

Alkylation of benzene using CO₂ and H₂ over ZnZrO_x/ZSM-5: the effect of Y doping

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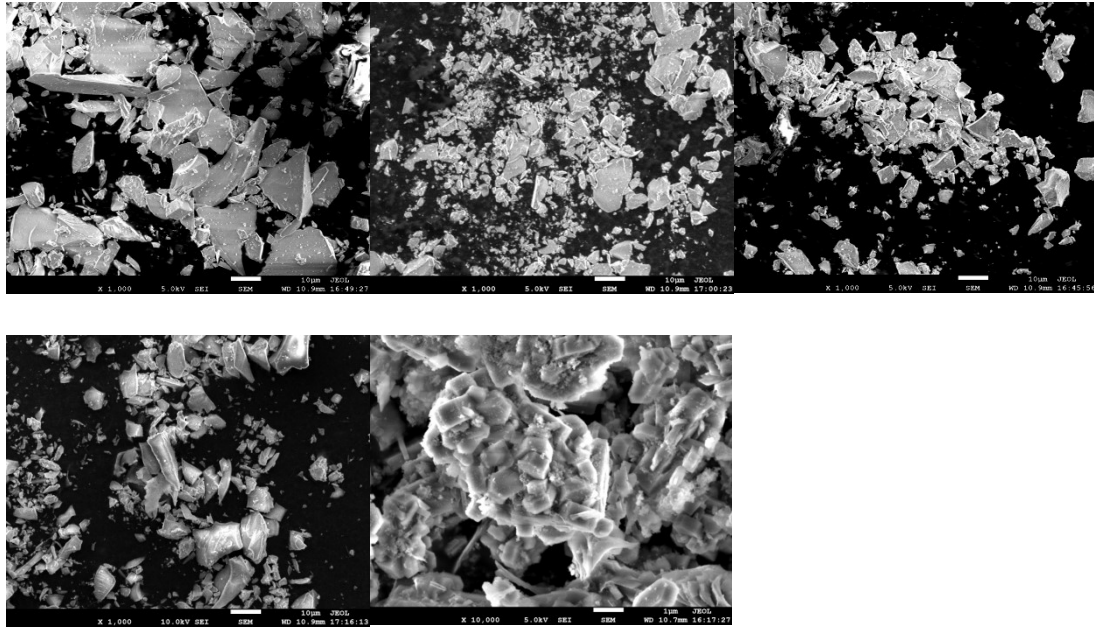


Fig.S1 Y0, Y0.05, Y0.1, Y0.3,ZSM-5 SEM images

Table S1 d-spacings of prepared catalysts calculated using the Bragg equation from XRD

	$2\theta / ^\circ$	d(011) (nm)	$2\theta / ^\circ$	d(110) (nm)	$2\theta / ^\circ$	d(020) (nm)	$2\theta / ^\circ$	d(121) (nm)
Y0	30.53	0.2926	35.38	0.2535	50.83	0.1795	60.4	0.1531
Y0.05	30.46	0.2932	35.28	0.2542	50.78	0.1797	60.33	0.1533
Y0.1	30.45	0.2933	35.27	0.2544	50.70	0.1799	60.23	0.1535
Y0.3	30.41	0.2937	35.15	0.2551	50.44	0.1808	59.94	0.1542

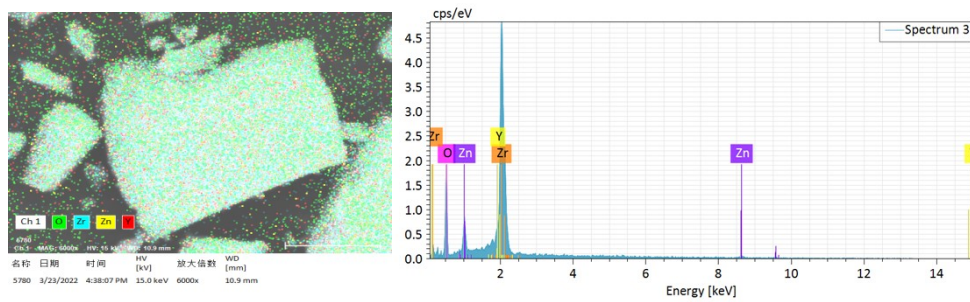


Fig.S2 EDS-mapping of Y0.1

Table S2 EDS-mapping element content analysis of Y0.1.

Element	Atomic number	Quality / %	Normalized Mass / %	Atoms / %
O	8	24.8	29.9	70.3
Zn	30	3.6	4.3	2.5
Y	39	3.8	4.6	1.9
Zr	40	50.8	61.3	25.3
		82.9	100	100

