

Supporting information

Ultra-high-rate CO₂ reduction reactions to multicarbon products with a current density of 1.7 A/cm² in neutral electrolyte

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Experimental Section

Chemical and materials

$\text{Cu}(\text{CH}_3\text{COO})_2 \cdot \text{H}_2\text{O}$ (99.99% trace metals basis) and 5 wt% Nafion dispersion were obtained from Sigma-Aldrich Chemical Co., Ltd. NaBH_4 , ethanol, isopropanol, DMSO, KCl, KOH and KHCO_3 were purchased from Wako Co., Ltd. We prepared three kinds of commercial carbon-based gas diffusion electrodes, GDL 34BC (Sigracet), GDS2130 (AvCarb) and PYROFIL MFK-A (Mitsubishi Chemical Co., Ltd.). Cu-based catalysts, in addition to the synthesized one as below, were purchased from Sigma-Aldrich Chemical Co., Ltd. A PTFE to be pasted to fix an electrode area was NITOFILONTM (No.900UL, thickness: 0.2 mm, Nitto). A proton-exchange membrane (Nafion 117) was purchased from Fuel Cell Store.

Preparation of the electrodes

We here explain how to prepare our optimized electrode. CuONPs were synthesized via a wet-chemical reduction method. Briefly, 0.61 g of $\text{Cu}(\text{CH}_3\text{COO})_2 \cdot \text{H}_2\text{O}$ was dissolved in 250 mL of deionized water, and the resultant solution was stirred under Ar bubbling for 30 min to remove residual oxygen. 1.25 g of NaBH_4 in 20 mL of deionized water was dropped slowly into the copper(II) ion solutions. The synthesized metal Cu nanoparticles

were rinsed with deionized water and ethanol. Then, we stored them at room temperature under ambient conditions for at least two weeks to oxidize by air. A homogeneous catalyst ink was prepared by sonication of 3.4 mg of CuONPs with 400 μL of isopropanol and 4.4 μL of a 5 wt% Nafion dispersion. The catalyst ink was drop-casted onto a GDL34BC at 80 $^{\circ}\text{C}$. A PTFE sheet with a hole (0.5 cm^2) was pasted on the GDE by hot pressing (250 $^{\circ}\text{C}$, 10 MPa for 1 minute) before catalyst coating to strictly fix the area of the electrode. The pasted PTFE would also be beneficial to suppress HER from the bare MPL. The target amount of CuONPs loading was obtained by repeatedly loading and drying the catalyst ink of 20 μl . We prepared electrodes with the same method even when varying catalysts or GDEs.

Characterization

Transmission electron microscopy (TEM) observation were conducted using a Hitachi H-9000NAR microscope. X-ray diffraction (XRD patterns) were collected using a Miniflex diffractometer (Rigaku) equipped with a Cu $K\alpha$ radiation source. X-ray photoelectron spectroscopy (XPS) analyses were conducted using an Axis Ultra spectrometer (Kratos Analytical) equipped with an Al $K\alpha$ radiation source. Field-emission scanning electron microscopy (FESEM) images were obtained using a JEOL JSM-7800F microscope.

Energy dispersive X-ray spectroscopy (EDX) elemental mappings were acquired using an Oxford Instruments X-MaxN spectrometer.

Electrochemical experiments

Electrochemical experiments were performed using electrochemical workstations (HAL3001A+HAL3001B10, Hokuto Denko and SI1287, Solartron). An in-house-built three-compartment electrochemical cell was used for all experiments (Figure S12). A proton-exchange membrane (Nafion 117) was used to separate the cathodic and anodic chambers. A Pt wire and an Ag/AgCl electrode with 3 M KCl solution were used as counter and reference electrodes, respectively. During the electrochemical experiments, CO₂ gas (99.99%) was supplied into the gas chamber at a rate of 15 sccm. Both catholyte and anolyte were flowed at a rate of 10 mL/min using peristaltic pumps and passed once through each chamber without circulation. The temperature of the catholyte at the outlet was 40 °C and constant during electrolysis. We used 1 M KOH and saturated KHCO₃ solutions as anolyte for alkaline and neutral CO₂RR, respectively. Saturated KHCO₃ solution was used for anolyte to reduce cell voltage. The gaseous products were analyzed using gas chromatography (GC-2030, Shimadzu) equipped with both thermal conductivity detector (TCD) and flame ionization detector (FID) as detectors, and

MICROPACKED-ST (Shinwa Chemical Industries Ltd.) as columns. The liquid products were analyzed using NMR spectroscopy (Unity-Inova500, Agilent) using presaturation mode. A 0.5 mL sample of the electrolyte after electrolysis was mixed with 0.1 mL of internal standard containing 1.40 mM DMSO solution diluted with D₂O.

It is difficult to accurately compensate applied potentials under high-rate electrolysis due to a significant IR drop and a large Nernstian potential loss associated with pH gradients.

In this work, we measured CVs using the current interruption technique^{S1,S2} for the IR compensation (Figure S13), and then, the relationship between J_{total} vs. U obtained in these CVs was utilized to evaluate applied potentials for the constant current measurements. The off time was set to 27 msec, and the On/Off ratio was set to 255 in the current interruption. Although we understand the difficulty of the compensation, it has been reported that the current interrupt is one of the ideal compensation methods for high-current CO₂ electrolysis because it can compensate the potential even if solution resistance varies during electrolysis^{S3}.

Supplementary results

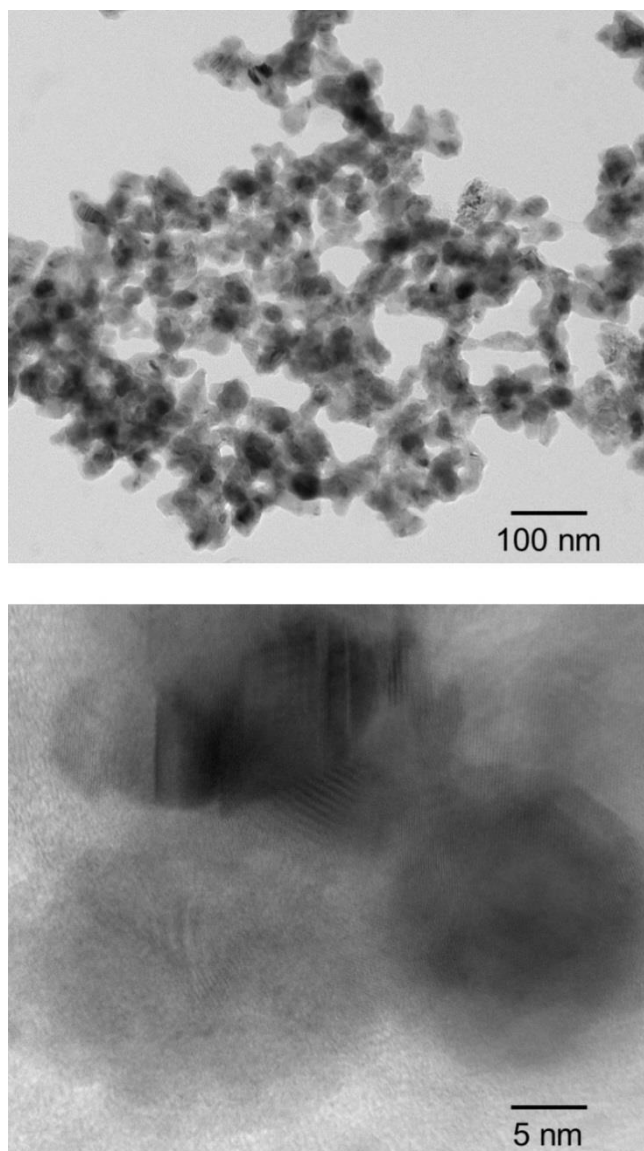


Figure S1 Representative TEM images of the synthesized CuONPs.

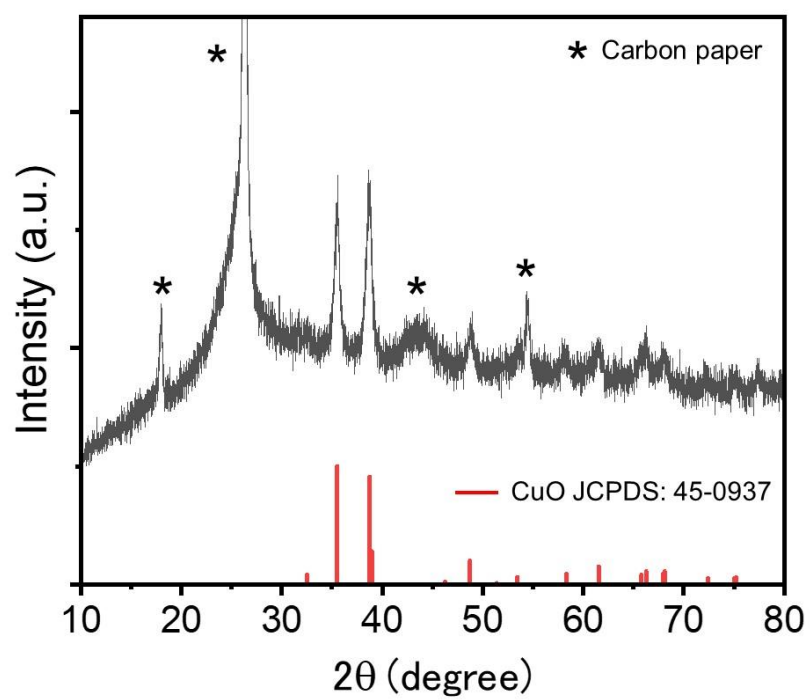


Figure S2 XRD pattern of a CuONPs-1.7/GDE.

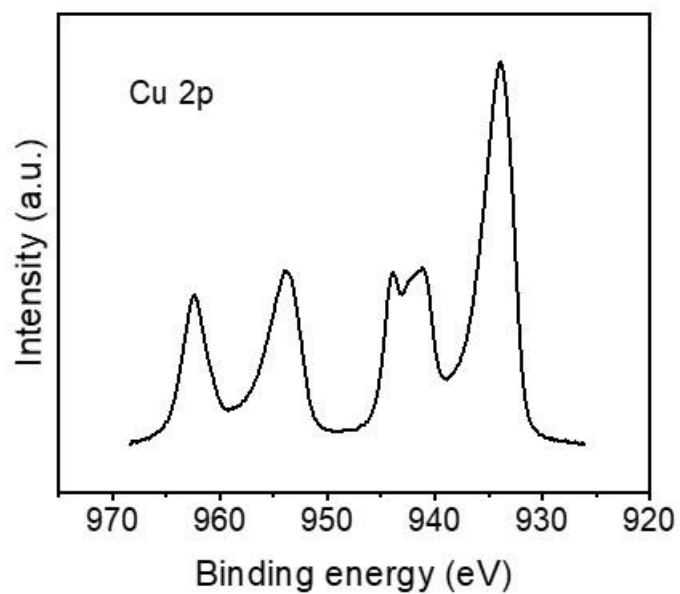


Figure S3 Cu 2p spectrum of CuONPs-1.7/GDE. The main Cu 2p_{3/2} peak at 933 eV corresponds to Cu(II) ions. Satellite peaks were observed on the higher binding energy side of the main peaks, which also indicated the presence of Cu(II).

