

Supplementary material to "Evaluation of the potential use of e-fuels in the European aviation sector: A comprehensive economic and environmental assessment including externalities."

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Contents

Abbreviations	2
Appendix A e-fuel composition and main properties	3
Appendix B LCA inventories	4
Appendix C Data for the economic evaluation	7
Appendix D LCA results at midpoint level	9
References	11

This document is divided into four appendixes, including critical data used in the calculations and some intermediate results as explained hereafter. In Appendix A, the design parameters of the Fischer-Tropsch (*FT*) and hydrocracking (*HC*) processes are given, along with the simulation results of a basic characterisation of e-jet fuel, including the weight-based distribution, density, net heating value (*NHV*), boiling point, flash point and freezing point, compared with standard values for conventional jet fuel A-1. Appendix B includes the life-cycle inventory (*LCI*) utilised for the *LCA* of green H₂ and e-jet fuels, the combustion factors for the fuels and additional information regarding the particular processes not included in Ecoinvent 3.5. Appendix C provides the information required for the economic assessment of green H₂ and e-jet fuels, *i.e.*, economic parameters and assumptions, equipment cost data, and costs of raw materials, utilities and by-products. Finally, in Appendix D, the *ReCiPe* 2016 *LCA* results at the midpoint level of the studied e-jet fuels are provided.

Abbreviations

α	Chain growth probability	ACC	Annualised capital cost
AP	Annual production	APOS	Allocation at the point of substitution
ASF	Anderson-Schulz-Flory	BAU	Business as usual
BECCS	Bioenergy with carbon capture and storage/sequestration	BOP	Balance of plant
CCU	Carbon capture and utilisation	CAPEX	Capital expenditure
CF	Capacity factor	CEPCI	Chemical engineering plant cost index
DE	Germany	D	Scaling factor
ES	Spain	EQ	Ecosystems quality
FR	France	FCI	Fixed capital investment
GB	United Kingdom	FT	Fischer-Tropsch
HC	Hydrocracking	GWP	Global warming potential
HI	Heat integration	HH	Human health
i	Interest rate	HRAT	Heat recovery approach temperature
LCA	Life cycle assessment	IT	Italy
NHV	Net heating value	MCC	Mortality cost of carbon emissions
OPEX	Operational expenditure	NPC	Net production cost
PEM	Polymer electrolyte membrane	PC	Purchased cost of equipment
PR-BM	Peng-Robinson equation of state with Boston-Mathias alpha function	PEMEL	PEM electrolyser
PV	Photovoltaic	PtF	Power-to-fuels
rWGS	Reverse water-gas shift	PtL	Power-to-liquids
SCC	Social cost of carbon emissions	RS	Resource scarcity
TCI	Total capital investment	S	Actual size of equipment
TRL	Technology readiness level	t	Plant economic life
y	Year	TOC	Total operating cost
		WC	Working capital

