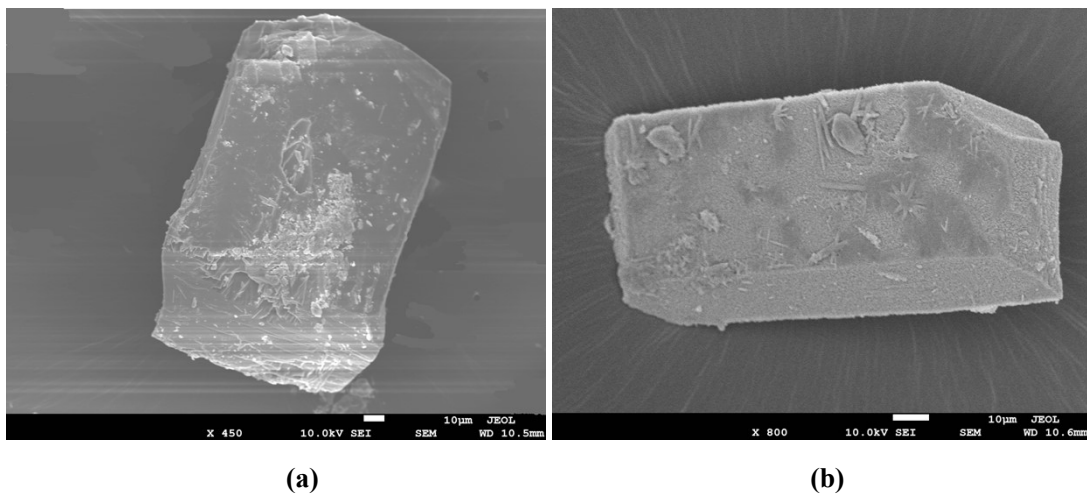
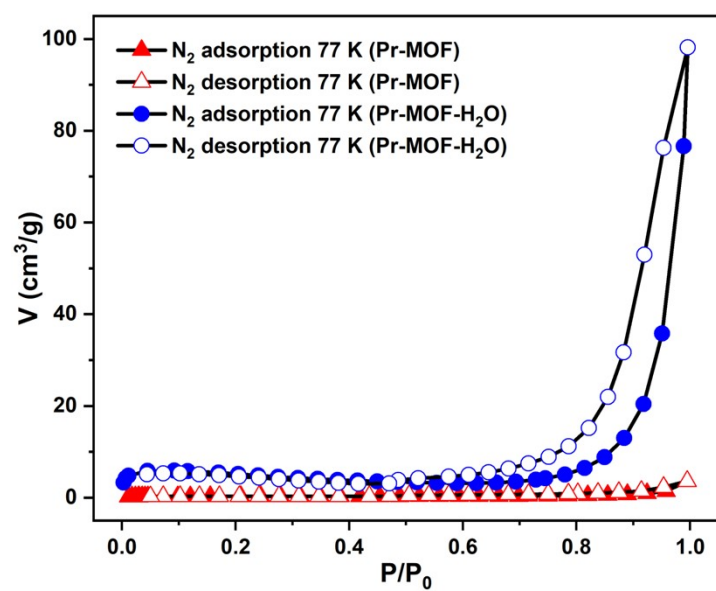


Figure S11. O 1s spectra before and after Pb<sup>2+</sup> adsorption.

