

Electronic Supplementary Material (ESI) for RSC Advances.
This journal is © The Royal Society of Chemistry 2022

Transparent TiO₂ thin films with high photocatalytic activity for indoor air purification

Jekaterina Sydorenko ^{a*}, Arvo Mere ^a, Malle Krunks ^a, Marina Krichevskaya ^b and Ilona Oja Acik ^a

^a Laboratory of Thin Films Chemical Technologies, Department of Materials and Environmental Technology, Tallinn University of Technology, Ehitajate tee 5, 19086 Tallinn, Estonia.

^b Laboratory of Environmental Technology, Department of Materials and Environmental Technology, Tallinn University of Technology, Ehitajate tee 5, 19086 Tallinn, Estonia

* Corresponding authors: Jekaterina Sydorenko email: jekaterina.spiridono@taltech.ee, Marina Krichevskaya email: marina.kritsevskaja@taltech.ee, Ilona Oja Acik email: ilona.oja@taltech.ee.

Supplementary Information Section

Content

1. Spray pyrolysis setup	S2
2. Setup used for gas-phase photocatalytic experiments.....	S2
3. Surface morphology	S3
4. Quantum efficiency calculations	S3
5. Langmuir-Hinshelwood reaction kinetics	S4
6. Reynolds number calculations.....	S4
7. The comparative table of photocatalytic oxidation of heptane and toluene on TiO ₂ thin films	S6
8. Conversion of compounds in 9 ppm of mixture under different operating parameters.....	S9
References.....	S10

1. Spray pyrolysis setup

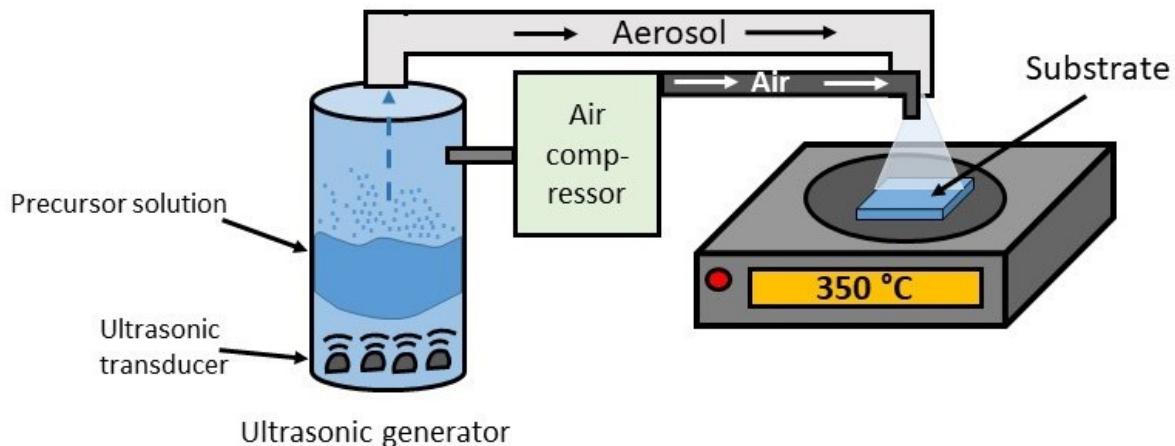


Fig. SI-1 The sheme of the ultrasonic spray pyrolysis setup.

