

**Electric potential-determined redox intermediates for effective
recycling of spent lithium-ion batteries**

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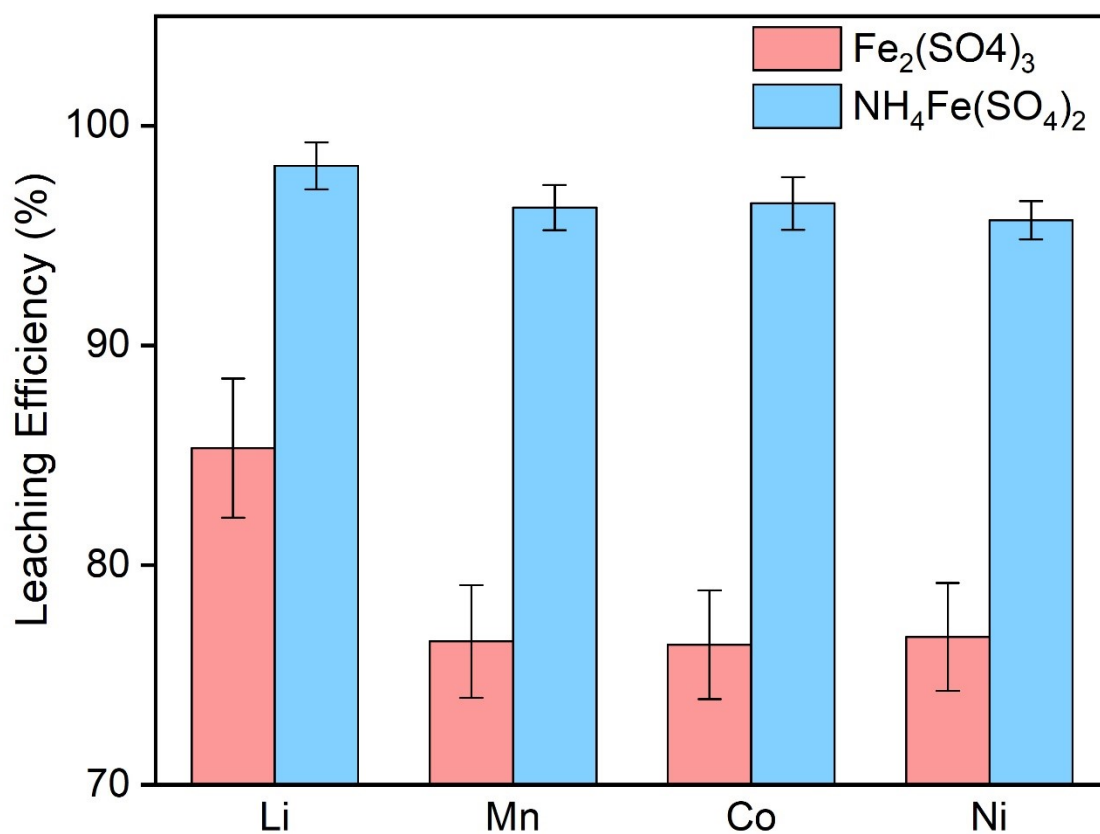


Fig. S1 Behaviors of synergistic metal leaching from NCM622 and LFP cathode by $\text{Fe}_2(\text{SO}_4)_3$ and $\text{NH}_4\text{Fe}(\text{SO}_4)_2$ (LFP/NCM622=1.8; $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$ /mixed cathode powder = 3:1, or $\text{Fe}_2(\text{SO}_4)_3$ /mixed powder=1.1:1 (all in g/g) at 50°C for 30 min)

