

Electronic Supplementary Information

Spatial Disposition of Square-Planar Mononuclear Nodes in Metal-Organic Frameworks for C₂H₂/CO₂ Separation

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Methods

All reagents and solvents were obtained commercially and used as received without further purification. The ligand 5-(3-methyl-5-(pyridin-4-yl)-4H-1,2,4-triazol-4-yl)-1,3-benzenedicarboxylic acid (H₂MPTBDC) was purchased from Shanghai Tensus Bio-tech Co., Ltd. Ultrahigh-purity-grade N₂ (> 99.999%), C₂H₂ (> 99.9%), and CO₂ (> 99.99%) were purchased from Dalian Special Gases.

Preparation of JNU-4: A mixture of Cu(NO₃)₂·3H₂O (2.27 mmol, 468 mg), H₂MPTBDC (0.94 mmol, 306 mg), acetonitrile (CH₃CN, 60 mL), deionized water (H₂O, 30 mL), and 0.1 M nitric acid was placed in a sealed glass vial (350 mL) and heated at 120 °C for 12 h. After cooling to room temperature, the dark blue crystals (as-synthesized JNU-4) were collected and washed with methanol 10 times, then filtered and activated under high vacuum at room temperature for 24 hours to afford the activated JNU-4 (JNU-4a, 0.210 g, 67.7 % yield based on H₂MPTBDC). Analytically calculated (found) for (C₁₆H₁₀Cu₂N₄O₄)·H₂O: C, 41.12 % (41.08 %); H, 2.59 % (4.49 %); N, 11.99 % (11.78 %).

Gas adsorption measurements

At least 120 mg of sample was used for each measurement. JNU-4a was activated at room temperature under a dynamic vacuum (below 5 μm Hg) for 24 h. Further degassing and single-component adsorption/desorption at different temperatures were conducted on a Micromeritics ASAP 2020 PLUS Analyzer.

Single-crystal X-ray diffraction analysis

Single-crystal diffraction data of JNU-4 was collected at 100 K *via* an Oxford Cryo stream system on a XtaLAB PRO MM007-DW diffractometer system equipped with a RA-Micro7HF-MR-DW (Cu/Mo) X-ray generator and HyPix-6000HE hybrid photon counting X-ray detector (Rigaku, Japan, Cu Kα, λ = 1.5418 Å). The structures were solved and refined using Olex 2 with the ‘XS’ and ‘XL’ plugins.

PXRD analysis

PXRD data were collected by using microcrystalline samples on a Rigaku Ultima IV diffractometer (40 kV, 40 mA, Cu Kα, λ = 1.5418 Å). The measurement parameters include a scan speed of 10° min⁻¹, a step size of 0.02°, and a scan range of 2θ from 5° to 30°.

The isosteric heat of adsorption (Q_{st})

The isosteric heat of adsorption for C₂H₂ and CO₂ were calculated by using the gas adsorption data collected at three different temperatures. The adsorption isotherms were first fitted with the virial equation^[1]:

$$\ln P = \ln N + \frac{1}{T} \sum_{i=0}^m a_i N^i + \sum_{i=0}^n b_i N^i$$

Where N is gas uptake (in mg g⁻¹), P is pressure (in mmHg), a and b are virial coefficients, m and n are the numbers of coefficients required to adequately describe

the isotherm. The parameters that were obtained from the fitting of the C₂H₂ and CO₂ adsorption isotherms can be found in Figures S9 and S10. All isotherms were fitted with $R^2 > 0.99$.

The obtained parameters were used to calculate Q_{st} in the range of adsorption capacity through the virial equation, which is as follows:

$$Q_{st} = -R \sum_{i=0}^m a_i N^i$$

IAST calculations of adsorption selectivity

The fitting of C₂H₂ and CO₂ adsorption isotherms were carried out by using the dual-site Langmuir-Freundlich (DSLFF) model. Their corresponding fitting parameters are displayed in Table S1. The Ideal Adsorbed Solution Theory (IAST) of Myers and Prausnitz^[2] was applied to quantitatively estimate the adsorption selectivity for C₂H₂/CO₂ (50/50) mixture, respectively.

Dual-site Langmuir-Freundlich (DSLFF) model is listed as below:

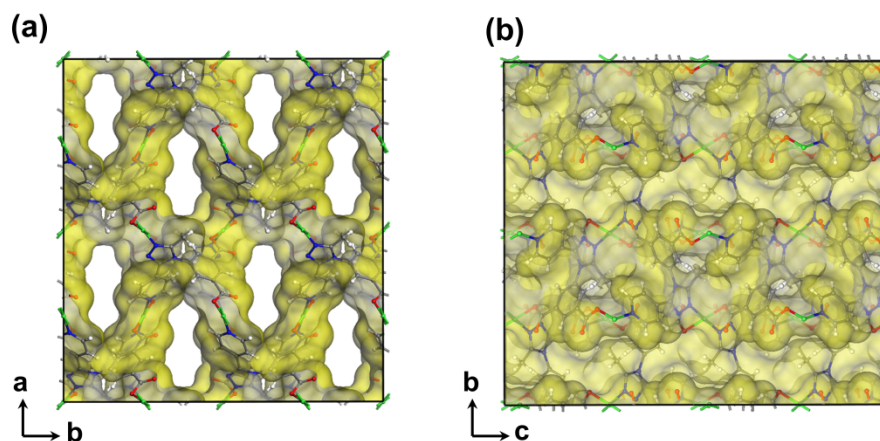
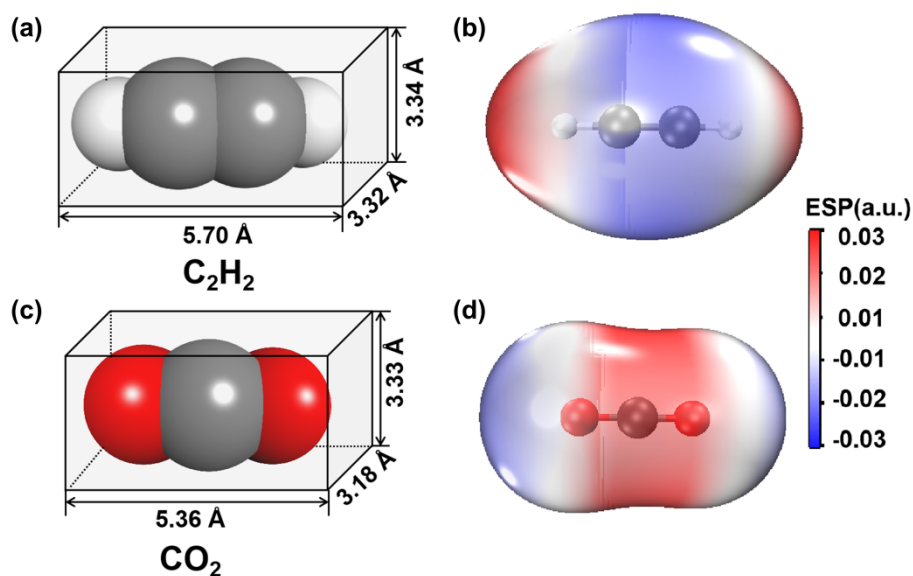
$$q = q_{A,sat} \frac{b_A P^{1/n_A}}{1 + b_A P^{1/n_A}} + q_{B,sat} \frac{b_B P^{1/n_B}}{1 + b_B P^{1/n_B}}$$

Where q is gas uptake (in mmol g⁻¹), P is pressure (in kPa), $q_{A,sat}$ and $q_{B,sat}$ are saturation uptakes (in mmol g⁻¹) for sites A and B, b_A and b_B are affinity coefficients (in kPa⁻¹) for sites A and B, and n_A and n_B represent the deviations from the ideal homogeneous surface for sites A and B. All isotherms were fitted with $R^2 > 0.999$.

