

Novel Methane Activation by Sulfur Dioxide and Molecular Oxygen via Trifluoroacetylsulfuric Acid

Supporting Information

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1. Experimental Results

1.1. Table S1. Methane sulfonation by using SO₂ and O₂.^a

Entry	Temperature (°C)	H ₂ O ₂ (mol %)	MSA (yield %) ^b	Conv. (% CH ₄)
1	50	15	67.6	15.0
2	50	20	74.3	16.5
3	60	15	73.1	12.9
4	60	20	75.2	18.5

Methane sulfonation was successfully conducted with SO₂ and O₂ resulting in high yields around 75 % at low temperatures. ^aReaction conditions: solvent, TFAOH (0.3 mL) and TFAA (0.3 mL); H₂O₂ (15–20 mol% based on SO₂, 0.11–0.15 mmol); SO₂ (40 psi, 0.73 mmol); O₂ (30 psi, 0.12 mmol); CH₄ (200 psi, 3–3.3 mmol); time (18 h). ^bThe percent yield of MSA was calculated based on SO₂.

1.2. Table S2. Time study.^a

Entry	Time (h)	MSA (yield %) ^b	Conv. (% CH ₄)
1	2	36.6	17.0
2	4	37.9	17.7
3	6	38.7	18.0
4	8	40.0	18.6
5	18	40.1	18.7

Time study was conducted for the methane sulfonation. ^aReaction conditions: Solvent, TFAA (0.6 mL); H₂O₂ (21 mol% based on SO₂, 0.27 mmol); SO₂ (80 psi, 1.3 mmol); O₂ (50 psi, 0.2 mmol); CH₄ (200 psi, 2.8 mmol); temperature (50 °C). ^bThe percent yield of MSA was calculated based on SO₂.

1.3. Table S3. Optimal ratio between sulfur dioxide and molecular oxygen during methane sulfonation conducted with 0.27 mmol trifluoroacetic acid.^a

Entry	1	2	3
	0.73 mmol SO₂	1.3 mmol SO₂	1.9 mmol SO₂
No O₂	9.7 %	5.6 %	3.4 %
20 psi O₂ (0.07 mmol)	38 %	19 %	11 %
30 psi O₂ (0.12 mmol)	54%	27 %	18 %
50 psi O₂ (0.20 mmol)	64 %	40 %	26 %
80 psi O₂ (0.36 mmol)	31 %	46 %	46 %

Under various concentrations of SO₂ and O₂, the optimal ratio between SO₂ and O₂ exhibiting a highest MSA percent yield was determined when 0.27 mmol of TFAO—OH was employed (SO₂/O₂=3.7). MSA yield was calculated based on SO₂ added. ^aReaction conditions: solvent, TFAOH (0.3 mL) and TFAA (0.3 mL); H₂O₂ (0.27 mmol); CH₄ (200 psi, 3 mmol); temperature (50 °C); time (18 h).

1.4. Table S4. Effects of anhydrous condition with the use of TFAA.^a

Entry	H ₂ O ₂ (mol %)	Reaction solution	MSA (yield %) ^c
1	20	Absence of TFAA (TFAOH only as a solvent)	32.8
2 ^b	20	Application of additional 2 μ L of water	6.8

The reaction was conducted 1) without TFAA in the reaction mixture after the addition of H₂O₂, and 2) with additional 2 μ L of water in the absence of TFAA to figure out the effects of anhydrous condition in methane sulfonation. ^aReaction conditions: solvent, TFAA (0.122 mL); H₂O₂ (20 mol% based on SO₂, 0.15 mmol); SO₂ (40 psi, 0.73 mmol); O₂ (30 psi, 0.12 mmol); CH₄ (200 psi, 3 mmol); temperature (50 °C); time (18 h); ^bAdditional water was applied to the reaction mixture (0.002 mL, 0.11 mmol). ^cThe percent yield of MSA was calculated based on SO₂.