Appendix A e-fuel composition and main properties

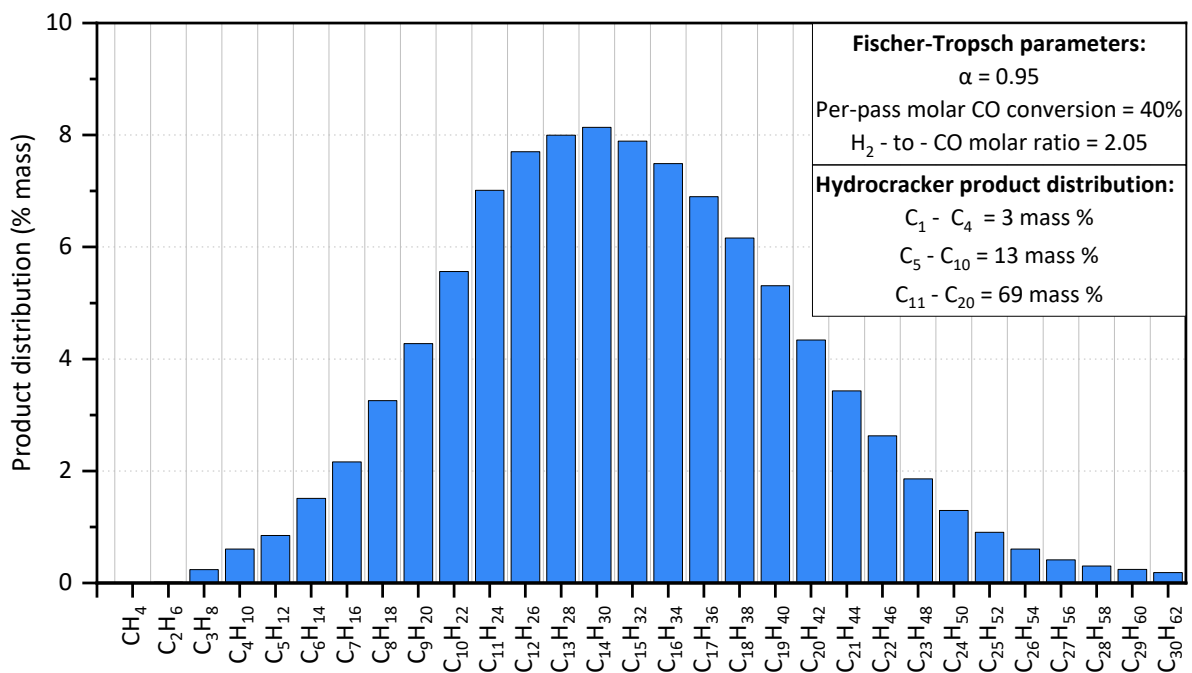


Fig. A-1: Mass-based product distribution.

Table A-1. Properties of conventional jet fuel A-1 and e-jet fuel.

Properties	e-jet fuel (from simulation)	Jet fuel A-1 (according to ASTM D7566)
Density @ 15°C (kg/m ³)	758.1	775-840
NHV (MJ/kg)	43.73	> 42.8
Average boiling point (°C)	229.35	150 to 300
Flash point (°C)	39.12	> 38
Freezing point (°C)	-51.6	Max. -47

Appendix B LCA inventories

Table B-1. Inventory data of the foreground system for the production of e-jet fuel after heat integration.

Products				
<i>Outputs to technosphere: Products and co-products</i>	Amount	Unit		
e-jet fuel	5.20×10 ⁸	kg		
Inputs				
<i>Inputs from nature</i>	Amount	Unit	Distribution	2SD
Air (for burner)	1.00×10 ⁹	kg	Lognormal	1.09
<i>Inputs from technosphere: materials/fuels</i>				
Water, deionised, from tap water	6.01×10 ⁸	kg	Lognormal	1.09
H ₂ from electrolysis including storage (see Table B-3)	2.51×10 ⁸	kg	Lognormal	1.09
Captured CO ₂ (see Table B-4)	1.95×10 ⁹	kg	Lognormal	1.09
rWGS: nickel-based catalyst ^{1,2}	9.68×10 ²	kg	Lognormal	1.09
FT: cobalt-based catalyst ^{3,4}	7.34×10 ²	kg	Lognormal	1.09
HC: platinum-based catalyst ^{5,6}	1.15×10 ³	kg	Lognormal	1.09
Steel, chromium steel 18/8, with 70% end-life recycling ⁷	4.04×10 ⁶	kg	Lognormal	1.09
<i>Inputs from technosphere: electricity/heat</i>				
Electricity, high voltage, market for	1.01×10 ⁶	MWh	Lognormal	1.09
Cooling water ⁸	2.03×10 ⁶	MWh	Lognormal	1.09
Outputs				
<i>Emissions to air</i>				
Water	1.09×10 ⁸	kg	Lognormal	1.51
Hydrogen	9.43×10 ¹	kg	Lognormal	1.51
Carbon monoxide	4.23×10 ³	kg	Lognormal	5.01
Oxygen	3.88×10 ⁷	kg	Lognormal	1.51
Carbon dioxide, process	3.50×10 ⁸	kg	Lognormal	1.09
<i>Outputs to technosphere: Waste treatment</i>				
Wastewater, market for	2.42×10 ⁶	m ³	Lognormal	1.09
Catalysts, used	2.35×10 ⁷	kg	Lognormal	1.09

Table B-2. Emission factors for the combustion of e-jet fuel and fossil jet fuel.