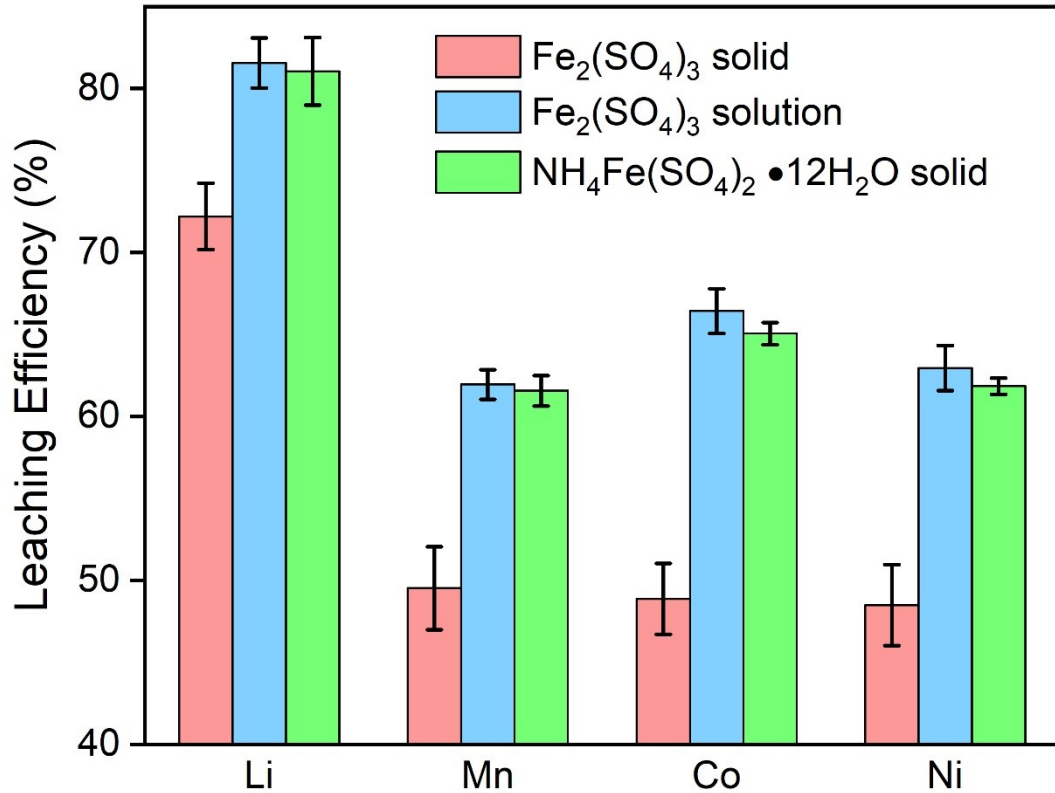


Fig. S2 Comparison of leaching efficiency by adding water with Fe₂(SO₄)₃ as solid powder and by preparing Fe₂(SO₄)₃ aqueous solution in advance, NH₄Fe(SO₄)₂·12H₂O also added for comparison (LFP/NCM622=1.8, Fe₂(SO₄)₃/mixed powder=1.2:1, NH₄Fe(SO₄)₂·12H₂O/mixed cathode powder = 3:1 (all in g/g) at 50°C for 10 min)