Adsorption selectivity, S_{ads} , is defined for the separation of a binary mixture of component i and j as follows:

$$S_{ads} = \frac{q_i/q_j}{p_i/p_j}$$

where q_i and q_j represent the molar loadings of component i and j that is in equilibrium; p_i and p_j represent the partial pressures of component i and j in the bulk gas phase.



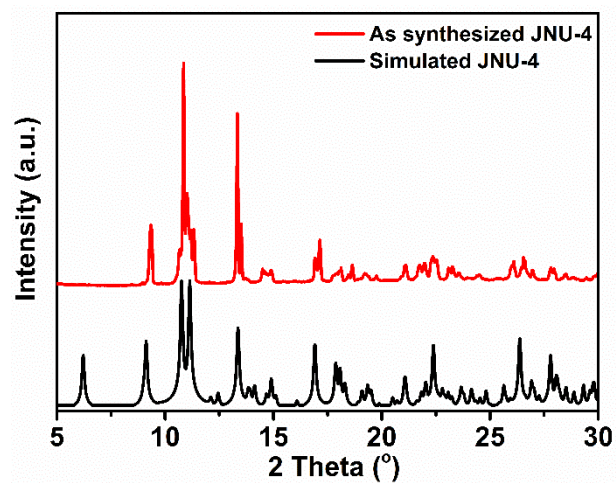


Figure S3. PXRD patterns of the simulated (black) and as-synthesized (red) JNU-4.

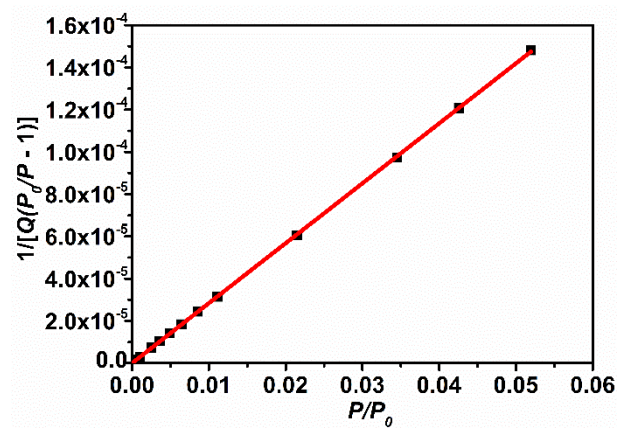


Figure S4. BET plot for surface area calculation.

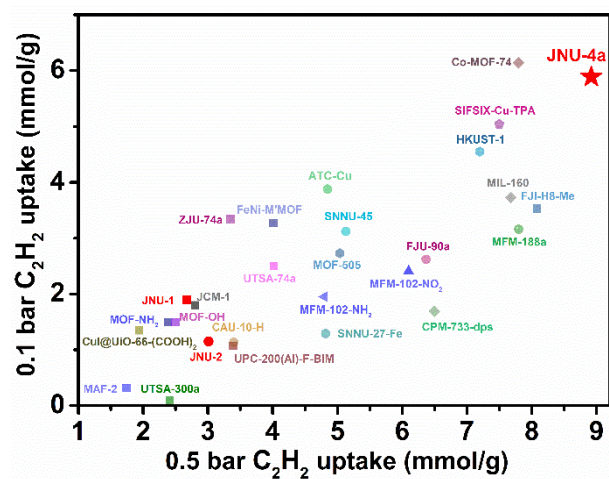


Figure S5. Comparison of C_2H_2 gravimetric capacity at 0.5 and 0.1 bar in JNU-4a and other porous materials at room temperature.

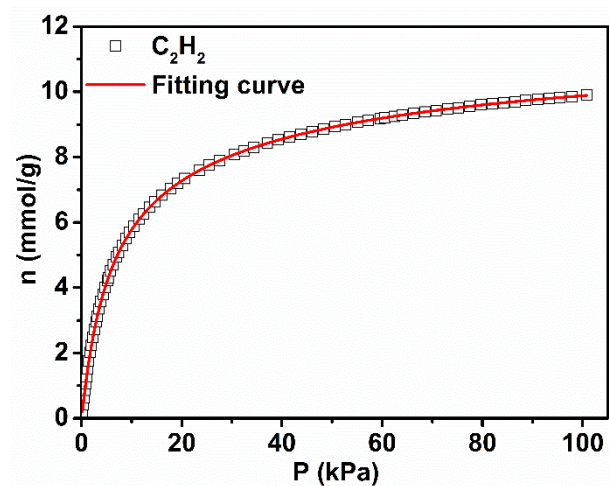


Figure S6. Dual-site Langmuir-Freundlich fitting of the C_2H_2 adsorption isotherm of JNU-4a at 298 K.

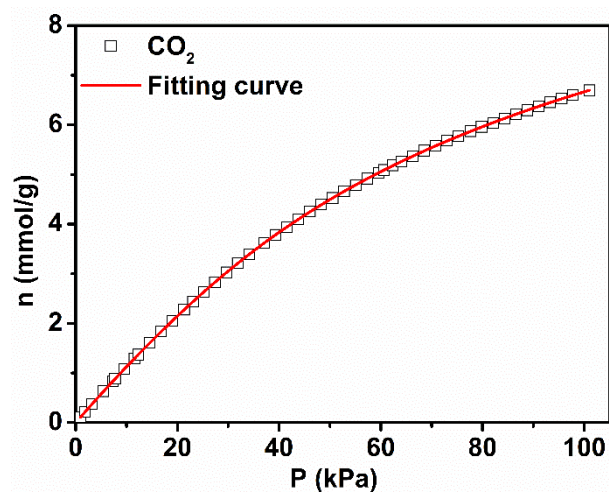


Figure S7. Dual-site Langmuir-Freundlich fitting of the CO₂ adsorption isotherm of JNU-4a at 298 K.

Table S1. Dual-site Langmuir-Freundlich parameters from the fitting of C₂H₂ and CO₂ adsorption isotherms of JNU-4a at 298 K. The R² values are also provided.