	Feedstock/Product	Fossil fuel emissions ⁹	e-jet fuel emissions*	Unit
CO ₂	Product	3.16	3.09	kg CO ₂ /kg fuel
H ₂ O	Product	1.24	1.21	kg H ₂ O /kg fuel
NO _x	Product	1.00	0.98	kg NO _x /kg fuel
CO	Product	1.75	1.71	kg CO/kg fuel
Air (24 wt.% O ₂)	Feedstock	14.17	13.84	kg air/kg fuel

* From the carbon balance of the components in the e-jet fuel product stream

Table B-3. Inventory data of the foreground system per kilogram of H₂ (30 bar) based on the results of the gAWE model for each location.

Products	GB	DE	FR	ES	IT	
<u>Outputs to technosphere: Products and co-products</u>						
	Amount	Amount	Amount	Amount	Amount	Unit
H ₂ from electrolysis	1	1	1	1	1	kg
O ₂ from electrolysis	7.94	7.94	7.94	7.94	7.94	kg
Inputs						
<u>Inputs from technosphere: materials/fuels</u>						
Water, deionised, from tap water	8.94	8.94	8.94	8.94	8.94	kg
H ₂ storage required (Type I tanks ^{10,11} or salt caverns ^{12,+})	0.0128	0.0265	0.01429	0.0238	0.0207	kg
<u>Inputs from technosphere: electricity/heat</u>						
Electricity, photovoltaic, open ground installation*	9.41	25.22	20.21	14.75	30.12	kWh
Electricity, wind, >3MW turbine*	46.89	31.08	36.09	41.55	26.18	kWh

* *Here, only the electricity consumption for compression and drying is considered

* We assume a current energy demand for water electrolysis of 56.3 kWh/kg H₂ (59% efficiency) ^{13,14}

Table B-4. Inventory data of the foreground system per kilogram of captured CO₂ (1 bar) for each source.

Products	C-PP¹⁵	NG-PP¹⁶	DAC-HT¹⁷	DAC-LT¹⁸	
<u>Outputs to technosphere: Products and co-products</u>					
	Amount	Amount	Amount	Amount	Unit
Captured CO ₂	1	1	1	1	kg
<u>Outputs to technosphere: Avoided products</u>					
Electricity, high voltage, production	0.88	3.29			kWh
Inputs					
<u>Inputs from nature</u>					
Air		20193.55			g
Cooling water, unspecified natural origin		1451.61			g
<u>Inputs from technosphere: materials/fuels</u>					
Light fuel oil, market for	6.22				g
Natural gas liquids, market for	0.82	478.45	125.00		g
Hard coal, market for	521.09				g
Monoethanolamine, market for	1.54	8.77			g
Neutralising agent, sodium hydroxide-equivalent, market for	0.12				g
Ammonia, liquid, market for	1.15				g
Limestone, crushed, washed, market for	43.12				g
Tap water, market for		1064.52	3105.26		g
Spent catalyst, market for		0.0029			g
Calcium carbonate, precipitated, market for			19.88		g
Adsorbent (Amine on alumina) ¹⁸				7.5	g
<u>Inputs from technosphere: electricity/heat</u>					
Electricity, high voltage, production mix			0.2340	0.7	kWh
Heat, district or industrial, municipal waste incinerat., market for				11.9	MJ
Outputs					
<u>Emissions to air</u>					
Particulates, < 2.5 um	0.11				g
Ammonia	0.27				g
Monoethanolamine	0.09	3.52			g
Nitrogen oxides	1.06	1.58			g
Sulfur dioxide	0.07				g
Carbon dioxide, fossil	52.44	328.65	-1000	-1000	g
Water		1645.16			g
<u>Outputs to technosphere: Waste treatment</u>					
Hazardous waste, treatment, underground deposit	2.27				g
Municipal solid waste, treatment, open dump	1.81				g
Wastewater, market for		0.0016			m ³
Spent catalyst, treatment		0.0029			g

Appendix C Data for the economic evaluation

Table C-1. Economic parameters and assumptions.

Parameter	Value				
	<i>GB</i> (56, -6)	<i>DE</i> (48, 12)	<i>FR</i> (48, 0)	<i>ES</i> (40, -6)	<i>IT</i> (40, 18)
Location (latitude, longitude)	<i>GB</i> (56, -6)	<i>DE</i> (48, 12)	<i>FR</i> (48, 0)	<i>ES</i> (40, -6)	<i>IT</i> (40, 18)
Base year	2018	2018	2018	2018	2018
Plant economic life (y) ¹⁹⁻²¹	20	20	20	20	20
Plant availability (h/y) ²²	8260	8260	8260	8260	8260
Interest rate (%) ²³	8.30%	6.80%	7.20%	8.20%	7.20%

Table C-2. H₂ production plant: Cost input data.

