

Electronic Supporting Information

Mechanistic insight into electrocatalytic glyoxal reduction on copper and its relation to CO₂ reduction

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S1. Electrochemical cell

Figure S1 shows the most important components of the electrochemical cell that was used in this study.

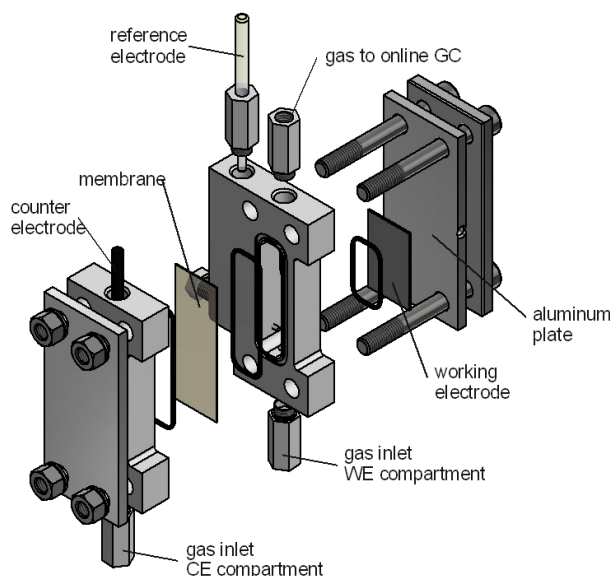
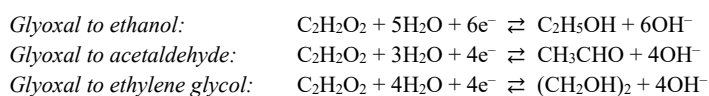


Figure S1. Electrochemical cell for steady-state electrolysis.

S2. Calculations of partial current density, faradaic efficiency and yield (carbon balance)

We considered the following electrochemical half-reactions:



The partial current density for the formation of a certain product, j_i (in A cm^{-2}), was calculated using Faraday's law (Equation S1):

$$j_i = \frac{n_i z_i F}{At} \quad (\text{S1})$$

where:

n_i is the moles of product i detected in the electrolyte in the end of electrolysis;
 z_i is the number of electrons exchanged for the formation of one molecule in the corresponding reaction;
 F is the faraday constant ($96,485 \text{ A s mol}^{-1}$);
 A is the geometric electrode area (1 cm^2);
 t is the duration of electrolysis ($2,400 \text{ s}$).

The faradaic efficiency for a certain product, FE_i (in %), was calculated by equation S2:

$$\text{FE}_i = \frac{j_i}{j_{\text{total}}} \cdot 100 \quad (\text{S2})$$

where:

j_{total} is the average current density recorded during the electrolysis experiment.

To determine the percentage of unreacted glyoxal, U (in %) and the yield for each product (Y_i , in %), the equations S3 and S4 were used:

$$U = \frac{(n_0 - n_{40})}{n_0} \cdot 100 \quad (\text{S3})$$

$$Y_i = \frac{n_i}{n_0} \cdot 100 \quad (\text{S4})$$

where:

n_0 is the moles of glyoxal prior to electrolysis ($1.8 \cdot 10^{-3}$ mol for the 9 mL catholyte);

n_{40} is the moles of glyoxal found in the electrolyte after 40 min of electrolysis.

S3. Gas and liquid phase corrections

The free energies of gas-phase molecules were approximated as: $G \approx E_{DFT} + ZPE - TS$. The ZPE values were obtained from vibrational frequency analyses and the TS values were extracted from thermodynamic tables at 298.15 K and 1 atm.¹ Using a method described elsewhere,² we applied corrections to the total energies of the gas phase, denoted GC. Moreover, we added liquid-phase corrections based on the entropy differences between liquid and gas phases as described elsewhere,³ denoted LC. The values used for all the liquids and gases in this study are listed in Table S1.

Table S1. Zero-point energy, entropy contributions, gas- and liquid-phase corrections to the free energies of molecules featured in this work. All values are in eV.

Molecule	ZPE	TS	GC	LC
H ₂	0.27	0.40	0.00	0.00
H ₂ O	0.57	0.58	0.00	-0.09
O ₂	0.10	0.63	-0.46	0.00
Glyoxal	0.97	0.84	-0.14	0.00
Acetaldehyde	1.46	0.82	-0.02	0.06
Ethanol	2.11	0.87	0.03	-0.07
Ethylene glycol	2.24	0.94	0.14	-0.27

S4. Contributions to the free energies of solvent-adsorbate interactions

Water-adsorbate interactions deemed “solvation” corrections (E_{sol} in $G \approx E_{DFT} + ZPE - TS + E_{sol}$) were computed on Cu(111) using an iterative method described elsewhere.⁴ The specific values are listed in Table S2.