Parameter	C ₂ H ₂	CO ₂
q _{A,sat}	4.649	11.92
b _A	0.03131	0.00978
1/n _A	0.8948	1.018
q _{B,sat}	7.086	0.5649
b _B	0.1862	1.388E-4
1/n _B	1.068	2.476
R ²	0.9999	1

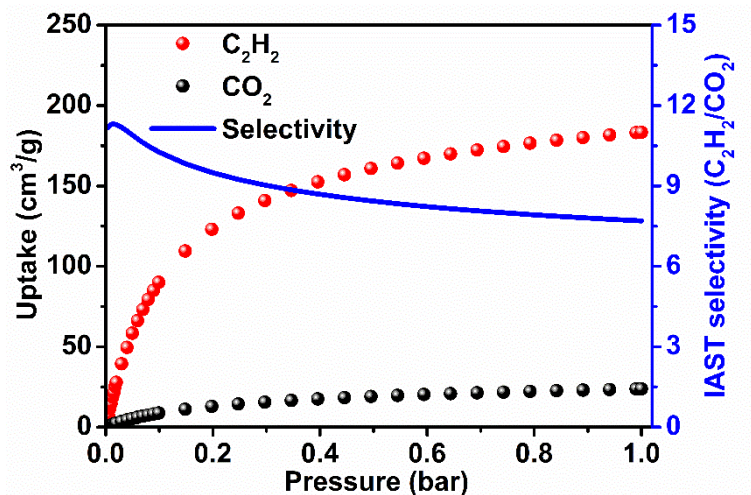


Figure S8. Predicted mixture adsorption isotherms and selectivity of JNU-4a predicted by the IAST method for a 50/50 C₂H₂/CO₂ mixture at 298 K.

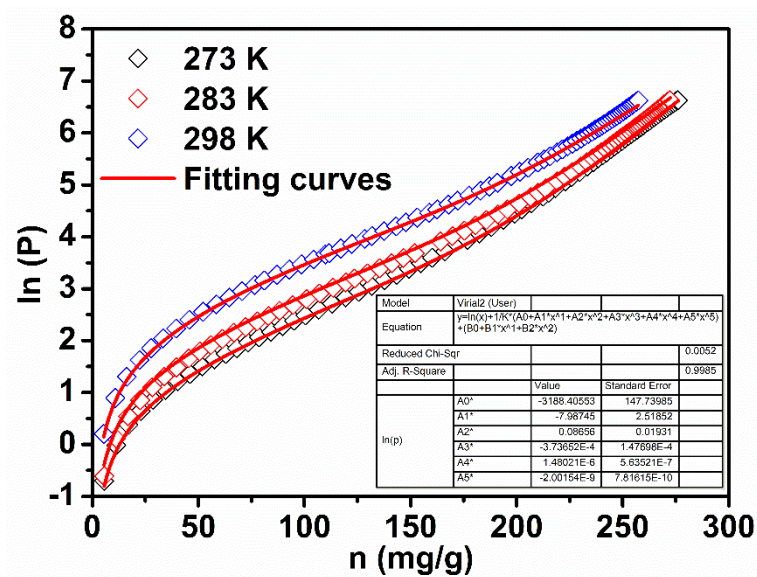


Figure S9. Virial equation fitting of the C₂H₂ adsorption isotherms of JNU-4a at 273, 283, and 298 K.

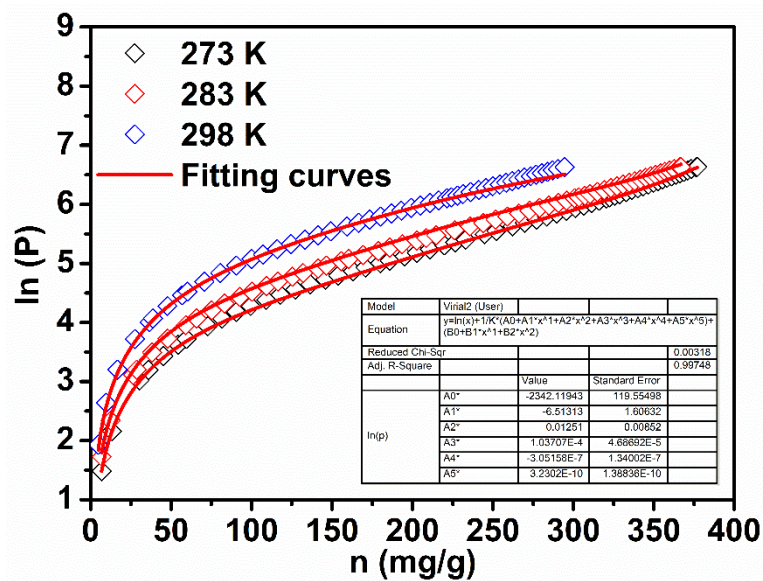


Figure S10. Virial equation fitting of the CO₂ adsorption isotherms of JNU-4a at 273, 283, and 298 K.

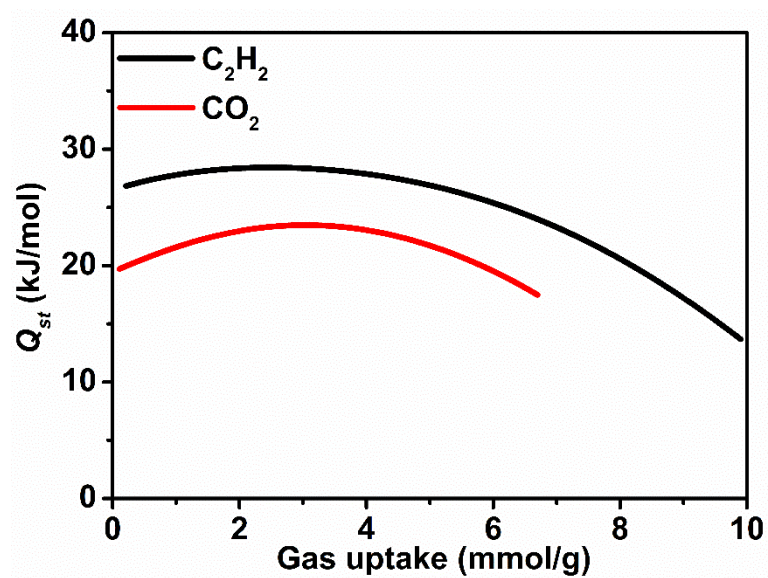


Figure S11. Calculated C₂H₂ and CO₂ adsorption enthalpy (Q_{st}) of JNU-4a.