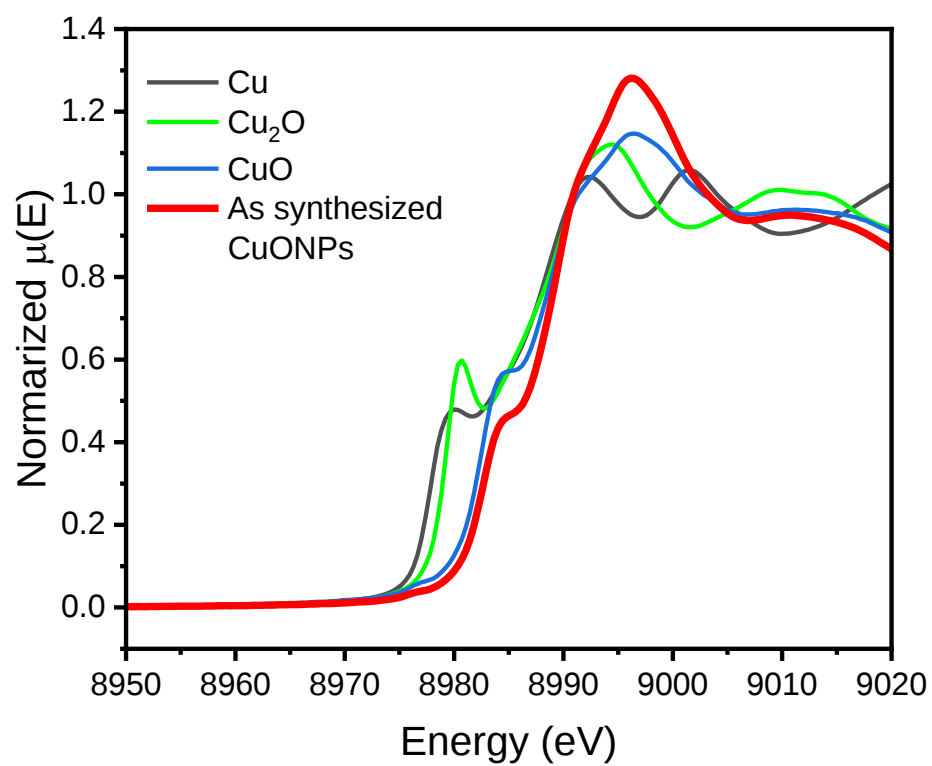


Figure S4 Normalized Cu K-edge XANES spectra of as-synthesized CuONPs.

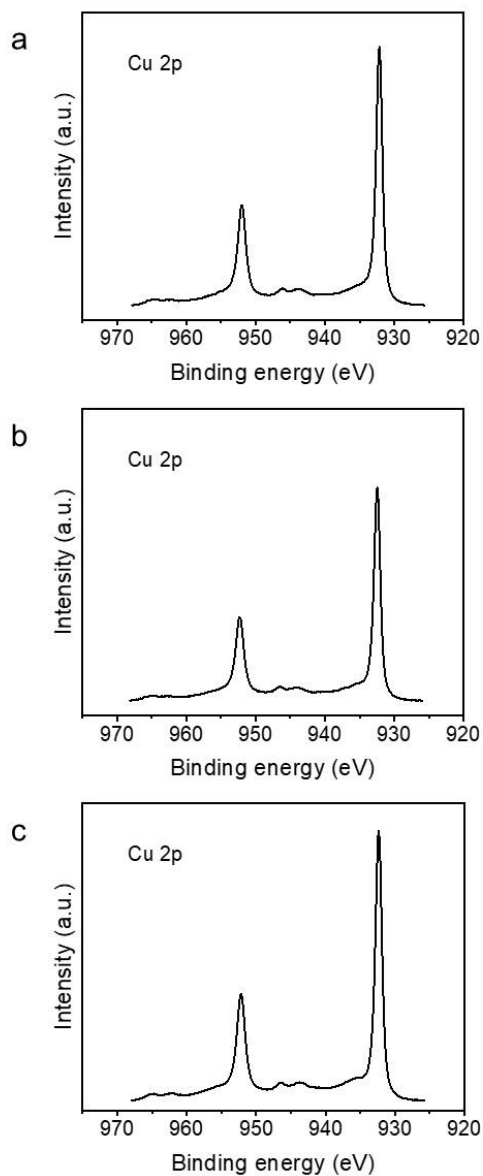


Figure S5 Cu 2p spectra of CuONPs-1.7/GDE after application of (a) $J_{\text{total}} = 2400 \text{ mA/cm}^2$ for 30 min in 1 M KOH, (b) $J_{\text{total}} = 2800 \text{ mA/cm}^2$ for 30 min in 1 M KOH, and (c) $J_{\text{total}} = 2400 \text{ mA/cm}^2$ for 30 min in 1 M KCl. Cu oxidation states were reduced to Cu(I)/Cu(0) during electrolysis, and there was no apparent difference in the surface chemical state of Cu under the different electrolysis conditions (electrolytes or current densities).

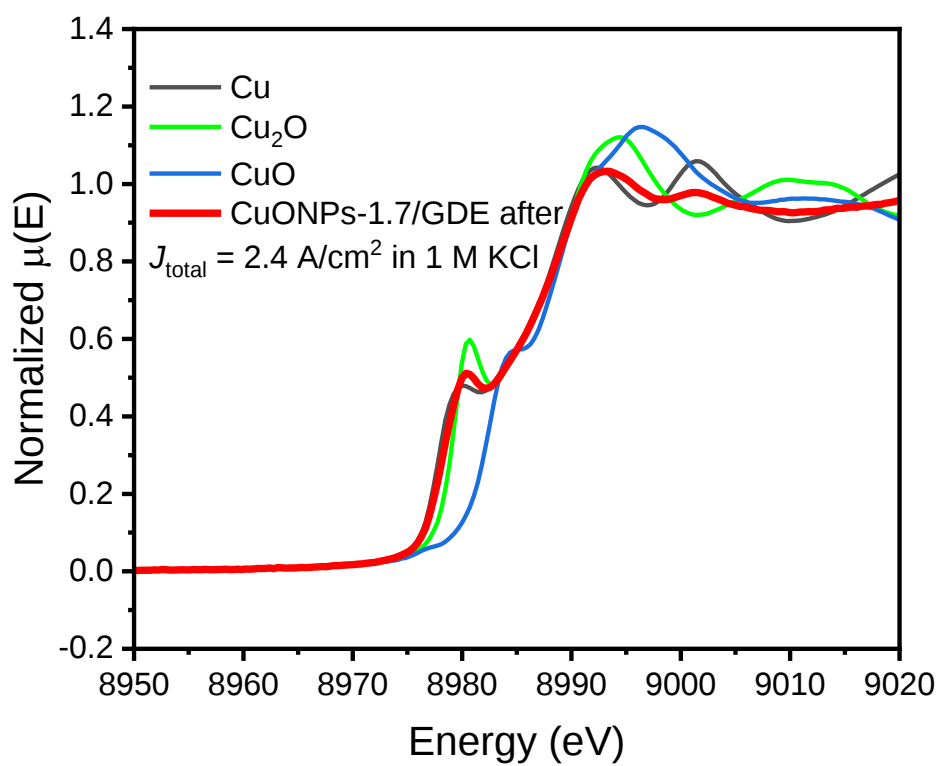


Figure S6 Normalized Cu K-edge XANES spectra of CuONPs-1.7/GDE after applying $J_{\text{total}} = 2400 \text{ mA/cm}^2$ for 30 min in 1 M KCl.

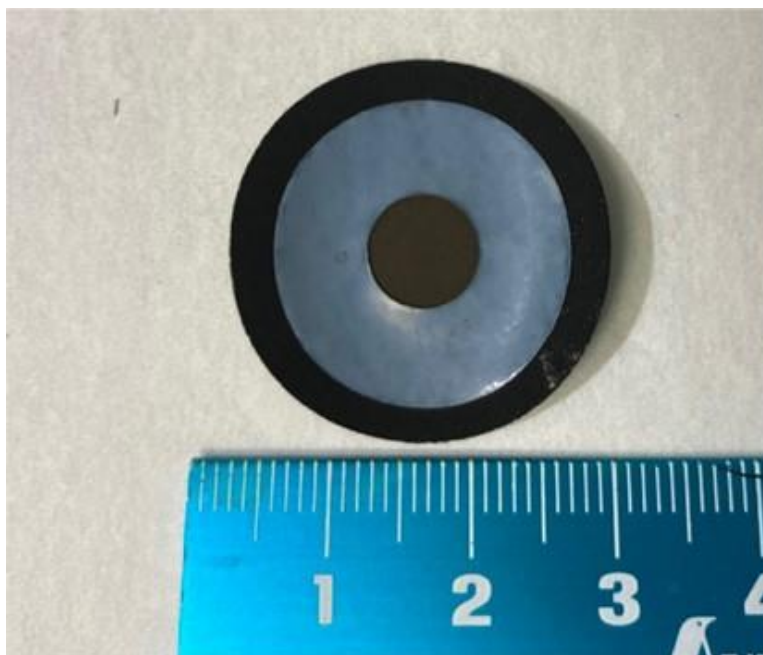


Figure S7 Photograph of the working electrode: CuONPs-deposited on GDE with thermocompressed PTFE (geometric area of the hole is 0.5 cm^2).

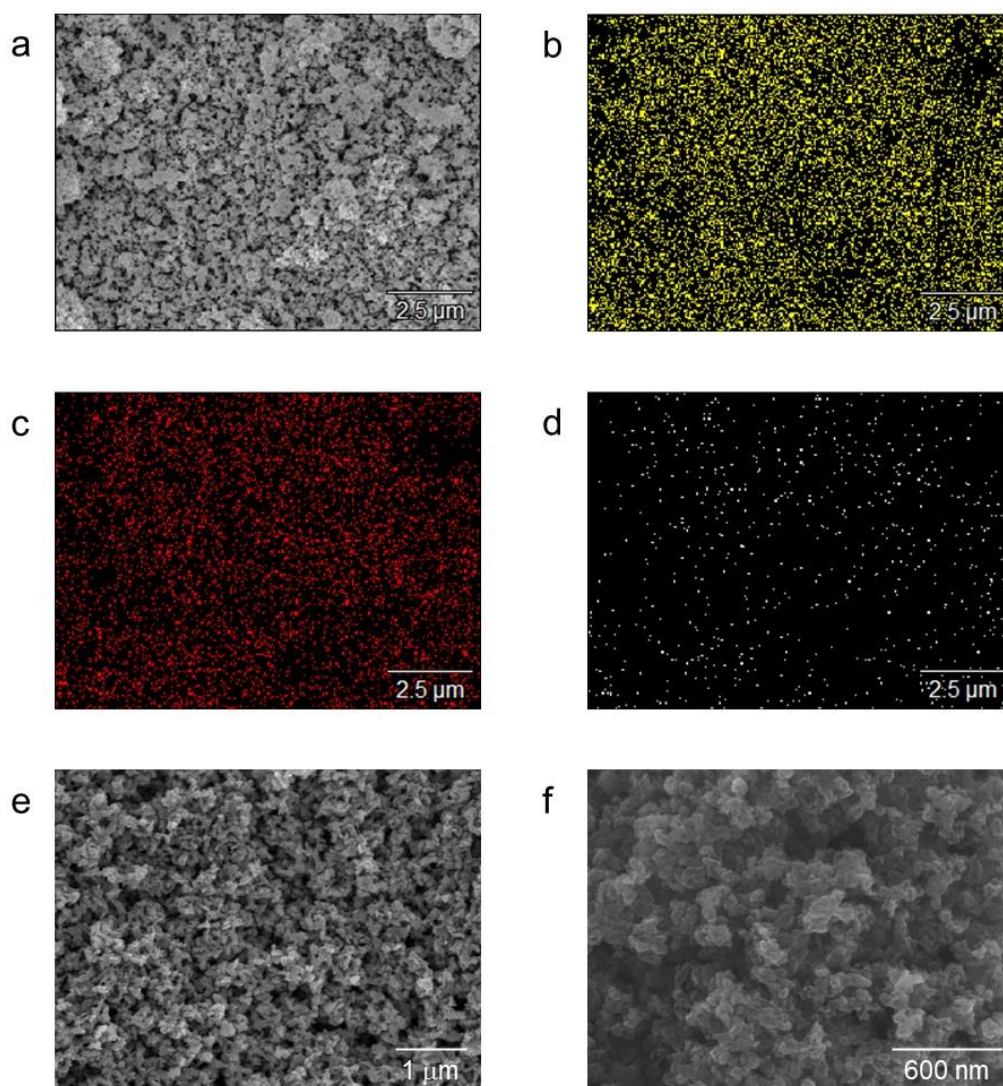


Figure S8 (a)-(f) Top-view SEM images of a CuONPs-1.7/GDE and the corresponding EDX mappings to (a) for (b) Cu, (c) O and (d) C atoms.