2. Setup used for gas-phase photocatalytic experiments.

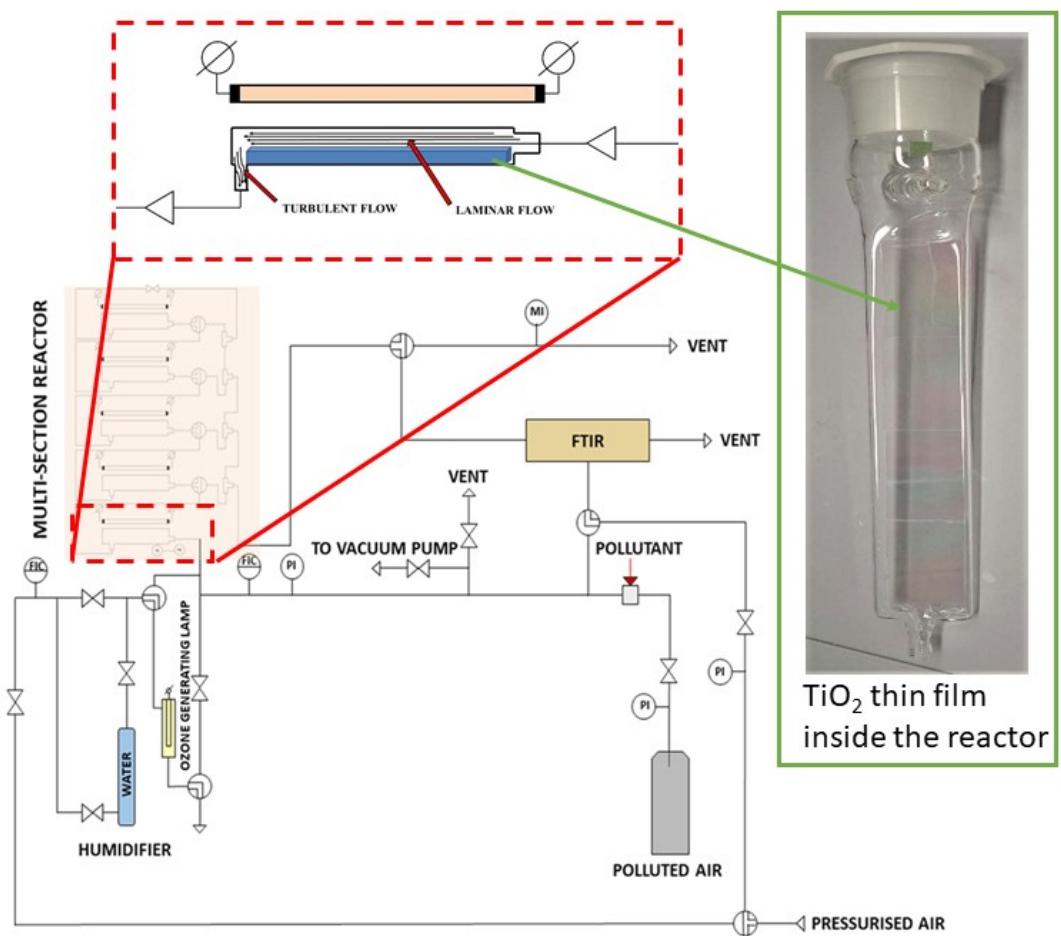


Fig. SI-2 The sheme of setup used for gas-phase photocatalytic experiments.

3. Surface morphology

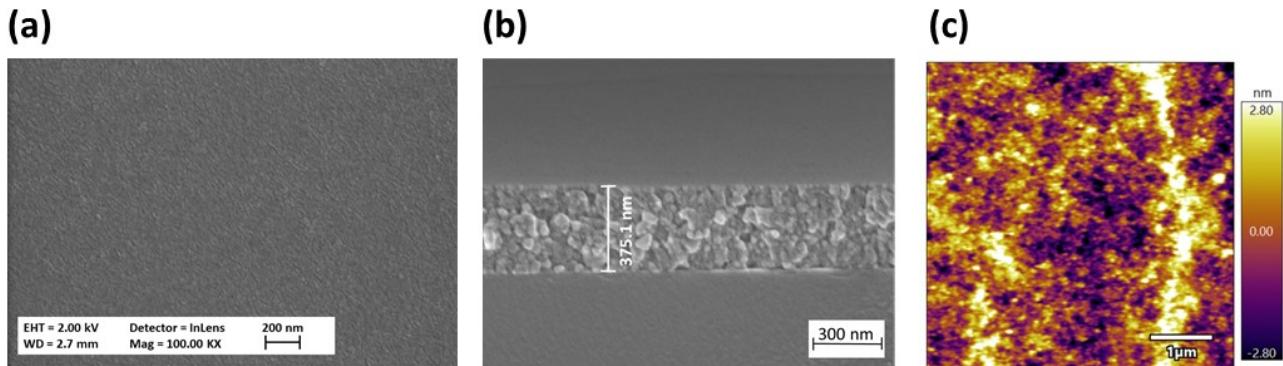


Fig. SI-3 Scanning electron microscopy (SEM) (a), cross-sectional SEM (b) and atomic force microscopy (AFM) (c) images of TiO_2 film.