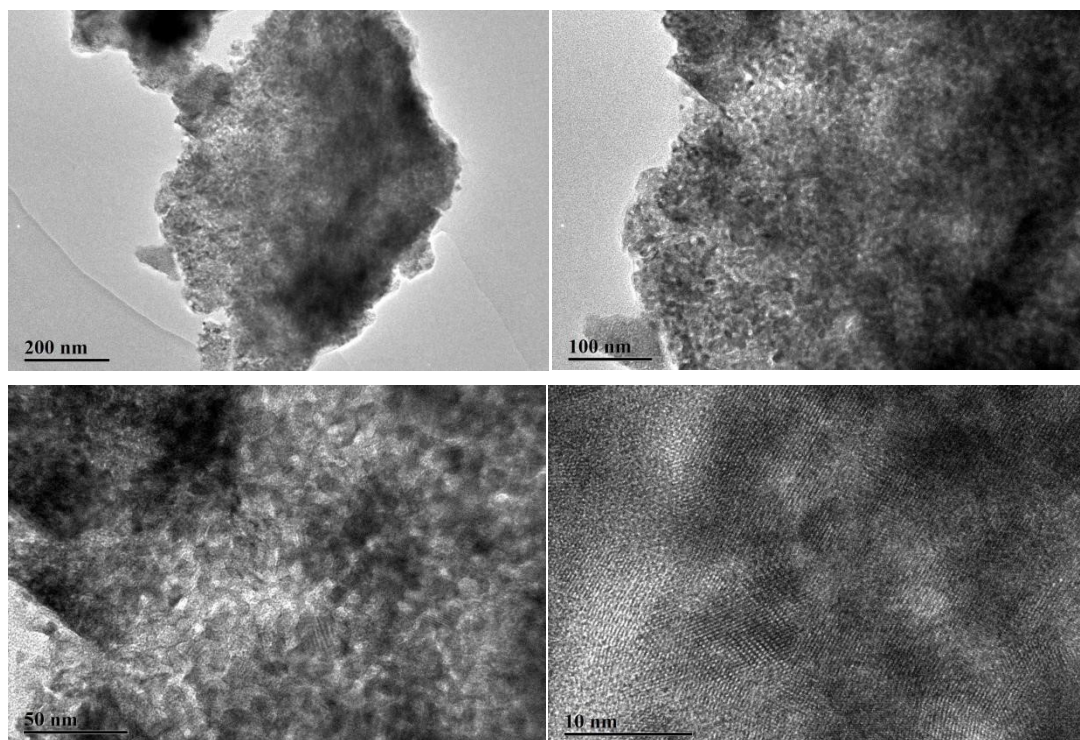


Fig. S3 Y0.1 TEM images of different magnifications

Table S3 Deconvolution results of O 1s XPS peaks.

Catalyst	O _{OH} / %	O _V / %	O _L / %
Y0	13.1	17.8	69.1
Y0.05	11.0	24.7	64.3
Y0.1	13.6	25.7	60.7
Y0.3	17.3	20.2	62.5

Table S4 Y-doped ZnZrOx/HZSM-5 catalyzed alkylation of CO₂ and benzene.

Catalyst	Conv. CO ₂ /%	Conv. benz./%	Selectivity/%			
			M _B	E _B	X _B	Other
Y0/ZSM-5	10.0	19.7	73.6	3.0	14.3	9.1
Y0.05/ZSM-5	10.2	22.7	61.8	2.6	12.4	23.2
Y0.1/ZSM-5	17.3	30.8	56.5	2.5	15.0	26.0
Y0.3/ZSM-5	14.5	18.3	73.3	3.0	11.5	12.2

Table S5 Liquid phase product distribution

Catalyst	Conv. benz. / %	Liquid phase product distribution / %				
		M _B	E _B	X _B	C ₉₊	
Y0/ZSM-5	19.7	80.2	3.3	15.5	1.0	
Y0.05/ZSM-5	22.7	79.8	3.3	16.1	0.7	
Y0.1/ZSM-5	30.8	74.8	3.3	20.0	1.9	
Y0.3/ZSM-5	18.3	81.5	3.3	12.8	2.3	
Zn0.1Ti/ZSM-5(30)	23.8	77.4	2.8	16.1	3.7	Ref.[1]

Table S6 Different mixing methods of Y0.1/HZSM-5 catalyzed alkylation of CO₂ and benzene.

	Conv. CO ₂ /%	Conv. benz./%	Selectivity/%			
			M _B	E _B	X _B	Other
dual-bed	12.8	9.33	56.8	5.9	6.2	31.1
granule-mixing	14.8	28.5	58.0	2.1	14.4	26.5
powder-mixing	17.3	30.8	56.5	2.5	15.1	25.9

Table S7 Gas phase products of Y0.1/ZSM-5 and Y0.1 for CO₂ hydrogenation to methanol

Catalyst	Conv. CO ₂ /%	Selectivity/%						
		Methane	Ethylene	Ethane	Propylene	Propane	Butane	CO
Y0.1/ZSM-5	17.3	1.4	0.1	0.2	0.3	0.3	0.3	56.3
Y0.1	13.5	3.7	0	0	0	0	0	91.8

Table S8 H₂ consumption amount of various catalysts.

Catalysts	ZnY-O-Zr / mmol/g	ZrO ₂ / mmol/g	(ZnY-O-Zr)/(ZnY-O-Zr+ZrO ₂)
Y0	0.08	0.52	0.13
Y0.05	0.18	0.58	0.24
Y0.1	0.24	0.34	0.41
Y0.3	0.11	0.54	0.17

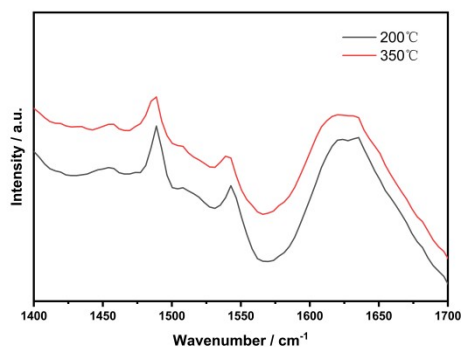


Fig. S4 IR spectra of the ZSM-5 after pyridine desorption

	BET Surface Area / m ² /g	Pore Volume / cm ³ /g	Pore Size / nm
Y0	28	0.03	3
Y0.05	33	0.04	3
Y0.1	29	0.04	3
Y0.3	14	0.01	3
ZSM-5	346	0.09	6

Table S9 Catalyst bet specific surface area, pore volume and pore size

1. Liu, X.; Pan, Y.; Zhang, P.; Wang, Y.; Xu, G.; Su, Z. *Frontiers of Chemical Science and Engineering* **2021**, *16* (3), 384-396.