

1 Supplement to: Development of Volatility Distributions of Biomass Burning Organic
2 Emissions
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8 Data underlying all figures in manuscript and supplement can be freely access at : doi:10.5061/dryad.jsxksn0ct

9 **Section S1: Comparison of aerosol mass in particle phase from partitioned TD/GC/MS and artifact**
10 **corrected filter measurements**

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12 To ensure consistency in our measurement approaches, we compare organic aerosol in the particle phase
13 as measured by collection on quartz filters against organic aerosol observed in TD/GC/MS filter-in-tube
14 chromatograms, after accounting for partitioning.

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16 Combustion emissions were sampled onto bare quartz (BQ) filters and analyzed using thermo-optical
17 methods to quantify organic carbon content. Primary organic carbon (OC) was estimated for positive
18 artifact due to vapor absorption using a quartz-behind teflon (QBT) filter method.¹ The artifact-corrected
19 OC is calculated as the difference between the OC concentration on a front quartz filter and the OC
20 concentration on a parallel quartz filter positioned behind a teflon filter. Note that the QBT filters were
21 not collected for field samples and so estimates from BQ filters were used directly. The artifact
22 percentage (QBT/BQ × 100) is less than 1% for burnhut, 17% for RWC-Startup and 14% for RWC-high
23 fire. The OC concentrations were also background corrected using measurements taken from background
24 filter samples collected at the test sites. To estimate primary organic aerosol concentrations (POA) we
25 applied a campaign average estimate of the OM/OC ratio of 1.53 to the calculated OC mass
26 concentrations. In the second method, we use the volatility distributions derived from TD/GC/MS
27 chromatograms from filter-in-tube sorbent samples (described in section 2.3) to estimate POA in the
28 particle phase. For each experiment, we use the partitioning equation (equation 1 in manuscript) at the

29 POA concentration measured by the quartz filter, to calculate the particle fraction (X_p) in each volatility
30 bin for the basis set of saturation concentration: [$10^{-2}, 10^{-1}, 10^0, 10^1, 10^2, 10^3, 10^4, 10^5, 10^6$] $\mu\text{g m}^{-3}$. We then
31 calculate the mass in the particle phase in each bin by using the total organic mass (particle + gas) in a

32 volatility bin as measured by the filter-in-tube chromatograms and the particle fraction, X_p . Figure S9
33 shows the particle phase masses summed up and presented as an emission factor.

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35 Comparing these two methods showed that EFs derived using the filter-in-sorbent tube method were
36 biased low relative to filter-derived derived POA EFs. The divergence was largest for open field burns
37 (burn-average correction factor of 10.36 – reflecting an order of magnitude divergence) and smallest for
38 residential woodstove emissions (test average correction factor of 2.82). Several issues may contribute to
39 the under-estimation of the TD/GC/MS mass. For example, it is possible that some organic material does
40 not elute from the chromatogram but is measured on filter samples or perhaps the difference in mass is
41 due to the uncertainty in response in the TIC analyzed using the *n*-alkane based calibration resulting in the
42 observed disparity. To reconcile this difference, an averaged correction factor was calculated using the
43 ratios of POA EFs from the two methods across the replicate samples of each combustion source. The bin
44 masses estimated from the TD/GC/MS method are then corrected using these factors. To make this
45 correction we assume that the impact of the divergence between the two methods is evenly distributed
46 across the volatility bins. This assumption cannot be directly tested and is thus a source of uncertainty.

47 The averaged correction factors applied for each combustion source type are shown in Figure S9.

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51 **Table S1:** Operating parameters of the TD/GC/MS system – Gerstel and Cooled Injection System inlet
52 conditions, GC oven conditions and MS conditions.