4. Quantum efficiency calculations

$$QE = \frac{\text{Number of degraded molecules}}{\text{Number of incident photons}}$$

$$\text{Number of degraded molecules per second} = \frac{G * A * r_o}{V_M}$$

Where G – Gas flow rate: $G=0.5 \text{ L/min}=0.0083 \text{ L/s}$

A – Avogadro number: $A= 6.02 \cdot 10^{23}$

r_o – Initial reaction rate: $r_o = -\frac{dC}{dt}$ For example, at heptane initial concentration 5 ppm $r_o = 0.34 \text{ ppm per 1 s} = 0.34 \cdot 10^{-6} \text{ mol / mol air}$

V_M – Molar volume of ideal gas: $V_M= 22.4 \text{ L/mol air}$

$$\text{Number of degraded molecules per second} = \frac{0.0083 \cdot 6.02 \cdot 10^{23} \cdot 0.34 \cdot 10^{-6}}{22.4} = 7.58 \cdot 10^{13} \text{ 1/s}$$

Number of incident photons per second:

$$\text{Number of incident photons} = \frac{\text{Energy of the lamp}}{\text{Energy of photons}} = \frac{0.42}{5.442 \cdot 10^{-19}} = 7.72 \cdot 10^{17} \text{ 1/s}$$

Energy of the lamp = Irradiated surface area · Irradiance · Time = $120 \cdot 3.5 \cdot 10^{-3} \cdot 1 = 0.42 \text{ J/s}$

Where irradiated surface area for one section of the reactor is 120 cm^2

Irradiance of the UV-A lamp is $3.5 \text{ mW/cm}^2 = 3.5 \cdot 10^{-3} \text{ W/cm}^2$

$$\text{Photon energy: } E = \frac{hc}{\lambda} = \frac{6.626 \cdot 10^{-34} \text{ J} \cdot \text{s} \cdot 299792458 \text{ m/s}}{3.65 \cdot 10^{-7} \text{ m}} = 5.442 \cdot 10^{-19} \text{ J},$$

Where h – is the Planck constant: $h=6.626 \cdot 10^{-34} \text{ J} \cdot \text{s}$

c – is the speed of the light in vacuum: $c=299792458 \text{ m/s}$

λ - is the photon's wavelength for UV-A lamps: $\lambda = 3.65 \cdot 10^{-7} \text{ m}$

Quantum efficiency for 5 ppm heptane degradation at air flow rate 0.5 L/min and RH 6%

$$QE = \frac{7.58 \cdot 10^{13}}{7.72 \cdot 10^{17}} = 9.82 \cdot 10^{-5} \text{ molecules / photons}$$

5. Langmuir-Hinshelwood reaction kinetics

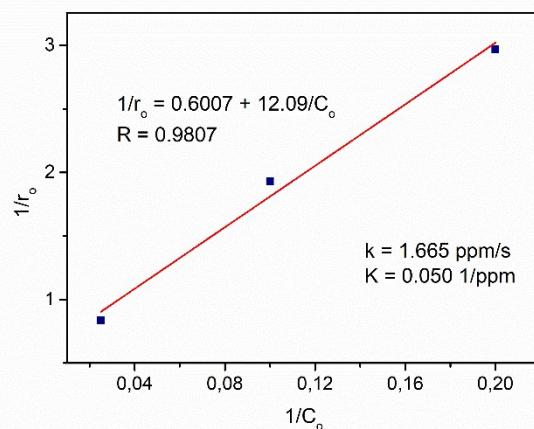


Fig. SI-4 Langmuir-Hinshelwood kinetic plot for the determination of heptane degradation reaction rate and adsorption constants.