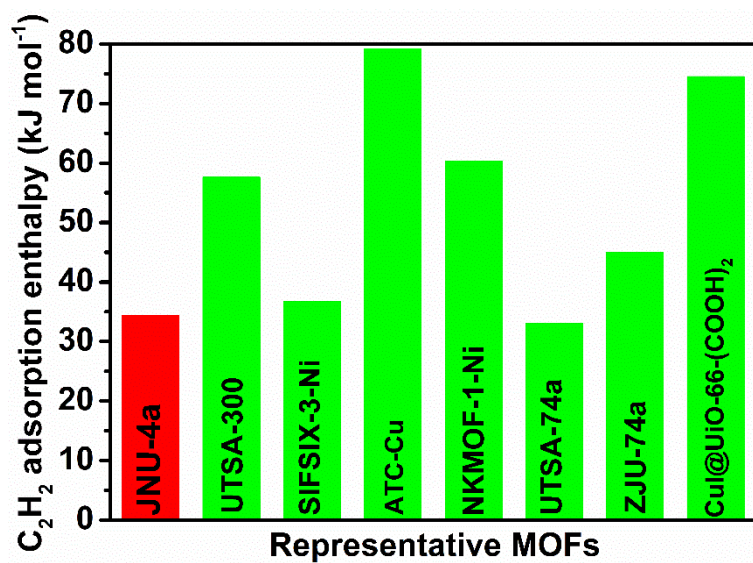


Figure S12. The maximum C₂H₂ adsorption enthalpy of JNU-4a and some selected high-performance MOFs.

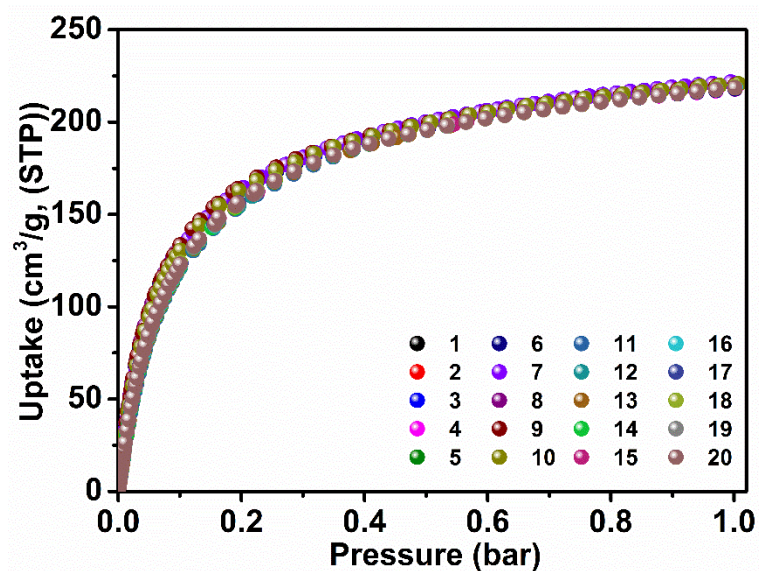


Figure S13. Continuous C₂H₂ adsorption measurements on JNU-4a at 298 K.

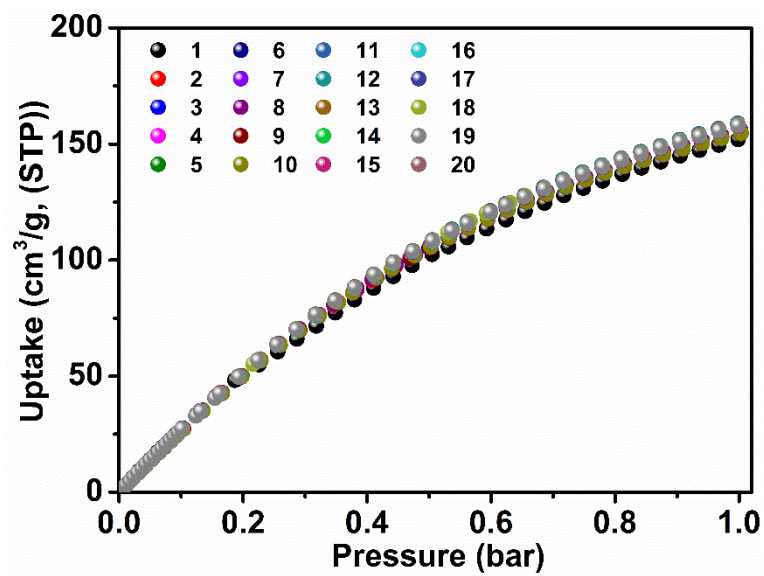


Figure S14. Continuous CO₂ adsorption measurements on JNU-4a at 298 K.

Theoretical Calculations

To better study the C₂H₂ adsorption and separation mechanism, Grand Canonical Monte Carlo (GCMC) simulations were performed to simulate the single-component adsorption of C₂H₂ and CO₂ on JNU-4a at 298 K and pressure up to 1 bar. The framework of JNU-4a was regarded as rigid during the simulation. The Lennard-Jones (LJ) parameters of JNU-4a were taken from the universal force field (UFF),^[6] whereas C₂H₂ and CO₂ molecules were obtained from literatures.^[7,8] The LJ parameters of different atom types were computed using the Lorentz-Berthelot mixing rules. The cut-off radius was chosen as 13 Å for the LJ potential, and the long-range electrostatic interactions were handled using Ewald summation technique. The equilibration steps and production steps were both set as 1.0×10^7 . The DDEC charges^[9] calculated by the Vienna ab initio simulation package (VASP),^{[10],[11]} were employed to the framework atoms. Perdew-Burke-Ernzerhof (PBE) functional with generalized gradient approximation (GGA) was used to evaluate the electron exchange correlation. The radial distribution functions $g(r)$ for host-guest atomic pairs at 298 K and 1 bar were further studied by Monte Carlo simulation in canonical (NVT) ensemble. All the simulations were performed by RASPA2 software.^{[12],[13]}

To further quantify the binding energies between framework and gas molecules, dispersion-corrected density functional theory (DFT-D) calculations were performed based on the cluster models extracted from the structures of JNU-4a. The truncated bonds of the cluster models were saturated with hydrogen atoms or methyl groups. All geometry optimizations were performed at the B3LYP-D3/6-31+G(d, p) level for the non-metal atoms.^[14-16] For Cu atom, the LanL2DZ basis set^[17] was used to consider the relativistic effects. Frequency analyses were performed at the same computational level to confirm local minima for each optimized structure. Based on the optimized geometries, these binding energies (ΔE) were corrected from the basis set superposition error (BSSE) by the counterpoise procedure.^[18] All these DFT-D calculations were accomplished using Gaussian 16 software.^[19]

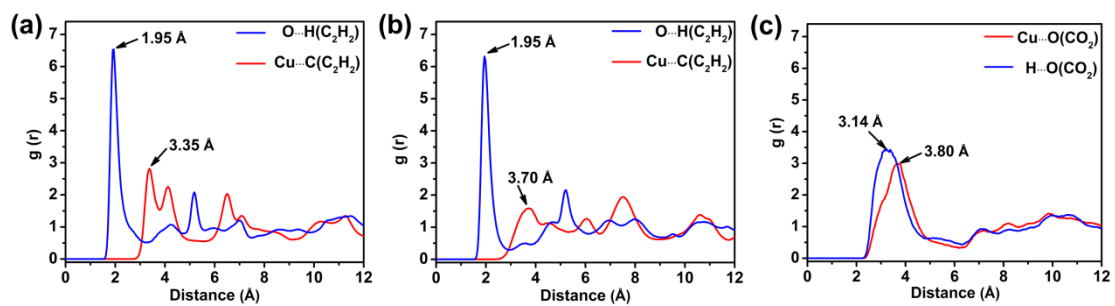


Figure S15. (a) Radial distribution function (RDF) of C_2H_2 at site I. (b) Radial distribution function (RDF) of C_2H_2 at site II. (c) Radial distribution function (RDF) of CO_2 at site I.