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Gerstel and CIS inlet conditions	
Gerstel Temperature (°C) ramp	25°C ramped to 300° at 60°C/sec hold 7 min
Inlet type	PTV
CIS cold trapping temperature	-100°C
Mode	Solvent Vent
Carrier gas	He
Purge flow to split vent (mL/min)	50
Column	30 m * .25 mm id HP 5 MS UI
Column flow rate (ml/min)	1
GC oven conditions	
Initial oven temperature (°C)	65
Initial oven hold time (min)	10
Oven temperature ramp rate (°C/min)	10
Final oven temperature (°C)	300
Final oven hold time (min)	26.5
Maximum column temperature (°C)	325
MS conditions	
solvent delay time (min)	5.5
GC/MS interface temperature (°C)	300
data collection mode	Scan
scan range (amu)	50-500
MS source temperature (°C)	
MS quad temperature (°C)	230
	150

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57 **Table S2:** Components of calibration compounds spiked on Carbotrap C/ Carbotrap F adsorbent tubes
 58 along with solvent (HIB solution) and internal standard. Spikes were prepared of 10 ng of each
 59 component for the sets of standard mixture.

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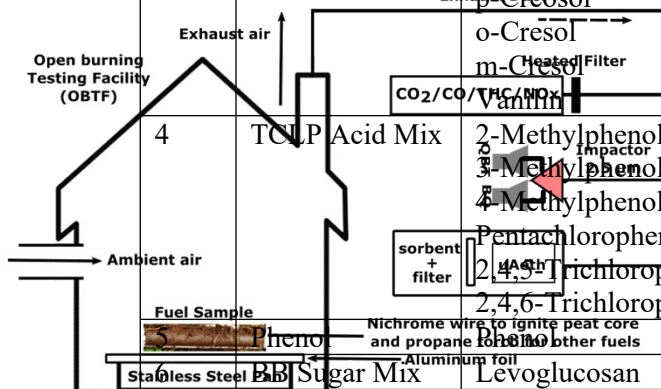
S.No.	Type of Standard	Components	Molecular Weight (g/mol)
1	Alkane Standard	C10 – C38 (all even)	142.3 – 535.0
2	PAH Standard	Acenaphthylene Anthracene Benz[a]anthracene Benzo[b]fluoranthene Benzo[k]fluoranthene Benzo[a]perylene Benzo[a]pyrene Chrysene Dibenz[a,h]anthracene Fluorene Indeno[1,2,3-cd]pyrene Phenanthrene Pyrene	152.2 178.2 228.3 252.3 252.3 276.3 252.3 228.3 278.4 166.2 276.3 178.2 202.3
3	Methoxy Phenol Mix	Syringol Guaiacol o-Cresol m-Cresol p-Cresol Vanillin	154.2 124.1 108.1 108.1 108.1 152.1
4	TCLP Acid Mix	2-Methylphenol (o-cresol) 3-Methylphenol (m-cresol) 4-Methylphenol (p-cresol) Pentachlorophenol 2,4,5-Trichlorophenol 2,4,6-Trichlorophenol Phenol	108.1 108.1 108.1 266.3 197.4 197.4 94.1
	Sugar Mix	Levoglucosan	162.4