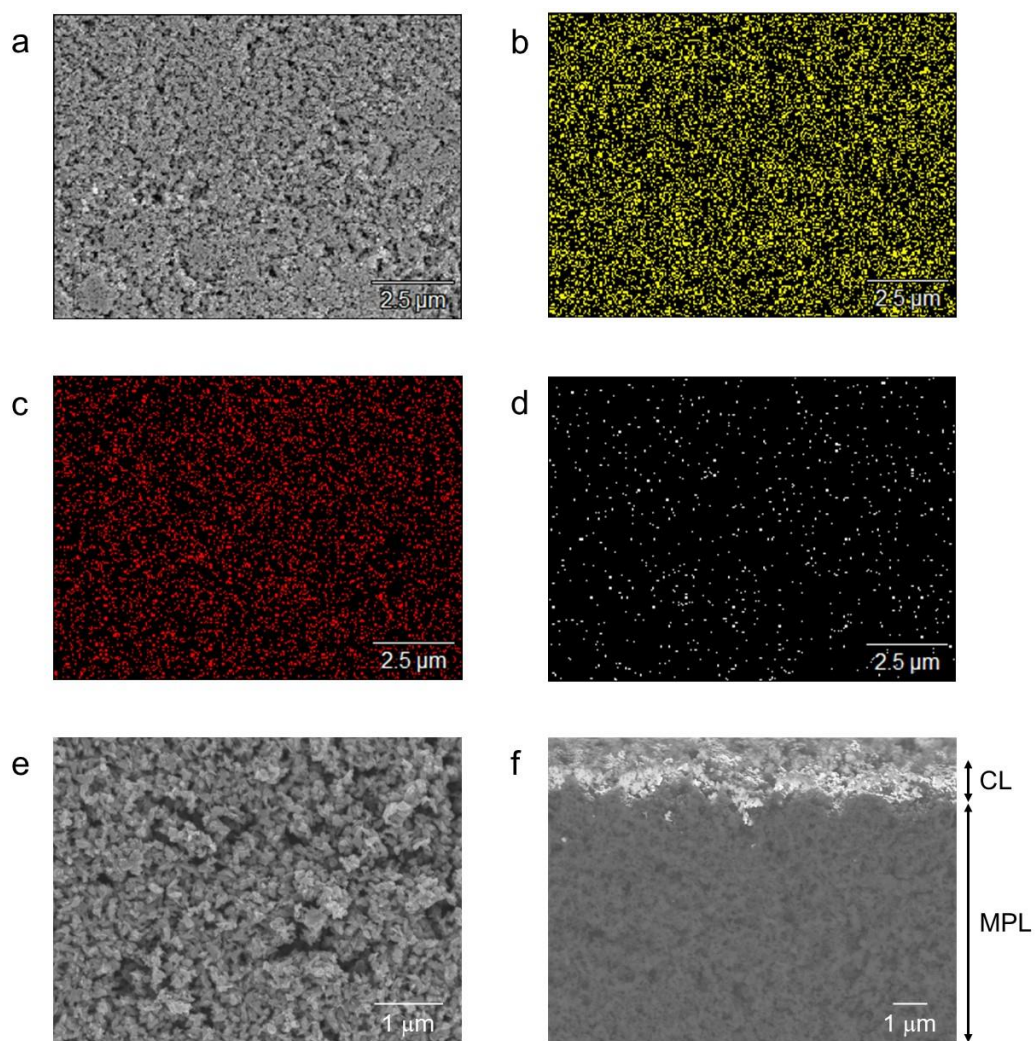


Figure S9 (a-e) Top-view and (f) cross-sectional SEM images of a CuONPs-0.34/GDE and the corresponding EDX mappings to (a) for (b) Cu, (c) O and (d) C atoms.

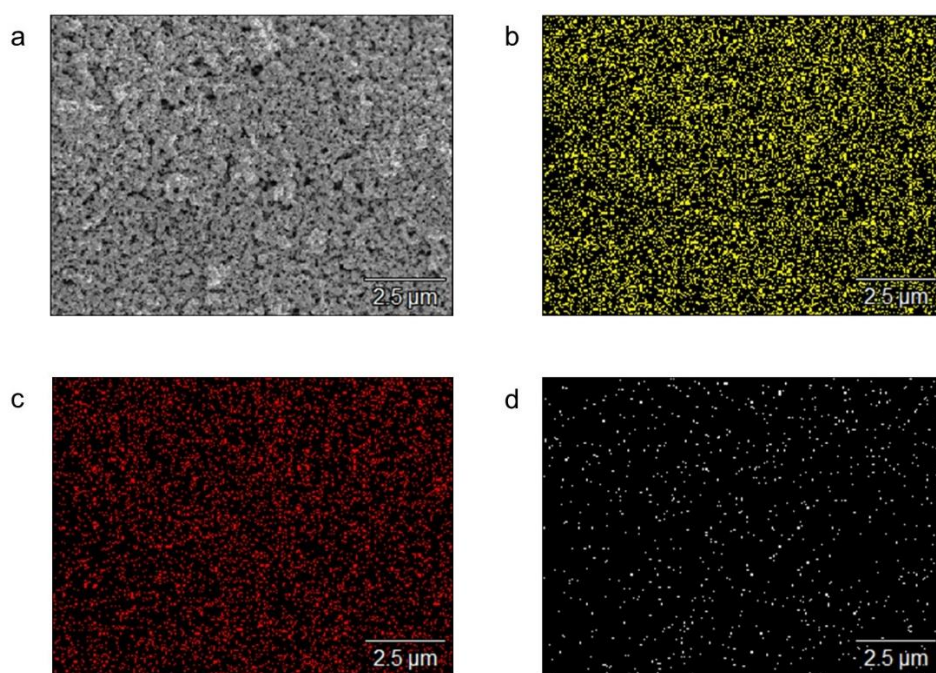


Figure S10 (a) Top-view SEM images of CuONPs-3.1/GDE and the corresponding EDX mappings to (a) for (b) Cu, (c) O and (d) C atoms.

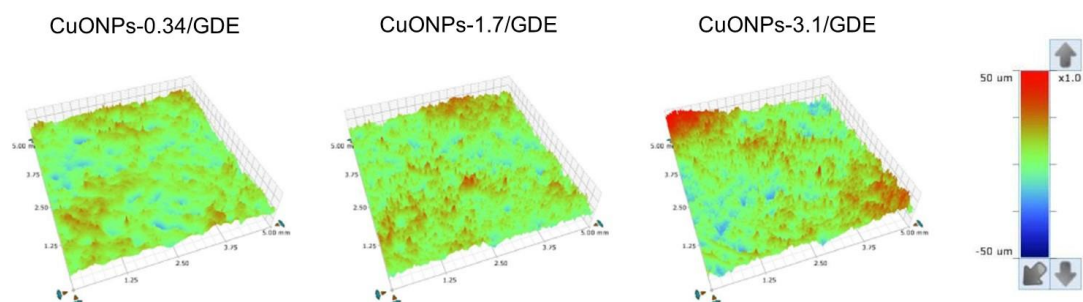


Figure S11 3D Maps of the electrode surface for CuONPs-0.34, 1.7, 3.1/GDE.

Table S1 Roughness factors for CuONPs-0.34, 1.7, 3.1/GDE

	Ra (μm)	Rq (μm)
CuONPs-0.34/GDE	5.697	7.283
CuONPs-1.7/GDE	6.667	8.468
CuONPs-3.1/GDE	8.686	11.32

Ra (arithmetic mean roughness): Average absolute value of deviation from the central plane to the surface on a quantitative surface

Rq (Root mean square roughness): Square root of the mean of the squares of the deviations from the central plane to the surface on a quantitative surface.

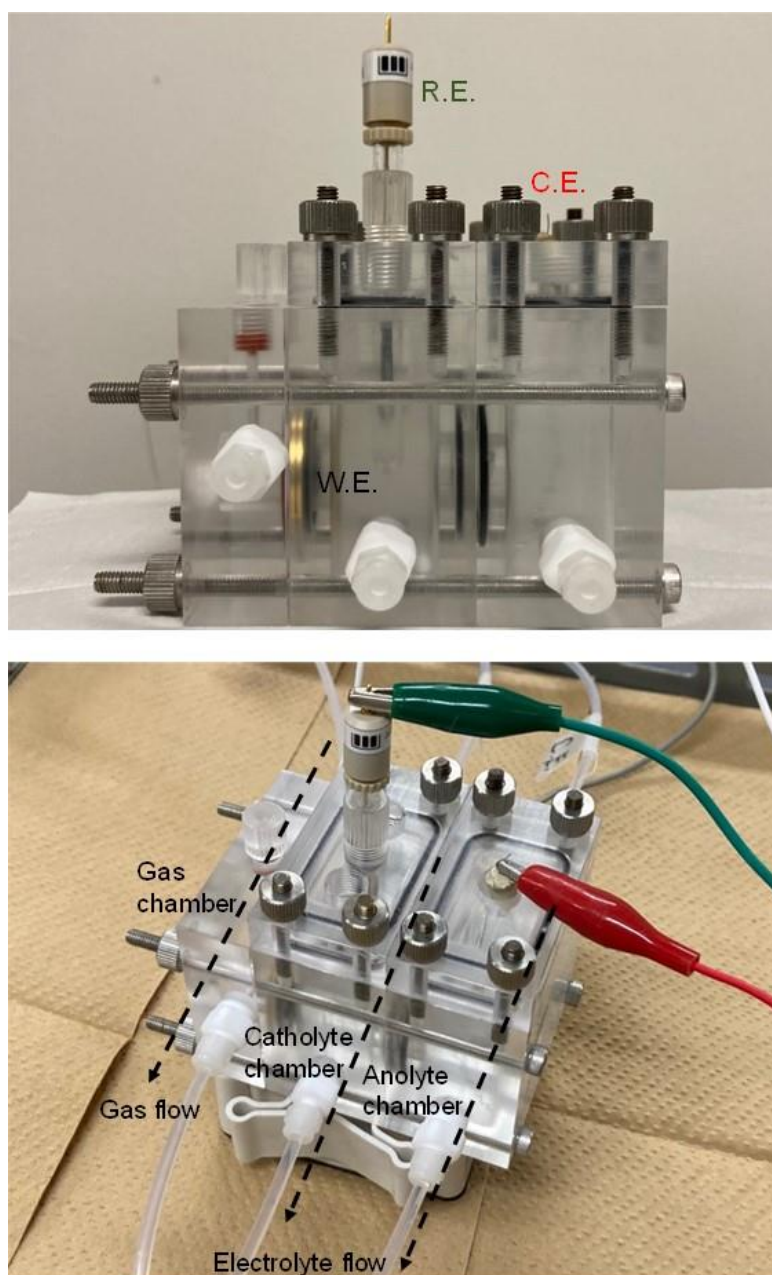


Figure S12 In-house-built three-compartment electrochemical cell for CO₂RR evaluation.