Column breakthrough experiments

The mixed-gas breakthrough separation experiments were conducted by using an in-house assembled system at 298 K and 1 bar (**Figure S16**). In a typical breakthrough experiment for C₂H₂/CO₂ (50:50) gas mixture, JNU-4a powder (0.82 g) was packed into a custom-made stainless-steel column (3.15 mm internal diameter × 450 mm long) with silica wool filling the void space. The sorbent was activated in-situ in the column with a high vacuum at 298 K for 24 h. After the activation process, a helium flow (50 mL min⁻¹) was introduced to purge the adsorbent. The flow of helium was then turned off and a gas mixture of C₂H₂/CO₂ (50:50) was allowed to flow into the column. Outlet effluent from the column was continuously monitored using gas chromatography (GC-7890B, Agilent) with a thermal conductivity detector (TCD). After the breakthrough experiment, the sample was regenerated in-situ in the column with a helium flow (100 mL min⁻¹) at 298 K for 6 h.

The completion of breakthrough was indicated by the downstream gas compositions reaching those in the feed gas. On the basis of the mass balance, the gas adsorption capacities can be determined as follows:^[20]

$$q_i = \frac{C_i V}{22.4 \times m} \times \int_0^t \left(1 - \frac{F}{F_0}\right) dt$$

Where q_i is the equilibrium adsorption capacity of gas i (mmol g⁻¹), C_i is the feed gas concentration, V is the volumetric feed flow rate (mL min⁻¹), t is the adsorption time (min), F_0 and F are the inlet and outlet gas molar flow rates, respectively, and m is the mass of the adsorbent (g). The separation factor (α) of the breakthrough experiment is determined as:

$$\alpha = \frac{q_A y_B}{q_B y_A}$$

in which y_i is the molar fraction of gas i ($i = A, B$) in the gas mixture.

The C₂H₂ purity (c) is defined by the peak area of C₂H₂, we calculated C₂H₂ purity according to the following equation:

$$c = \frac{C_i(\text{C}_2\text{H}_2)}{C_i(\text{C}_2\text{H}_2) + C_i(\text{CO}_2)}$$

where $C_i(\text{CO}_2)$ and $C_i(\text{C}_2\text{H}_2)$ represent the peak areas of component CO₂ and C₂H₂ in a single injection.

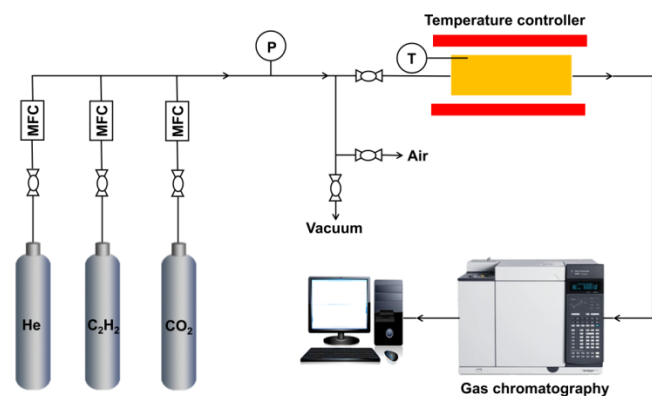


Figure S16. Schematic illustration of the setup for breakthrough experiments.

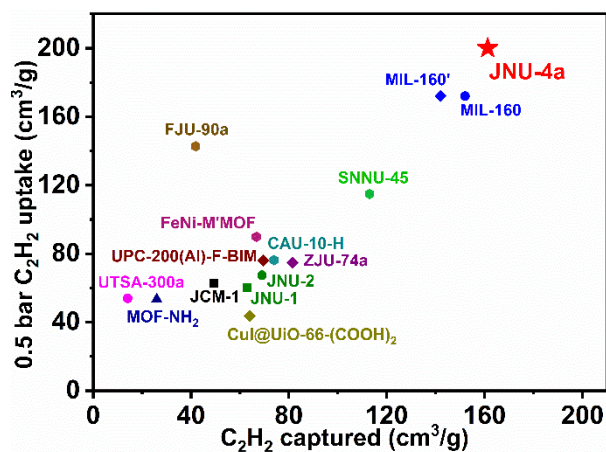


Figure S17. Comparison of the estimated amount of C_2H_2 captured on breakthrough column for an equimolar mixture of C_2H_2/CO_2 (JNU-4a and other top-performing materials).

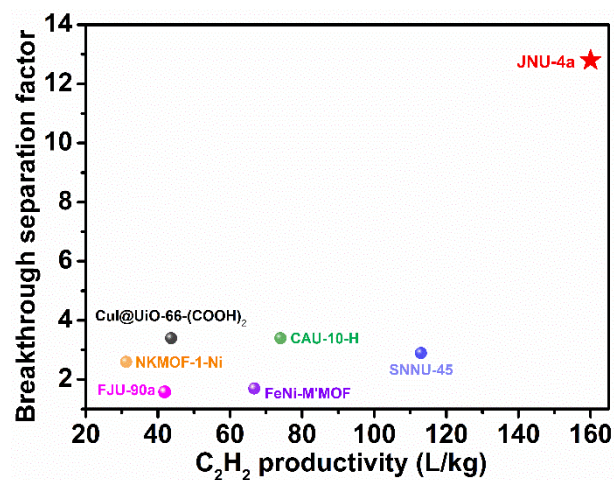


Figure S18. Comparison of the estimated amount of C_2H_2 captured and separation factor on breakthrough column for an equimolar mixture of C_2H_2/CO_2 in JNU-4a and other top-performing materials.

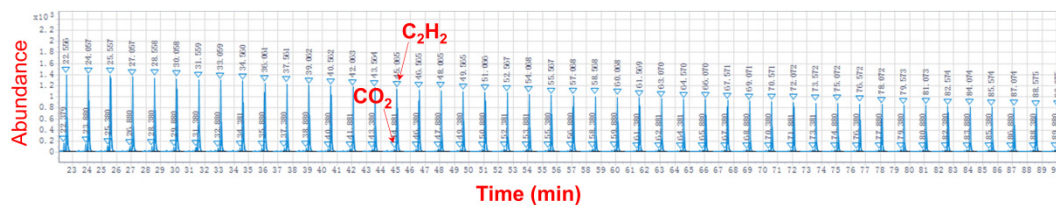


Figure S19. Desorption curve and its corresponding GC chromatogram for JNU-4a with $\text{C}_2\text{H}_2/\text{CO}_2$ (50/50, 4 mL min^{-1}) as feed gas.