1.5. Table S5. Effects of higher pressure in methane sulfonation.^a

Entry	H ₂ O ₂ (mol %)	Final pressure (psi)	MSA (yield %) ^b	Conv. (% CH ₄)
1	15	58 psi with CH ₄	33.0	45.2
2	20	59 psi with CH ₄	33.1	46.2
3	15	400 psi with N ₂	48.7	56.0
4	20	420 psi with N ₂	47.3	54.5

By adding N₂ gas after charging with SO₂, O₂, and CH₄, the sulfonation of methane was conducted under higher pressure. ^aReaction conditions: solvent, TFAOH (0.3 mL) and TFAA (0.3 mL); H₂O₂ (15–20 mol% based on SO₂, 0.11–0.15 mmol); SO₂ (40 psi, 0.73 mmol); O₂ (30 psi, 0.1 mmol for entry 1–2; 0.04 mmol for entry 3–4); CH₄ (0.5–0.6 mmol); N₂ (~ 400 psi); temperature (50 °C); time (18 h). ^bThe percent yield of MSA was calculated based on SO₂.

1.6. Table S6. High methane conversion yields.^a

Entry	H ₂ O ₂ (mol %)	N ₂ (psi)	MSA (yield %) ^b	Conv. (% CH ₄)
1	15	230	23.2	93.6
2	20	210	24.5	94.6

With the help of additional N₂, methane conversion yields increased up to 95% when CH₄ was employed as a limiting reagent. ^aReaction conditions: solvent, TFAOH (0.3 mL) and TFAA (0.3 mL); H₂O₂ (20 mol% based on SO₂, 0.15 mmol); SO₂ (40 psi, 0.73mmol); O₂ (30 psi, 0.04mmol); CH₄ (0.18—0.19mmol); N₂ (~ 230 psi); temperature (50 °C); time (18 h). ^bThe percent yield of MSA was calculated based on SO₂.

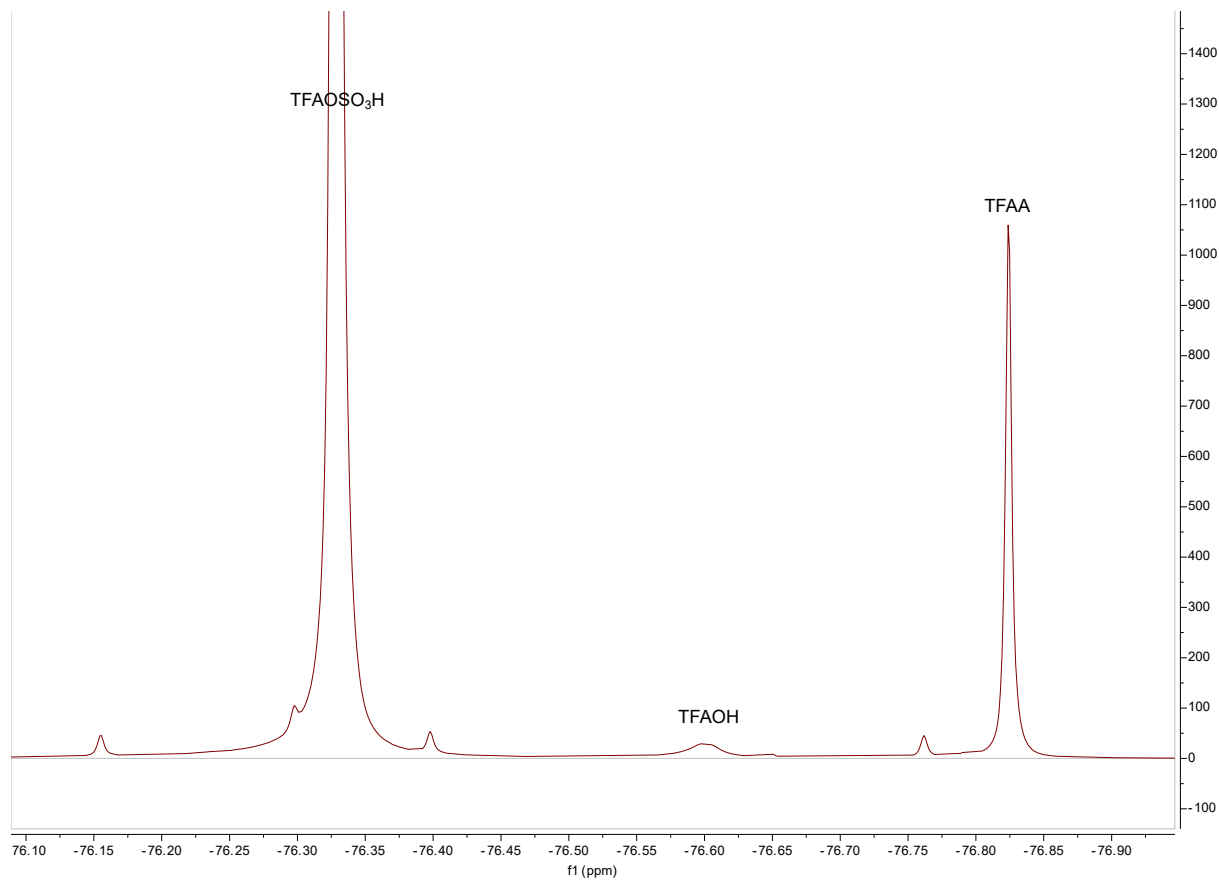
1.7. Table S7. Confirmation of free radical mechanism of the methane sulfonation using radical scavenger.^a

