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1 2	Supplementary information
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5	Lithium-selective hybrid capacitive deionization system with Ag-
6	coated carbon electrode and stop-flow operation
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² **Fig. S2** Galvanostatic charging/discharging profile of the activated carbon (AC) electrode and Ag

3 coated AC electrode (Current density: 0.5 mA/cm2, Cut-voltage: 0.3 V / -0.1 V, Electrolyte: 2 M

4 LiCl₂)



Fig. S3 Cyclic voltammetry profiles of lithium manganese oxide electrode (Electrolyte: 2 M LiCl;

- 6 Scan rate: 1 mV/s; Reference electrode: Ag/AgCl KCl sat'd).

Counter electrode	Operation mode (Current density)	Solution compositio n	Li ⁺ recovery capacity / Energy consumption (mol _{Li} /Wh)	Reference
Ag coated AC electrode	CC mode (0.5 mA/cm²)	Li ⁺ 10 mM	0.34	This study
Ag	CC mode (0.5 mA/cm²)	Li⁺ 210 mM	1.0	[1]
AC	CC mode (0.5 mA/cm²)	Li ⁺ 30 mM (LiCl, NaCl, KCl, MgCl ₂ , and CaCl ₂)	0.24	[2]
Zn	CC mode (0.5 mA/cm²)	Li+ 210 mM	0.16	[3]
PANI	CC mode (0.5 mA/cm²)	Li⁺ 64 mM	0.25	[4]
NiHCF	CC mode (1 C)	Li⁺ 42 mM	0.28	[5]

Table S1 Li⁺ recovery capacity per unit energy consumption of lithium recovery system
 according to the counter electrode (AC: Activated carbon, Ag: Silver, Zn: Zinc, PANI:
 Polyaniline, NiHCF: Nickel Hexacyanoferrate)

37 Table R1 provides the Li⁺ recovery capacity per unit energy consumption from the result 38 in Fig 2 and Eq. (5) and from previous studies. It is noted that comparisons were made with 39 literature values evaluated under similar current density conditions. As shown in Table R1, 40 Li* recovery capacity per unit energy consumption of this system (HCDI with Ag coated AC 41 electrode) showed 0.34 molu/Wh, which was better than the values reported in the 42 literature, except the system using the Ag electrode. On the other hand, 1.0 mol_{ui}/Wh was 43 reported for the Li recovery system with Ag electrode as counter electrode.¹ Therefore, a 44 lithium recovery system with Ag counter electrode is more advantageous in aspect of 45 lithium recovery capacity per unit energy consumption than HCDI with Ag coated AC electrode. 46

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47 However, Ag is a precious and expensive metal. It appears that a significant cost is 48 expected (estimated at $222 - 300 \text{ USD/m}^2$) considering the amount and price of Ag in the

- 1 Ag electrode $(30 40 \text{ mg/cm}^2)$.^{1,6} On the other hand, only 4 5.3% of Ag is required for Ag
- 2 coating in this study (estimated at 1.2 USD/m²).6 Therefore, since the Ag electrode and the
- 3 Ag coated AC electrode have clearly different advantages in terms of energy consumption
- 4 and Ag cost, they could be used selectively according to the user's priority.





Fig. S4 Electrochemical capacity retention ratio of Li-selective hybrid capacitive deionization
 system (Negative electrode: lithium manganese oxide electrode; Positive electrode: Ag-coated
 activated carbon electrode; Current: 10 mA/cm²; Voltage cut-off: 1.0 V/-1.0 V)



Fig. S5 Cell voltage profile with cut-off voltage (Feed: 10 mM LiCl; Negative electrode: lithium
 manganese oxide electrode; Positive electrode: activated carbon (AC) electrode or Ag-coated

4 AC electrode; Cut-off voltage: 0.5–0.8 V; Current: 0.5 mA/cm² at adsorption/-0.5 mA/cm² at

5 desorption; Flow rate: 2 mL/min)



Fig. S6 Cationic concentration in the product solution and Li⁺ selectivity coefficient in the Li-selective hybrid capacitive deionization system under conventional flow (From Fig. 5), stop-flow (From Fig. 5) and conventional flow with cleaning step (Negative electrode: lithium manganese oxide electrode; Positive electrode: Ag-coated activated carbon electrode; Feed: 5 mM LiCl + 5 mM NaCl; Current: 0.5 mA/cm2; Voltage cut-off: 1.0 V/-1.0 V; Flow rate: 2 mL/min).



Fig. S7 Selectivity coefficient with Na/Li ratio in feed solution of the Li-selective hybrid capacitive
 deionization system with LMO/Ag-coated AC electrode configuration. Blue section: selectivity
 coefficient > Na/Li ratio, Red section: selectivity coefficient < Na/Li ratio. LMO: lithium
 manganese oxide; AC: activated carbon.

1 References

- M. Pasta, A. Battistel, F. La Mantia, Batteries for lithium recovery from brines, Energy
 Environ. Sci., 2012, 5, 9487–9491.
- 4 2 S. Kim, J. Lee, J.S. Kang, K. Jo, S. Kim, Y.-E. Sung, J. Yoon, Lithium recovery from brine using 5 a λ -MnO₂/activated carbon hybrid supercapacitor system, Chemosphere, 2015, **125**, 50–
- **6 56**.
- S. Kim, J. Lee, S. Kim, S. Kim, J. Yoon, Electrochemical lithium recovery with a LiMn₂O₄-zinc
 battery system using zinc as a negative electrode, Energy Technol., 2018, 6, 340–344.
- battery system using zine as a negative electrode, Energy rectiniti., 2018, **0**, 540–544.
- 9 4 A. Zhao, J. Liu, X. Ai, H. Yang, Y. Cao, Highly Selective and Pollution-Free Electrochemical
 10 Extraction of Lithium by a Polyaniline/LixMn2O4 Cell. ChemSusChem, 2019, **12**, 136111 1367.
- 12 5 R. Trócoli, C. Erinmwingbovo, F. La Mantia, Optimized Lithium Recovery from Brines by
- 13 using an Electrochemical Ion-Pumping Process Based on λ -MnO2 and Nickel
- 14 Hexacyanoferrate. ChemElectroChem, 2017, **4**, 143-149.
- 15 6 IMF primary commodity price database, <u>https://www.imf.org/en/Research/commodity-</u>
- 16 prices, (accessed October 2022).