A) Open Field Burns

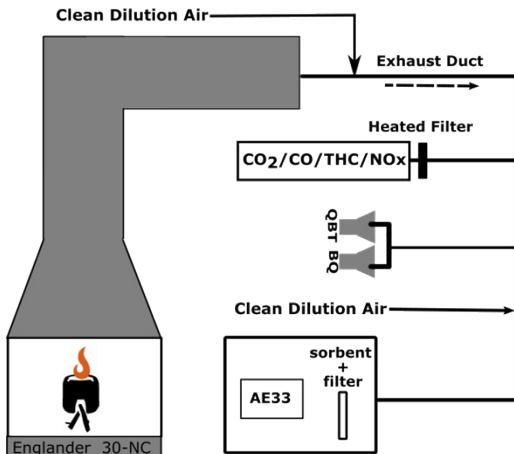


Measurement Package placed downwind burning field

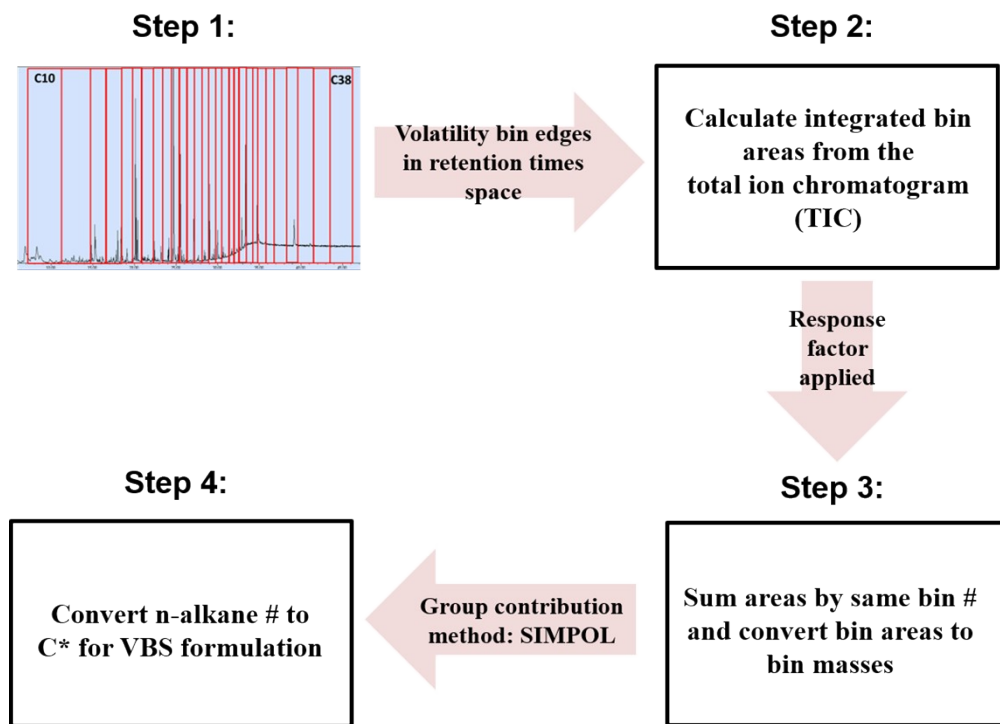
B) Laboratory Open Burn



C) Laboratory Woodstove Testing

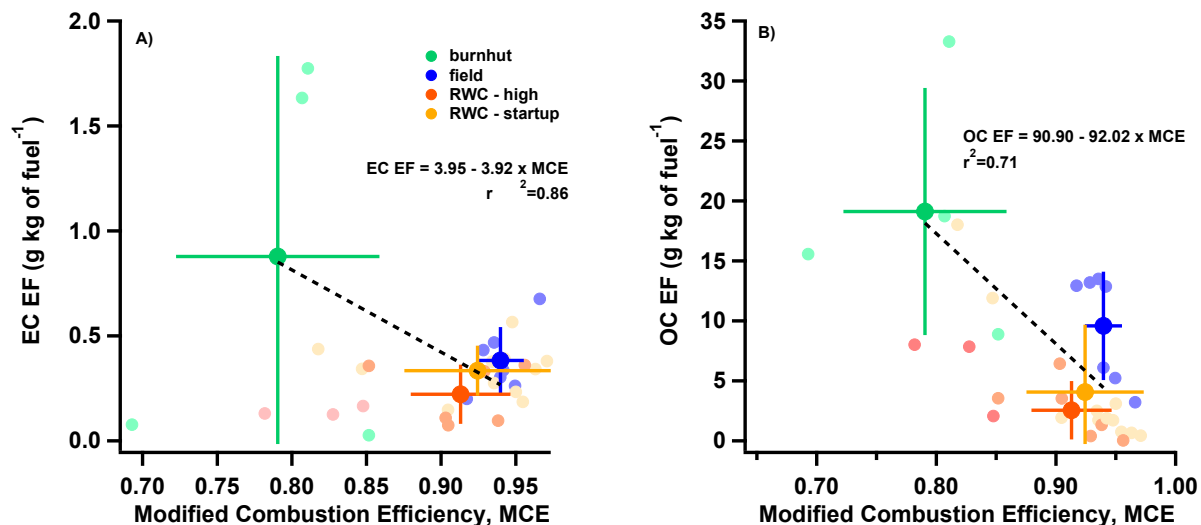


65 **Figure S1: A) Experimental schematic for collection of emissions from open field burning. The**
 66 **measurement package was placed downstream of the burning field and included gas and particle**
 67 **phase measurements. B) Experimental schematic for collection of emissions from laboratory**
 68 **simulated open burning. Testing was carried out in the open burning testing facility (OBTF)¹ C)**
 69 **Experimental schematic for collection of emissions from laboratory woodstove testing.**
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 72 **Figure S2: Flow chart depicting the various steps involved in the transformation of the raw total**
 73 **ion chromatogram (TIC) to depictions of volatility distribution using the volatility basis set (VBS)**
 74 **framework.**

