### Supporting Information

# Excellent Room Temperature Catalytic Activity for Formaldehyde Oxidation on a Single-Atom Iron Catalyst in a Moist Atmosphere

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Fig. S1 Formaldehyde calibration curve.



Fig. S2 Intermediate states, transition states, and bond length changes in the oxidation of formaldehyde on three catalyst surfaces.



Fig. S3 TEM images of Fe-N-C sample at 10, 20, 50, and 100 nm.



Fig. S4 Gas chromatogram of gas after fixed bed catalytic reaction.



Fig. S5 Removal efficiency test of formal dehyde on nitrogen doped carbon materials at 25  $^{\circ}\mathrm{C}$  and 0% RH.



Fig. S6 Stability test results of Fe-N-C catalyst at 25 °C and 0% RH.



Fig. S7 Stability test results of Fe-N-C catalyst at 110 °C and 75% RH.



Fig. S8 Adsorptive configurations of  $O_2$  on  $Fe_{SA}$ -N<sub>5</sub>-C without  $H_2O$  (a) and with  $H_2O$  (b).



Fig. S9 The LUMO orbital distributions of oxygen (a) and formaldehyde (b); the HOMO orbital distributions of  $Fe_{SA}-N_3-C$  (c),  $Fe_{SA}-N_4-C$  (d) and  $Fe_{SA}-N_5-C$  (e).



**Fig. S10** The *d*-band centers ( $\varepsilon_d$ ) of three catalysts (a), the relationship curve between  $E_{ads}(O_2)$  and  $\varepsilon_d$  (b), with the relationship between  $E_{ads}(HCHO)$  and  $\varepsilon_d$  (c).

#### **DFT Calculation:**

To perform a thermodynamic analysis of the pathway to be selected, the heat of reaction at different reaction temperatures is calculated to express Gibbs free energy ( $\Delta G_F$ ) from:

$$\Delta G_F = G_{FS} - G_{IS} \tag{S1}$$

where  $G_{FS}$  (J·mol<sup>-1</sup>) denotes the Gibbs free energy of the final state;  $G_{IS}$  (J·mol<sup>-1</sup>) denotes the Gibbs free energy of the initial state.<sup>1</sup>

To analyze the structural stability of the catalyst, the formation energy  $(E_{for})$  and the binding energy  $(E_{bin})$  of the gas are calculated according to the following equations:

$$E_{for} = E_{tot} + x\mu_C - E_G - y\mu_N - E_{Fe}$$
(S2)

$$E_{bin} = E_{tot} - E_{sub} - E_{Fe} \tag{S3}$$

where  $E_{tot}$  is the total energy of the system;  $E_{sub}$  is the total energy of the graphenebased substrate; x is the number of carbon atoms removed from the pristine graphene;  $\mu_C$  is the chemical potential of carbon defined as the total energy per carbon atom for pristine graphene; y is the number of nitrogen atoms added;  $\mu_N$  is the chemical potential of nitrogen (defined as half of the total energy of an N<sub>2</sub> molecule);  $E_{Fe}$  is the total energy of an isolated Fe atom in the vacuum.<sup>2</sup>

The adsorption energy  $(E_{ads})$  of gas without entropy is calculated according to the following equation:

$$E_{ads} = E_{tot} - E_{gas} - E_{sub} \tag{S4}$$

where  $E_{tot}$  is the total energy of the system;  $E_{gas}$  represents the total energy of isolated gas molecules;  $E_{sub}$  is the total energy of the graphene-based substrate.