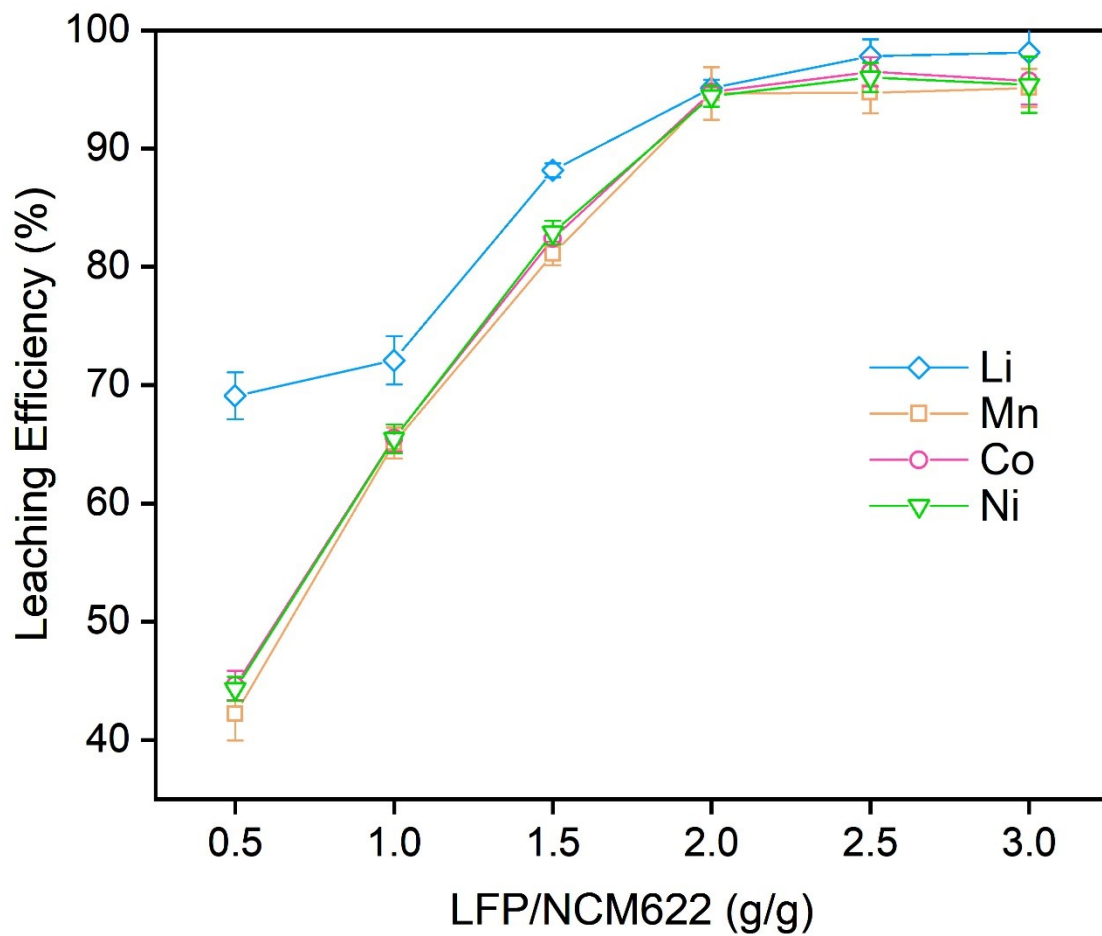


Fig. S3 Leaching efficiencies of metals under different LFP/NCM622 mass ratios

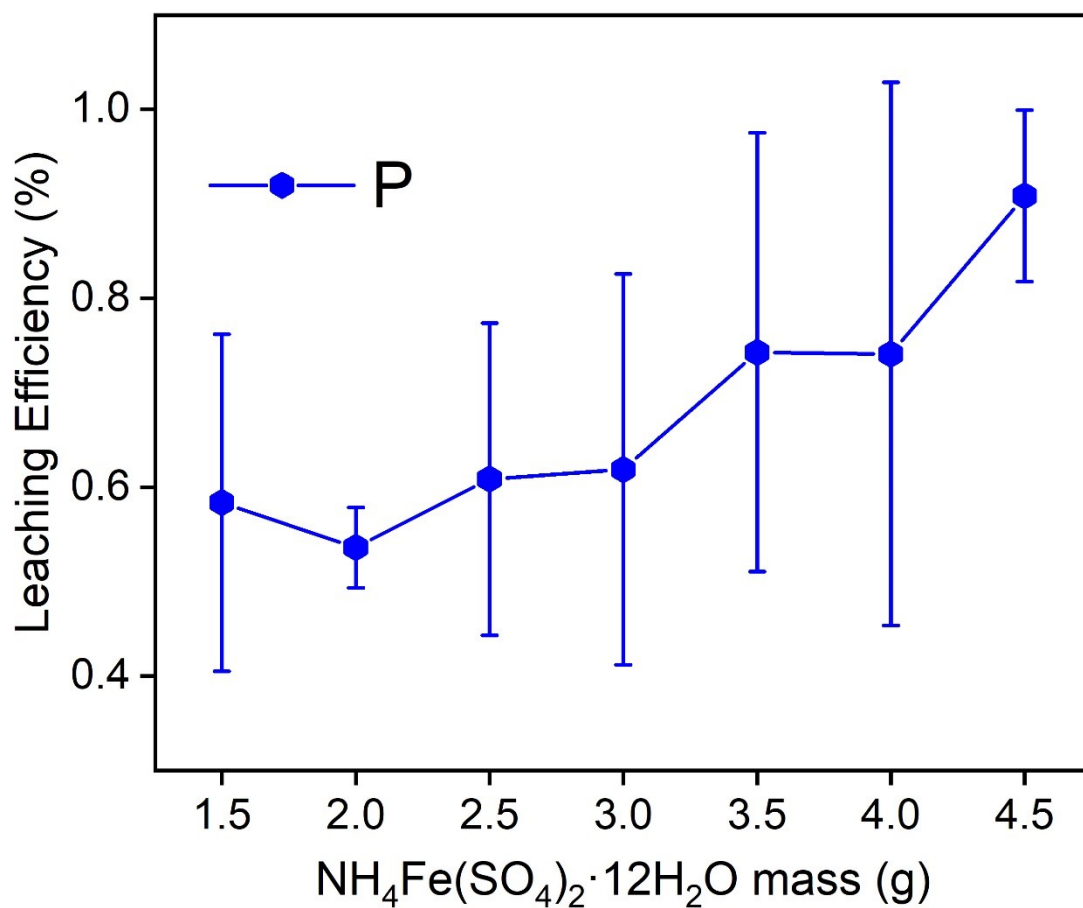


Fig. S4 Leaching efficiencies of phosphate with different added amount of $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$. The phosphate was hardly extracted at all time.