6. Reynolds number calculations

To determine the flow pattern Reynolds number calculations were performed.

When $Re < 2300$ flow is laminar.

When $2300 < Re < 4000$ transient.

When $Re > 4000$ turbulent.

Reynolds number was found:

$$Re = \frac{\rho v L}{\mu} \quad S1$$

Where ρ – density of air, kg/m^3 for air at $T = 40^\circ\text{C}$ $\rho = 1.127 \text{ kg/m}^3$

v – flow speed of air, m/s

L – characteristic linear dimension of the reactor, m

μ - dynamic viscosity of air, $\text{Pa}\cdot\text{s}$ for air at $T = 40^\circ\text{C}$ $\mu = 19.07 \cdot 10^{-6} \text{ Pa}\cdot\text{s}$

$$L = \frac{4 A_{cross}}{P}$$

Where A_{cross} – cross-section area

P – wetting perimeter

For used in the study reactor $A_{cross} = 4.32 \text{ cm}^2$ and $P = 10.16 \text{ cm}$

$$L = \frac{4 \cdot 4.32}{10.16} = 1.7 \text{ cm} = 0.017 \text{ m}$$

At air flow rate 0.5 L/min:

$$v = \frac{\text{air flow rate}}{\text{Across}} = \frac{500 \frac{\text{cm}^3}{\text{min}}}{4.32 \text{ cm}} = 115.74 \frac{\text{cm}}{\text{min}} = 0.0193 \frac{\text{m}}{\text{s}}$$

$$Re = \frac{1.127 \cdot 0.0193 \cdot 0.017}{19.07 \cdot 10^{-6}} = 19.39$$

At air flow rate 1 L/min:

$$v = 0.0386 \frac{\text{m}}{\text{s}}$$

$$Re = \frac{1.127 \cdot 0.0386 \cdot 0.017}{19.07 \cdot 10^{-6}} = 38.78$$

At air flow rate 1.5 L/min:

$$v = 0.0578 \frac{\text{m}}{\text{s}}$$

$$Re = \frac{1.127 \cdot 0.0578 \cdot 0.017}{19.07 \cdot 10^{-6}} = 58.14$$

At air flow rate 2 L/min:

$$v = 0.0772 \frac{\text{m}}{\text{s}}$$

$$Re = \frac{1.127 \cdot 0.0772 \cdot 0.017}{19.07 \cdot 10^{-6}} = 77.52$$

At air flow rate 2.5 L/min:

$$v = 0.0965 \frac{\text{m}}{\text{s}}$$

$$Re = \frac{1.127 \cdot 0.0965 \cdot 0.017}{19.07 \cdot 10^{-6}} = 96.90$$

7. The comparative table of photocatalytic oxidation of heptane and toluene on TiO₂ thin films

Table SI-1. The comparative table of photocatalytic oxidation of heptane and toluene on TiO₂ thin films prepared in current study and on other thin films available from the scientific literature.

<i>Photocatalyst</i>	<i>Thickness</i>	<i>Pollutant</i>	<i>Initial Concentration</i>	<i>Reactor</i>	<i>Catalyst surface area</i>	<i>Light source</i>	<i>Oxidation conditions</i>	<i>Conversion/ degradation rate</i>	<i>Reaction time</i>	<i>Ref</i>
Spray pyrolysis-synthesized TiO ₂ thin film	370 nm	Heptane	10 ppm	Continuous flow reactor	360 cm ²	UV-A, 3.5 mW/cm ²	Air flow rate 0.5 L/min, RH 6%	100%	46.8 s	This study
Spray pyrolysis-synthesized TiO ₂ thin film	370 nm	Heptane	10 ppm	Continuous flow reactor	600 cm ²	UV-A, 3.5 mW/cm ²	Air flow rate 0.5 L/min, RH 40%	91%	78 s	This study
Spray pyrolysis-synthesized TiO ₂ thin film	370 nm	Heptane	10 ppm	Continuous flow reactor	600 cm ²	VIS, 3.3 mW/cm ²	Air flow rate 0.5 L/min, RH 6%	44%	78 s	This study
Spray pyrolysis-synthesized TiO ₂ thin film	200 nm	Heptane	10 ppm	Continuous flow reactor	600 cm ²	UV-A, 3.5 mW/cm ²	Air flow rate 0.5 L/min, RH 6%	48%	78 s	s ²
Spray pyrolysis-synthesized TiO ₂ thin film	200 nm	Heptane	10 ppm	Continuous flow reactor	600 cm ²	UV-A, 3.5 mW/cm ²	Air flow rate 0.5 L/min, RH 40%	20%	78 s	s ²
Spray pyrolysis-	370 nm	Toluene	10 ppm	Continuous	600 cm ²	UV-A, 3.5	Air flow rate	55%	78 s	This

