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## **Supporting Material**

Metal oxyhydroxide nanosheet assisted fabrication of ultrathin carbon molecular sieve membrane for hydrogen separation

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Figures



**Fig. S1** (a) Schematic showing the production of FeCoNiOOH nanosheets via a surfactantassisted self-assembly process; (b-d) TEM image of FeCoNiOOH nanosheets prepared with 3h, 6h and 12h, respectively.



**Fig. S2** (a-b) SEM images of the FeCoNiOOH nanosheets deposited on AAO; (c) Lateral size distribution of the nanosheets measured from SEM images over 250 nanosheets with a Gaussian fit.



**Fig. S3** (a) TEM image and (b) Corresponding selected area electron diffraction pattern at the edge of an ultrathin FeCoNiOOH nanosheet.



**Fig. S4** SEM EDX spectrum of the FeCoNiOOH nanosheets deposited on a Si substrate with the relevant table of element component inserted. (The sharp peak of Si showing in the EDX spectrum is attributed to the Si substrate for depositing the nanosheets.)



**Fig. S5** (a) Schematic of the hydrogen boding formed between furfuryl alcohol molecules and FeCoNiOOH nanosheet; (b) Tyndall effect of the nanosheets dispersed in furfuryl alcohol.



**Fig. S6** (a-c) TEM characterization of FeCoNiOOH nanosheets after pyrolysis at 400 °C: (a) TEM image of the decomposed nanosheets showing generated nanopores and nanoparticles; (b) TEM image of the decomposed nanosheets showing numerous nanoparticles with corresponding SAED pattern inserted; (c) HRTEM image of the decomposed nanosheets showing nanoporous structure. (d-f) TEM characterization of PFA after pyrolysis at 450 °C: (d) TEM image of the carbonized PFA; (e) HRTEM image of the carbonized PFA with corresponding SAED pattern inserted; (f) Locally magnified HRTEM image of the carbonized PFA showing random packing of carbon plates and clusters. (g-i) TEM characterization of the

FeCoNiOOH nanosheets/PFA derived CMS membranes pyrolyzed at 450 °C: (g) TEM image of the CMS membrane cross-section; (h) HRTEM image of the nanoparticles shown in the CMS membrane due to the decomposition of the FeCoNiOOH nanosheets; (i) HRTEM image showing disordered pore structure of the carbon phase in the CMS membrane.



**Fig. S7** XRD results of the AAO substrate, FeCoNiOOH nanosheets deposited on AAO before and after pyrolysis at 400 °C.



**Fig. S8** SEM (a-e) surface and (f-j) cross-sectional images of FeCoNiOOH nanosheets/PFA based carbon membranes pyrolyzed under 525 °C with 0.9, 1.8, 3.5, 8.8 and 17.6 wt% of nanosheets loaded.



**Fig. S9** Effective membrane thickness change of FeCoNiOOH nanosheets/PFA based carbon membranes with different nanosheets loading and pyrolyzed under 525 °C.



**Fig. S10** (a) SEM cross-sectional image of 0.9 wt% FeCoNiOOH nanosheets/PFA based carbon membranes pyrolyzed under 525 °C presenting the infiltration of polymer into the AAO substrate owing to insufficient nanosheets introduced; (b) SEM surface image of 8.8 wt% FeCoNiOOH nanosheets/PFA based carbon membranes pyrolyzed under 525 °C showing the generation of pinholes when excessive amount of nanosheets incorporated.



**Fig. S11** The permeance and ideal selectivity as a function of permeation temperature from 20 to 100 °C for FeCoNiOOH nanosheet/PFA derived carbon membrane sample with 1.8wt% nanosheets pyrolyzed at 525 °C.

Carbonization temperature	H <sub>2</sub> permeance	$H_2/N_2$	$H_2/CO_2$
(°C)	(10 <sup>-8</sup> mol m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	ideal selectivity	ideal selectivity
25	0.37	1.1	-
450	1.78	3	3.4
525	3.32	46	11.4
600	9.6	5.3	5.9

**Table S1** Gas separation performance of MOOH nanosheet/PFA derived carbon membraneswith a loading of 1.8 wt% of nanosheetspyrolyzed at different temperatures.

Loading	Membrane	H <sub>2</sub> permeance $(10^{-8} \text{ mol})$		Ideal sele	ectivities	
of MOOH nanosheets	thickness (nm)	$m^{-2} s^{-1} Pa^{-1}$ )	H <sub>2</sub> /N <sub>2</sub>	H <sub>2</sub> /CO <sub>2</sub>	H <sub>2</sub> /CH <sub>4</sub>	H <sub>2</sub> /O <sub>2</sub>
0.9	_[a]	0.26	4	5	3.1	-
1.8	$95\pm17$	3.32	46	11.4	38.3	34.8
3.5	$123\pm23$	7.88	4.2	4.4	3.1	-
8.8	$455\pm33$	15.63	3.8	4.6	2.9	-
17.6	$1257\pm125$	48	3.5	3.9	2.5	-

**Table S2** Gas separation performance of MOOH nanosheet/PFA derived carbon membraneswith different nanosheet loadings pyrolyzed at 525 °C.