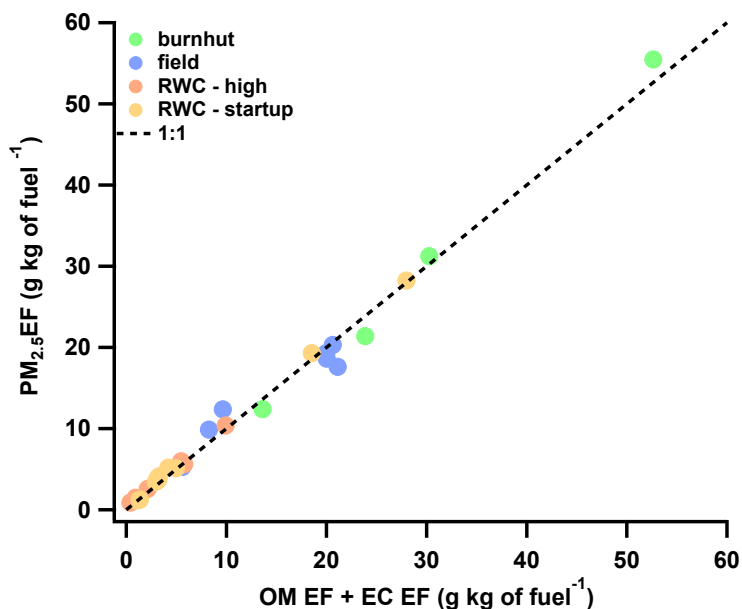
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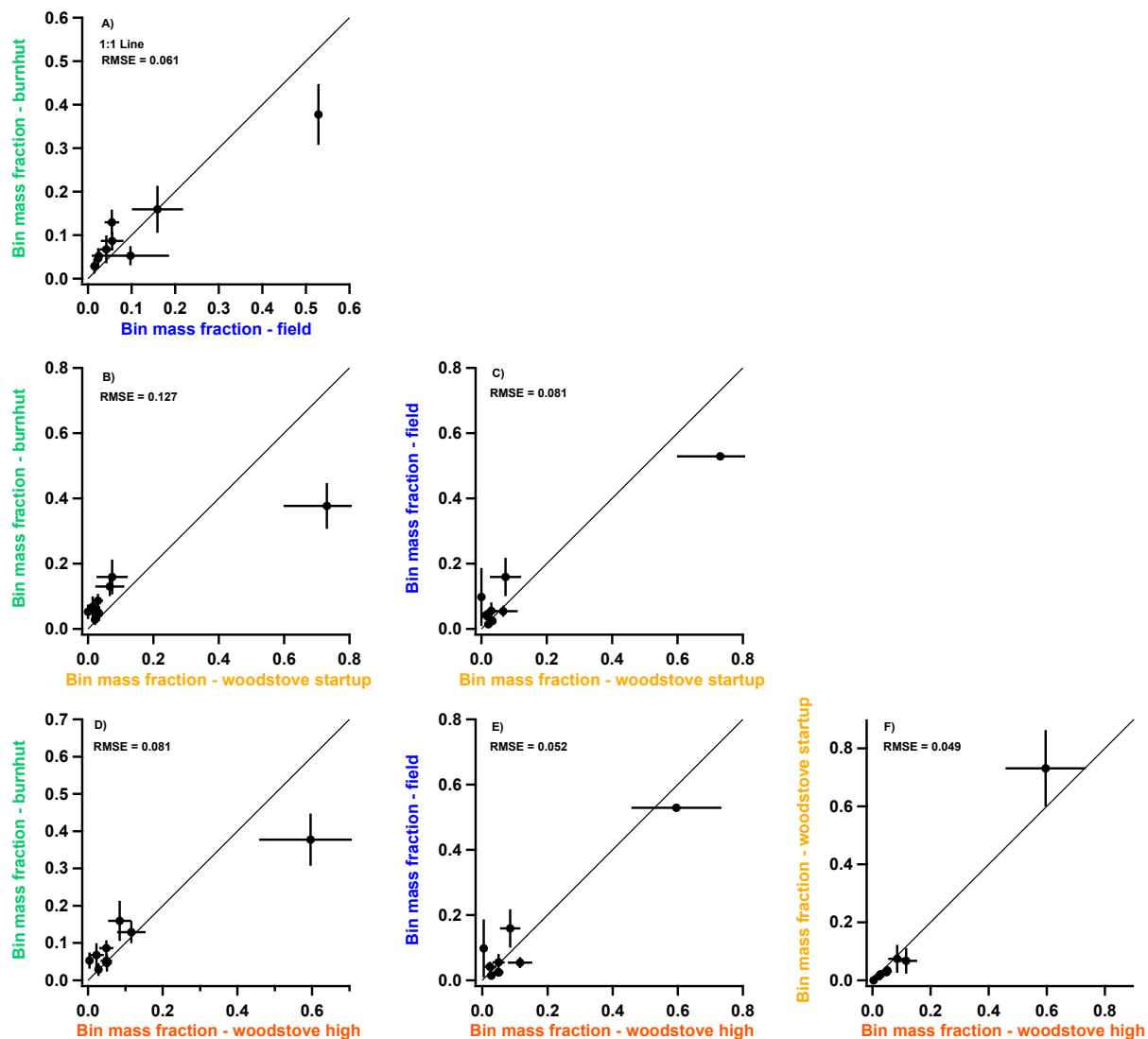
77 **Figure S3: A) Elemental carbon emission factors (EC EFs) and B) Organic carbon emission factors**
 78 **(OC EF) as function of modified combustion efficiency (MCE) for different source emissions –**
 79 **burnhut, field, RWC phases (delineated by color). Faded markers represent test-averaged**
 80 **observations from integrated filter measurements while darker markers show the average PM_{2.5} EF**
 81 **and MCE from a source emissions type with the error bars denoting the standard deviation across**
 82 **individual tests.**