Equipment	Sizing based on:	USD ₂₀₁₈ per size unit	Reference
Photovoltaic (PV) solar panels	1 kW installed capacity	1210	²⁴
Wind turbines onshore	1 kW installed capacity	1497	²⁴
Wind turbines offshore	1 kW installed capacity	4353	²⁴
<i>PEMEL</i>	1 kg/h H ₂	56300	¹⁴
Electrical energy storage: Lithium-ion batteries	1 kWh electricity	418	²⁵
H ₂ storage: Type I tanks	1 kg H ₂	755	¹¹
H ₂ storage: Salt caverns	1 kg H ₂	215	²⁶

Table C-3. Fuel production plant: CAPEX of special equipment cost data.

Equipment	PC _{ref}	Unit	S _{ref}	Design variable	Unit	D	Reference year	Reference
Burner	2.62	MUSD	20.00	Heat duty	MW	0.83	2014	²²
Hydrocracker	10.36	MUSD	1.13	Feed rate	kg/s	0.70	2014	²²
<i>rWGS</i> reactor	3.19	MUSD	2556.00	Flowrate	t/day	0.65	2014	²²
<i>FT</i> reactor	10.50	MUSD	2.52	Feed rate	Mscf/h	0.72	2003	²⁷

Table C-4. Fuel processing plant: OPEX data at 2018 prices.

Raw material/Utility	Value for 2018	Unit	Reference
CO ₂ from <i>C-PP</i>	0.0043	USD ₂₀₁₈ /kg	²⁸
CO ₂ from <i>NG-PP</i>	0.064	USD ₂₀₁₈ /kg	²⁸
CO ₂ from <i>DAC-HT</i>	0.16	USD ₂₀₁₈ /kg	¹⁷
CO ₂ from <i>DAC-LT</i>	1.10	USD ₂₀₁₈ /kg	²⁹
Grid electricity (Non-household consumers) (<i>GB</i>)	158.67	USD ₂₀₁₈ /MWh	³⁰
Grid electricity (Non-household consumers) (<i>DE</i>)	127.68	USD ₂₀₁₈ /MWh	³⁰
Grid electricity (Non-household consumers) (<i>FR</i>)	62.18	USD ₂₀₁₈ /MWh	³⁰
Grid electricity (Non-household consumers) (<i>ES</i>)	103.16	USD ₂₀₁₈ /MWh	³⁰

Grid electricity (Non-household consumers) (IT)	110.72	USD ₂₀₁₈ /MWh	30
Process H ₂ O	1.09	USD ₂₀₁₈ /t	19
Cooling water	1.35	USD ₂₀₁₈ /MWh	31
Wastewater disposal	0.44	USD ₂₀₁₈ /t	19

Appendix D LCA results at midpoint level

Table D-1. e-jet fuel from CO₂ from coal-based power plants (C-PP).