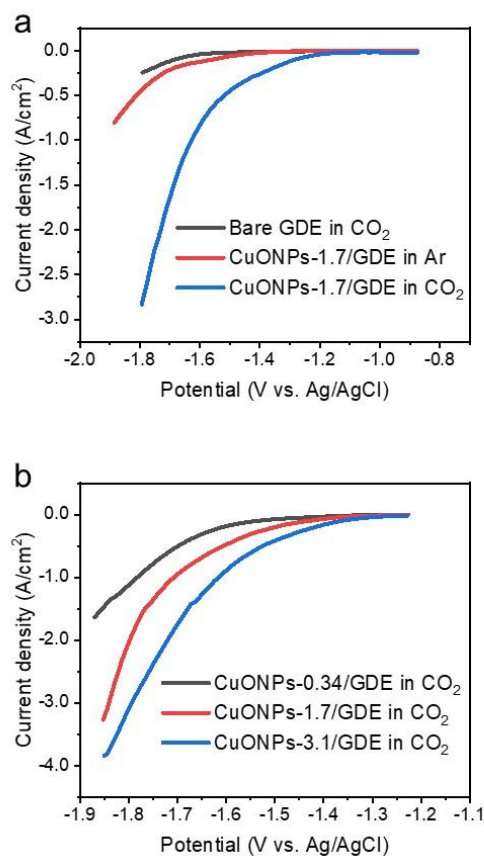


Figure S13 (a) J_{total} vs. U curves for the bare GDE under CO_2 , and CuONPs-1.7/GDE under Ar and CO_2 conditions in 1 M KCl electrolyte. (b) J_{total} vs. U curves for the CuONPs-0.34, 1.7, 3.1/GDE under CO_2 conditions in 1 M KOH electrolyte. Scan rate: 50 mV/s

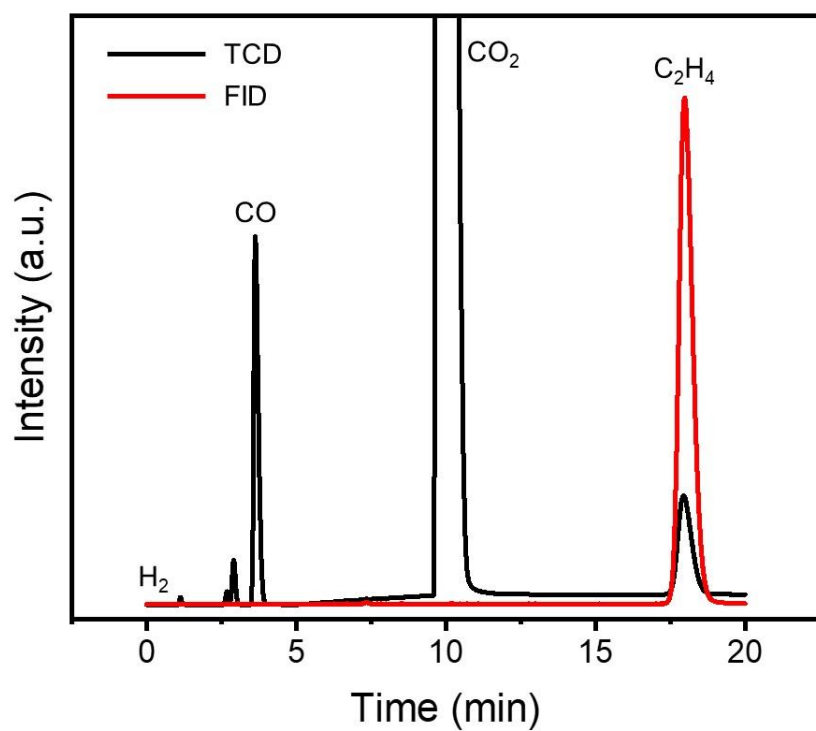


Figure S14 Representative gas chromatography profiles. The gaseous products were analyzed using a gas chromatograph (Shimadzu GC-2030) equipped with a thermal conductivity detector (TCD) and flame ionization detector (FID). CO₂RR conditions: constant current density of $J_{\text{total}} = 1000 \text{ mA/cm}^2$ for 30 min in 1 M KCl electrolyte.

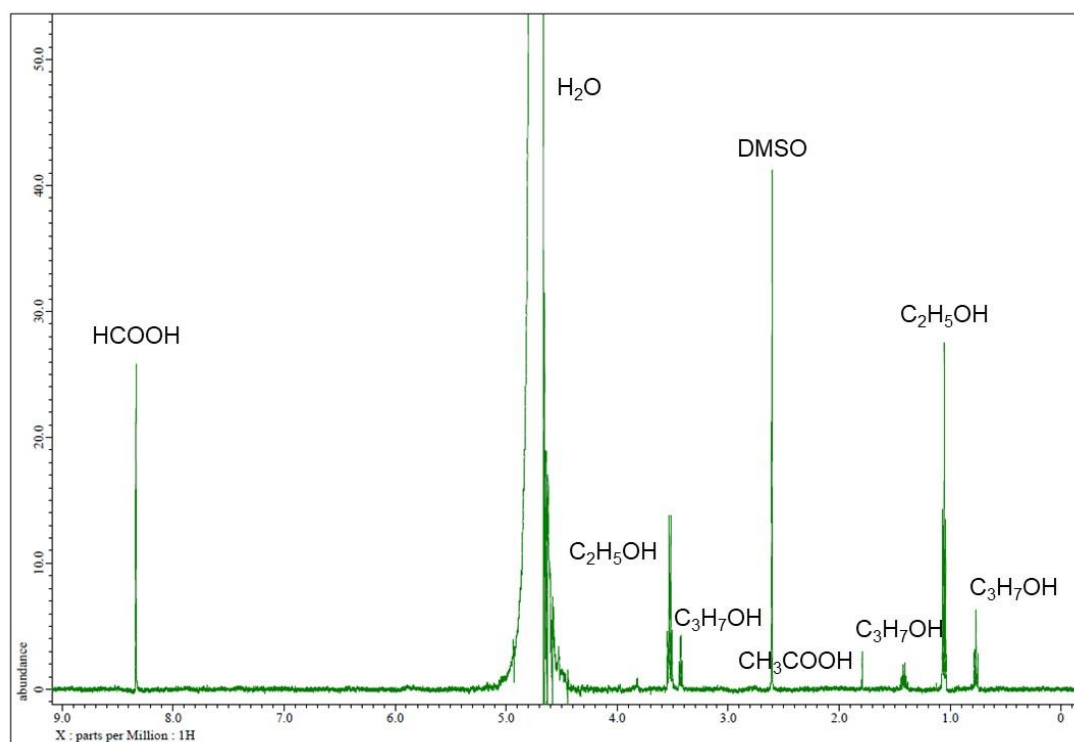


Figure S15 Representative ^1H -NMR spectrum. ^1H -NMR samples were prepared by mixing 500 μL of the catholyte and 100 μL of DMSO internal standard solution (1.40 mM). ^1H -NMR spectra were collected with a water presaturation mode. CO_2RR conditions: constant current density of $J_{\text{total}} = 2000 \text{ mA/cm}^2$ for 30 min in 1 M KCl electrolyte.

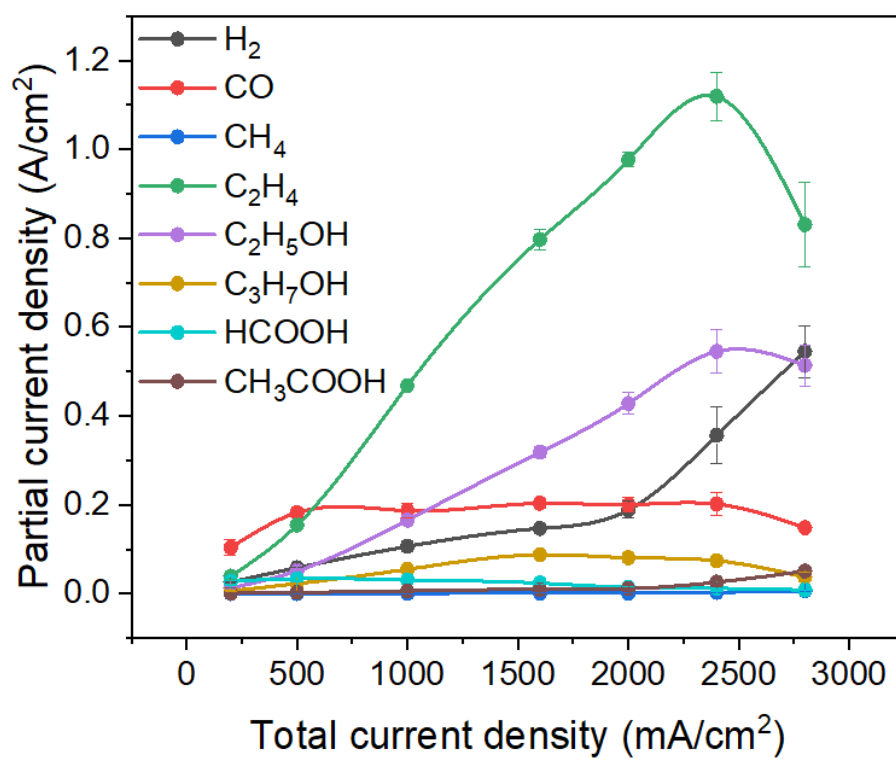


Figure S16 Partial current density of each CO₂RR product on CuONPs-1.7/GDE in 1 M KCl. Reaction time: 30min

Table S2 The comparison of CO₂RR activity in neutral electrolytes. The table shows the highest value of j_{C2+} and FE_{C2+} under those conditions in each reference.

Sample	Electrolyte	FE_{C2+} (%)	j_{C2+} (A/cm ²)	Ref
CuONPs-1.7/GDE	1 M KCl	73	1.74	This work
Cu(100)/Cu(111) interface	1 M KHCO ₃	75	0.22	S4
Cu ₂ O particle / 30 wt% Nafion	0.1 M KHCO ₃	62	0.44	S5
Electrodeposited Cu	2 M KCl	67	0.13	S6
Cu derived from Cu	1 M KHCO ₃	68	0.34	S7
Cu-12	1 M KHCO ₃	86	0.28	S8
Surface reconstructed Cu	1 M KHCO ₃	75	0.43	S9

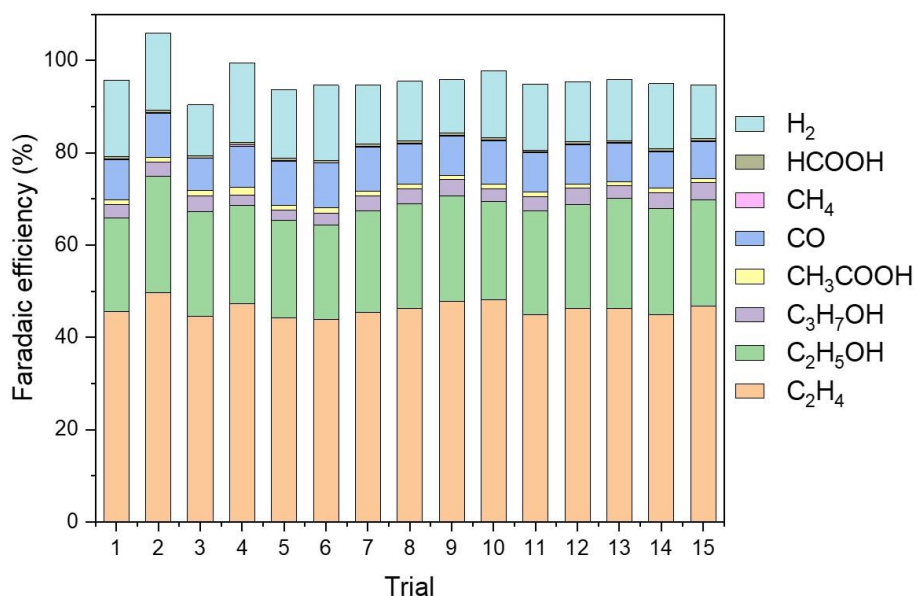


Figure S17 Reproducibility of the CO₂RR results under $J_{\text{total}} = 2400 \text{ mA/cm}^2$ ($j_{\text{C2+}} > 1.7 \text{ A/cm}^2$) on CuONPs-1.7/GDE using different batches of electrodes in 1 M KCl. Reaction time: 30 min.

Table S3 Reproducibility of $j_{\text{C2+}}$ and faradaic efficiency at $J_{\text{total}} = 2400 \text{ mA/cm}^2$ on CuONPs-1.7/GDE using different batches of electrodes in 1 M KCl. Reaction time: 30min.