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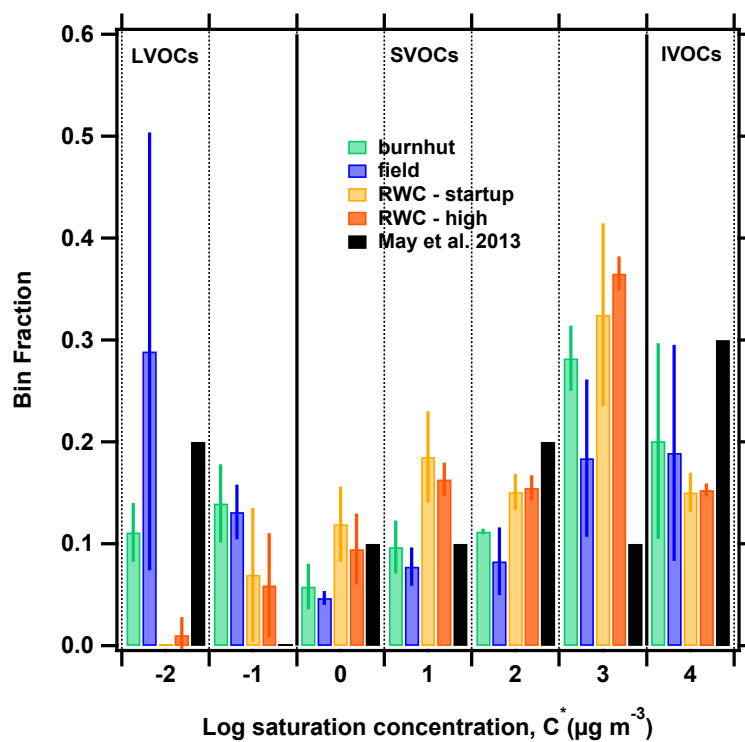
85 **Figure S4: PM_{2.5} emission factors, PM_{2.5} EF (from gravimetric filter measurements) plotted against**
 86 **OM EF + EC EF (thermo-optical filter measurements). OC EFs are converted to OM EFs using an**
 87 **OM/OC ratio of 1.53, the average for all samples calculated assuming OM + EC = PM_{2.5} in all cases**
 88 **(a simplification). Combustion sources are delineated by color. The dashed black line shows the 1:1**
 89 **line**