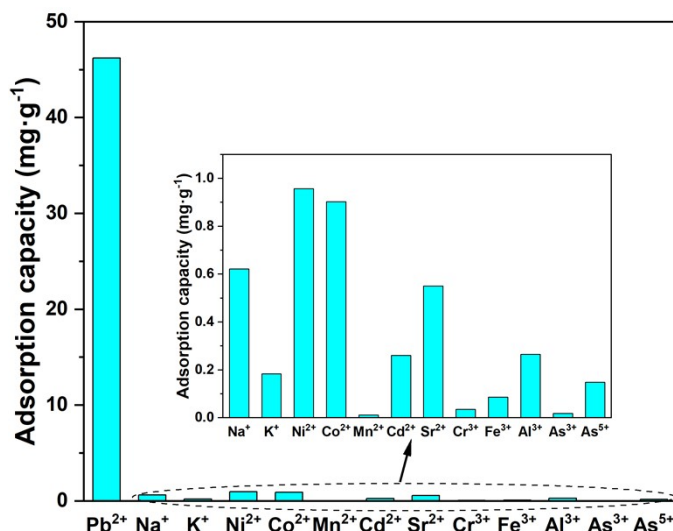




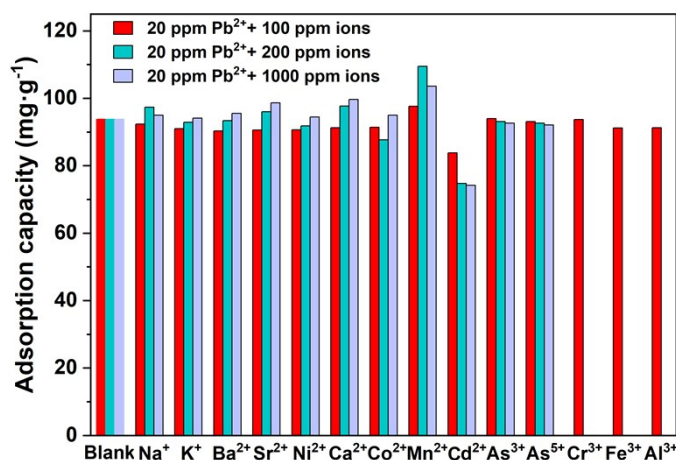
**Figure S12.** The SEM images of (a) **Pr-MOF** and (b) **Pr-MOF** after soaking in  $\text{H}_2\text{O}$  for 24 h.



**Figure S13.** Gas adsorption isotherms of as-synthesized **Pr-MOF** and **Pr-MOF** after soaking in water for 24 h.



**Figure S14.** Selective adsorption of **Pr-MOF** for different metal ions.  $T = 298\text{ K}$ ,  $C_0 = 10\text{ ppm}$ ,  $\text{pH} = 6$ ,  $m_{\text{adsorbent}} = 9\text{ mg}$  and  $V = 50\text{ mL}$ . Based on the  $K_{\text{sp}}$  values of  $[\text{Al}(\text{OH})_3]$  ( $1.3 \times 10^{-33}$ ),  $[\text{Cr}(\text{OH})_3]$  ( $6.3 \times 10^{-31}$ ) and  $[\text{Fe}(\text{OH})_3]$  ( $4.0 \times 10^{-38}$ ), the metal ions of  $\text{Al}^{3+}$ ,  $\text{Cr}^{3+}$  and  $\text{Fe}^{3+}$  are easily subject to precipitation at the tested  $\text{pH}$  of 6.0, and the residual concentration of these metal ions were calculated to be  $3.51 \times 10^{-5}\text{ ppm}$  for  $\text{Al}^{3+}$ ,  $3.28 \times 10^{-2}\text{ ppm}$  for  $\text{Cr}^{3+}$  and  $2.23 \times 10^{-9}\text{ ppm}$  for  $\text{Fe}^{3+}$ , respectively. Thus, the selective measurements for  $\text{Al}^{3+}$ ,  $\text{Cr}^{3+}$  and  $\text{Fe}^{3+}$  were tested in a single system, with a solution  $\text{pH}$  of 4.0 for  $\text{Al}^{3+}$ , 5.0 for  $\text{Cr}^{3+}$  and 2.0 for  $\text{Fe}^{3+}$ , to guarantee concentration of these metal ions in solution is 10 ppm.



**Figure S15.** The effects of competing ions on  $\text{Pb}^{2+}$  removal by **Pr-MOF**. The anti-interference experiment was performed at  $\text{pH}$  of 6.0 to evaluate the effect of the presence of the interference ions on  $\text{Pb}^{2+}$  adsorption. For the metal ions of  $\text{Al}^{3+}$ ,  $\text{Cr}^{3+}$  and  $\text{Fe}^{3+}$ , they are easily subject to precipitation at the tested  $\text{pH}$  of 6.0. Based on the  $K_{\text{sp}}$  value for each ion ( $K_{\text{sp}}[\text{Al}(\text{OH})_3] = 1.3 \times 10^{-33}$ ,  $K_{\text{sp}}[\text{Cr}(\text{OH})_3] = 6.3 \times 10^{-31}$  and  $K_{\text{sp}}[\text{Fe}(\text{OH})_3] = 4.0 \times 10^{-38}$ ), the residual concentrations of  $\text{Al}^{3+}$ ,  $\text{Cr}^{3+}$  and  $\text{Fe}^{3+}$  at  $\text{pH}$  6.0 were calculated to be  $3.51 \times 10^{-5}\text{ ppm}$ ,  $3.28 \times 10^{-2}\text{ ppm}$  and  $2.23 \times 10^{-9}\text{ ppm}$ , respectively. Thus, the anti-interference experiment for these metal ions was investigated at  $\text{pH}$  6.0, with a concentration of  $3.51 \times 10^{-5}\text{ ppm}$  for  $\text{Al}^{3+}$ ,  $3.28 \times 10^{-2}\text{ ppm}$  for  $\text{Cr}^{3+}$  and  $2.23 \times 10^{-9}\text{ ppm}$  for  $\text{Fe}^{3+}$ . As shown in Fig. S15, negligible effect was posed on  $\text{Pb}^{2+}$  adsorption by  $\text{Al}^{3+}$ ,  $\text{Cr}^{3+}$  and  $\text{Fe}^{3+}$ .

