Supporting Information for

Atomically Ordered Pt₃Mn Intermetallic Electrocatalysts for Oxygen Reduction Reaction in Fuel Cells

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Calculation of mass activity

The kinetic current (j_k) was calculated by using the Koutecky-Levich equation,¹ which is expressed by

$$j_{k} = \frac{j_{d} \times j}{|j_{d} - j|}, \ \frac{1}{j} = \frac{1}{j_{k}} + \frac{1}{j_{d}} = \frac{1}{j_{k}} + \frac{1}{0.62nF(D_{0_{2}})^{2/3}v^{-1/6}C_{0_{2}}\omega^{1/2}}$$

where *j* is the measured current density, j_d is the diffusion-limited current density, *n* is the number of electrons transferred, *F* is Faraday's constant (96,485 C mol⁻¹), D_{O2} is the diffusion coefficient of O₂ in 0.1 M HClO₄ solution (1.93 × 10⁻⁵ cm² s⁻¹), *v* is the kinematic viscosity of the electrolyte (1.01 × 10⁻² cm² s⁻¹), C_{O2} is the concentration of oxygen in 0.1 M HClO₄ solution (1.26 × 10⁻⁶ mol cm⁻³), and ω is the angular rate of the rotating disk electrode.

From calculated kinetic current, mass activity was calculated using below equation.

Mass activity = $\frac{j_k}{m_{pt}}$ where m_{Pt} is the total mass of Pt loaded on the electrode.

Calculation of electrochemically active surface area (ECSA)

ECSA was calculated by integration of the hydrogen adsorption region (Q_H) between 0.05 and 0.4 V_{RHE} using total mass of Pt loaded on the electrode (m_{Pt}) and 210 µC cm⁻² of monolayer hydrogen adsorption charge on platinum (q_H) as follows.²

$$ECSA = \frac{Q_H}{m_{Pt} \times q_H}$$

Calculation of specific activity

 $Specific \ activity = \frac{Mass \ activity}{ECSA}$



Fig. S1. TEM images of (a) commercial Pt/C, (b) Mn-Pt/C, and (c) Pt₃Mn intermetallic/C.



Fig. S2. Particle size distribution of (a) Pt/C, (b) Mn-Pt/C, and (c) Pt₃Mn intermetallic/C. Average particle sizes are 2.55, 3.16, and 4.23 nm for Pt/C, Mn-Pt/C, and Pt₃Mn intermetallic/C. For comparison, particle size distributions of Pt/C, Mn-Pt/C, and Pt₃Mn intermetallic/C are presented in (d).



Fig. S3. EDS mapping images of Mn-Pt/C. Mn (green) atoms are mostly observed on Pt (red) nanoparticles.



Fig. S4. XRD patterns of Mn-Pt/C annealed at 500, 600, 700, and 800 °C. With an increase in the annealing temperature, the XRD peaks from the Pt_3Mn intermetallic phase are intensified. Pt_3Mn intermetallic/C catalyst was annealed at 700 °C in this work.



Fig. S5. (a-d) STEM and EDS mapping images of Pt₃Mn intermetallic/C.



Fig. S6. HR-STEM images and their intensity profiles of Pt₃Mn intermetallic nanoparticles with [100] zone axis.



Fig. S7. Mn 2p XPS spectra of (a) Mn-Pt/C and (b) Pt₃Mn intermetallic/C. Pt 4f XPS spectra

of (c) Mn-Pt/C, (d) Pt₃Mn intermetallic/C, and (e) Pt/C.



Fig. S8. ORR polarization and CV curves of pristine Pt₃Mn intermetallic/C (700 °C), Mn-Pt/C, and commercial Pt/C catalysts.



Fig. S9. (a) TEM image of Mn-Pt/C annealed at 800 °C under Ar/H_2 reductive environment for 4 hours (Mn-Pt/C_800 °C). (b) Cyclic voltammograms and (c) ORR polarization curves of Mn-Pt/C_800 °C and Mn-Pt/C_700 °C (Pt₃Mn intermetallic/C). The values of ECSAs, mass activity, and specific activity are summarized in Table S3.



