

Electronic Supplementary Information

Mobilization of platinum and palladium from exhausted catalytic converters using bio-cyanide and ionic-liquid as mass transport carriers†

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Table S1. Literature summary of PGMs' extraction using ionic liquids at different conditions and salient features.

Ionic liquid	Optimal Concentration	Important remarks	References
Polymerized supported IL	IL 20% yielded 86% Pt and 96% Pd recovery of purity 99%.	PSILP material demonstrated excellent separation of PGMs from major accompanying interferences in a single separation step.	[1]
Aliquat-336	3 mg/L Aliquat-336 yielded >99% extraction efficiency of PGMs, selective stripping of Pd in 1.0 mol.L ⁻¹ NaOH and Pt in 1.0 mol.L ⁻¹ thiourea was achieved.	The authors obtained a good selectivity over Au(III) over Pt and Pd in the extraction stage.	[2]
[Tf ₂ N] ⁻ IL	100% as such solvent used disulfide, alkenyl, and nitrile group attached ionic liquid exhibited high Pd-extraction.	Cation ring structure showed a large influence on the extraction process.	[3]
Cyphos IL 104	Without dilution used IL yielded selective Ru(III) with 70% efficacy, leaving all Rh(III) into raffinate.	Stripping was performed using 0.1 mol.L ⁻¹ thiourea in 0.5 mol.L ⁻¹ HCl.	[4, 5]
Cyphos IL 101	0.6 g/L IL 101 used that yielded >99% Pt-Pd extraction over Rh. Co-extracted Pt and Pd was separated by sequential stripping with NaSCN and CH ₄ N ₂ S.	Stoichiometry requirement of ionic liquid changes from 1 to 3 times with differing acid concentration from 0.1–4.0 mol.L ⁻¹ ; however, Pt did not show any effect of acid concentration.	[5, 6]

Table S2. Summary of the test procedures adopted for toxicity assessment.

Item description	TCLP	SPLP	TTLC
Leaching agents	C ₂ H ₄ O ₂ , H ₂ O	H ₂ SO ₄ , H ₂ O	HNO ₃ , HCl, H ₂ O ₂ , H ₂ O
Sample amount	100 g	100 g	1.0 g
Volume	2 L	2 L	100 mL
Duration	18 h	18 h	48 h
Analyte	Heavy metals	Heavy metals	Heavy metals
Instrument used	ICP-MS	ICP-MS	ICP-MS

Table S3. The conditions used for determining the energy consumption for milling of exhausted catalytic converters to size reduction up to 150 μm .

Milling type	Equation applied for power consumption	Conditions
Gyratory milling	$\{W_i \times Q [\sqrt{f_{80}} - \sqrt{P_{80}}] \times \sqrt{(100/P_{80})}\} / \sqrt{f_{80}}$ (in kW) where	Where, W_i is work index = 15 kWh.t^{-1} ; Q is capacity = 1 t.h^{-1} ; f_{80} is the size through which 80% of the mineral feed passes = 50 mm; P_{80} is the size through which 80% of the product passes = 5 mm
Ball milling	$W = W_i \times ((10/\sqrt{P}) - 10/\sqrt{F})$ $W_i = 1.1 \times 44.5 / (P_k^{0.23} G^{0.82} ((10/\sqrt{P}) - 10/\sqrt{F}))$	Where, W is the energy consumption for grinding (in kWh.t^{-1}); W_i is work index (in kWh.t^{-1}); P is the screen aperture through which 80% of the material passes before grinding (in μm); F is the screen aperture size through which 80% of the material passes before grinding (in μm) Where, W_i is work index (in kWh.t^{-1}); P is the screen aperture through which 80% of the material passes before grinding (in μm); F is the screen aperture size through which 80% of the material passes before grinding (in μm); P_k is the aperture size of test screen used for determination of the work index (in μm); G is the newly formed mass passing a test screen each mill revolution (in g).