synthesized TiO ₂ thin film				flow reactor		mW/cm ²	0.5 L/min, RH 6%			study
Spray pyrolysis-synthesized TiO ₂ thin film	370 nm	Toluene	10 ppm	Continuous flow reactor	600 cm ²	UV-A, 3.5 mW/cm ²	Air flow rate 0.5 L/min, RH 40%	51%	78 s	This study
Spray pyrolysis-synthesized TiO ₂ thin film	370 nm	Toluene	10 ppm	Continuous flow reactor	600 cm ²	VIS, 3.3 mW/cm ²	Air flow rate 0.5 L/min, RH 6%	6%	78 s	This study
Sol-gel dip-coated TiO ₂ thin film	470 nm	Toluene	192 ppm	Batch 0.55 L recirculating reactor	20 cm ²	UV-A, 4W	Recirculation flow rate 0.075 L/min, Dry air	60%	2 h	s ³
Sol-gel dip-coated Ti _{0.90} Zr _{0.10} O ₂ thin film	540 nm	Toluene	192 ppm	Batch 0.55 L recirculating reactor	20 cm ²	UV-A, 4W	Recirculation flow rate 0.075 L/min, Dry air	70%	2 h	s ³
Sol-gel dip-coated 10% ZrO ₂ /TiO ₂ thin film	410 nm	Toluene	192 ppm	Batch 0.55 L recirculating reactor	20 cm ²	UV-A, 4W	Recirculation flow rate 0.075 L/min, Dry air	50%	2 h	s ³
Sol-gel dip-coated TiO ₂ thin film	Not reported	Toluene	50-180 ppm	Batch 1.1 L reactor	68 cm ²	UV-LED, 10 mW/cm ²	Dry air	1.83 x 10 ⁻⁴ mol m ⁻³ min ⁻¹	1 h	s ⁴
Sol-gel dip-coated 0.7% Fe-TiO ₂ thin film	Not measured	Toluene	50-180 ppm	Batch 1.1 L reactor	68 cm ²	UV-LED, 10 mW/cm ²	Dry air	2.57 x 10 ⁻⁴ mol m ⁻³ min ⁻¹	1 h	s ⁴
Sol-gel dip-coated	0.9 µm	Toluene	1 ppm	Continuous	50 cm ²	UV-A, 1	Air flow rate	46%	0.2 s	s ⁵

TiO ₂ thin film				flow reactor		mW/cm ²	0.5 L/min, RH 50%			
Sol-gel dip coated TiO ₂ thin film	350 nm	Toluene	155 ppb	Benchtop continuous flow reactor	1.2 cm ²	UV-C, 3.0 mW/cm ²	Air flow rate 0.5 L/min, dry air	78%	1 s	s ⁶
Sol-gel dip coated TiO ₂	1.3 μm	Toluene	0.5 ppm	Continuous flow tubular reactor	184 cm ²	UV-A, 10W	Air flow rate 0.2 L/min, dry air	95%	25 s	s ⁷
Sol-gel dip coated porphyrin- sensitized TiO ₂ thin films	1.3 μm	Toluene	0.5 ppm	Continuous flow tubular reactor	184 cm ²	VIS, 10W	Air flow rate 0.2 L/min, dry air	15%	25 s	s ⁷
E-beam evaporated TiO ₂ thin films	20 nm	Toluene	5 ppm	Batch 0.314 L reactor	18.75 cm ²	UV-A, 0.304 W/cm ²	Water vapour atmosphere	40%	30 min	s ⁸