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91 **Figure S5: Scatter plots of the bin mass fraction contributions from volatility distributions in the**
 92 **range $-2 \leq \log C^* \leq 6$ derived from TD/GC/MS chromatograms. The plots presented here include**
 93 **all combinations of comparisons between burnhut, field, RWC – high and RWC – startup**
 94 **distributions (delineated by label colors). The markers represent the average bin mass fraction**
 95 **from replicate (N=3) filter-in-tube samples while the error bars show the standard deviations in the**
 96 **replicates. The solid black line shows the 1:1 line in each plot with the root mean square error**
 97 **(RMSE) to the 1:1 line printed in each plot.**

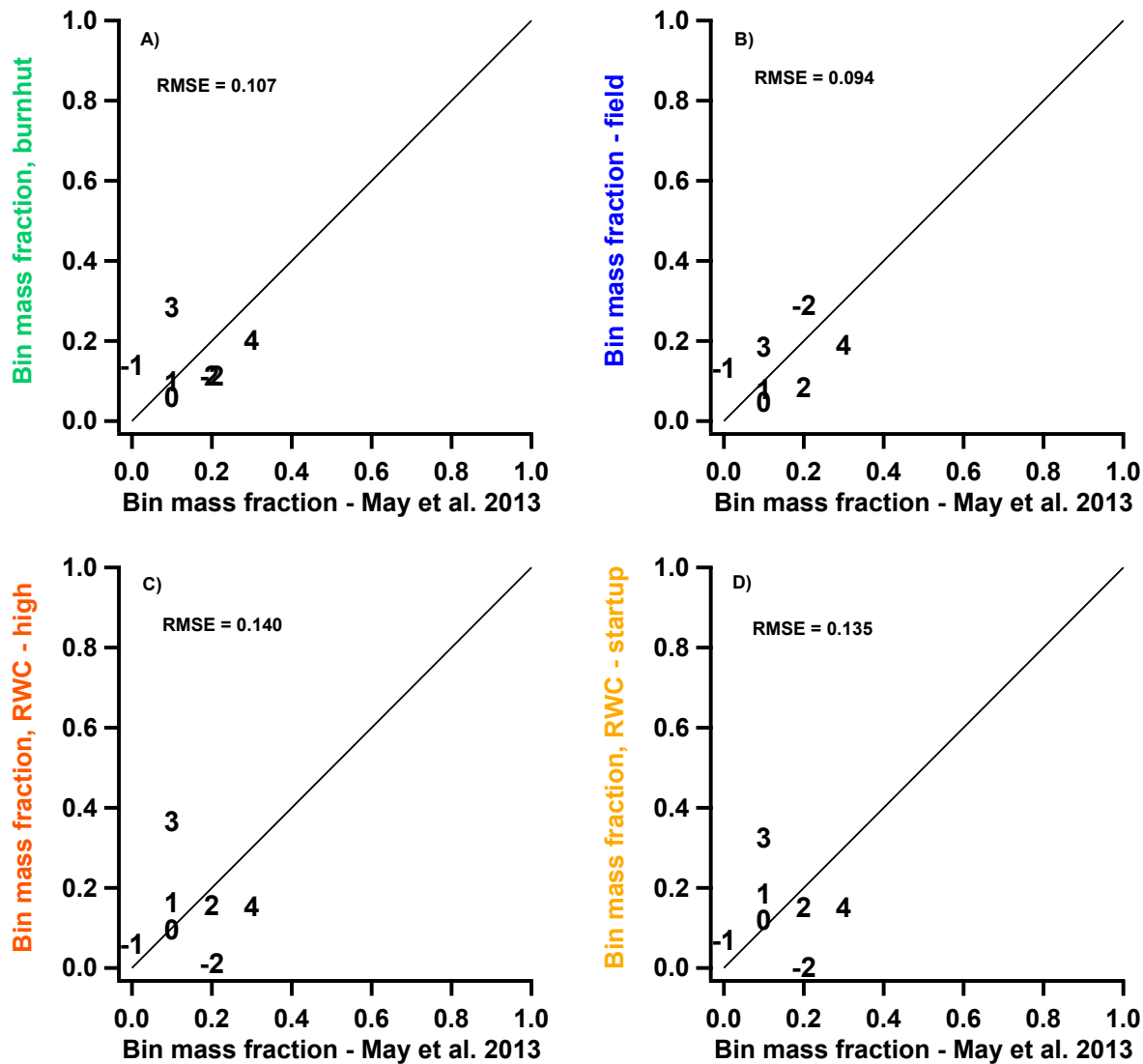
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100 **Figure S6: Volatility distributions of biomass burning combustion sources - burnhut, field,**
 101 **woodstove – high fire and woodstove – start up (delineated by color) re-normalized to the range**
 102 **$-2 \leq \log C^* \leq 4$ to enable comparison with the volatility distributions presented in May et al.²**
 103 **Distributions are presented in terms of mass fraction in each $\log C^*$ bin. The mass fraction showed**
 104 **in each bin is the average bin mass from replicate (N=3) samples while the error bars show the**
 105 **standard deviations in the replicates. The black bars show the distribution from May et al.**