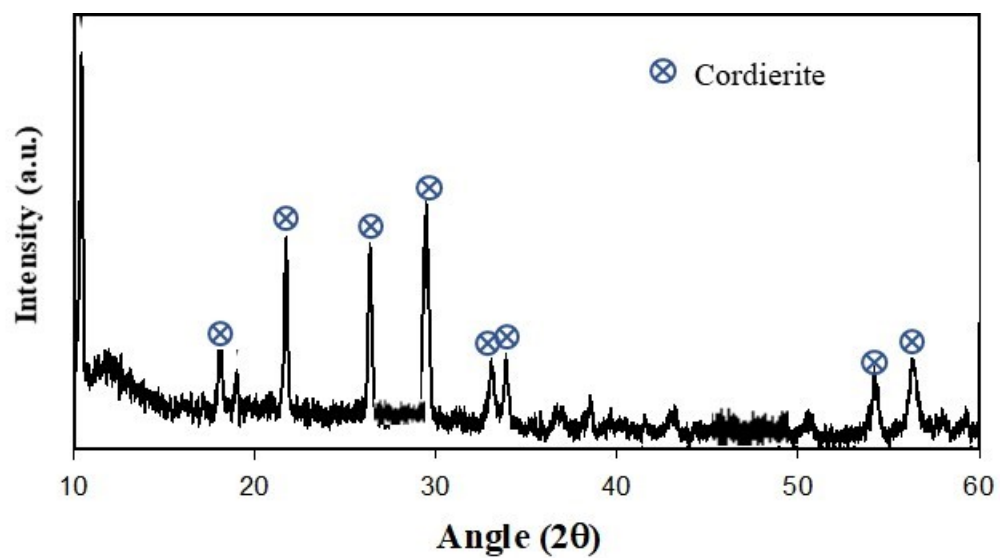


Fig. S1. XRD pattern of exhausted catalytic converters.

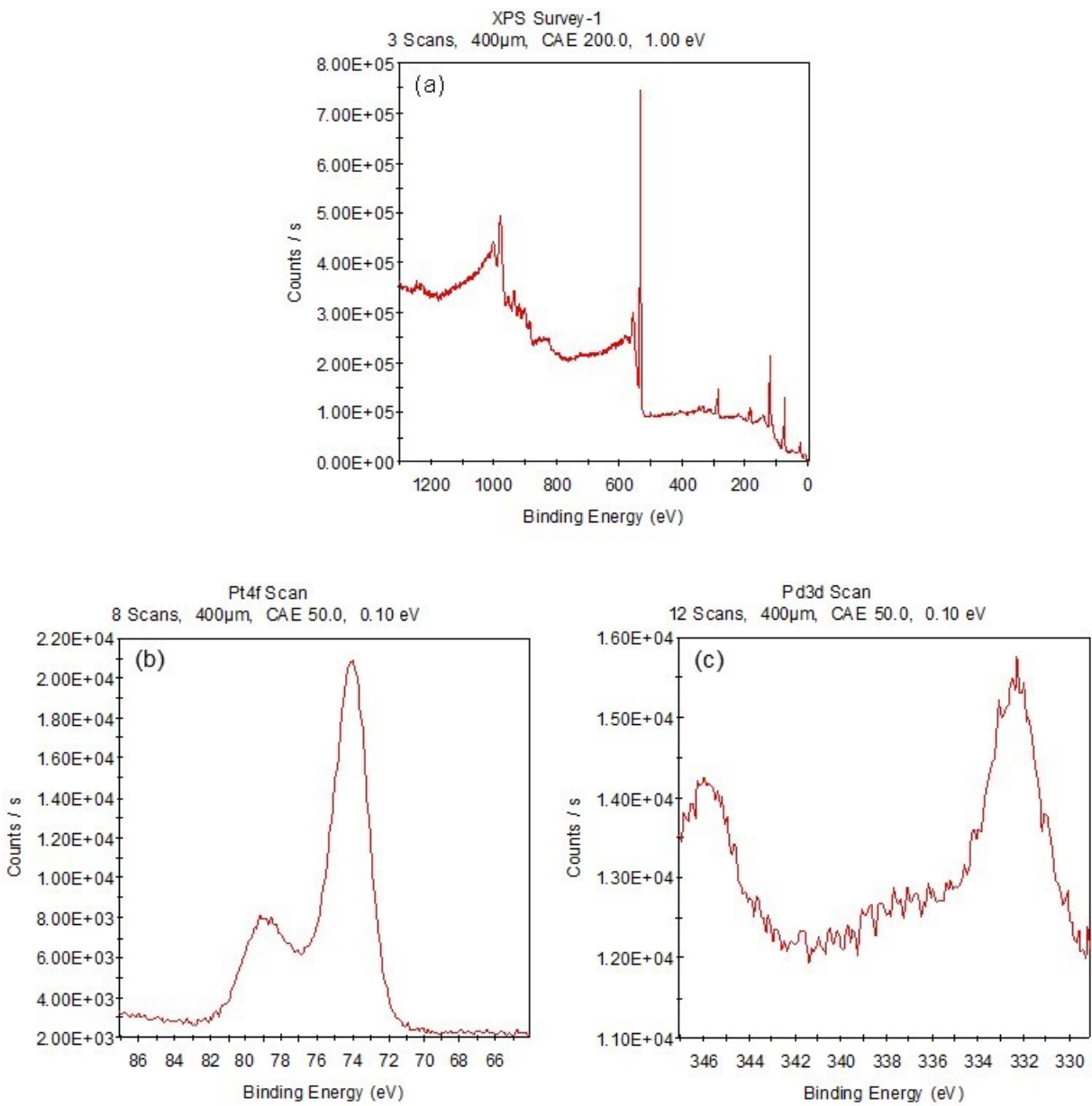


Fig. S2. XPS analysis of the sample for full scan **(a)**, Pt **(b)**, and Pd **(c)** scan.