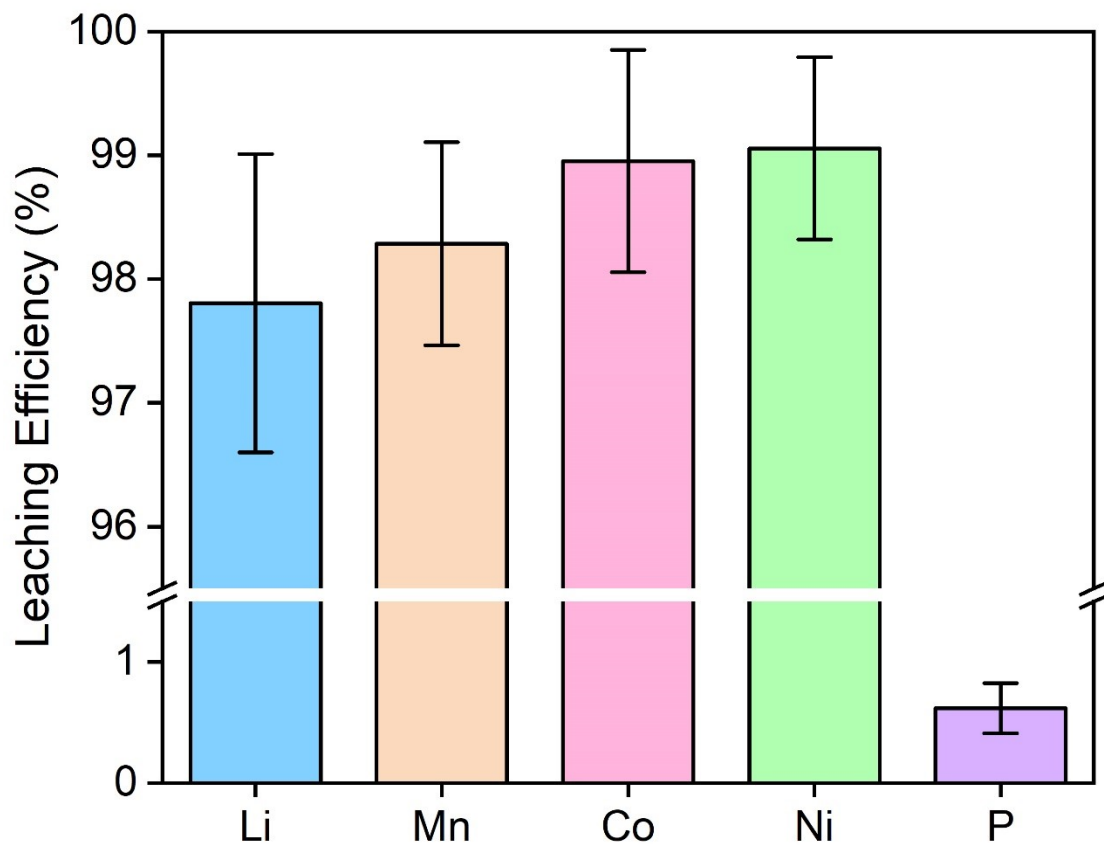


Fig. S5, Leaching efficiencies of Li, Mn, Co, Ni and P under optimized condition (LFP/NCM622=1.8 (g/g), $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$ /mixed cathode powder =3:1 (g/g), 50g/L, 50°C, 30min).

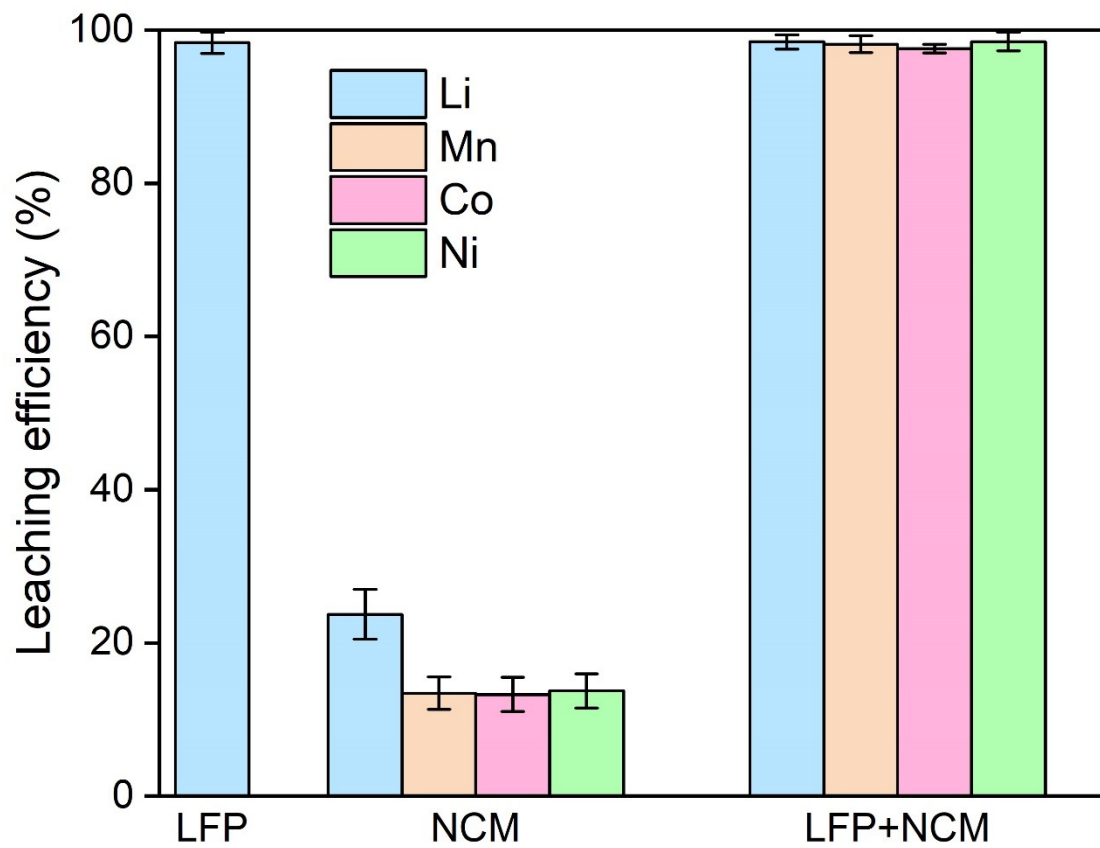


Fig. S6 Comparison of leaching effects using $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$ + LFP alone, $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$ + NCM alone, and $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$ + mixed powder.