The kinetic analysis of each reaction step is performed using conventional transition state theory, and the reaction equilibrium constant ( $k^{TST}$ ) is calculated from:

$$k^{TST} = \frac{k_B T}{h} \times exp\left(\frac{-\Delta G_b}{k_B T}\right)$$
(S5)

where  $k_B$  (1.381×10<sup>-23</sup> J·K<sup>-1</sup>) is Boltzmann's constant; h (6.626×10<sup>-34</sup> J·s) is Planck's constant; T (K) denotes the reaction temperature;  $\Delta G_b$  (eV) denotes the reaction energy barrier expressed in Gibbs free energy expressed as the reaction energy barrier.<sup>3</sup>

#### **Formaldehyde Removal Experiment:**

To calculate the formaldehyde conversion rate of the catalyst, it is necessary to draw the formaldehyde calibration curve in advance. The procedure of absorbance determination of formaldehyde standard solution is shown in **Figure 1b**. First, filled the absorption tube with 20 mL of distilled water and collected 1 liter of the gas to be tested, and diluted the absorption solution to 50 mL. Accurately measured 5 mL of absorption solution in a 25 mL colorimetric tube and diluted to 10 mL, and then added 2 mL of 0.25% acetylacetone solution prepared in advance. Put the colorimetric tube into a water bath and heated it with boiling water for three minutes, then took it out and cool it to room temperature. Next, used a spectrophotometer to measure the absorbance value of the absorbing liquid. The model of the spectrophotometer is TU-1900, and the wavelength of the light source is 413 nm. Finally, subtracted the absorbance value of each standard solution and the absorbance value of the blank group (distilled water) to obtain a series of calibrated absorbance values, as shown in **Table S1**.

 Table S1 Formaldehyde content of formaldehyde standard solution and calibrated absorbance value.

Tube no.	1	2	3	4	5	6
Formaldehyde content/µg	1	4	10	20	30	35
Calibrated absorbance	0.021	0.078	0.200	0.409	0.618	0.723

The calibration curve was plotted using the formaldehyde content as the horizontal coordinate and the calibration absorbance as the vertical coordinate, as shown in **Figure S1**. The equation for fitting the formaldehyde calibration curve is shown in **Equation S6**:

$$y = 0.02072x - 0.00382 \tag{S6}$$

In the formula, y represents the calibrated absorbance; x represents the formaldehyde content ( $\mu g$ ).

ir adsorption (re <sub>SA</sub> -N <sub>3</sub> -C).								
	Gas	∆ <b>h</b> /Å	$\Delta q_{Fe}^{\prime}/e$	$\Delta q_{sub}/e$	$\Delta q_{gas}/e$			
	0 <sub>2</sub>	0.20	-0.33	-0.43	0.78			
	HCHO	0.36	-0.86	-2.82	3.7			
	CO <sub>2</sub>	0.30	-0.87	-4.24	5.12			
	H <sub>2</sub> O	0.33	-0.21	0.26	-0.07			

**Table S2** Vertical height difference, charge change of Fe atoms before and after molecular adsorption ( $Fe_{SA}-N_3-C$ ).

Table S3 Vertical height difference, charge change of Fe atoms before and after molecular adsorption ( $Fe_{SA}-N_4-C$ ).

Gas	∆ <i>h</i> /Å	$\Delta q_{Fe}^{\prime}/\mathrm{e}$	$\Delta q_{sub}/e$	$\Delta q_{gas}/e$
O	0.34	-0.12	-0.32	0.44
HCHO	0.43	-0.02	-0.36	0.38
CO <sub>2</sub>	0.05	-0.02	-0.02	0.04
H <sub>2</sub> O	0.15	-0.06	0.08	-0.02

**Table S4** Vertical height difference, charge change of Fe atoms before and after molecular adsorption ( $Fe_{SA}-N_5-C$ ).

Gas	∆ <i>h</i> /Å	$\Delta q_{Fe}^{\prime}/\mathrm{e}$	$\Delta q_{sub}/e$	$\Delta q_{gas}/e$
0 <sub>2</sub>	0.17	-0.14	-0.29	0.43
HCHO	-0.02	-0.04	0.06	-0.02
$CO_2$	-0.02	-0.02	0.05	-0.03
H <sub>2</sub> O	-0.01	-0.02	0.04	-0.03

Table S5 Entropy of four gases at 298K and 1bar (calculated by NIST database).