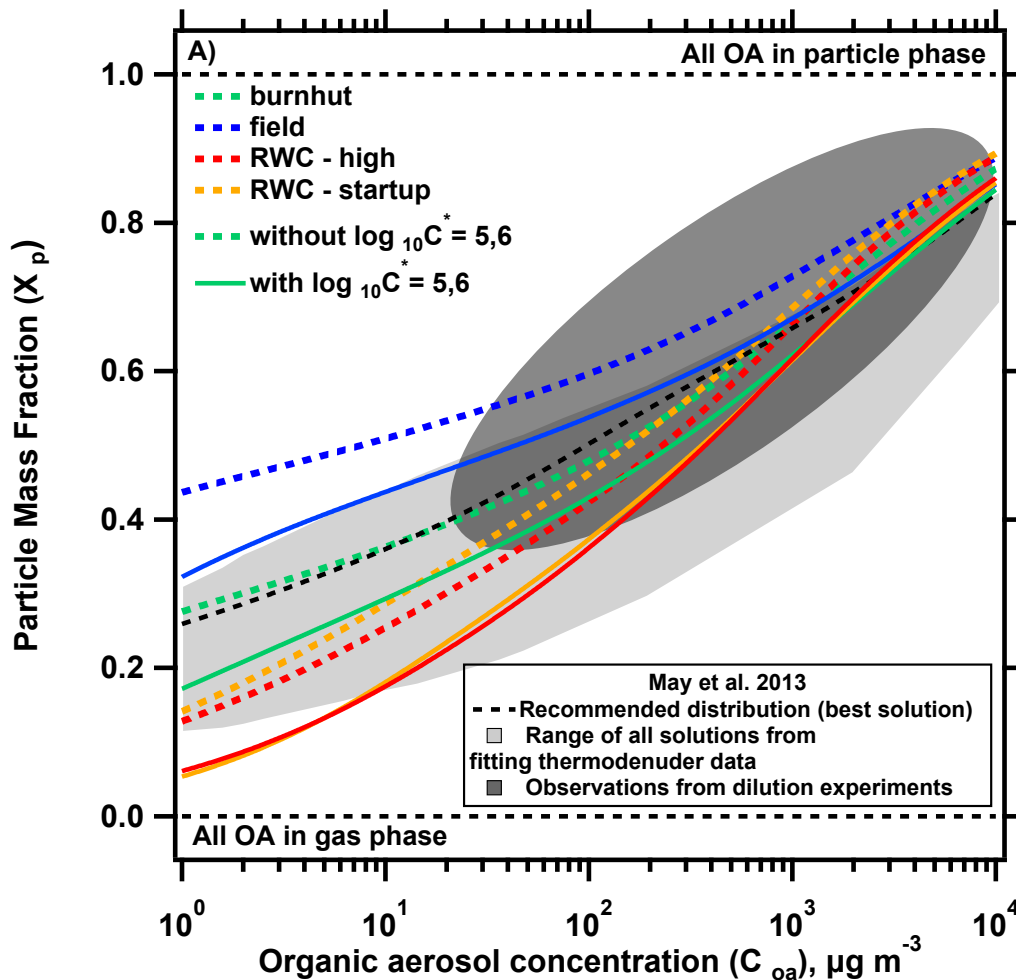
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108 Figure S7: Scatter plots of the bin mass fraction contributions from volatility distributions re-
 109 normalized to the range $-2 \leq \log C^* \leq 4$ to enable comparison with volatility distributions
 110 presented in the literature.² The plots presented here compare re-normalized burnhut, field, RWC
 111 – high and RWC – startup distributions to May et al. (delineated by label colors). The markers
 112 represent the average bin mass fraction from replicate (N=3) filter-in-tube samples. The solid black
 113 line shows the 1:1 line in each plot with the root mean square error (RMSE) to the 1:1 line printed
 114 in each plot.