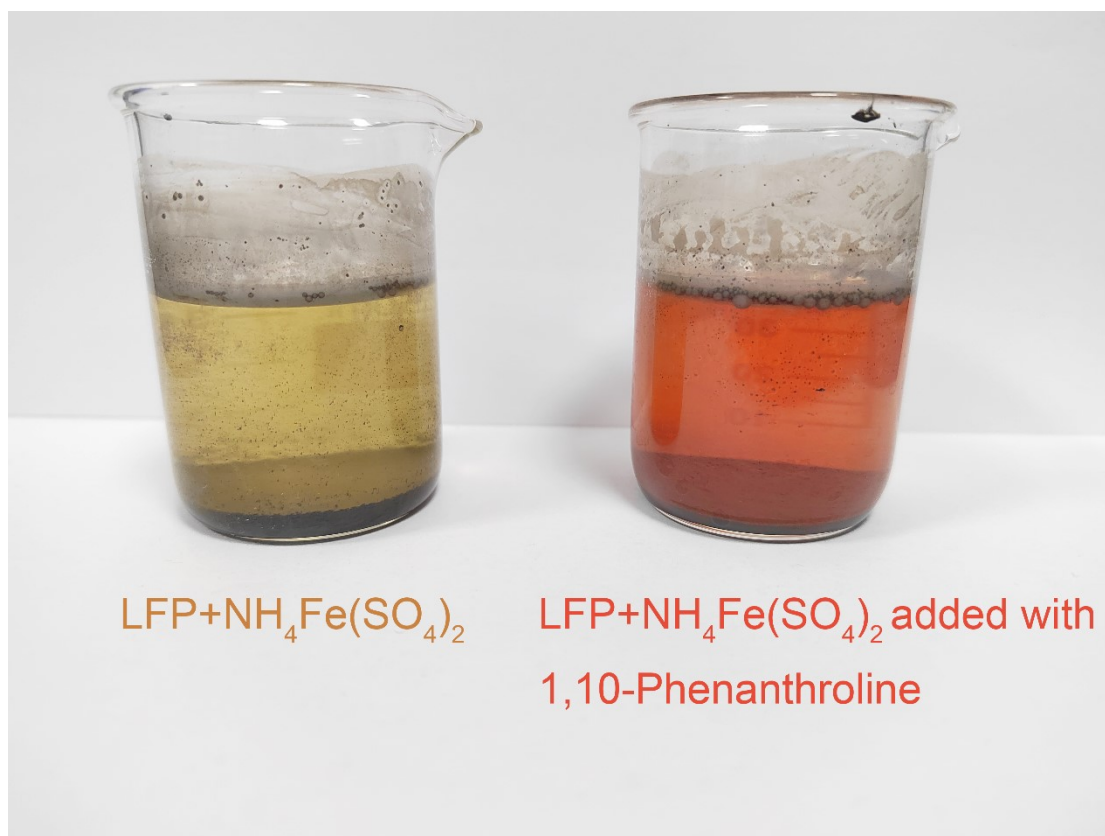


Fig. S7 Solution after reaction between LFP and $\text{NH}_4\text{Fe}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$.
1,10-Phenanthroline is added and the red color verifies the generation of Fe^{2+} .