Table S2. Stabilization (in eV) provided by water-adsorbate interactions to the adsorption energies.

Adsorbate	Solvation correction
*CHOCHO	-0.36
*CHOHCHO	-0.31
*CH ₂ OCHO	0.00

*CHCHO	-0.34
*CHOHCHOH	-0.28
*CH ₂ OHCHO	-0.39
*CHOHCH ₂ O	-0.30
*CHOHCH ₂ OH	-0.19

S5. Free energies and active sites

The ZPE, TS_{vib}, solvation energy (E_{sol}), and the corresponding ΔG values obtained for the different adsorbates on the different model surfaces featured in the electroreduction of glyoxal to ethylene glycol are shown in Table S3. Note that gas-phase glyoxal and the clean surfaces were used as a reference for the free energies of the intermediates.

Table S3. Free energies of adsorption and their contributions (in eV) for the adsorbed species involved in the most favorable pathway of the electrochemical reduction of glyoxal to ethylene glycol.

Cu(111)	ZPE	TS	E_{sol}	ΔG
*CHOCHO	1.02	0.25	-0.36	-0.56
*CHOHCHO	1.32	0.31	-0.31	-0.48
*CHOHCHOH	1.61	0.52	-0.28	-0.45
*CHOHCH ₂ OH	1.93	0.38	-0.19	-0.11
Cu(100)	ZPE	TS	E_{sol}	ΔG
*CHOCHO	1.03	0.22	-0.36	-1.09
*CHOHCHO	1.32	0.29	-0.31	-0.89
*CHOHCHOH	1.62	0.39	-0.28	-0.50
*CHOHCH ₂ OH	1.94	0.39	-0.19	-0.36
Cu(211)	ZPE	TS	E_{sol}	ΔG
*CHOCHO	1.02	0.29	-0.36	-1.32
*CHOHCHO	1.34	0.30	-0.31	-1.07
*CHOHCHOH	1.61	0.36	-0.28	-0.75
*CHOHCH ₂ OH	1.94	0.35	-0.19	-0.67
4AD@Cu(100)	ZPE	TS	E_{sol}	ΔG
*CHOCHO	1.04	0.22	-0.36	-1.56
*CHOHCHO	1.34	0.27	-0.31	-1.40
*CHOHCHOH	1.61	0.42	-0.28	-0.76
*CHOHCH ₂ OH	1.95	0.37	-0.19	-0.73
4AD@Cu(111)	ZPE	TS	E_{sol}	ΔG
*CHOCHO	1.03	0.22	-0.36	-1.80
*CHOHCHO	1.34	0.26	-0.31	-1.44
*CHOHCHOH	1.62	0.32	-0.28	-0.79

*CHOHCH2OH	1.95	0.42	-0.19	-0.86
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The ZPE, TS_{vib} , solvation energy (E_{solv}), and the corresponding ΔG values obtained for the different adsorbates on the different model surfaces featured in the electroreduction of glyoxal to ethanol are shown in Table S4. From *CH₂CHO on the values are extracted from previous works^{5,6} and adapted because the gas-phase references are different. Here, gas-phase glyoxal and the clean surfaces were used as a reference for the free energies of the intermediates.

Table S4. Free energies of adsorption and their contributions (in eV) for the species involved in the electrochemical reduction of glyoxal to ethanol. Values extracted and adapted from previous works^{5,6} are shown in *italics*. Liquid acetaldehyde was used when it was more stable than its adsorbed counterpart.