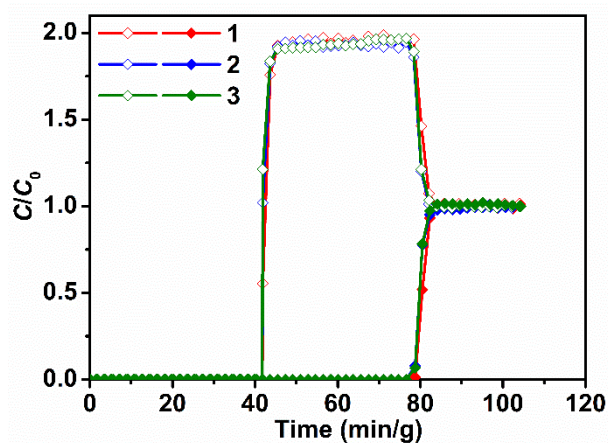


Figure S20. Breakthrough curves (from 1 to 3) for a $\text{C}_2\text{H}_2/\text{CO}_2$ (50:50) mixture flowing through a fixed column packed with JNU-4a at 298 K (flowrate: 4 mL min^{-1}).

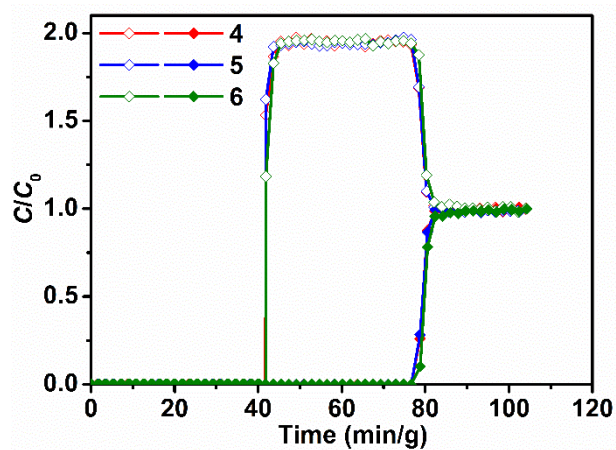


Figure S21. Breakthrough curves (from 4 to 6) for a C_2H_2/CO_2 (50:50) mixture flowing through a fixed column packed with JNU-4a at 298 K (flowrate: 4 mL min^{-1}).

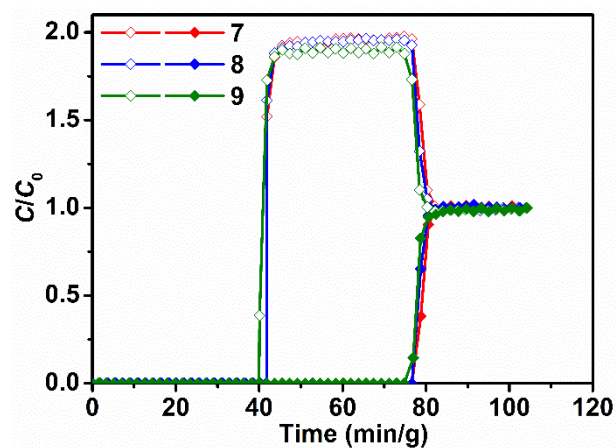


Figure S22. Breakthrough curves (from 7 to 9) for a C_2H_2/CO_2 (50:50) mixture flowing through a fixed column packed with JNU-4a at 298 K (flowrate: 4 mL min^{-1}).

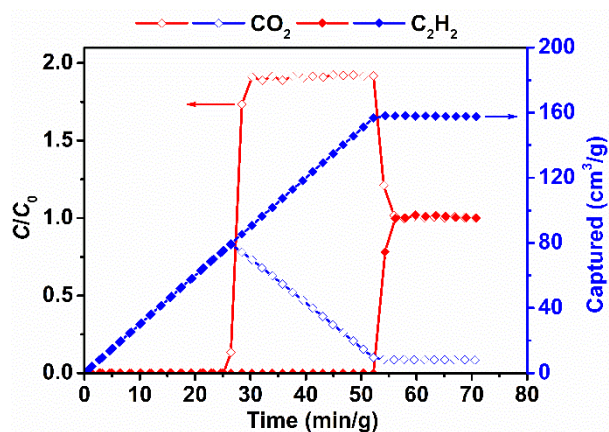


Figure S23. Breakthrough curves (left y -axis) of C_2H_2 and CO_2 on JNU-4a for an equimolar mixture of $\text{C}_2\text{H}_2/\text{CO}_2$ (6.0 mL min^{-1}) at 298 K. Empty squares depict the estimated amount of C_2H_2 and CO_2 captured on breakthrough column (right y -axis).

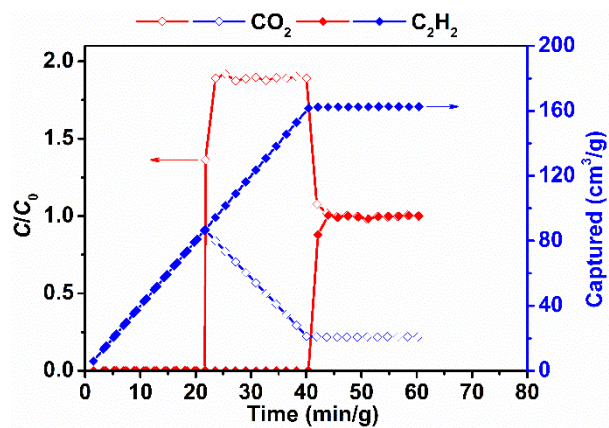


Figure S24. Breakthrough curves (left y -axis) of C_2H_2 and CO_2 on JNU-4a for an equimolar mixture of $\text{C}_2\text{H}_2/\text{CO}_2$ (8.0 mL min^{-1}) at 298 K. Empty squares depict the estimated amount of C_2H_2 and CO_2 captured on breakthrough column (right y -axis).

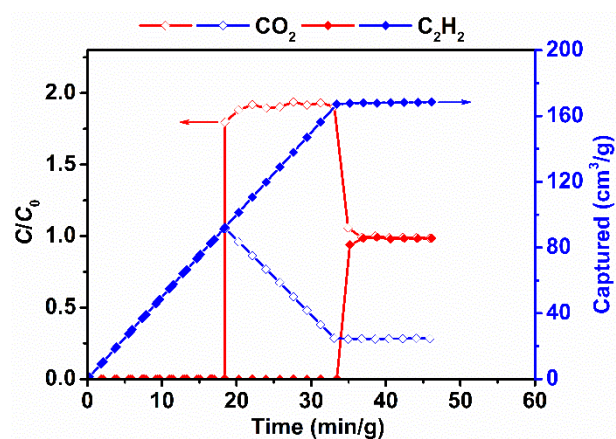


Figure S25. Breakthrough curves (left y-axis) of C₂H₂ and CO₂ on JNU-4a for an equimolar mixture of C₂H₂/CO₂ (10.0 mL min⁻¹) at 298 K. Empty squares depict the estimated amount of C₂H₂ and CO₂ captured on breakthrough column (right y-axis).