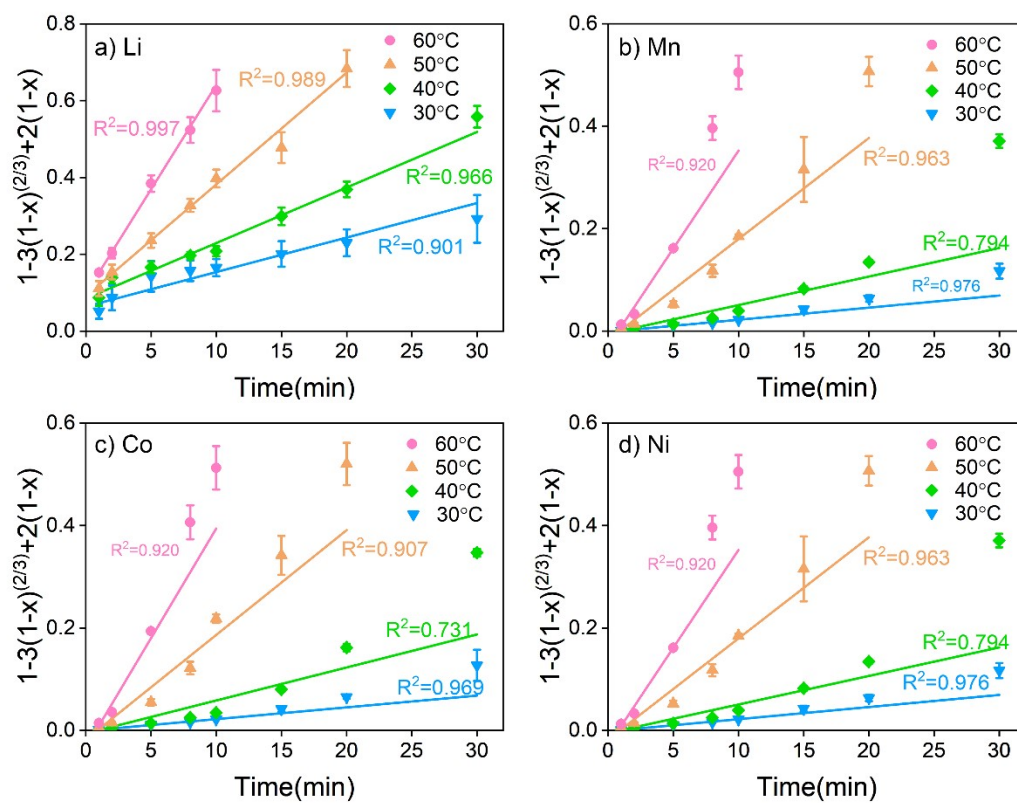


Fig. S8 Fitting results of a) Li, b) Mn, c) Co and d) Ni according to surface diffusion model.

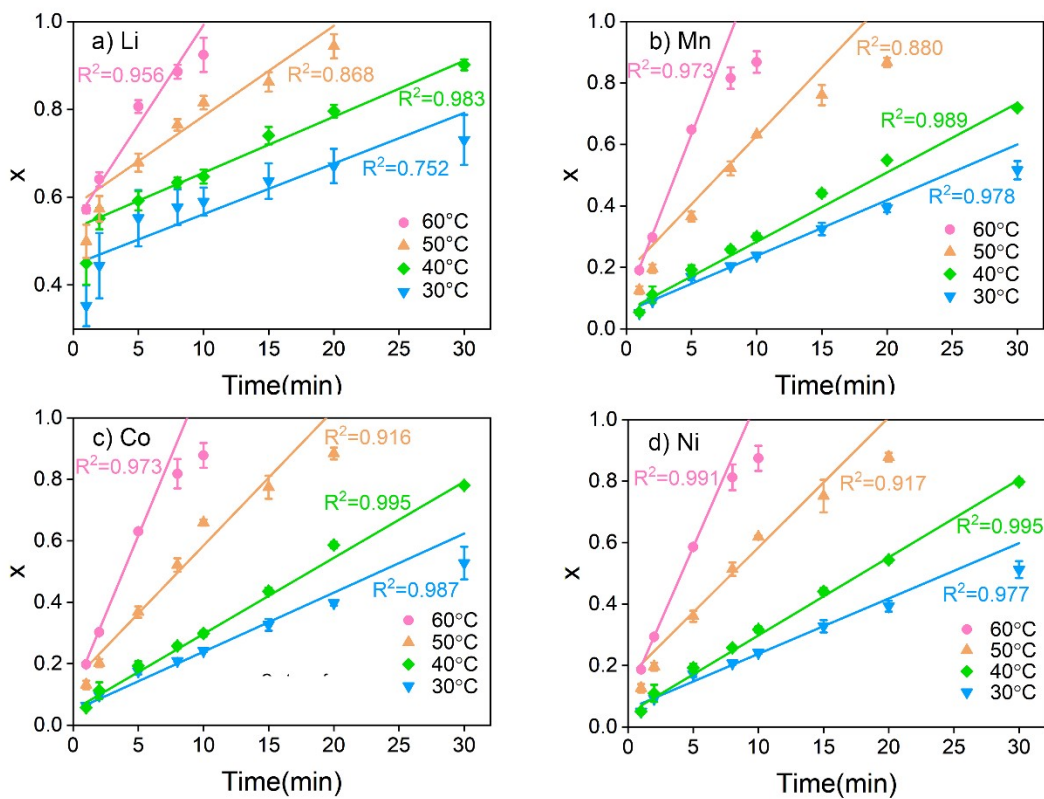


Fig. S9 Fitting results of a) Li, b) Mn, c) Co and d) Ni according to mass transfer model.