Trial	FE _{C2+}	$j_{\text{C2+}}$	FE _{C2H4}	FE _{C2H5OH}	FE _{C3H7OH}	FE _{CH3COOH}	FE _{CO}	FE _{CH4}	FE _{HCOOH}	FE _{H2}
1	69.8	1.67	45.6	20.3	2.9	1.0	8.7	0.2	0.5	16.6
2	79.0	1.90	49.7	25.2	3.0	1.1	9.5	0.1	0.5	16.8
3	71.8	1.72	44.5	22.7	3.4	1.2	7.0	0.1	0.5	11.1
4	72.4	1.74	47.3	21.3	2.2	1.6	9.0	0.2	0.5	17.4
5	68.7	1.65	44.3	21.2	2.1	1.1	9.5	0.2	0.5	14.9
6	68.0	1.63	44.0	20.4	2.5	1.2	9.7	0.2	0.4	16.4
7	71.7	1.72	45.4	21.9	3.4	1.0	9.6	0.1	0.4	13.0
8	73.1	1.76	46.2	22.7	3.4	0.9	8.8	0.1	0.5	12.9
9	75.1	1.80	47.7	23.0	3.6	0.8	8.6	0.1	0.6	11.5
10	73.1	1.75	48.2	21.3	2.7	0.9	9.5	0.2	0.5	14.5
11	71.5	1.72	44.9	22.6	3.1	1.0	8.5	0.1	0.4	14.3
12	73.2	1.76	46.3	22.5	3.5	0.8	8.6	0.1	0.5	13.0
13	73.7	1.77	46.4	23.7	2.7	1.0	8.3	0.2	0.4	13.2
14	72.3	1.74	45.0	23.0	3.4	1.0	8.0	0.2	0.5	14.1
15	74.4	1.79	46.7	23.1	3.7	0.8	8.0	0.1	0.6	11.6
Average	72.5±3.5	1.74±0.08	46.1±1.5	22.3±1.3	3.0±0.5	1.0±0.2	8.8±0.7	0.1±0.04	0.5±0.05	14.1±2.0

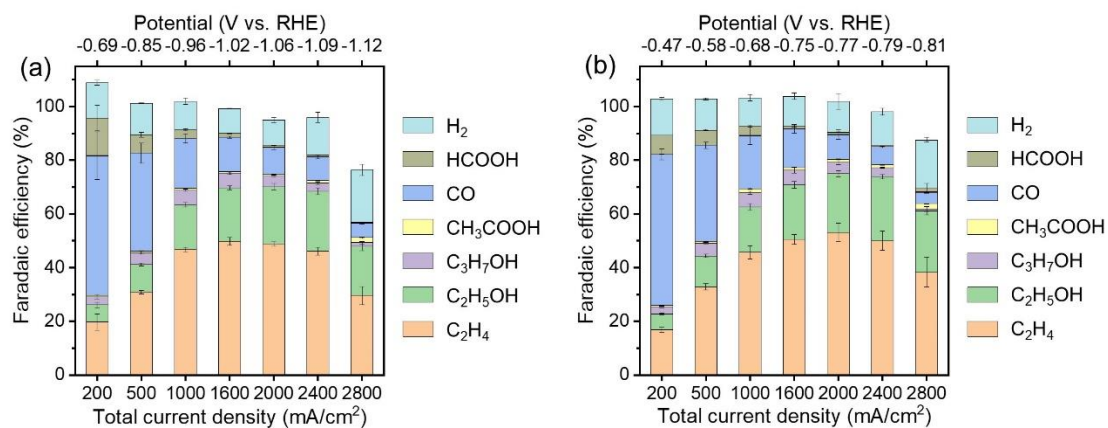


Figure S18 FE_s of the CO₂RR products under various applied potentials (V vs. RHE) on CuONPs-1.7/GDE in (a) 1 M KCl (pH: 8) and (b) 1 M KOH (pH: 14).

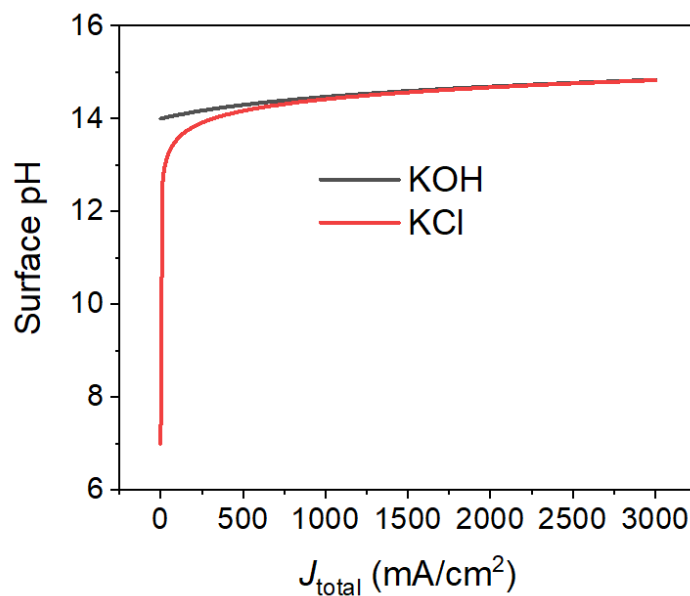


Figure S19 Calculated local pH using a rough reaction-diffusion model.

Table S4 Summary of the reported local pH obtained by theoretical simulations

Electrolyte	Total current density (mA/cm ²)	local pH	References
1 M KCl	200	13.8	this work
1 M KCl	2000	14.7	this work
1 M KOH	200	14.1	this work
1 M KOH	2000	14.7	this work
1 M KCl	200	13.5	S10
1 M KOH	200	14	S10
1 M KOH	200	13.8	S2
1 M KOH	750	15	S11
1 M KCl	100	11.6	S12
1 M KOH	100	12.7	S12
1 M KOH	500	13.2	S12

Table S5 The comparison of CO₂RR activity in alkaline electrolytes. The table shows the highest value of $j_{\text{C2+}}$ and $\text{FE}_{\text{C2+}}$ under those conditions in each reference.

Sample	Electrolyte	$\text{FE}_{\text{C2+}}$ (%)	$j_{\text{C2+}}$ (A/cm ²)	Ref
CuONPs-1.7/GDE	1 M KOH	78	1.88	This work
3D CIBH	7 M KOH	78	1.21	S13
F-Cu	0.75 M KOH	80	1.28	S14
Cu-nr/CC3	1 M KOH	76	1.29	S15
N-Cu	1 M KOH	74	0.91	S16
Abrupt Cu interface	3.5 M KOH + 5 M KI	80	0.60	S11
CuAg-wire	1 M KOH	85	0.26	S17
CuS/Cu-V	1 M KOH	53	0.21	S18
CuO-FEP	1 M KOH	77	0.62	S19
Porous Cu	1 M KOH	62	0.40	S20
Cu(100)-rich film	Anion Exchange Membrane	70	0.34	S21
Cu/Fe-N-C s-GDE	0.5 M KOH	90	> 1	S22

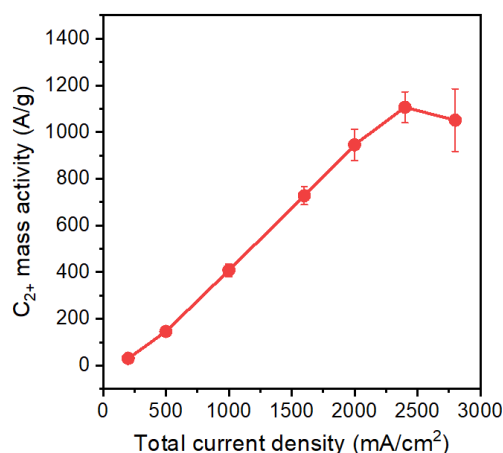


Figure S20 Mass activity for C₂₊ and H₂ production on CuONPs-1.7/GDE in 1 M KOH. Reaction time: 30 min.

Supplementary notes – calculation of TOF (CuONPs-1.7/GDE at $J_{\text{total}} = 2400 \text{ mA/cm}^2$ in 1 M KOH as an example)

1. Surface area of a CuNP with a diameter of 20.0 nm.

$$4 \times \pi \times (10.0 \times 10^{-9})^2 = 1.26 \times 10^{-15} \text{ m}^2$$

2. Area per copper atom on the surface of CuNPs (assuming the Cu(100) surface, lattice constant: $3.61 \times 10^{-10} \text{ m}$).

$$\frac{(3.61 \times 10^{-10})^2}{2} = 6.52 \times 10^{-20} \text{ m}^2$$

3. Number of Cu atoms on the surface of a CuNP.

$$\frac{1.26 \times 10^{-15}}{6.52 \times 10^{-20}} = 1.93 \times 10^4$$

4. Volume of a CuNP with a diameter of 20 nm.

$$\frac{4 \times \pi \times (10.0 \times 10^{-9})^3}{3} = 4.19 \times 10^{-24} \text{ m}^3$$

5. Mass of a CuNP with a diameter of 20 nm (assuming that the density is $8.96 \times 10^6 \text{ g m}^{-3}$).

$$4.19 \times 10^{-24} \times 8.96 \times 10^6 = 3.75 \times 10^{-17} \text{ g}$$

6. Number of CuNPs when the amount of catalyst loading is 1.7 mg/cm².

$$\frac{1.7 \times 10^{-3}}{3.75 \times 10^{-17}} = 4.53 \times 10^{13}$$

7. Number of Cu atoms when the amount of catalyst loading is 1.7 mg/cm².

$$1.93 \times 10^4 \times 4.53 \times 10^{13} = 8.74 \times 10^{17}$$

Elementary charge: 1.602×10^{-19}

$$\text{TOF}_{\text{C}_2\text{H}_4} = \frac{j_{\text{C}_2\text{H}_4}}{1.602 \times 10^{-19} \times 8.74 \times 10^{17} \times 12} = 0.72$$

$$\text{TOF}_{\text{C}_2\text{H}_5\text{OH}} = \frac{j_{\text{C}_2\text{H}_5\text{OH}}}{1.602 \times 10^{-19} \times 8.74 \times 10^{17} \times 12} = 0.34$$

$$\text{TOF}_{\text{C}_3\text{H}_7\text{OH}} = \frac{j_{\text{C}_3\text{H}_7\text{OH}}}{1.602 \times 10^{-19} \times 8.74 \times 10^{17} \times 12} = 0.03$$

$$\text{TOF}_{\text{CH}_3\text{COOH}} = \frac{j_{\text{CH}_3\text{COOH}}}{1.602 \times 10^{-19} \times 8.74 \times 10^{17} \times 8} = 0.03$$

$$\text{TOF}_{\text{C}_2+} = \text{TOF}_{\text{C}_2\text{H}_4} + \text{TOF}_{\text{C}_2\text{H}_5\text{OH}} + \text{TOF}_{\text{C}_3\text{H}_7\text{OH}} + \text{TOF}_{\text{CH}_3\text{COOH}} = 1.11 \text{ s}^{-1}$$

TOF_{C₂+} is 1.03 s⁻¹ in 1 M KCl on CuONPs-1.7/GDE.

The obtained TOF significantly exceeded the values that have been reported in most of the previous reports. In contrast, several reports exhibited comparable or better TOFs for Cu catalysts^{S5, S7, S13, S14}, suggesting that our catalysts are not special, but our electrode maximized the potential of Cu catalysts. It must be noted here that we cannot deny a transport limitation affects the TOF values, and thus, these values are just for reference purposes.