Fig S10. ORR polarization curves of Pt₃Mn intermetallic/C and commercial Pt/C catalysts before and after 10 k ADT potential cycling test in 0.1 M HClO₄ solution.



Fig. S11. STEM image of Pt₃Mn intermetallic nanoparticle after 10k cycles.



Fig. S12. Low magnification EDS mapping images of (a) Pt_3Mn intermetallic and (b) Mn-Pt/C after 10k cycles. Corresponding chemical compositions are summarized in Table S4.

| | Mn Dt/C | Pt ₃ Mn intermetallic/C | Pt ₃ Mn intermetallic/C | |
|----------------|----------|------------------------------------|------------------------------------|--|
| | WIII-FUC | (pristine) | (after RDE 10k cycles) | |
| Pt | 75.2 | 75.1 | 74.7 | |
| Mn | 24.8 | 24.9 | 25.3 | |
| Pt-to-Mn ratio | 3.03 | 3.02 | 2.95 | |

Table S1. Chemical composition of Mn-Pt/C and Pt₃Mn intermetallic/C measured using ICP-OES (at%).

Table S2. Mass activity, ECSA, and specific activity of Pt₃Mn intermetallic/C, Mn-Pt/C, and commercial Pt/C. (RDE results)

| | Mass activity | ECSA _{Hupd} | Specific activity | | |
|------------------------------------|---|----------------------|------------------------|--|--|
| | $[\mathrm{A} \mathrm{mg}_{\mathrm{Pt}}^{-1}]$ | $[m^2 g_{Pt}^{-1}]$ | [mA cm ⁻²] | | |
| Pt ₃ Mn intermetallic/C | 0.386 | 44 | 0.877 | | |
| Mn-Pt/C | 0.014 | 30 | 0.047 | | |
| Commercial Pt/C | 0.125 | 62 | 0.202 | | |

Table S3. ECSA, mass activity (@ 0.9 V_{RHE}) and specific activity (0.9 V_{RHE}) of Mn-Pt/C annealed at 700 °C (Pt₃Mn intermetallic/C) and Mn-Pt/C annealed at 800 °C catalysts. (RDE results)

| | ECSA _{Hupd} | Mass activity | Specific activity | | |
|----------------|----------------------|--|-------------------|--|--|
| | $[m^2 g_{Pt}^{-1}]$ | $[\mathrm{A}\ \mathrm{mg}_{\mathrm{Pt}}^{-1}]$ | $[mA cm^{-2}]$ | | |
| Mn-Pt/C_700 °C | 44 | 0.386 | 0.877 | | |
| Mn-Pt/C_800 °C | 38.94 | 0.312 | 0.801 | | |

Table S4. Chemical composition changes of Pt_3Mn intermetallic/C and Mn-Pt/C after 10k cycles.

| Catalyst after 10k cycles | W | t% | at% | | |
|------------------------------------|------|-------|-------|-------|--|
| (RDE) | Mn | Pt | Mn | Pt | |
| Pt ₃ Mn intermetallic/C | 7.62 | 92.38 | 22.65 | 77.35 | |
| Mn-Pt/C | 0.81 | 99.19 | 2.83 | 97.17 | |

| | Mn | Pt | |
|------------------------------------|---------|-------|--|
| Blank | 0.048 | 0.015 | |
| Pt ₃ Mn intermetallic/C | 38.757 | 0.650 | |
| Mn-Pt/C | 205.477 | 4.213 | |

Table S5. Concentrations of Pt and Mn in the electrolytes dissolved from Pt_3Mn intermetallic/C and Mn-Pt/C during 10k potential cycles. (ICP-MS, unit: ppb = μ g/L).