Cu(111)	ZPE	TS	E_{solv}	ΔG
*CHOCHO	1.02	0.25	-0.36	-0.56
*CHOHCHO	1.32	0.31	-0.31	-0.48
*CHCHO	0.90	0.19	-0.34	-1.29
*CH ₂ CHO	-	-	-	<i>-1.66</i>
CH ₃ CHO _(l)	-	-	-	<i>-1.81</i>
*CH ₃ CH ₂ O	-	-	-	<i>-0.99</i>
Cu(100)	ZPE	TS	E_{solv}	ΔG
*CHOCHO	1.03	0.22	-0.36	-1.09
*CHOHCHO	1.32	0.29	-0.31	-0.89
*CHCHO	0.91	0.17	-0.34	-1.64
*CH ₂ CHO	-	-	-	<i>-1.93</i>
CH ₃ CHO _(l)	-	-	-	<i>-1.81</i>
*CH ₃ CH ₂ O	-	-	-	<i>-1.36</i>
Cu(211)	ZPE	TS	E_{solv}	ΔG
*CHOCHO	1.02	0.29	-0.36	-1.32
*CHOHCHO	1.34	0.30	-0.31	-1.07
*CHCHO	0.91	0.17	-0.34	-1.65
*CH ₂ CHO	-	-	-	<i>-2.09</i>
*CH ₃ CHO	-	-	-	<i>-2.01</i>
*CH ₃ CH ₂ O	-	-	-	<i>-1.54</i>
4AD@Cu(100)	ZPE	TS	E_{solv}	ΔG
*CHOCHO	1.04	0.22	-0.36	-1.56
*CHOHCHO	1.34	0.27	-0.31	-1.40
*CHCHO	0.91	0.17	-0.34	-2.03
*CH ₂ CHO	-	-	-	<i>-2.24</i>
*CH ₃ CHO	-	-	-	<i>-2.03</i>
*CH ₃ CH ₂ O	-	-	-	<i>-1.86</i>
4AD@Cu(111)	ZPE	TS	E_{solv}	ΔG
*CHOCHO	1.03	0.22	-0.36	-1.80
*CHOHCHO	1.34	0.26	-0.31	-1.44
*CHCHO	0.91	0.16	-0.34	-2.03

*CH ₂ CHO	-	-	-	-2.47
*CH ₃ CHO	-	-	-	-2.11
*CH ₃ CH ₂ O	-	-	-	-2.05

Figure S2 shows the top views of the five active sites under study. The generalized coordination number $\overline{CN}(i)$ is arithmetically calculated as shown in Equation S5 for a given surface site “*i*”:

$$\overline{CN}(i) = \sum_{j=1}^{n_i} \frac{cn(j)}{cn_{max}} \quad (S5)$$

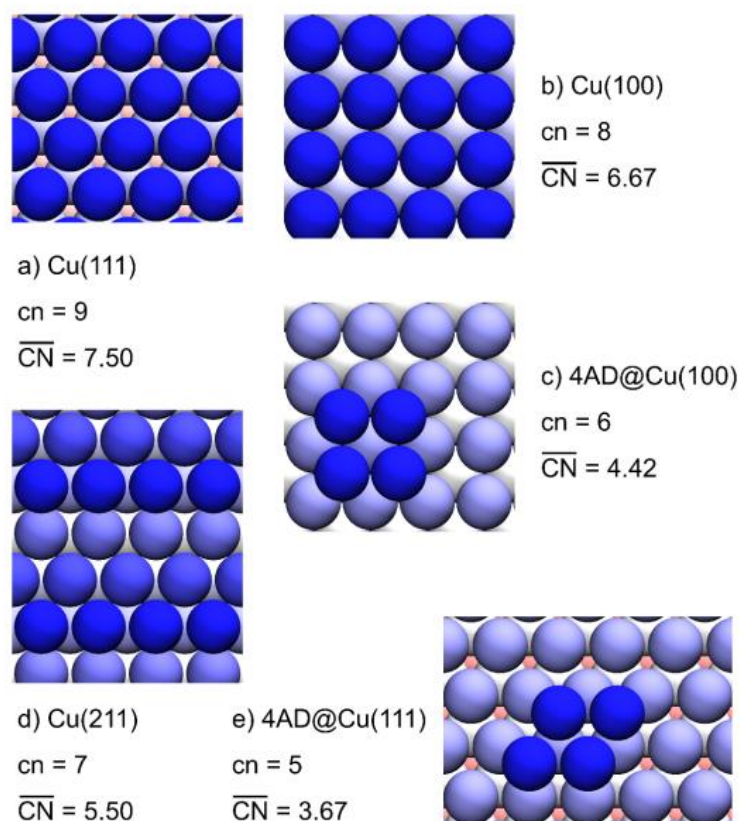


Figure S2. Top views of the five slabs under study. Different shades of blue together with white and pink colors different depths.