Supplementary notes – calculation of energy efficiency (CuONPs-1.7/GDE at $J_{\text{total}} = 2400$ mA/cm² in 1 M KCl and 1 M KOH)

$$EE_{\text{full}} = \frac{E_{\text{ox}} - E_{\text{red}}}{E_{\text{cell}}} \times FE$$

EE_{full} : full-cell energy efficiency

E_{ox} : thermodynamic potential for water oxidation, i.e. 1.23 V vs. RHE

E_{red} : thermodynamic potential for cathode reaction products

$E_{\text{red}} = 0$ V vs. RHE for H₂

$E_{\text{red}} = -0.10$ V vs. RHE for CO

$E_{\text{red}} = 0.17$ V vs. RHE for CH₄

$E_{\text{red}} = 0.08$ V vs. RHE for C₂H₄

$E_{\text{red}} = 0.09$ V vs. RHE for C₂H₅OH

$E_{\text{red}} = 0.10$ V vs. RHE for C₃H₇OH

$E_{\text{red}} = -0.12$ V vs. RHE for HCOOH

$E_{\text{red}} = 0.11$ V vs. RHE for CH₃COOH

$$EE_{\text{half}} = \frac{E_{\text{ox}} - E_{\text{red}}}{E_{\text{ox}} - E_{\text{W-R}}} \times FE$$

$E_{\text{W-R}}$: cathode potential (V. vs. RHE)

We also calculated an IR-compensated EE_{half} .

$$EE_{\text{half-IRcomp}} = \frac{E_{\text{ox}} - E_{\text{red}}}{E_{\text{ox}} - E_{\text{W-R-IRcomp}}} \times FE$$

Table S6 Summary of energy efficiency at $J_{\text{total}} = 2400$ mA/cm² in neutral and alkaline electrolytes, respectively.

	Neutral	Alkaline
EE_{full}	6.2 %	7.2 %
EE_{half}	10.5 %	16.7 %
$EE_{\text{half-IRcomp}}$	48.6 %	56.8 %

Although we really understand that energy efficiency is essential for social implementation, the present study focuses on knowing and elucidating the maximum potential of the CO₂RR electrodes in a half-reaction. Therefore, the gap between the anode and cathode is wide (5 cm), and the anode has not been optimized. Therefore, we are now tackling installing this electrode to membrane electrode assembly cells to achieve a high current density and high energy efficiency simultaneously.

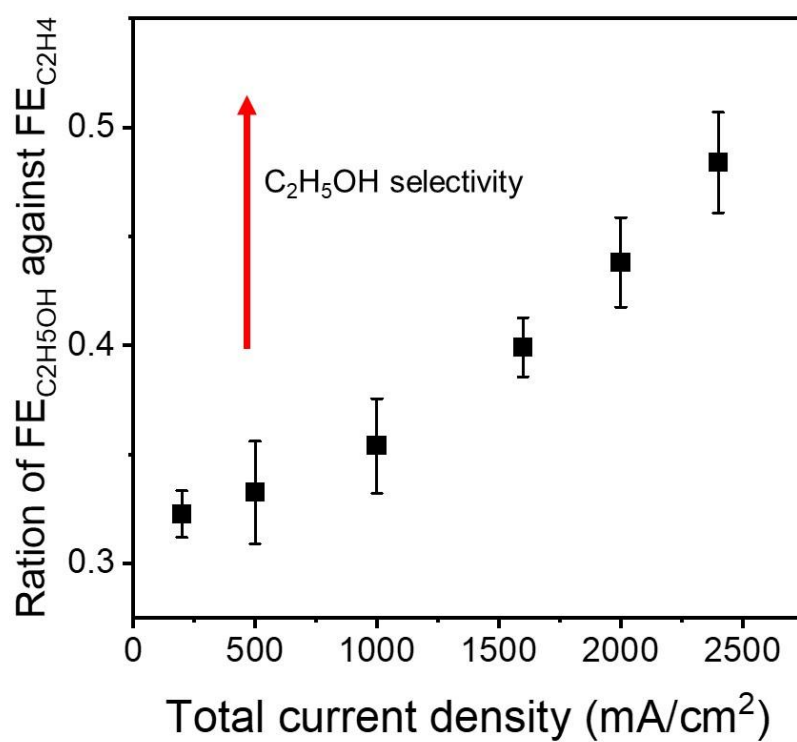


Figure S21 Ratio of $FE_{C_2H_5OH}$ and $FE_{C_2H_4}$ against current density over CuONPs-1.7/GDE in 1 M KCl.

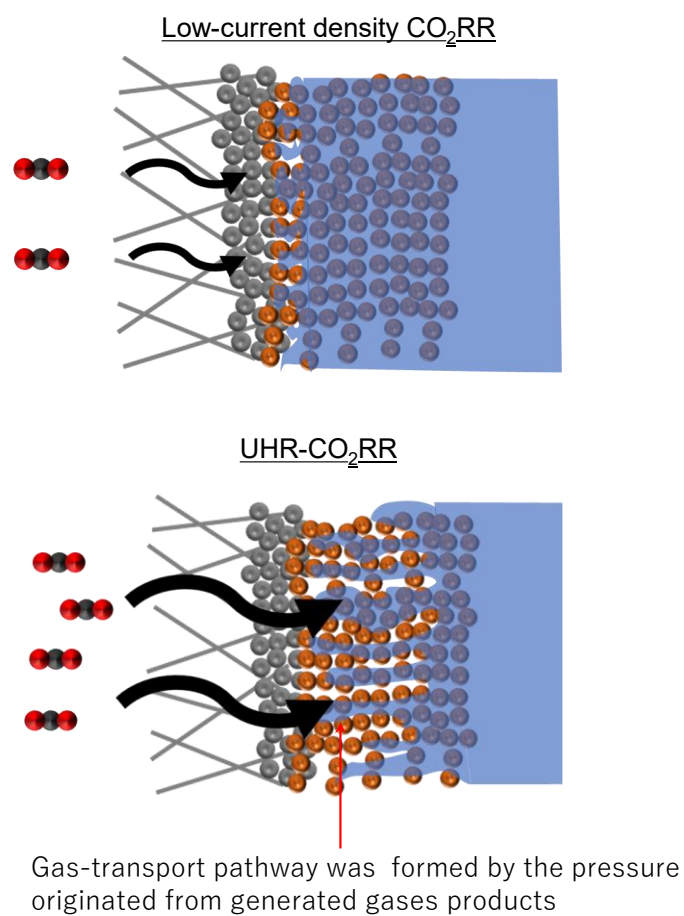


Figure S22 A schematic illustration of *in situ* formation of the gas-transport pathway.

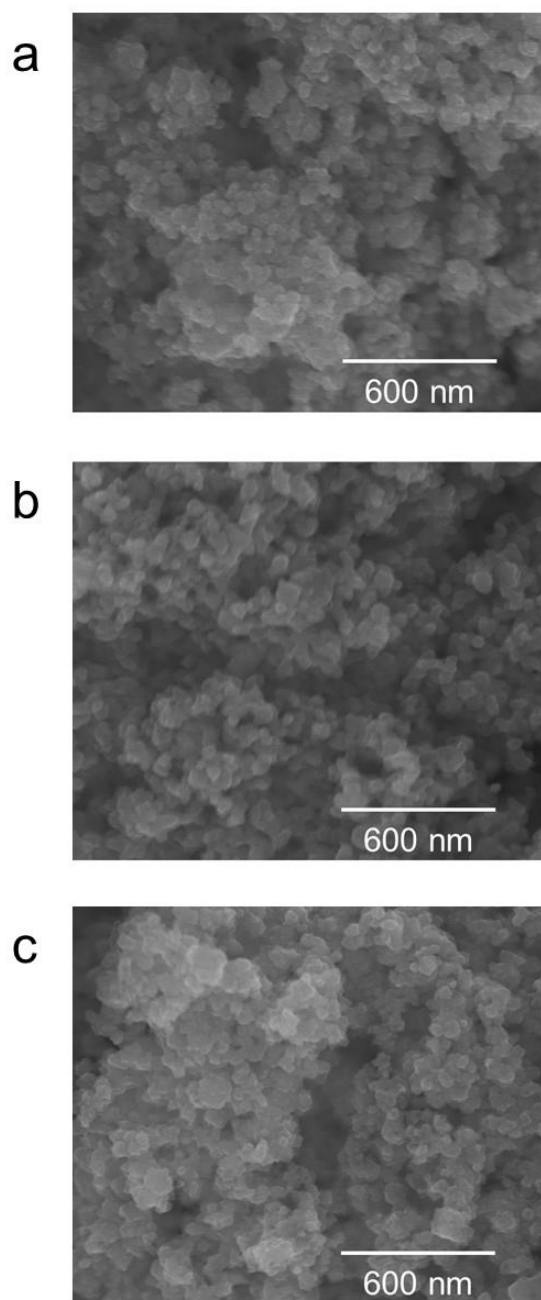


Figure S23 Top-view SEM images of CuONPs-1.7/GDE after application of $J_{\text{total}} =$ (a) 2400 mA/cm² in 1 M KCl, (b) 2800 mA/cm² in 1 M KCl, and (c) 2400 mA/cm² in 1 M KOH for 30 min.

The surface morphology did not significantly change during CO₂RR. These SEM images were acquired after rinsing the surface and drying under vacuum conditions.

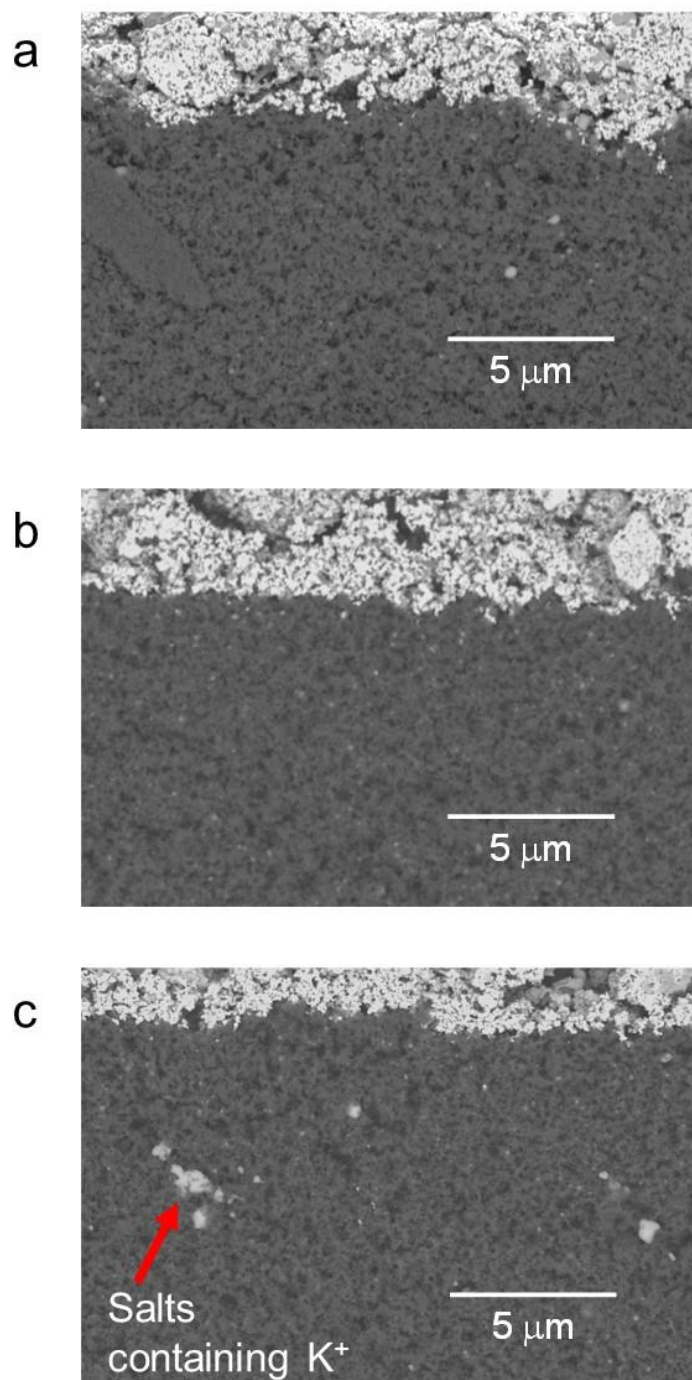
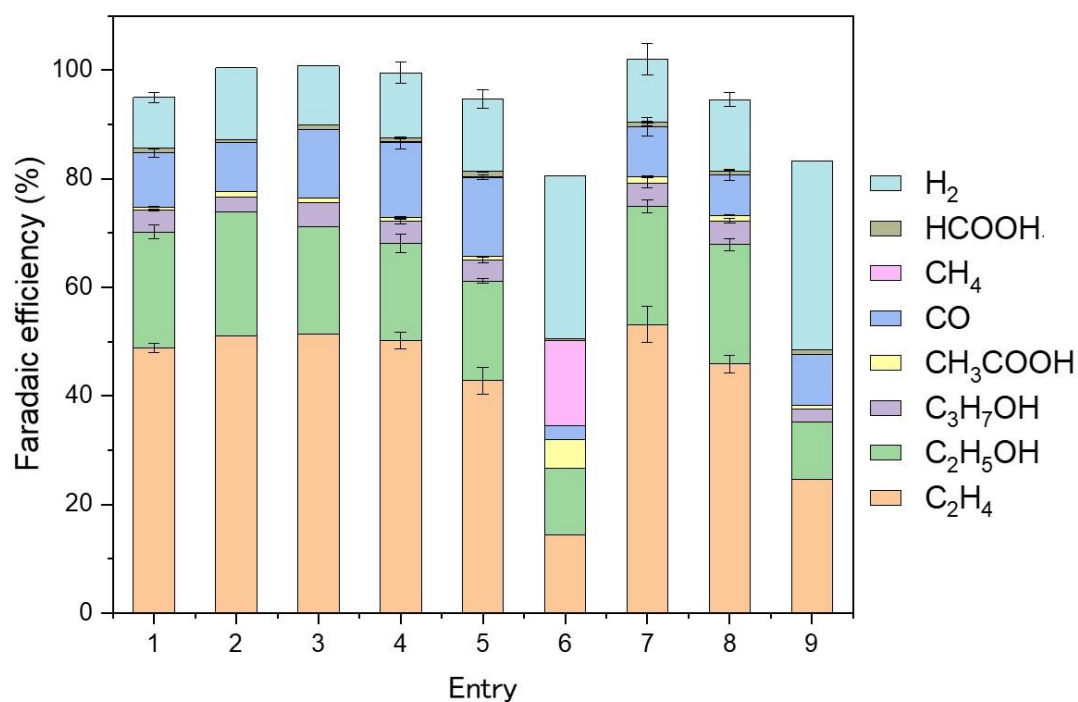