S(eV/K)	$O_2$	HCHO	$CO_2$	$H_2O$
	0.00213	0.00229	0.00221	0.00197

**Table S6** Entropy of four gases adsorbed on the surface of single atom catalyst (calculated by vaspkit).

S(eV/K)	$O_2$	НСНО	$CO_2$	$H_2O$
Fe <sub>SA</sub> -N <sub>3</sub> -C	0.00176	0.00211	0.00224	0.00188
Fe <sub>SA</sub> -N <sub>4</sub> -C	0.00204	0.00185	0.00215	0.0017
Fe <sub>SA</sub> -N <sub>5</sub> -C	0.00138	0.0016	0.00188	0.002

**Table S7** Entropy of state in formaldehyde oxidation reaction on  $Fe_{SA}-N_3-C$  (calculated by vaspkit).

Fe <sub>SA</sub> -N <sub>3</sub> -C	IS	IM01	IS1	TS1
S(eV/K)	0.0024	0.00253	0.00269	0.00238
IM1	TS2	IM2	TS3	IM3

0.00213	0.00242	0.00214	0.00238	0.0025
TS4	IM4	IM5	FS	
0.00262	0.00341	0.00261	0.00342	

**Table S8** Entropy of state in formaldehyde oxidation reaction on Fe<sub>SA</sub>-N<sub>4</sub>-C (calculated by vaspkit).

Fe <sub>SA</sub> -N <sub>4</sub> -C	IS	IM02	IS2	TS6	IM6
S(eV/K)	0.0024	0.00253	0.00269	0.00238	0.00213
TS7	IM7	TS8	IM8	TS7	TS9
0.00242	0.00214	0.00238	0.0025	0.00242	0.00211
IM9	TS10	IM10	IM11	FS	
0.00293	0.00274	0.00325	0.00353	0.00289	

**Table S9** Entropy of state in formaldehyde oxidation reaction on  $Fe_{SA}-N_5-C$  (calculated by vaspkit).

Fe <sub>SA</sub> -N <sub>5</sub> -C	IS	IM03	IS3	TS12
S(eV/K)	0.0034	0.00339	0.00329	0.00208
IM12	TS13	IM13	TS14	IM14
0.00273	0.00216	0.00271	0.00263	0.00256
TS15	IM15	IM16	FS	
0.00268	0.004	0.00398	0.00331	

Sample quality /mg	Constant volume /ml	Measured element	Meter reading	Unit	Converted content	Unit	Mass fraction /%
39.7	100	Fe	2.03	mg/L	5110.83	mg/kg	0.51

 Table S10 Measurement of Fe content in catalyst.

Table S11 Fe K-edge EXAFS curve fitting parameters for Fe-N-C.

-	Path	CN	$\frac{R(\text{Å})}{R(\text{Å})}$	$\sigma^2$ (Å <sup>2</sup> )	$\Delta E_0$	$R_6 \%$
-		011		· (11)	0	
	Fe-N	5.1	2.00	0.007	4.0	1 7
	Fe-O	1.0	1.83	0.002	-4.2	1.7

*R* represents the distance between absorber and backscatter atoms; *N* represents the coordination number;  $\sigma^2$  represents the Debye-Waller factor to account for both thermal and structural disorders;  $\Delta E_0$  represents the inner potential correction; R-factor ( $R_f$ , %) indicates the goodness of the fit. The fitting range is 3.0 - 10.8 Å<sup>-1</sup> in k space and 1.0 - 2.2 Å in R space.

Table S12 Contents of  $CO_2$ ,  $N_2$  and other gases in the tail gas.