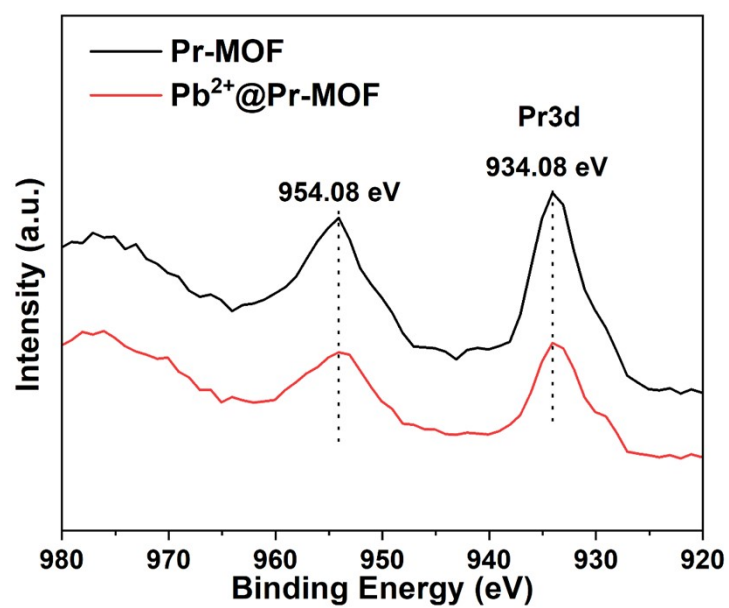


Figure S16. Pr 3d XPS spectrum of Pr-MOF and Pb<sup>2+</sup>@Pr-MOF.

**Table S1.** Adsorption constants for Langmuir and Freundlich isotherm models.

Langmuir			Freundlich		
$q_{\max}$	$K_L$	$R^2$	$K_F$	$n$	$R^2$
584.79	0.0848	0.999	74.652	0.403	0.825

**Table S2.** Comparison of  $Pb^{2+}$  maximum uptake capacity for **Pr-MOF** with other adsorbents.

Adsorbents	Maximum uptake capacity ( $mg\ g^{-1}$ )	References
Cu-BTC-Th	732.86	2
Fe doped HKUST-1	565	3
<b>Pr-MOF</b>	<b>560.26</b>	<b>this work</b>
Tb-MOF	547	4
Zn-MOF	463.52	5
Co-Al-LDH@Fe <sub>2</sub> O <sub>3</sub> /DPCNF	426.76	6
AMCA-MIL-53(Al)	390	7
Cu-BTC	333	8
Zn-BTC	312	8
Fe <sub>3</sub> O <sub>4</sub> /MIL-96(Al)	301.5	9
Fe <sub>3</sub> O <sub>4</sub> @ZIF-8	276.06	10
MIL-101(Fe)/GO	128.6	11
DUT-67	98.5	12
CMP-3a	93.2	13
Cd-MOF	60.857	14

**Table S3.** Kinetic parameters for adsorption of  $\text{Pb}^{2+}$ .

T/K	Pseudo-first-order model				Pseudo-second-order model		
	$q_{e,\text{exp}}$	$k_1$	$q_{e,\text{cal}}$	$R^2$	$k_2$	$q_{e,\text{cal}}$	$R^2$
298	46.356	0.0258	20.655	0.951	0.0046	47.148	0.999

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