Impact category	Unit	GB		DE		FR		ES		IT	
		Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns
Global warming	kg CO ₂ eq	3.361	3.357	4.446	4.437	2.806	2.802	2.780	2.772	3.731	3.725
Stratospheric ozone depletion	mg CFC-11 eq	1.488	0.709	1.926	0.320	1.586	0.719	1.991	0.549	1.925	0.671
Ionising radiation	kBq Co-60 eq	0.992	0.459	1.532	0.435	1.885	1.293	1.440	0.454	1.133	0.275
Ozone formation, Human health	g NO _x eq	5.864	4.775	12.083	9.838	4.399	3.187	0.217	-1.800	6.818	5.064
Fine particulate matter formation	g PM _{2.5} eq	2.497	1.221	9.365	6.733	2.071	0.650	-0.756	-3.122	4.571	2.515
Ozone formation, Terrestrial ecosystems	g NO _x eq	6.476	4.902	13.312	10.069	5.105	3.354	1.248	-1.666	7.813	5.280
Terrestrial acidification	g SO ₂ eq	2.551	1.985	18.432	17.265	0.270	-0.360	-9.511	-10.559	6.177	5.265
Freshwater eutrophication	g P eq	2.108	1.509	4.895	3.661	2.141	1.475	2.530	1.421	2.772	1.808
Marine eutrophication	g N eq	0.258	0.159	0.523	0.319	0.296	0.186	0.344	0.160	0.359	0.200
Terrestrial ecotoxicity	kg 1,4-DCB	33.511	25.618	60.430	44.160	41.791	33.006	41.302	26.682	51.056	38.348
Freshwater ecotoxicity	kg 1,4-DCB	1.012	0.952	1.169	1.045	0.968	0.902	1.024	0.913	0.941	0.844
Marine ecotoxicity	kg 1,4-DCB	1.265	1.181	1.492	1.319	1.220	1.127	1.289	1.133	1.199	1.063
Human carcinogenic toxicity	kg 1,4-DCB	0.147	0.183	0.298	0.373	0.192	0.232	0.110	0.177	0.203	0.262
Human non-carcinogenic toxicity	kg 1,4-DCB	8.383	6.300	13.386	9.093	8.794	6.476	9.975	6.117	10.207	6.854
Land use	m ² a crop eq	0.340	0.230	0.694	0.468	0.427	0.305	0.413	0.210	0.593	0.417
Mineral resource scarcity	g Cu eq	29.064	26.630	40.239	35.222	32.950	30.241	31.602	27.094	34.753	30.834
Fossil resource scarcity	kg oil eq	1.103	0.823	1.682	1.105	1.004	0.693	1.240	0.722	1.411	0.961
Water consumption	m ³	0.039	0.025	0.086	0.058	0.058	0.042	0.056	0.030	0.082	0.060

Table D-2. e-jet fuel from CO₂ from natural gas-based power plants (NG-PP).

Impact category	Unit	GB		DE		FR		ES		IT	
		Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns
Global warming	kg CO ₂ eq	3.651	3.647	3.770	3.761	0.751	0.746	1.833	1.825	2.636	2.629
Stratospheric ozone depletion	mg CFC-11 eq	0.981	0.202	1.736	0.130	-0.356	-1.222	0.768	-0.674	0.775	-0.479
Ionising radiation	kBq Co-60 eq	1.000	0.468	1.552	0.454	1.902	1.309	1.449	0.462	1.150	0.293
Ozone formation, Human health	g NO _x eq	5.009	3.920	5.996	3.751	1.717	0.505	4.412	2.395	4.695	2.942
Fine particulate matter formation	g PM _{2.5} eq	6.020	4.744	7.745	5.113	4.977	3.556	7.005	4.640	6.918	4.862
Ozone formation, Terrestrial ecosystems	g NO _x eq	5.772	4.199	7.224	3.981	2.458	0.707	5.527	2.613	5.690	3.157
Terrestrial acidification	g SO ₂ eq	12.239	11.673	12.446	11.279	7.769	7.139	11.739	10.690	11.695	10.783
Freshwater eutrophication	g P eq	2.235	1.637	4.812	3.578	2.113	1.447	2.579	1.470	2.737	1.773
Marine eutrophication	g N eq	0.381	0.282	0.637	0.433	0.407	0.297	0.457	0.274	0.472	0.313
Terrestrial ecotoxicity	kg 1,4-DCB	34.334	26.442	60.509	44.239	42.772	33.987	42.134	27.515	51.341	38.633
Freshwater ecotoxicity	kg 1,4-DCB	1.023	0.963	1.167	1.044	0.967	0.900	1.030	0.919	0.940	0.844
Marine ecotoxicity	kg 1,4-DCB	1.268	1.183	1.484	1.311	1.208	1.115	1.296	1.140	1.197	1.061
Human carcinogenic toxicity	kg 1,4-DCB	0.209	0.245	0.300	0.375	0.194	0.234	0.154	0.221	0.207	0.266
Human non-carcinogenic toxicity	kg 1,4-DCB	8.545	6.462	13.319	9.026	8.784	6.466	10.043	6.185	10.183	6.829
Land use	m ² a crop eq	0.323	0.214	0.673	0.447	0.406	0.284	0.393	0.190	0.572	0.396
Mineral resource scarcity	g Cu eq	30.165	27.731	40.769	35.752	32.925	30.217	31.281	26.773	35.119	31.201
Fossil resource scarcity	kg oil eq	0.662	0.382	0.826	0.249	-0.249	-0.561	0.143	-0.376	0.619	0.168
Water consumption	m ³	0.037	0.023	0.084	0.055	0.052	0.037	0.066	0.040	0.082	0.060

Table D-3. e-jet fuel from CO₂ from direct air capture based on a high temperature, liquid solvent system (DAC-HT).