[a] The effective membrane thickness cannot be estimated here due to the polymer infiltration into the substrate.

Sample	H <sub>2</sub> permeance (10 <sup>-8</sup> mol m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	H <sub>2</sub> /CO <sub>2</sub> ideal selectivity	Average H <sub>2</sub> permeance (10 <sup>-8</sup> mol m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	Average H <sub>2</sub> /CO <sub>2</sub> ideal selectivity
1	3.32	11.4		
2	2.71	9.3	$2.78\pm0.51$	$10.1 \pm 1.1$
3	2.31	9.7		

**Table S3** Gas separation performance of FeCoNiOOH nanosheet/PFA derived carbonmembrane samples with 1.8wt% nanosheets pyrolyzed at 525 °C.

 Table S4 Comparison of single-gas and mixed-gas permeation results for FeCoNiOOH

 nanosheet/PFA derived carbon membrane sample with 1.8wt% nanosheets pyrolyzed at 525

 °C.

Tests	H <sub>2</sub> permeance	$H_2/CO_2$	
	(10 <sup>-8</sup> mol m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	selectivity	
Single-gas permeation	3.32	11.4	
Mixed-gas permeation	3.2	10.5	

Permeation	H <sub>2</sub> permeance	CO <sub>2</sub> permeance	$H_2/CO_2$
temperature (°C)	(10 <sup>-8</sup> mol m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	(10 <sup>-8</sup> mol m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	ideal selectivity
20	3.32	0.29	11.4
40	3.53	0.31	11.3
60	3.72	0.35	10.5
80	4.4	0.44	10
100	5.17	0.53	9.83

**Table S5** Permeance and selectivity at different permeation temperatures for the FeCoNiOOHnanosheet/PFA derived carbon membrane sample with 1.8wt% nanosheets pyrolyzed at 525°C.

		Membrane	Pyrolysis	$H_2$	$H_2/CO_2$	
Method	Precursor	thickness	temperature	permeance	ideal	Ref.
		(µm)	(°C)	(GPU) <sup>[a]</sup>	selectivity	
Dip coating	PFA	10	600	20.3	11	1
Ultrasonic deposition	PFA	4.7	450	7.76	13.7	2
Vapour deposition	PFA	3.1	600	76.1	4.4	3
CNT scaffolding	PFA	0.32	500	56.4	5.9	4
Substrate transferring	Matrimid	0.1	500	761	1.53	5
2D templating	Polyimide	40	425	2.42	5.1	6
2D self- sacrificial templating	PFA	0.11	525	99.1	11.4	This work

**Table S6** Comparison of gas separation performance for the MOOH nanosheet/PFA derived

 carbon membrane with carbon membranes produced with other methods.

[a] 1 GPU =  $3.35 \times 10^{-10}$  mol m<sup>-2</sup> s<sup>-1</sup> Pa<sup>-1</sup>

Membranes	Membrane thickness (µm)	H <sub>2</sub> permeance (GPU) <sup>[a]</sup>	H <sub>2</sub> /CO <sub>2</sub> ideal selectivity	References
ZIF-8 on polysulfone	3.6	1403	2.7	7
ZIF-8 on ammoniated PVDF	0.87	3552	3	8
ZIF-8 on layered double hydroxide (LDH) modified alumina	20	439	4.2	9
ZIF-8/Graphene oxide	0.1	163	1.6	10
ZIF-22 on titania	40	439	7.2	11
ZIF-7 on alumina	1.5	239	6.7	12
ZIF-90 on alumina	20	749	7.2	13
UiO- 66/Poly(acrylic acid)	0.32	1.23	20.3	14
MOF-5/Matrimid	35	1.51	2.7	15
ZIF-8/Matrimid	40	0.446	3.8	16

**Table S7** Comparison of gas separation performance for the MOOH nanosheet/PFA derivedcarbon membrane with different types of membranes.

ZSM-5/Matrimid	40	0.547	2.57	17
ZIF-8/				
Polybenzimidazole	5.88	64.5	12.3	18
s (PBIs)				
ZIF-8/PBI hollow	0.307	107	16.1	19
fiber membrane				
Polyamide	0.2	25.8	14.3	20
PBI on polyimide	0.1	48.5	33.3	21
Poly(benzoxazole-	70	72 8	3.4	22
co-imide)	70	72.0	5.1	
m-PBI	20	23.9	24	23
TADPS-IPA	21.5	14.9	19	24
TADPS-TPA	19.5	19	13	24
MOOH nanosheets				
/ PFA derived	0.11	99.1	11.4	This work
carbon membrane				

[a] 1  $\overline{\text{GPU} = 3.35 \times 10^{-10} \text{ mol } \text{m}^{-2} \text{ s}^{-1} \text{ Pa}^{-1}}$ 

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