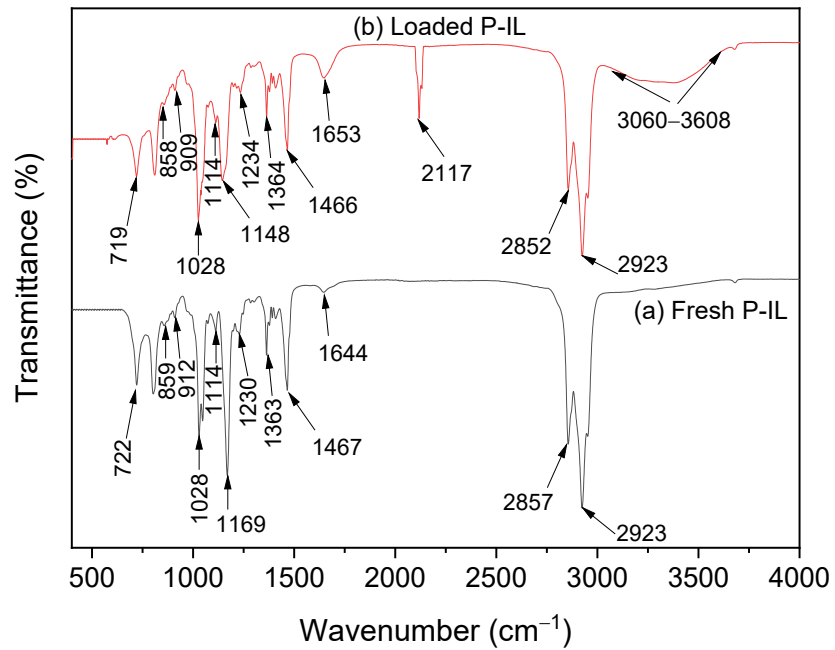


Fig. S3. FTIR spectrum of fresh ionic-liquid Cyphos IL101 **(a)** and (Pt,Pd)-loaded ionic-liquid phase **(b)**.