Figure S24 Accumulation of salts containing K^+ in the MPL of CuONPs-1.7/GDE after application of $J_{\text{total}} =$ (a) 1000 mA/cm^2 , (b) 2000 mA/cm^2 , and (c) 2800 mA/cm^2 for 30 min under CO_2RR conditions in 1 M KCl. These SEM images were acquired after freeze-drying the electrodes.



Entry	GDL	Catalyst	Electrolyte
1	34BC	CuONPs-1.7/GDE	1 M KCl
2	MFK-A	CuONPs-1.7/GDE	1 M KCl
3	GDS2130	CuONPs-1.7/GDE	1 M KCl
4	34BC	CuO 50 nm (sigma)-1.7/GDE	1 M KCl
5	34BC	CuONPs-1.7/GDE	1 M KHCO ₃
6	34BC	CuONPs-0.34/GDE	1 M KOH
7	34BC	CuONPs-1.7/GDE	1 M KOH
8	34BC	CuONPs-3.1/GDE	1 M KOH
9	34BC	CuONPs-10/GDE	1 M KOH

Figure S25 and Table S7 Faradaic efficiency of CO₂RR products under $J_{\text{total}} = 2000$ mA/cm² when changing GDEs, catalysts, the thickness of CL, and electrolytes.

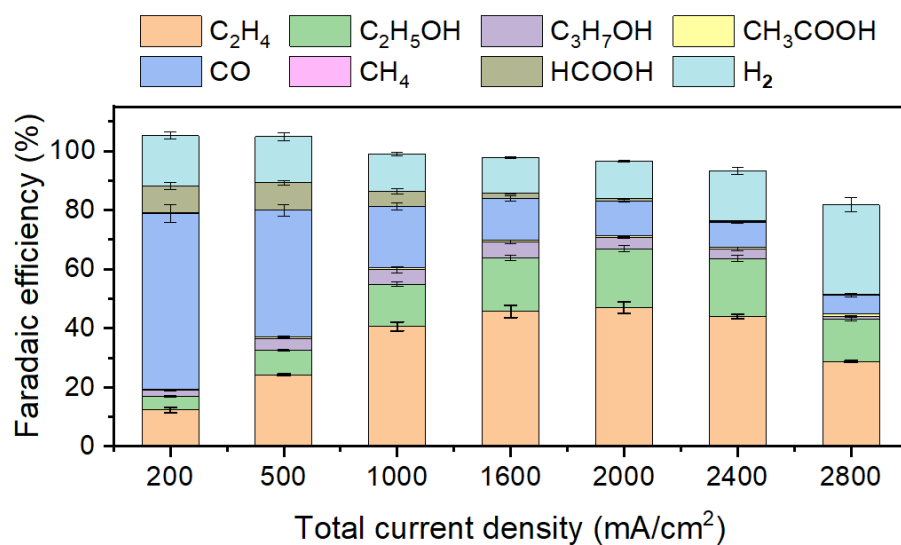


Figure S26 FE_s of the CO₂RR products under different applied potentials over CuONPs-3.1/GDE in 1 M KCl under constant current measurements. Reaction time: 30 min.

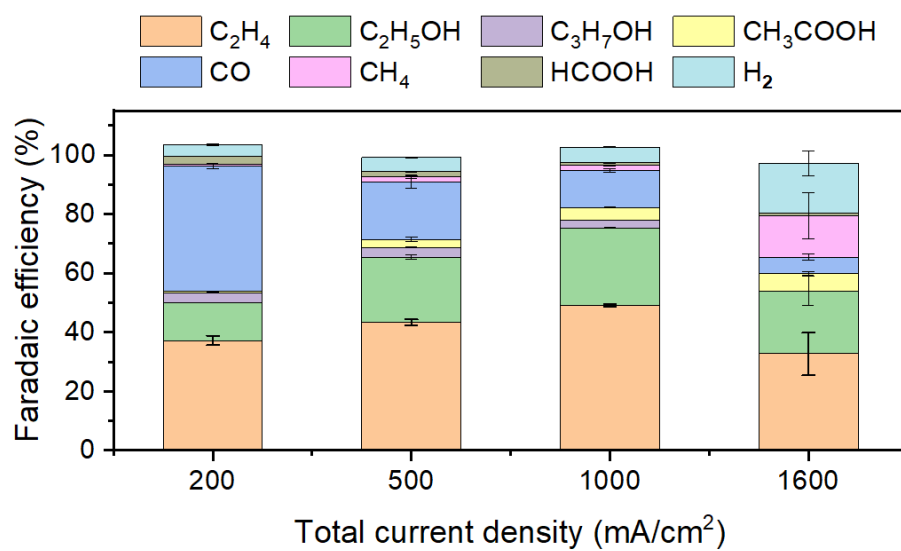


Figure S27 FEs of the CO₂RR products under different applied potentials over CuONPs-0.34/GDE in 1 M KCl under constant current measurements. Reaction time: 30 min.

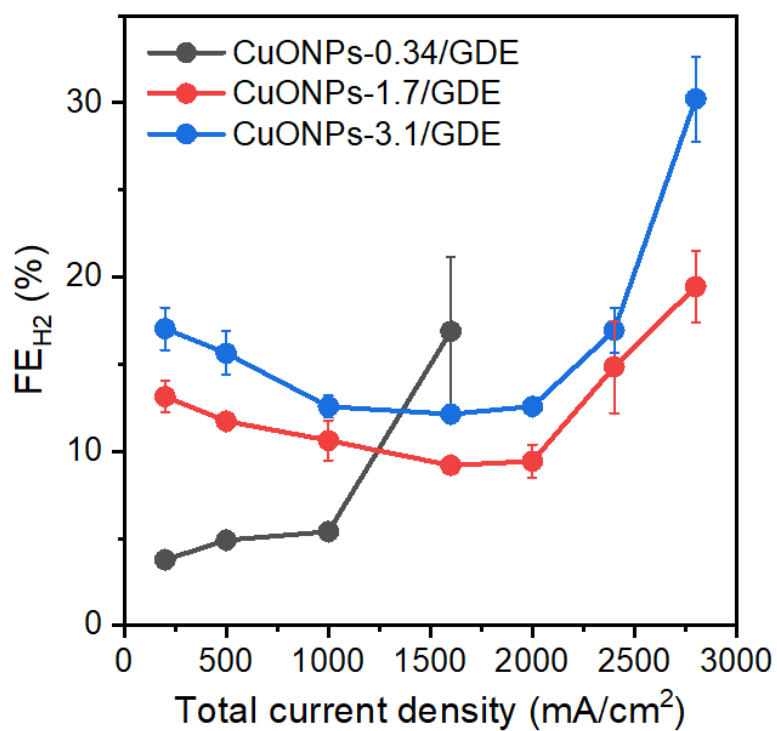


Figure S28 FE_{H_2} against J_{total} for various amounts of Cu loading (CuONPs-0.34, -1.7 and -3.1/GDE) in 1 M KCl. Reaction time: 30 min.

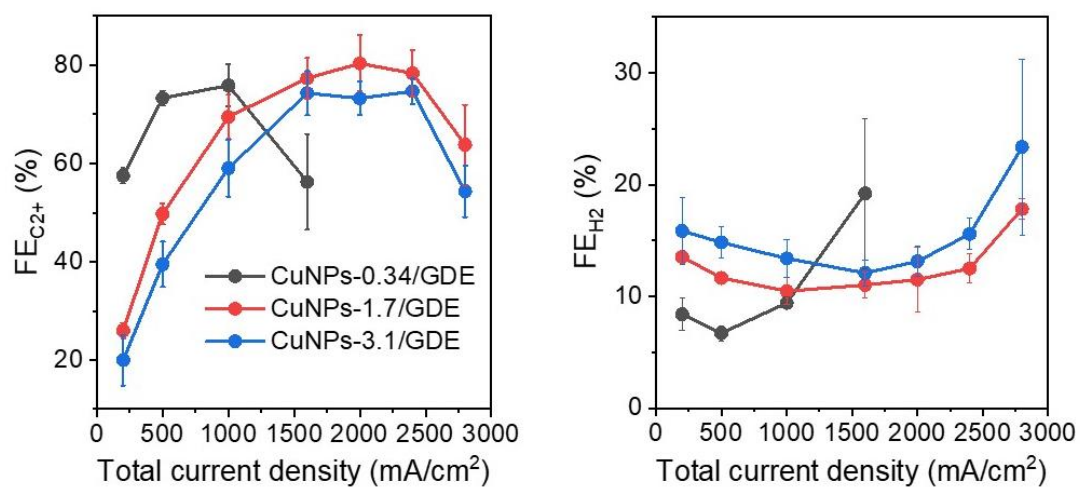


Figure S29 (a) $\text{FE}_{\text{C}_2\text{H}_4}$ and (b) FE_{H_2} against J_{total} for various amounts of Cu loading (CuONPs-0.34, -1.7 and -3.1/GDE) in 1 M KOH. Reaction time: 30 min.