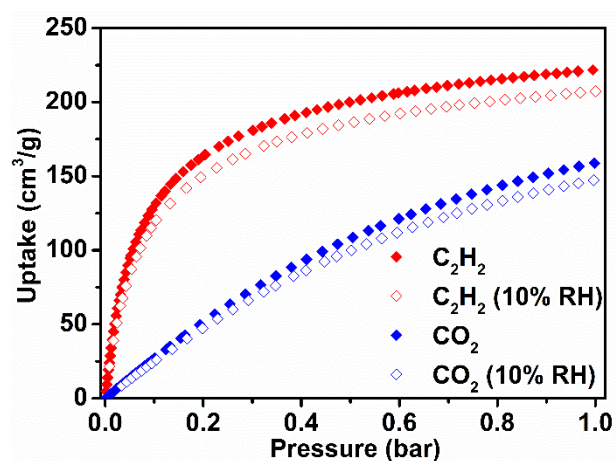


Figure S26. Adsorption isotherms of C₂H₂ (red) and CO₂ (blue) at 298 K and up to 1 bar under dry (0% RH) and humid conditions (10% RH).

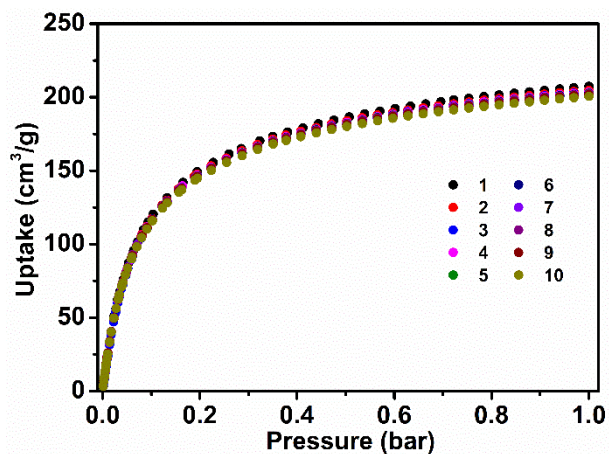


Figure S27. (a) Continuous adsorption measurements of C₂H₂ with 10% RH on JNU-4a at 298 K.

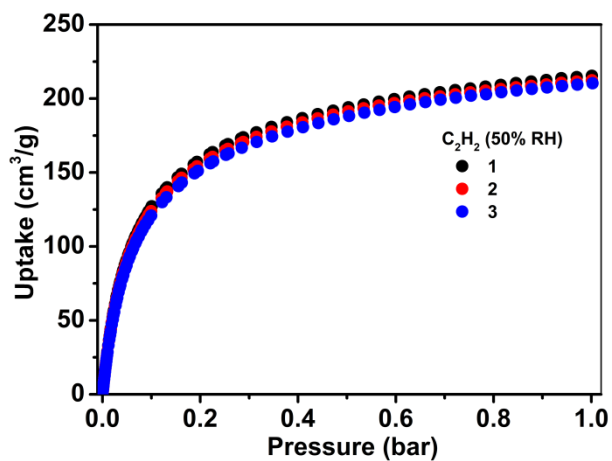


Fig. S28. Three consecutive adsorption measurements of C₂H₂ on JNU-4a under 50% RH at 298 K.

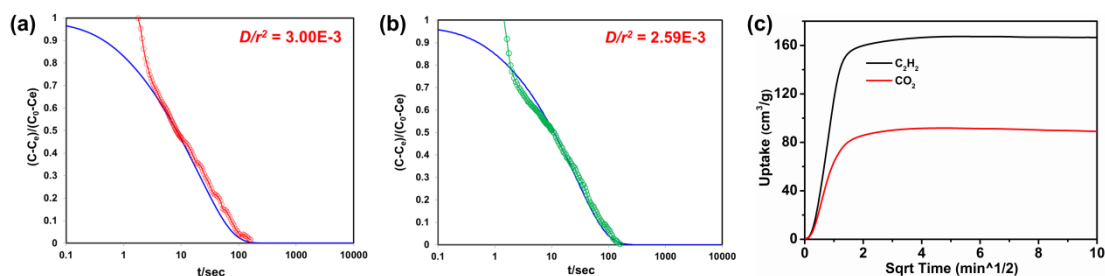


Fig. S29. Calculated diffusion rate constants of (a) C_2H_2 and (b) CO_2 in JNU-4a at 298 K, data were collected on a BEL MAX II sorption analyzer and fitted automatically with BEL-Master software according to the Crank theory. (c) Time-dependent C_2H_2 and CO_2 gravimetric adsorption on JNU-4a at 298 K, data were collected on a thermogravimetric analyzer (TGA) at a flow rate of 50 mL min^{-1} and 1.0 bar.

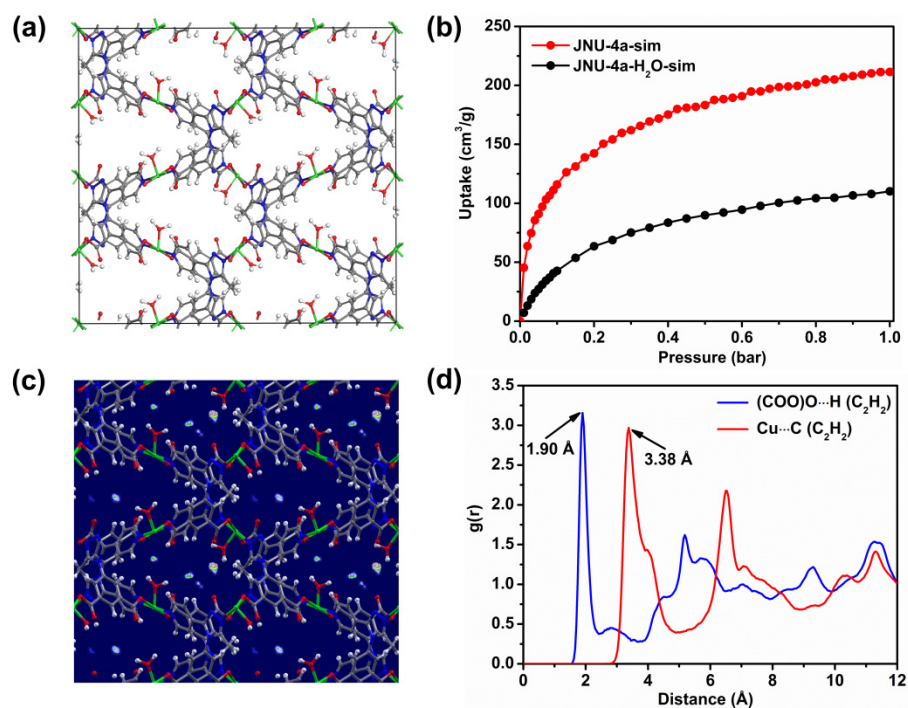


Fig. S30. (a) Crystal structure of JNU-4a- H_2O built by using the Forcite module embedded in Materials Studio 2018 (MS 2018). (b) Simulated C_2H_2 adsorption isotherms of JNU-4a and JNU-4a- H_2O at 298 K and up to 1 bar. (c) GCMC simulated adsorption density distributions of C_2H_2 in JNU-4a- H_2O at 298 K and 1 bar. (d) Radial distribution function (RDF) of C_2H_2 in JNU-4a- H_2O .