Impact category	Unit	GB		DE		FR		ES		IT	
		Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns
Global warming	kg CO ₂ eq	2.806	2.802	3.980	3.971	1.838	1.834	2.321	2.314	3.160	3.154
Stratospheric ozone depletion	mg CFC-11 eq	1.952	1.173	3.799	2.193	1.958	1.091	2.593	1.151	3.117	1.863
Ionising radiation	kBq Co-60 eq	1.162	0.630	1.659	0.561	2.423	1.831	1.615	0.628	1.156	0.298
Ozone formation, Human health	g NO _x eq	7.588	6.499	9.605	7.360	5.730	4.518	8.628	6.610	8.937	7.184
Fine particulate matter formation	g PM _{2.5} eq	6.329	5.052	8.538	5.906	5.436	4.015	7.871	5.506	8.037	5.981
Ozone formation, Terrestrial ecosystems	g NO _x eq	8.253	6.680	10.884	7.641	6.481	4.730	9.711	6.796	9.990	7.457
Terrestrial acidification	g SO ₂ eq	13.299	12.733	15.417	14.250	9.265	8.635	13.878	12.829	15.449	14.537
Freshwater eutrophication	g P eq	2.367	1.768	5.650	4.416	2.107	1.441	2.713	1.605	2.844	1.880
Marine eutrophication	g N eq	0.264	0.165	0.567	0.363	0.289	0.179	0.341	0.158	0.355	0.196
Terrestrial ecotoxicity	kg 1,4-DCB	34.860	26.967	61.090	44.820	43.490	34.706	42.928	28.309	52.037	39.329
Freshwater ecotoxicity	kg 1,4-DCB	1.027	0.967	1.191	1.067	0.969	0.902	1.037	0.926	0.946	0.850
Marine ecotoxicity	kg 1,4-DCB	1.288	1.204	1.523	1.349	1.222	1.128	1.309	1.152	1.207	1.071
Human carcinogenic toxicity	kg 1,4-DCB	0.218	0.254	0.342	0.417	0.200	0.241	0.173	0.240	0.219	0.277
Human non-carcinogenic toxicity	kg 1,4-DCB	8.704	6.622	13.984	9.691	8.864	6.546	10.230	6.372	10.356	7.002
Land use	m ² a crop eq	0.356	0.246	0.689	0.463	0.410	0.288	0.404	0.201	0.589	0.412
Mineral resource scarcity	g Cu eq	30.209	27.776	41.543	36.526	34.367	31.659	32.942	28.434	36.181	32.263
Fossil resource scarcity	kg oil eq	1.385	1.105	1.896	1.319	1.115	0.803	1.454	0.936	1.636	1.185
Water consumption	m ³	0.057	0.043	0.106	0.077	0.077	0.061	0.075	0.049	0.106	0.084

Table D-4. e-jet fuel from CO₂ from direct air capture based on a low temperature, solid sorbent system (DAC-LT)