Conventional coordination numbers (*cn*) count only the first nearest neighbors of the active site “*i*” and assume all neighbors to be equivalent. Conversely, \overline{CN} weights every neighbor “*j*” by their respective coordination number (*cn*(*j*)). Both \overline{CN} and *cn* span the range of 0-12, because the factor cn_{max} corresponds to the maximum number of first nearest neighbors in the bulk. Hence, for atop sites $cn_{max} = 12$. \overline{CN} was calculated for the five sites in this study by means of Equation S5 and the coordination number matrix in Table S5. For example for 4AD@Cu(111) we have: $\overline{CN} = \frac{(6 \times 2 + 10 \times 2 + 12 \times 1)}{12} = 3.67$.

Table S5. Coordination number matrix for the five Cu sites under study.

Site/coordination	3	4	5	6	7	8	9	10	11	12	<i>cn</i>	\overline{CN}
Cu(111)	0	0	0	0	0	0	6	0	0	3	9	7.50
Cu(100)	0	0	0	0	0	4	0	0	0	4	8	6.67
Cu(211)	0	0	0	0	2	0	9	1	0	2	7	5.50
4AD@Cu(100)	0	0	0	2	0	0	1	2	0	1	6	4.42

S6. Intermediates of the most favorable pathways

In the following, we show the intermediates of the most favorable pathways for the electroreduction of glyoxal to ethylene glycol (Figure S3) and ethanol (Figure S4).

- PLS₁ in Figure 3 corresponds to $*CHOHCHO + H^+ + e^- \rightarrow *CHOHCHOH$.

- PLS₂ corresponds to $*CHOHCHOH + H^+ + e^- \rightarrow *CHOHCH_2OH$.

- PLS₃ corresponds to $*CH_2CHO + H^+ + e^- \rightarrow *CH_3CHO$ (or $*CH_2CHO + H^+ + e^- \rightarrow *CH_3CHO$ if acetaldehyde is not adsorbed, see Table S4).

- PLS₄ corresponds to $*CH_3CHO + H^+ + e^- \rightarrow *CH_3CH_2O$ (or $*CH_3CHO + H^+ + e^- \rightarrow *CH_3CH_2O$, see Table S4).

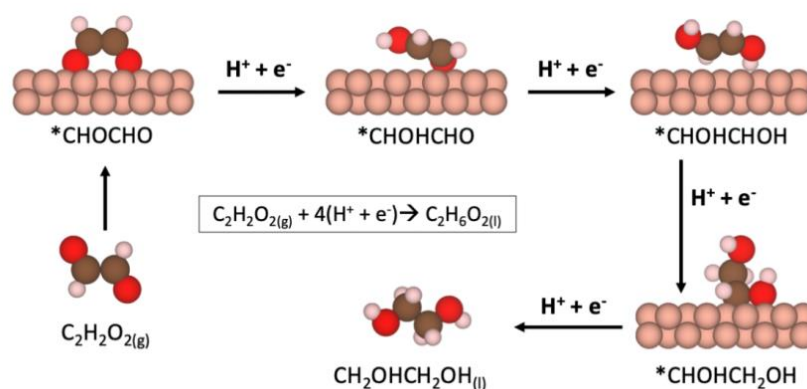


Figure S3. Most favorable electrocatalytic pathway for the GRR to ethylene glycol.

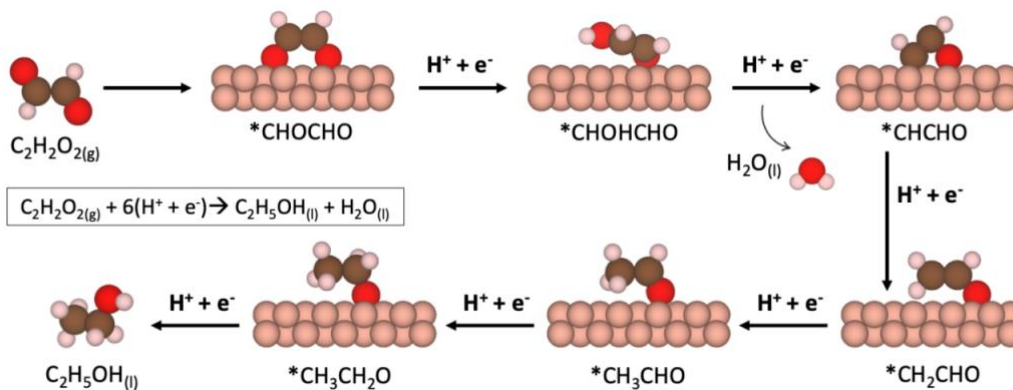


Figure S4. Most favorable electrocatalytic pathway for the GRR to ethanol.