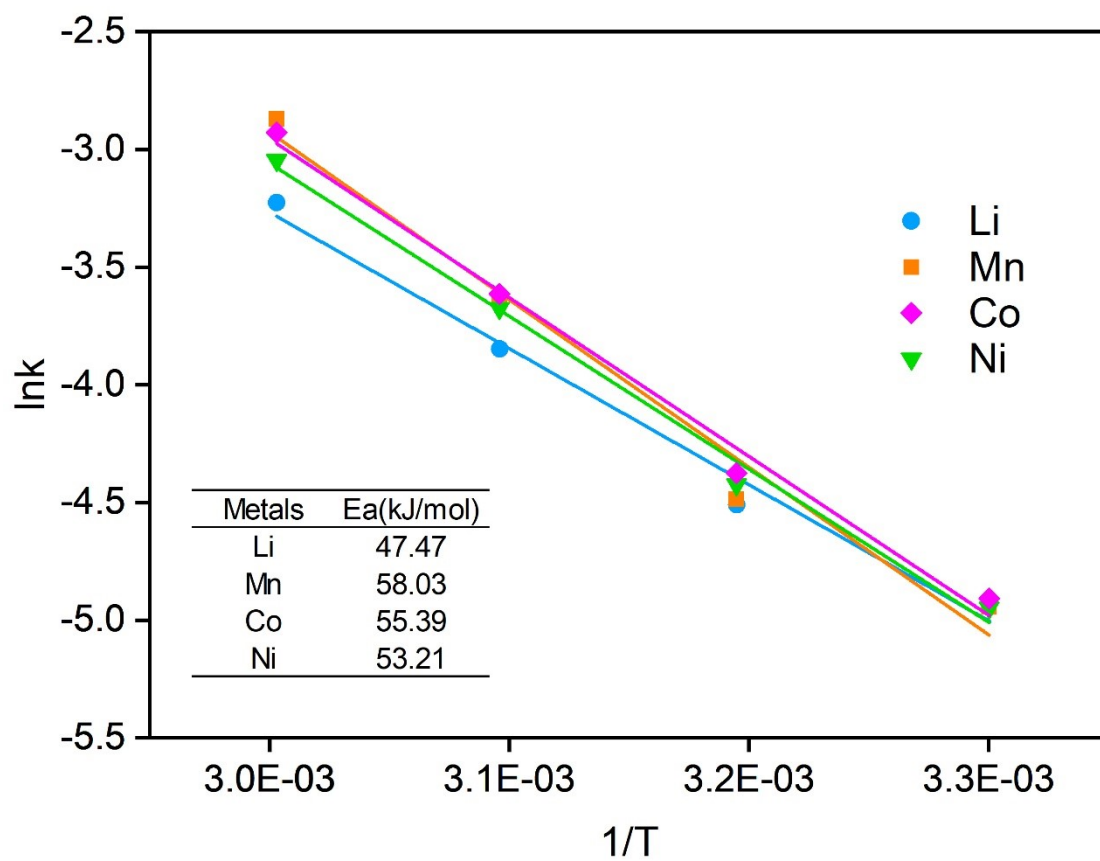


Fig. S10 Activation energy calculation of Li, Mn, Co and Ni according to Arrhenius equation in the range of 30-60°C