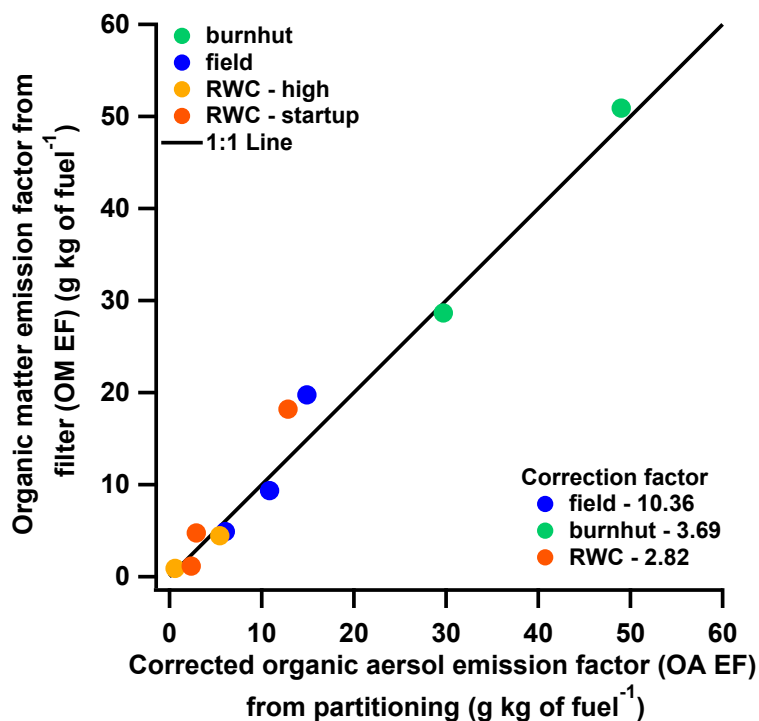
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117 **Figure S8: Partitioning plot showing the particle mass fraction (X_p) calculated using Equation 1 and**
 118 **volatility distributions shown in Figure 3A (containing bins 5 and 6) indicated by the solid and lines**
 119 **and Figure S6 (re-normalized after removing bins 5 and 6) indicated by the dashed lines vs organic**
 120 **aerosol concentration (C_{OA}). The biomass burning sources are delineated by color. Also plotted are**
 121 **observations from May et al.² The curves including bins 5 and 6 show the same general trends as**
 122 **those using renormalized distributions, but are shifted to lower X_p across the C_{OA} range, as these**
 123 **distributions encompass more material. This shift in X_p is less pronounced at higher C_{OA} values as**
 124 **more of the IVOC material partitions into the particle phase under these conditions**

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127 **Figure S9: Organic matter emission factor (OM EF) as measured via thermo-optical analysis of**
 128 **quartz filters (converted from OC using a campaign average OM/OC ratio of 1.53) plotted against**
 129 **organic aerosol emission factor (OA EF) as estimated from particle phase partitioning of total**
 130 **organic matter measured by filter-in-tube filter+sorbents. Colors delineate biomass burning**
 131 **combustion source types. The solid black line is the 1:1 line. The correction factors (average of ratio**
 132 **for each source type) used to reconcile differences between the two EF estimation methods are**
 133 **printed on the graph for each combustion source type.**

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135 References

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