Impact category	Unit	GB		DE		FR		ES		IT	
		Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns	Tanks	Caverns
Global warming	kg CO ₂ eq	3.954	3.950	5.495	5.487	2.978	2.973	4.011	4.004	5.296	5.290
Stratospheric ozone depletion	mg CFC-11 eq	3.681	2.902	6.091	4.485	5.674	4.807	4.250	2.808	5.481	4.227
Ionising radiation	kBq Co-60 eq	1.572	1.039	1.940	0.843	3.545	2.952	1.962	0.976	1.238	0.380
Ozone formation, Human health	g NO _x eq	11.401	10.312	12.325	10.080	11.231	10.019	16.747	14.730	15.725	13.972
Fine particulate matter formation	g PM _{2.5} eq	8.435	7.159	10.015	7.383	8.384	6.963	11.579	9.214	12.984	10.928
Ozone formation, Terrestrial ecosystems	g NO _x eq	12.081	10.508	13.624	10.381	12.012	10.261	17.862	14.948	16.833	14.300
Terrestrial acidification	g SO ₂ eq	19.376	18.810	20.204	19.037	18.195	17.565	24.626	23.578	31.201	30.289
Freshwater eutrophication	g P eq	2.831	2.232	7.696	6.462	2.234	1.567	3.013	1.905	3.175	2.211
Marine eutrophication	g N eq	0.365	0.267	0.768	0.564	0.381	0.271	0.430	0.247	0.448	0.289
Terrestrial ecotoxicity	kg 1,4-DCB	37.484	29.591	65.701	49.431	48.821	40.037	47.145	32.525	58.360	45.652
Freshwater ecotoxicity	kg 1,4-DCB	1.055	0.995	1.276	1.152	0.983	0.916	1.055	0.943	0.969	0.872
Marine ecotoxicity	kg 1,4-DCB	1.334	1.250	1.642	1.468	1.245	1.151	1.336	1.180	1.242	1.107
Human carcinogenic toxicity	kg 1,4-DCB	0.281	0.317	0.474	0.549	0.238	0.278	0.220	0.288	0.267	0.326
Human non-carcinogenic toxicity	kg 1,4-DCB	9.694	7.611	16.599	12.305	9.425	7.107	10.867	7.009	11.145	7.792
Land use	m ² a crop eq	0.865	0.755	0.859	0.634	0.725	0.603	0.883	0.680	1.012	0.836
Mineral resource scarcity	g Cu eq	35.555	33.121	56.095	51.078	39.635	36.926	36.310	31.802	40.673	36.754
Fossil resource scarcity	kg oil eq	1.930	1.651	2.034	1.457	1.249	0.937	1.678	1.160	2.046	1.595
Water consumption	m ³	0.055	0.041	0.107	0.078	0.102	0.087	0.103	0.077	0.151	0.129