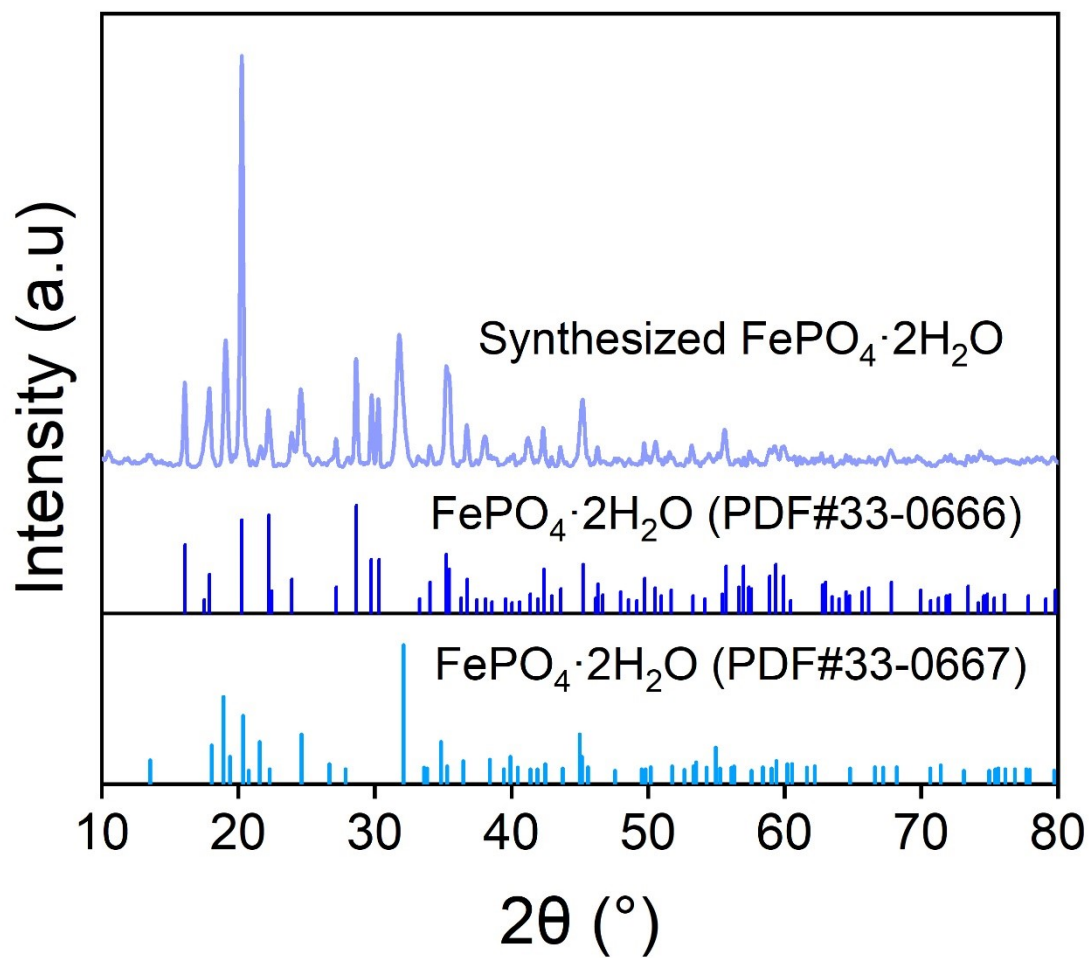


Fig. S11 XRD pattern of recovered FePO₄·2H₂O after washing the residue with H₃PO₄+NH₄H₂PO₄ at PH=2-2.5

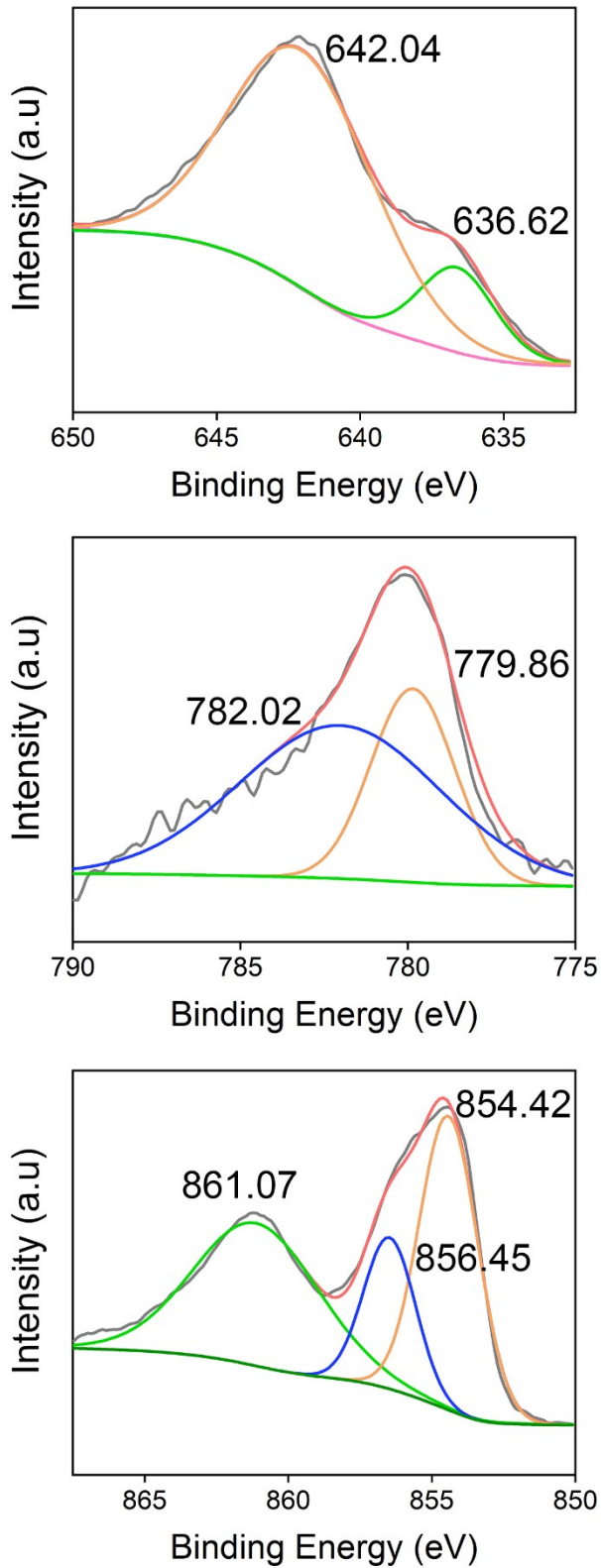


Fig. S12 XPS analysis of recovered MnCoNi oxide after 900°C calcination