Table S6. Numbers of Pt atoms and Mn atoms in each sublayer of the slabs.

| Lavan | | Sla | Slab (1) | | Slab (2) | | Slab (3) | | Slab (4) | |
|---------|-------|-----|----------|----|----------|----|----------|----|----------|--|
| Layer | | Pt | Mn | Pt | Mn | Pt | Mn | Pt | Mn | |
| Pt-skin | | 4 | 0 | 4 | 0 | 4 | 0 | 4 | 0 | |
| | 1st | 4 | 0 | 3 | 1 | 2 | 2 | 1 | 3 | |
| Sub- | 2nd | 2 | 2 | 3 | 1 | 4 | 0 | 4 | 0 | |
| surface | 3rd | 3 | 1 | 3 | 1 | 3 | 1 | 4 | 0 | |
| | 4-5th | 3 | 1 | 3 | 1 | 3 | 1 | 3 | 1 | |

| | Operating Condition | | Loading | Voltage | Current | Power Density | |
|---------------------------------------|--|------------------------|---------------------------------|---------|-----------------------------------|-----------------------|--------------|
| Catalyst | Gas | Back pressure | $\frac{C/A}{(mg_{Pt} cm^{-2})}$ | (V) | Density (mA cm ⁻²) | (W cm ⁻²) | Ref. |
| Pt ₃ Mn intermetallic/C | H ₂ -Air (1.5:2.0) | No backpressure | 0.15 / 0.15 | 0.7 | 550 | 0.38 | This work |
| fcc-PtFe/C | H ₂ -Air (1.5:8.0) | No backpressure | 0.2 / 0.2 | 0.7 | ~300 | ~0.21 | 3 |
| MOF-derived Pt ₃ Co | H ₂ -Air | 1.5 bar _{abs} | 0.13 / N/A | 0.8 | 270 | 0.22 | 4 |
| L1 ₀ -CoPt/Pt | H ₂ -Air (500/100 0 sccm) | 1.5 bar _{abs} | 0.105 / N/A | 0.7 | ~700 | 0.49 | 5 |

 Table S7. Single-cell performance of representative Pt-based intermetallic ORR catalysts.

Computational Details

We performed DFT calculations using the Vienna Ab initio Simulation Package (VASP), in which a plane-wave basis set is employed.⁶⁻⁹ The kinetic energy cutoff was set to 500 eV to expand the plane wave. The generalized gradient approximation (GGA) was used to describe the exchange-correlational interactions with the Perdew-Burke-Ernzerhof (PBE) functional.¹⁰ The projector-augmented wave method was used to treat core and valence electrons.¹¹ To describe the oxygen reduction reaction on the intermetallic Pt₃Mn and Pt, we modeled the (111) surfaces of periodically repeated 2×2 supercells with 6 atomic layers and a vacuum width of 15 Å. Pt₃Mn (111) was modeled by a so-called Pt-skin structure, where the outermost layer of 6 atomic layers was composed of only platinum atoms and the two bottom-most layers were fixed for both Pt₃Mn and Pt. The Brillouin zone was sampled with a $4 \times 4 \times 1$ Monkhorst–Pack k-point mesh. The geometries were optimized until the Hellmann-Feynman forces were less than 10^{-2} eV/Å, and the electronic structures were relaxed with a convergence criterion of 10^{-5} eV. An implicit solvation model was implemented to describe the solvent effect by using VASPsol.¹²

In this study, the free energy changes of each step were calculated based on a computational hydrogen electrode model reported by Nørskov et al.¹³ Adding entropy term (T Δ S) and zeropoint energy (ZPE) corrections to the DFT-calculated energies, we could obtain the Gibbs free energy diagram as follows:

 $\Delta G = \Delta E_{DFT} + \Delta ZPE - T\Delta S - neU,$

where ΔE_{DFT} is the change in the total energy calculated by DFT method; ΔZPE is the difference in zero-point energy; ΔS is the change in entropy; T is temperature, which was set

to the room temperature (298.15K); n is the number of electrons involved in each ORR reaction step; and U is the electrode potential.

The dissolution potential of Pt atoms was calculated as

$$U_{dissolution} = U_{dissolution+}^{Bulk Pt} \frac{1}{2n_{dissolved}} \left\{ E(Pt_{n-n_{dissolved}}M_m) + n_{dissolved}E(Pt_{bulk}) - E(Pt_nM_m) \right\},$$

where $U_{dissolution}$ and $U_{dissolution}^{Bulk Pt}$ are the dissolution potentials of a surface and bulk Pt into Pt²⁺.

Here, we calculated $U_{dissolution}^{Bulk Pt}$ as 1.188 V, and $n_{dissolved}$ is defined as the number of Pt atoms dissolved.

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