8. Conversion of compounds in 9 ppm of mixture under different operating parameters

Table SI-2. Conversion of compounds in 9 ppm of mixture heptane, acetone and acetaldehyde (3 ppm each compound) under different operating parameters at different photocatalytic surface areas. ***AD*** – acetaldehyde, ***AC*** – acetone and ***HEP*** - heptane

Operating parameters			Conversion (%)														
Air flow rate (L/min)	Relative humidity (%)	Irradiation	Surface of catalyst 120 cm ²			Surface of catalyst 240 cm ²			Surface of catalyst 360 cm ²			Surface of catalyst 480 cm ²			Surface of catalyst 600 cm ²		
			<i>AD</i>	<i>AC</i>	<i>HEP</i>												
0.5	6	UV-A	100	93	77	100	99	92	100	100	100	100	100	100	100	100	100
1	6	UV-A	63	63	56	86	84	81	92	91	90	100	100	100	100	100	100
0.5	40	UV-A	46	31	30	65	55	48	83	76	67	100	87	77	100	100	82
0.5	6	VIS	39	33	15	51	53	26	71	71	40	87	85	59	100	100	78

Table SI-3. Conversion of compounds in 9 ppm of mixture toluene, acetone and acetaldehyde (3 ppm each compound) under different operating parameters at different photocatalytic surface areas. ***AD*** – acetaldehyde, ***AC*** – acetone and ***TOL*** – toluene

Operating parameters			Conversion (%)														
Air flow rate (L/min)	Relative humidity (%)	Irradiation	Surface of catalyst 120 cm ²			Surface of catalyst 240 cm ²			Surface of catalyst 360 cm ²			Surface of catalyst 480 cm ²			Surface of catalyst 600 cm ²		
			<i>AD</i>	<i>AC</i>	<i>TOL</i>												
0.5	6	UV-A	78	70	71	100	100	97	100	100	100	100	100	100	100	100	100
1	6	UV-A	40	40	48	61	60	67	82	81	85	91	86	100	100	93	100
0.5	40	UV-A	40	32	37	65	51	65	78	68	70	88	81	78	100	100	90
0.5	6	VIS	20	24	16	21	25	28	33	34	28	36	38	29	52	53	31

References

- S1 C. Geankolis, *Transport processes and unit operations*, 3rd edn., 1993, 921.
- S2 I. Dundar, M. Krichevskaya, A. Katerski, M. Krunks and I. O. Acik, *Catalysts*, 2019, **9**, 915, DOI:10.3390/catal9110915.
- S3 M. D. Hernández-Alonso, I. Tejedor-Tejedor, J. M. Coronado and M. A. Anderson, *Appl. Catal. B Environ.*, 2011, **101**, 283-293, DOI:10.1016/j.apcatb.2010.09.029.
- S4 T. Rojviroon, A. Laobuthee and S. Sirivithayapakorn, *Int. J. Photoenergy*, 2012, **8**, DOI:10.1155/2012/898464.
- S5 N. Negishi, S. Matsuzawa, K. Takeuchi and P. Pichat, *Chem. Mater.*, 2007, **19**, 3808-3814, DOI:10.1021/cm070320i.
- S6 N. Quici, M. L. Vera, H. Choi, G. L. Puma, D. D. Dionysiou, M. I. Litter and H. Destaillats, *Appl. Catal. B Environ.*, 2010, **95**, 312-319, DOI:10.1016/j.apcatb.2010.01.009.
- S7 P. C. Yao, S. T. Hang, C. W. Lin and D. H. Hai, *J. Taiwan Inst. Chem. Eng.*, 2011, **42**, 470-479, DOI:10.1016/j.jtice.2010.08.013.
- S8 C. Garlisi and G. Palmisano, *Appl. Surf. Sci.*, 2017, **420**, 89-93, DOI:10.1016/j.apsusc.2017.05.077.