Figures S5 and S6 show the free-energy diagrams corresponding to the pathways in Figures S3 and S4 on the five active sites under study.

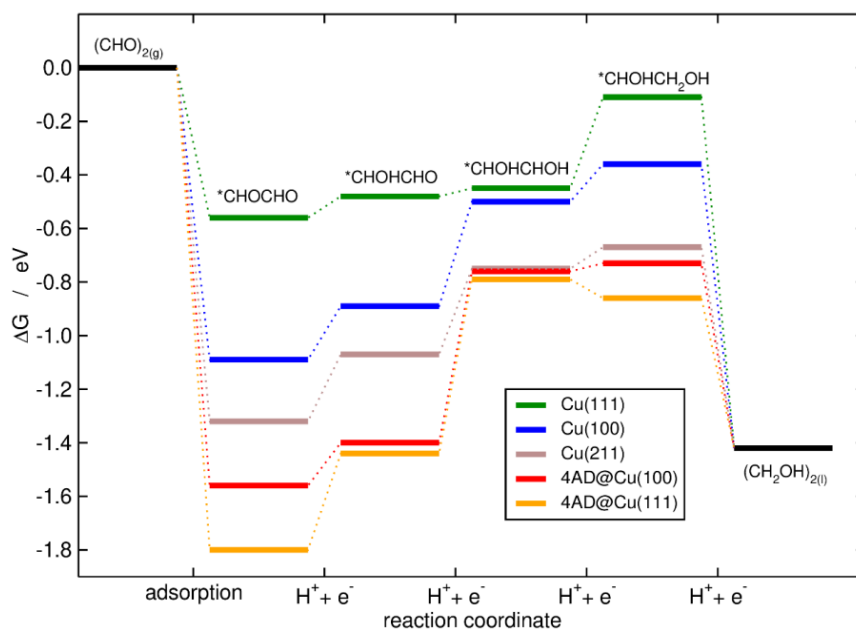


Figure S5. Free-energy diagrams at 0 V vs RHE of the most favorable pathway for glyoxal reduction to ethylene glycol on Cu(111) (green), Cu(100), Cu(211) (brown), 4AD@Cu(100) (red), and 4AD@Cu(111) (orange). The corresponding intermediates are noted for each electrochemical step. Figure S3 provides schematic views of the reaction intermediates.

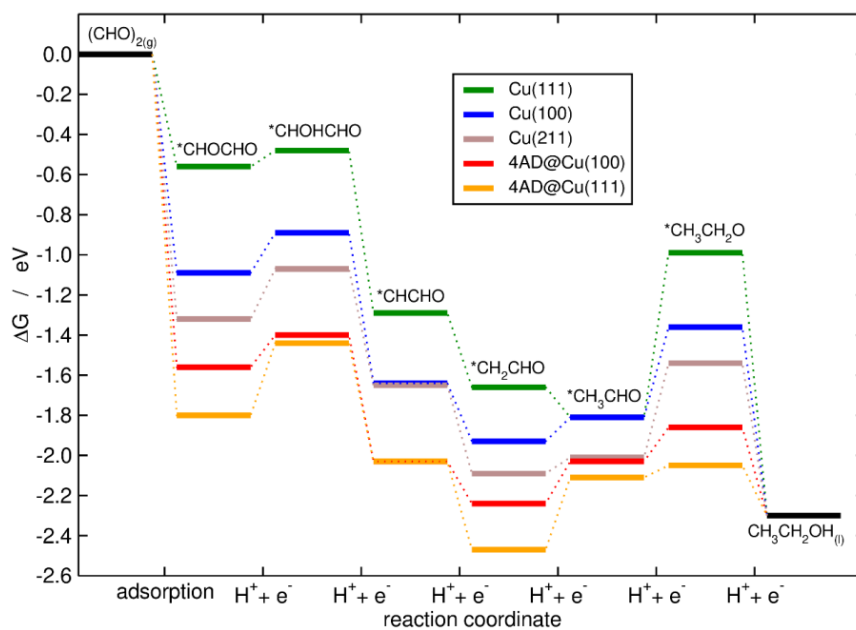


Figure S6. Free-energy diagrams at 0 V vs RHE for glyoxal reduction to ethanol on Cu(111) (green), Cu(100) (blue), Cu(211) (brown), 4AD@Cu(100) (red), and 4AD@Cu(111) (orange). The corresponding intermediates are noted for each electrochemical step. Figure S4 provides schematic views of the reaction intermediates.

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