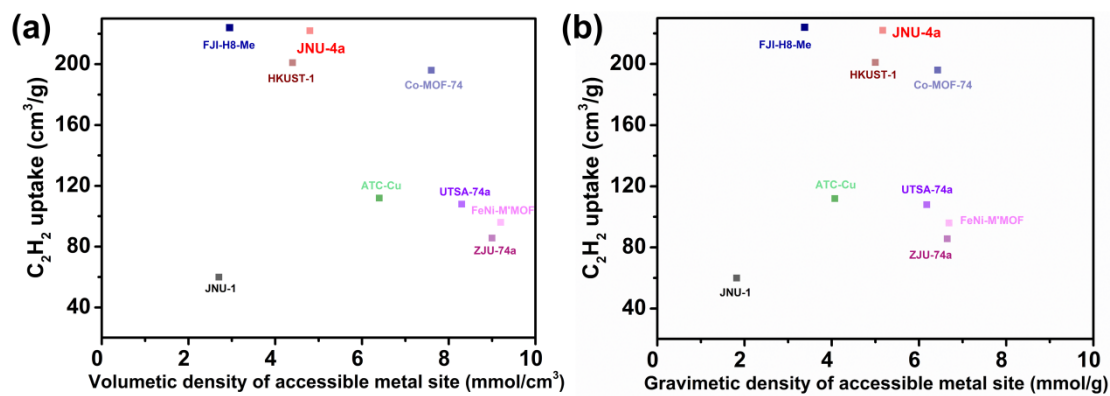


Fig. S31. Comparison of the (a) volumetric density and (b) gravimetric density of OMSs and C_2H_2 uptake in JNU-4a and some selected porous materials at room temperature.

Table S2. Summary of the adsorption capacity and Q_{st} of C_2H_2 and CO_2 , as well as captured amount of C_2H_2 from 50:50 C_2H_2/CO_2 mixture in some selected MOFs (reorganized from refs. 21-37).

MOFs	C_2H_2 uptake (mmol/g)	CO_2 uptake (mmol/g)	Q_{st} of C_2H_2 (kJ/mol)	Q_{st} of CO_2 (kJ/mol)	Captured amount of C_2H_2	Ref
JCM-1	3.35	1.70	36.9	33.4	2.2	[21]
JNU-1	2.68	–	13-47.6	–	2.81	[22]
MAF-2	3.125	0.85	29.8-33.7	25.8-26.9	–	[23]
UTSA-74a	4.82	3.0	31	25	–	[24]
UTSA-300a	3.1	0.183	57.6	–	0.63	[25]
MFM-188	10.35	5.36	32.5	21	–	[26]
SIFSIX-3-Ni	3.3	2.7	36.7	50.9	–	[27]
MOF-NH ₂	2.67	1.4	17.6	24.2	1.16	[28]
MOF-OH	3.04	1.2	16.8	20.6	1.25	[28]
ZJU-74a	3.83	3.02	65	32	3.64	[29]
UPC-200(Al)- F-BIM	6.45	2.48	20.5	–	3.1	[30]
CuI@UiO-66- COOH	2.31	0.93	74.5	28.9	2.89	[31]
FJI-H8-Me	10.2	4.73	33.70	21.77	–	[32]
SNNU-27-Fe	8.14	2.92	24.1	19.8	–	[33]
CAU-10-H	4.01	2.68	27	–	3.3	[34]
ATC-Cu	5.01	4.02	79.1	–	–	[35]
FJU-90a	8.04	4.6	25.1	20.7	1.87	[36]
SNNU-45	6.0	4.35	40	27	5.04	[33]
FeNi-M' MOF	4.29	2.72	27 ~ 32.8	24.5	2.98	[37]
MIL-160	8.53	4.01	31.8	26.9	6.8	[38]
JNU-4a	9.82	7.1	13.7 ~ 28.4	17.5 ~ 23.4	7.1	This work

Table S3. Crystal data of JNU-4.

JNU-4	
Temperature	100 K
Formula	C ₁₆ H ₁₀ CuN ₄ O ₄ [+ Solvent]
CCDC number	2160960
Space group	<i>P</i> 2 ₁ /c
Crystal system	monoclinic
a (Å)	14.23(1)
b (Å)	13.23(1)
c (Å)	14.62(2)
α (deg)	90
β (deg)	93.15(1)
γ (deg)	90
V (Å)³	2751.90(5)
Z	4
ρ calcg/cm³	1.336
μ/mm⁻¹	1.557
Final R	R1=0.1134
[I>2σ(I)]	wR1=0.2955
GooF	1.049
Completeness	100%

Table S4. Summary of C₂H₂ adsorption capacity from a 50:50 C₂H₂/CO₂ mixture in some selected MOFs and their respective experimental parameters.

Material	Column size (D × L, mm)	Flow rate (mL/min)	Packing density	Temperature (°C)	Adsorption capacity (cm³/g)
JNU-4a	3.15 × 450	4	–	25	160
MIL-160	4 × 150	2	–	25	152
FeNi-M²MOF	4 × 150	2	–	25	66.7
CuI@UiO-66-(COOH)₂	4.6 × 100	2	–	25	64.7
ZJU-74	4 × 120	2	–	25	81.5
SNNU-45	40 × 120	4	–	25	112.8
UPC-200(Al)- F-BIM	–	4	–	25	69
CAU-10-H	4 × 90	2	–	25	74

Table S5. Comparison of the volumetric density of OMSs and C₂H₂ uptake in JNU-4a and some other MOFs.

MOF	Formula	Formula weight (g mol ⁻¹)	Density (g cm ⁻³)	Volumetric density of OMSs (mmol cm ⁻³)	Gravimetric density of OMSs (mmol g ⁻³)	C ₂ H ₂ uptake (cm ³ g ⁻¹)
JNU-1	Zn ₃ C ₁₄ H ₈ N ₆ O ₆	552.4	1.484	2.7	1.82	60
FJI-H8	CuC _{11.5} H _{5.5} O _{5.5}	295	0.873	2.95	3.38	224
HKUST-1	Cu ₃ C ₁₈ H ₆ O ₁₂	604.87	0.879	4.4	5.0	201
JNU-4a*	CuC ₁₆ H ₁₀ N ₄ O ₄	385.5	0.928	4.8	5.17	222 (This work)
ATC-Cu	CuC ₉ H ₇ O	242.69	1.571	6.4	4.07	112
Co-MOF-74	Co ₂ C ₈ H ₂ O ₆	311.96	1.181	7.6	6.43	196
UTSA-74a*	Zn ₂ C ₈ H ₂ O ₆	324.88	1.342	8.3	6.18	108
ZJU-74*	NiC ₈ H ₄ CoN ₆	301.81	1.353	9.0	6.65	85.7
FeNiM'MOF*	FeNiC ₈ H ₄ N ₆	298.70	1.375	9.2	6.69	96

*Note that every open metal center in these MOFs have two accessible sites.

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