CO <sub>2</sub> content	N <sub>2</sub> content	Other gas content	
0.73%	92.42%	6.85%	

	Reaction conditions			Conversion	
Catalyst	Concentration	Airspeed	Temp		Refs.
	(ppm)	$(h^{-1}/L \cdot h^{-1} \cdot g^{-1})$	. (°C)	rate (%)	
FeCo@NC	100	-/60	25	72.7	4
Pt/H-Beta-TEA-12	400	-/60	25	62.8	5
$Ir_{0.75}Pt_{0.25}/Nb_2O_5$	240	-/60	25	60	6
0.5IrAl-CD	180	-/30	25	57.8	7
$0.2wt\% Pr/\gamma$ -Al <sub>2</sub> O <sub>3</sub>	30	-/24	25	47.2	8
0.2Pd@TS-1(30)	100	-/100	25	45	9
Ir/Nb <sub>2</sub> O <sub>5</sub>	240	-/60	25	37.2	6
Pt/Fe <sub>2</sub> O <sub>3</sub>	90	-/120	25	35.9	10
2wt% Au/CeO <sub>2</sub> - Co <sub>3</sub> O <sub>4</sub>	8	-/15	25	30	11
1wt% Rh/TiO <sub>2</sub>	100	50000/-	25	22.3	12
0.48wt% Au/Co <sub>3</sub> O <sub>4</sub>	8	-/15	25	22	11
2.52wt% Au/Fe-O	6.25	-/54	25	12	13
0.4wt% Pt/ATiO2	50	-/30	25	11.2	14
Fe-N-C	60	73000/180	25	85	This work

 Table S13 Performance of different catalysts for the oxidation of formaldehyde.

Table S14 HOMO and LUMO orbitals of Fe-N<sub>3</sub>-C, Fe-N<sub>4</sub>-C, Fe-N<sub>5</sub>-C, O<sub>2</sub> and HCHO.

	Fe-N <sub>3</sub> -C	Fe-N <sub>4</sub> -C	Fe-N <sub>5</sub> -C	$O_2$	НСНО
HOMO (eV)	-1.79	-1.26	-0.91	-8.00	-6.18
LUMO (eV)	-0.86	-0.89	-0.57	-1.96	-2.70

## Reference

- 1. M.Z.M. Salem and M. Böhm. *BioResources*. 2013, 8, 4775-4790.
- W. Yang, S. Xu, K. Ma, C. Wu, I. Gates, X. Ding, W. Meng and Z. Gao. *Nano Materials Science*. 2020, 2, 120-131.
- 3. T. Salthammer, S. Mentese and R. Marutzky. Chemical Reviews. 2010, 110, 2536-2572.
- D. Zhu, M. Chen, Yu Huang, R. Li, T. Huang, J. Cao, Z. Shen, and S. Lee, *Journal of Hazardous Materials*, 2022, 424, 127593.
- L. Zhang, L. Chen, Y. Li, Y. Peng, F. Chen, L. Wang, C. Zhang, X. Meng, H. He and F. Xiao, *Applied Catalysis B: Environmental*, 2017, 219, 200-208.
- S. H. Ammar, M. D. Salman and R. F. Shaf. Colloid and Interface Science Communications, 2020, 38, 100305.
- H. Chen, R. Zhang, H. Wang, W. Bao and Y. Wei, *Applied Catalysis B: Environmental*, 2020, 278, 119311.
- T. Yang, Y. Huo, Y. Liu, Z. Rui and H. Ji, *Applied Catalysis B: Environmental*, 2017, 200, 543-551.
- 9. X. Sun, J. Lin, Y. Wang, L. Li, X. Pan, Y. Su and X. Wang, *Applied Catalysis B:* Environmental, 2020, 268, 118741.
- M. Chen, H. Yin, X. Li, Y. Qiu, G. Cao, J. Wang, X. Yang, and P. Wang, *Journal of Hazardous Materials*, 2020, 395, 122628.
- B. Liu, Y. Liu, C. Li, W. Hua, P. Jing, Q. Wang and J. Zhang, *Applied Catalysis B:* Environmental, 2012, 127, 47-58.
- 12. C. Zhang, H. He and K. Tanaka. Applied Catalysis B: Environmental, 2006, 65, 37-43.
- C. Li, Y. Shen, M. Jia, S. Sheng, M. O. Adebajo and H. Zhu, *Catalysis Communications*, 2008, 9, 355-361.
- H. Chen, Z. Rui and H. Ji. Industrial & Engineering Chemistry Research, 2014, 53, 7629-7636.