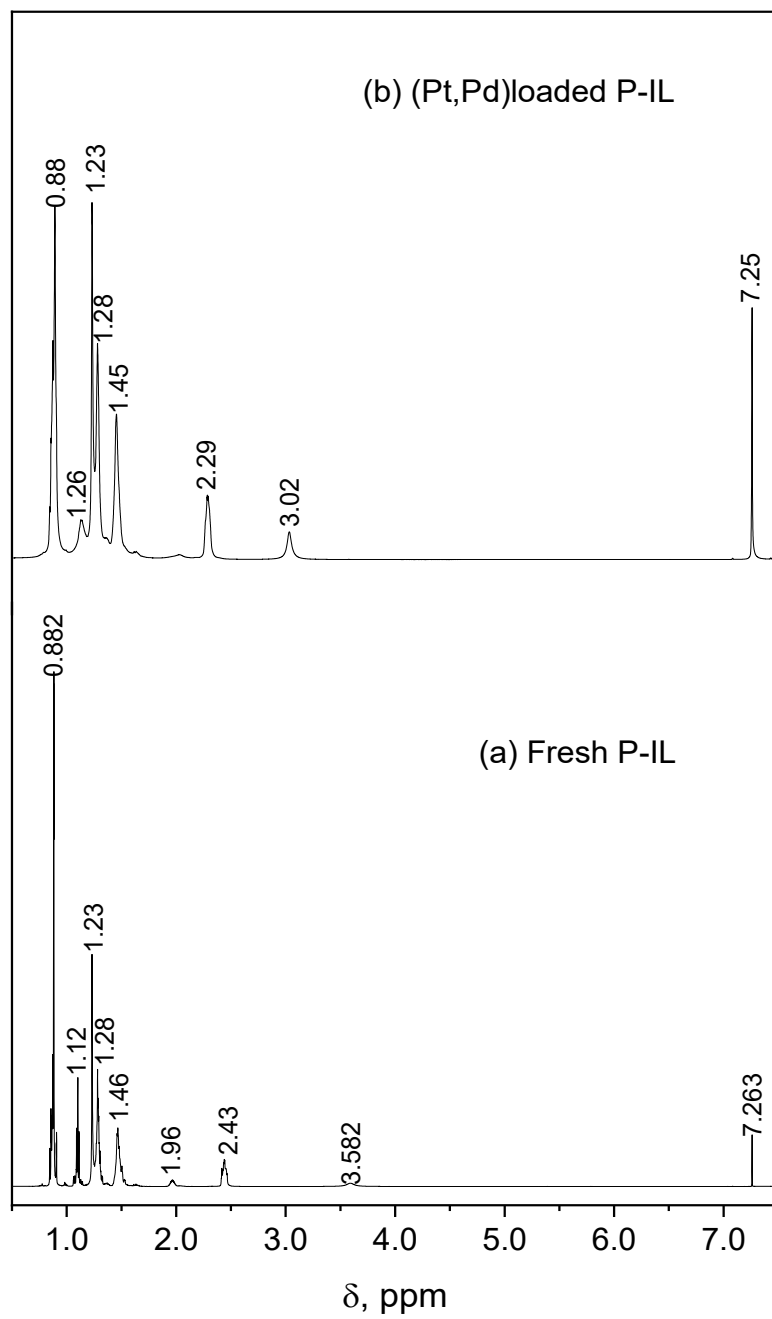


Fig. S4. ¹H-NMR of fresh **(a)** and (Pt,Pd)-loaded **(b)** ionic liquid phase.

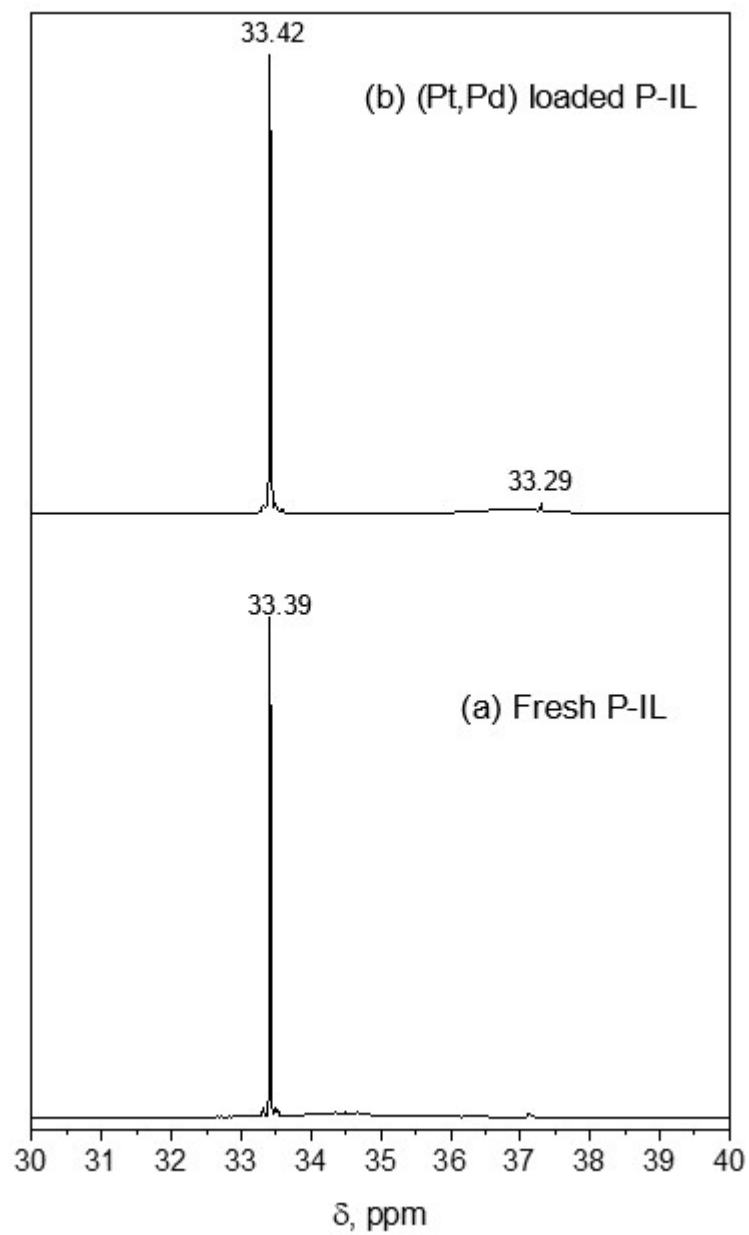


Fig. S5. ^{31}P NMR of fresh (a) and (Pt,Pd)-loaded (b) ionic liquid phase.

References

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