Entry	H ₂ O ₂ (mol %)	Radical Scavenger	MSA (yield %) ^b	Conv. (% CH ₄)
1	20	-	74.3	16.5
2	-	-	0	0
3	20	20 mol% TEMPO	3.3	0.7
4	20	20 mol% BHT	0	0

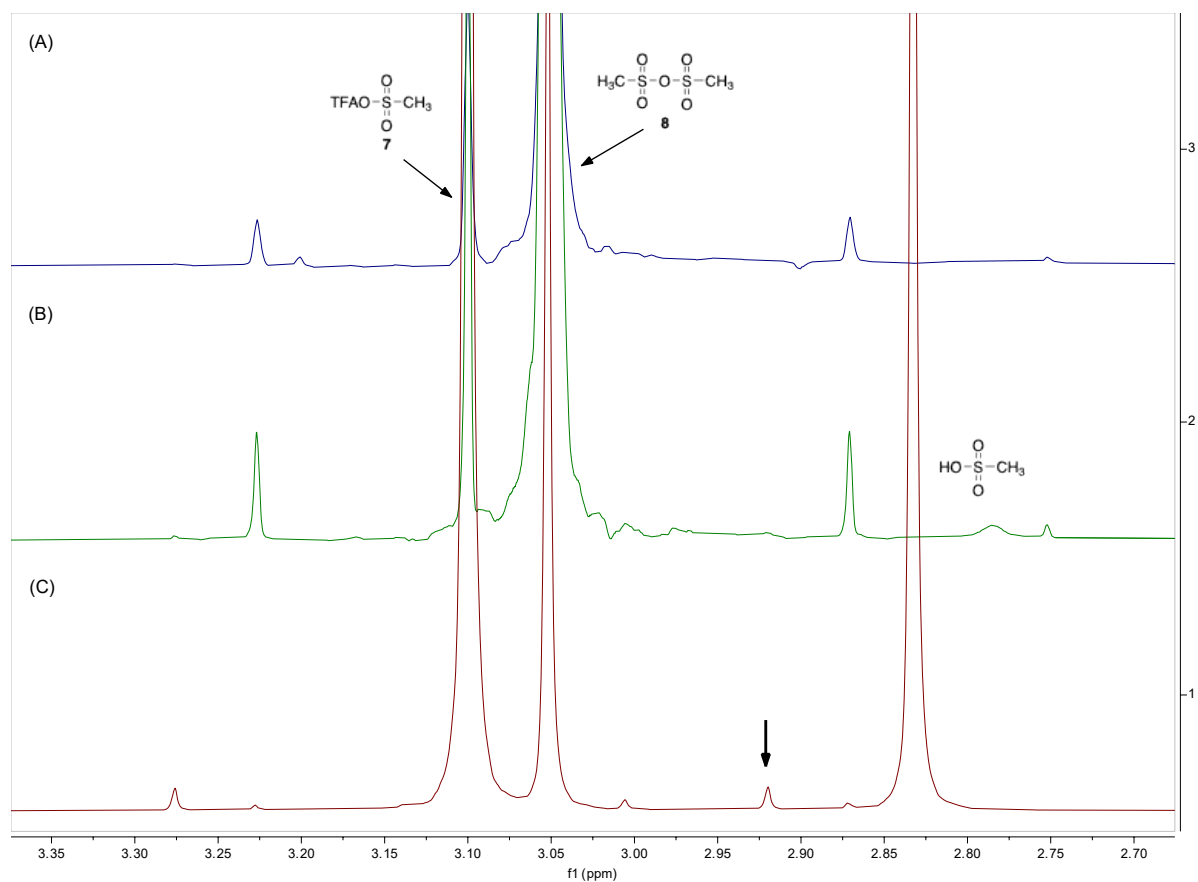
^aReaction conditions: solvent, TFAOH (0.3 mL) and TFAA (0.3 mL); H₂O₂ (20 mol% based on SO₂, 0.15 mmol); SO₂ (40 psi, 0.73 mmol); O₂ (30 psi, 0.12 mmol); CH₄ (200 psi, 3—3.3 mmol); time (18 h). ^bThe percent yield of MSA was calculated based on SO₂.

2. NMR analysis

2.1. ^{19}F NMR spectrum: (470 MHz, TFAD): Generation of trifluoroacetylsulfuric acid (TFAOSO_3H).



After the reaction mixture containing TFAA, TFAOH, H_2O_2 , SO_2 and O_2 was stirred at $50\text{ }^\circ\text{C}$ for 16 h, TFAOSO_3H was extracted with DCM-d_2 for NMR analysis. TFAOH, TFAA and H_2O diluted in DCM-d_2 were added separately to distinguish the observed peaks from each other. Depending on the amount and the ratio of TFAOH and TFAOSO_3H , TFAOH and TFAOSO_3H peaks shifted, however, the pattern between TFAOSO_3H , TFAOH, and TFAA remained the same.



2.2. ¹H NMR spectrum (400 MHz, TFAD): Unknown peak at 2.92 ppm.

Reaction conditions: (A) When methanesulfonic anhydride (**8**) was added to the solution of 0.3 mL TFAD and 0.2 mL TFAA, the formation of **7** was detected to exhibit **7** and **8**. (B) When 3 μ L H₂O₂ was added to the solution of (A), no peak was observed at around 2.92 ppm. (C) When 10 μ L TFAOSO₃H was added to the solution of (A), a small peak around 2.92 ppm was detected.

In Figure 4, we identified **7**, **8**, and MSA, however small peaks at 3.18 and 2.82 ppm were not elucidated unambiguously. However, we conducted the experiments using unlabeled MSAA (**8**) and obtained NMR spectra as shown here. We identified **7** and **8** along with MSA in these solvent systems, and observed a minor peak at 2.92 ppm, which would correspond with the small peaks at 3.18 and 2.82 ppm in the previous experiment and its NMR

spectrum. Thus we speculate the peak at 2.92 ppm as one of the methanesulfonic anhydride derivative such as