References

- 1 R. Frazier, E. Jin and A. Kumar, Life Cycle Assessment of Biochar versus Metal Catalysts Used in Syngas Cleaning, *Energies*, 2015, **8**, 621–644.
- 2 N. Laosiripojana, W. Sutthisripok and S. Assabumrungrat, Synthesis gas production from dry reforming of methane over CeO₂ doped Ni/Al₂O₃, *Chemical Engineering Journal*, 2005, **112**, 13–22.
- 3 N. Jungbluth, R. Frischknecht, Faist Emmenegger, M., Steiner, R. and M. Tuchschnid, Life Cycle Assessment of BTL-fuel production: Inventory Analysis., 2007.
- 4 K. Ibrik, Kinetics of the Fischer-Tropsch Reaction Over Alumina Supported Cobalt Catalyst in a Slurry Reactor, *Qatar Foundation Annual Research Forum Proceedings*, 2011, EGPS2.
- 5 T. Hengsawad, C. Srimingkwanchai, S. Butnark, D. E. Resasco and S. Jongpatiwut, Effect of Metal–Acid Balance on Hydroprocessed Renewable Jet Fuel Synthesis from Hydrocracking and Hydroisomerization of Biohydrogenated Diesel over Pt-Supported Catalysts, *Industrial & Engineering Chemistry Research*, 2018, **57**, 1429–1440.
- 6 Y. Liu, K. Murata, K. Okabe, M. Inaba, I. Takahara, T. Hanaoka and K. Sakanishi, Selective hydrocracking of fischer-tropsch waxes to high-quality diesel fuel over pt-promoted polyoxocation-pillared montmorillonites, *Topics in Catalysis*, 2009, **52**, 597–608.
- 7 R. D. Pehlke, in *Encyclopedia of materials*, ed. K. H. J. Buschow, Elsevier, Amsterdam, New York, 2001, pp. 8824–8832.
- 8 Aspen Technology, AspenTech: Knowledge Base, https://esupport.aspentech.com/S_Article?id=000067208, (accessed 6 January 2020).
- 9 H. Nojumi, I. Dincer and G. F. Naterer, Greenhouse gas emissions assessment of hydrogen and kerosene-fueled aircraft propulsion, *International Journal of Hydrogen Energy*, 2009, **34**, 1363–1369.
- 10 N. Belmonte, C. Luetto, S. Staulo, P. Rizzi and M. Baricco, Case Studies of Energy Storage with Fuel Cells and Batteries for Stationary and Mobile Applications, *Challenges*, 2017, **8**, 9.
- 11 V. Tietze, S. Luhr and D. Stolten, in *Hydrogen Science and Engineering : Materials, Processes, Systems and Technology*, ed. P. D. Stolten and D. B. Emonts, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim, Germany, 2016, pp. 659–690.
- 12 C. Wulf, M. Reuß, T. Grube, P. Zapp, M. Robinus, J.-F. Hake and D. Stolten, Life Cycle Assessment of hydrogen transport and distribution options, *Journal of Cleaner Production*, 2018, **199**, 431–443.
- 13 D. J. Jovan and G. Dolanc, Can Green Hydrogen Production Be Economically Viable under Current Market Conditions, *Energies*, 2020, **13**, 6599.
- 14 C. Ganzer and N. Mac Dowell, A comparative assessment framework for sustainable production of fuels and chemicals explicitly accounting for intermittency, *Sustainable Energy Fuels*, 2020. DOI: 10.1039/C9SE01239G.
- 15 D. Iribarren, F. Petrakopoulou and J. Dufour, Environmental and thermodynamic evaluation of CO₂ capture, transport and storage with and without enhanced resource recovery, *Energy*, 2013, **50**, 477–485.
- 16 F. Petrakopoulou, D. Iribarren and J. Dufour, Life-cycle performance of natural gas power plants with pre-combustion CO₂ capture, *Greenhouse Gas Sci Technol*, 2015, **5**, 268–276.
- 17 D. W. Keith, G. Holmes, D. St. Angelo and K. Heidel, A Process for Capturing CO₂ from the Atmosphere, *Joule*, 2018, **2**, 1573–1594.
- 18 S. Deutz and A. Bardow, Life-cycle assessment of an industrial direct air capture process based on temperature–vacuum swing adsorption, *Nat Energy*, 2021, **6**, 203–213.
- 19 S. Michailos, S. McCord, V. Sick, G. Stokes and P. Styring, Dimethyl ether synthesis via captured CO₂ hydrogenation within the power to liquids concept, *Energy Conversion and Management*, 2019, **184**, 262–276.
- 20 B. V. Mathiesen, I. Ridjan, D. Connolly, M. P. Nielsen, P. V. Hendriksen, M. B. Mogensen, S. H. Jensen and S. D. Ebbesen, *Technology data for high temperature solid oxide electrolyser cells, alkali and PEM electrolysers. Technology data for high temperature solid oxide electrolyser cells, alkali and PEM electrolysers*, Department of Development and Planning, Aalborg University 978-87-91404-46-7 [Add to Citavi project by ISBN], 2013.
- 21 M. Carmo, D. L. Fritz, J. Mergel and D. Stolten, A comprehensive review on PEM water electrolysis, *International Journal of Hydrogen Energy*, 2013, **38**, 4901–4934.
- 22 F. G. Albrecht, D. H. König, N. Baucks and R.-U. Dietrich, A standardized methodology for the techno-economic evaluation of alternative fuels – A case study, *Fuel*, 2017, **194**, 511–526.
- 23 P. Fernandez, M. Martinez and I. Fernández Acín, Market Risk Premium and Risk-Free Rate Used for 69 Countries in 2019: A Survey, *SSRN Journal*, 2019. DOI: 10.2139/ssrn.3358901.
- 24 E. Asmelash and Prakash, Gayathri, Kadir, Maisarah, Wind and Solar PV – what we need by 2050, 2020.
- 25 O. Schmidt, S. Melchior, A. Hawkes and I. Staffell, Projecting the Future Levelized Cost of Electricity Storage Technologies, *Joule*, 2019, **3**, 81–100.

- 26 J. Speirs, P. Balcombe, E. Johnson, J. Martin, N. Brandon and A. Hawkes, A greener gas grid: What are the options, *Energy Policy*, 2018, **118**, 291–297.
- 27 L. Hoseinzade and T. A. Adams, Techno-economic and environmental analyses of a novel, sustainable process for production of liquid fuels using helium heat transfer, *Applied Energy*, 2019, **236**, 850–866.
- 28 E. S. Rubin, J. E. Davison and H. J. Herzog, The cost of CO₂ capture and storage, *International Journal of Greenhouse Gas Control*, 2015, **40**, 378–400.
- 29 H. J. Herzog, Direct air capture: A process engineer's view, 2021.
- 30 Eurostat, Electricity prices for non-household consumers, https://ec.europa.eu/eurostat/databrowser/view/nrg_pc_205/default/table?lang=en, (accessed 9 January 2022).
- 31 R. Turton, *Analysis, synthesis, and design of chemical processes*, Prentice Hall, Boston, 5th edn., 2018.