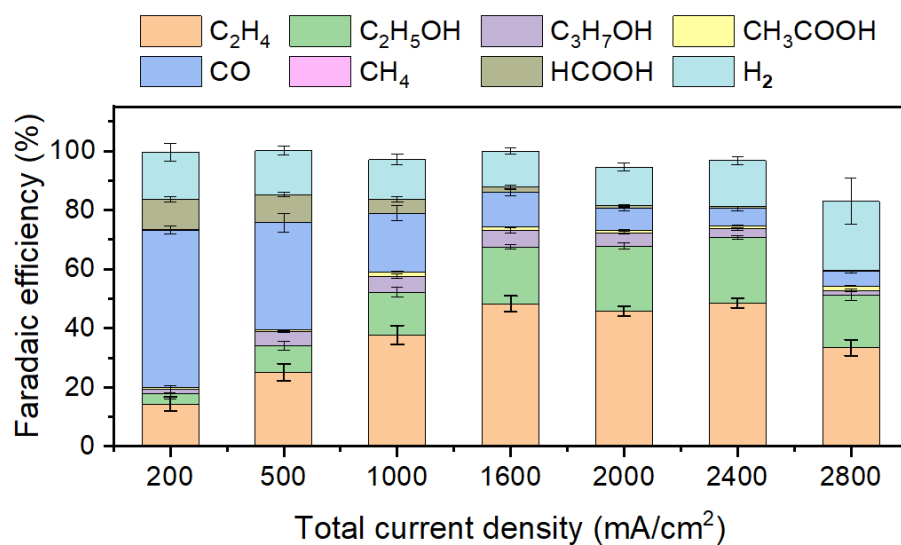


Figure S30 FE_s of the CO₂RR products under different applied potentials over CuONPs-3.1/GDE in 1 M KOH under constant current measurements. Reaction time: 30 min.

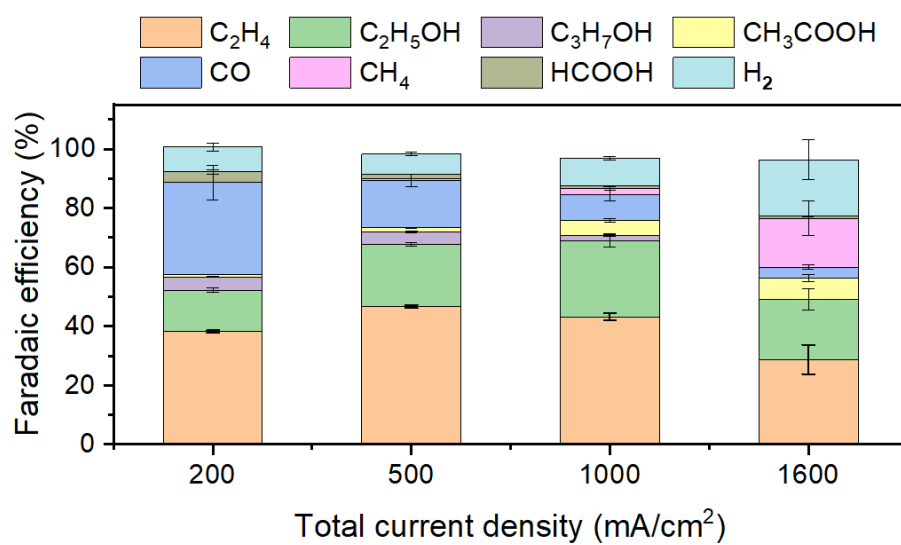


Figure S31 FE_s of the CO₂RR products under different applied potentials over CuONPs-0.34/GDE in 1 M KOH under constant current measurements. Reaction time: 30 min.

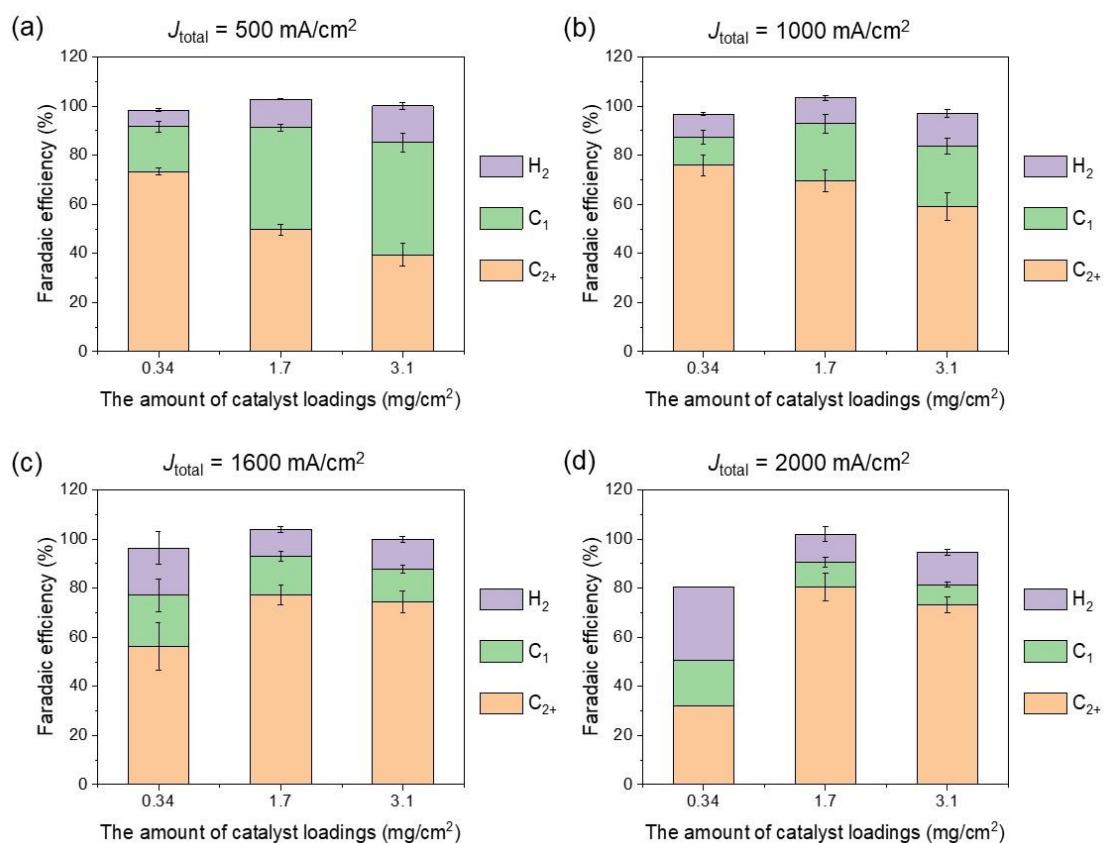


Figure S32 $FE_{C_{2+}}$, FE_{C_1} , and FE_{H_2} depending on the amount of catalyst loadings at J_{total} = (a) 500 mA/cm², (b) 1000 mA/cm², (c) 1600 mA/cm² and (d) 2000 mA/cm² in 1 M KOH. Reaction time: 30min.

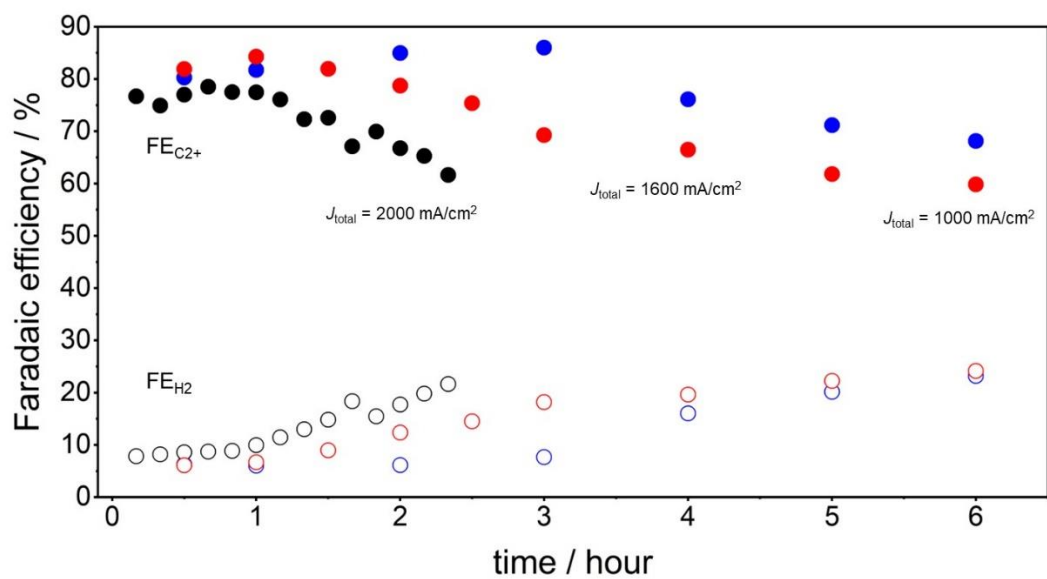


Figure S33 Stability tests with respect to the total current density. The filled and blank points show FE_{C2+} and FE_{H2} , respectively, over CuONPs-1.0/GDE in 1 M KCl under $J_{total} = 2000$ mA/cm² (black), 1600 mA/cm² (red) and 1000 mA/cm² (blue).

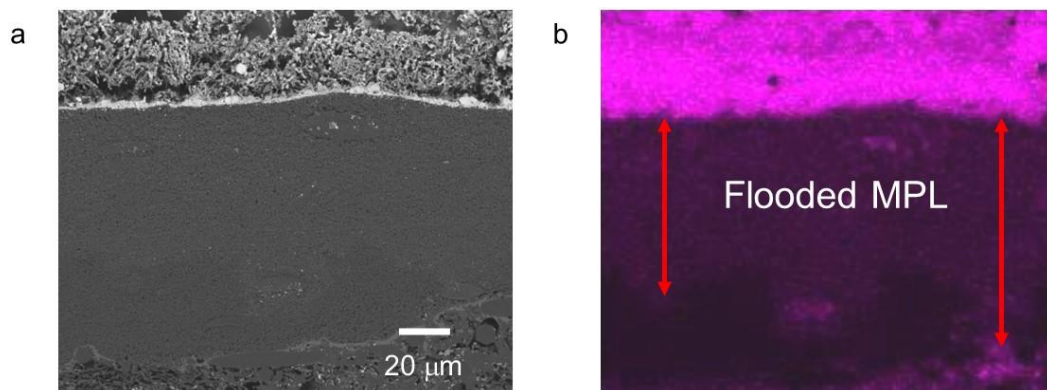


Figure S34 (a) A cross-sectional SEM image of CuONPs-1.0/GDE and (b) K⁺ distribution (purple) obtained by EDX after application of $J_{\text{total}} = 1600 \text{ mA/cm}^2$ for 6 h under CO₂RR conditions in 1 M KCl.

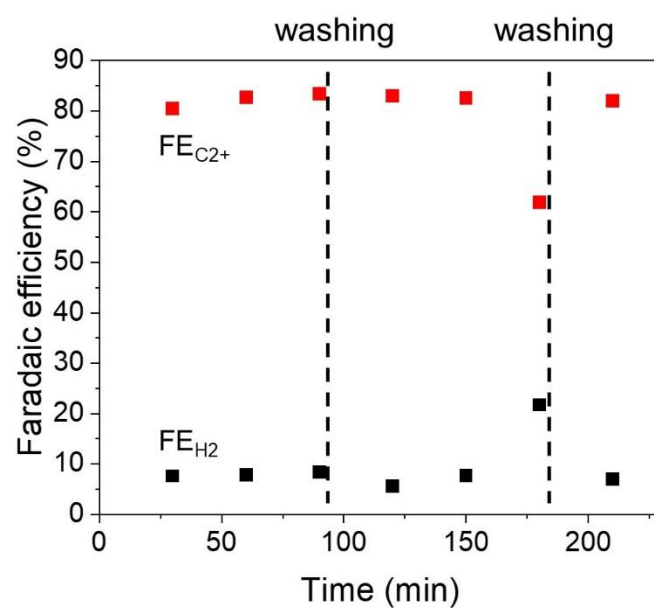


Figure S35 Recycling test on CuONPs-1.0/GDE in 1 M KCl under $J_{\text{total}} = 1600$ mA/cm². FE_{C2+} value was recovered by washing the electrode with pure water indicating that the decrease in FE_{C2+} after prolonged operation was due to the salt precipitation induced by flooded MPL.

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