Supporting Information

Highly-selective light olefins production *via* photothermal Fischer–Tropsch synthesis over α/γ -Fe₂O₃-derived Fe₅C₂ under low pressure

Lizhu Song, a Shuxin Ouyang, *b Peng Lic and Jinhua Yea,d

^a TJU-NIMS International Collaboration Laboratory, School of Materials Science and Engineering, Tianjin University, Tianjin 300072, P. R. China.

^bKey Laboratory of Pesticide and Chemical Biology, Ministry of Education, College of Chemistry, Central China Normal University, Wuhan 430079, P. R. China.

^cCollege of Materials Science and Technology, Jiangsu Key Laboratory of Materials and Technology for Energy Conversion, Nanjing University of Aeronautics and Astronautics, Nanjing 210016, P. R. China ^dInternational Center for Materials Nanoarchitectonics (WPI-MANA), National Institute for Materials Science (NIMS), 1-1 Namiki, Tsukuba 305-0047, Japan

*Corresponding author. *E-mail address:* oysx@mail.ccnu.edu.cn (S. Ouyang).

Experimental Procedures

Catalyst precursor synthesis. The method to synthesize the Fe-based catalysts for photothermal Fischer-Tropsch synthesis included the following steps: (1) 10 g Fe(NO₃)₃·9H₂O (Sinopharm Chemical Reagent Co.,Ltd, 80072718) was calcined in a tube furnace under Ar atmosphere at 500 °C for 2 h to obtain α -Fe₂O₃; (2) 0.5 g α -Fe₂O₃, 3 ml of 0.03 mol/L KNO₃ (Tianjin Guangfu Fine Chemical Research Institute, 50116) were added to 20 ml deionized water (according to the K⁺ loading amounts, 0.7%); the suspension solution was stirred at 80 °C to paste, and then further dried at 70 °C for 24 h under vacuum conditions. The γ -Fe₂O₃ (Aladdin, F141282-25g) is prepared in the same steps.

Photothermal synthesis of pre-catalyst. Typically, 50 mg sample was placed in a CO atmosphere and activated for 30 min under a 300 W Xenon lamp in an enclosed-circuit reaction system (OLPCRS-3, Shanghai Boyi Scientific Instrument Co., China). After cooling to room temperature and evacuated, the reaction system was reinjected 30 kPa of air, then the sample was under irradiation again for 0, 10, 30, 50 min, respectively. Here we labeled them α (or γ)-CmAn (m, n = 0, 10, 30, 50), in which α or γ represent α (or γ)-Fe₂O₃-0.7 K⁺ unless there is a special description; C and A represent the pre-catalyst was photothermally treated in CO and air, respectively; m and n signify the processing time in each atmospheric condition. In addition, γ -At means γ -Fe₂O₃-0.7 K⁺ directly under irradiation in the air.

Sample characterization. The crystal structure was characterized by X-ray diffractometer (D/max-2500, Rigaku, Japan). The light adsorption properties of the catalysts were measured by Ultraviolet-visible (UV-Vis) spectroscopy (UV-2700, Shimadzu, Japan). The microstructure of the catalyst was performed on Scanning electron microscopy (SEM, Quanta FEG 250) and Transmission electron microscopy (TEM, JEM-F200). The spatial distribution of element was confirmed by energy-dispersive X-ray spectroscopy (EDS). The chemical valence state of the element was measured by Xray photoelectron spectroscopy (XPS, Escalab 250Xi, Thermo Fisher Scientific, England). The temperature of the catalyst surface was measured by a thermocouple (DT-311N). Mössbauer spectroscopy is powerful in distinguishing and quantifying the phases of Fe-based materials that are difficult to be identified by XRD. The data analysis was using the least-squares method. Spectral fits were based on Lorentzian curves. Component identification base on the isomer shift (IS), quadrupole splitting (QS), and hyperfine magnetic field (H). **Catalyst performance evaluation.** The Photothermal Fischer-Tropsch synthesis was evaluated in an enclosed-circuit reaction system (OLPCRS-3, Shanghai Boyi Scientific Instrument Co., China, as presented in **Fig. S1**). 300W Xe lamp (CEL-HXF300, CEAULIGHT) was used as a photothermocatalytic light source, 50 mg of catalyst, CO: $H_2 = 1$: 3, 55.5 kPa. The gas composition of the products after the reaction was detected by gas chromatography (GC-2014C, Shimadzu Co., Japan) using N₂ as the carrier gas, equipped with a Paropak Q chromatographic column, a flame ionization detector (FID) and a methanizer. The components of gas products were analyzed by gas chromatography-mass spectrometry (Shimadzu, GCMS-QP2010 Ultra).

The catalytic performances were typically evaluated through the following indicators.

CO conversion rate was calculated by the following formula (S1):

$$CO_{con}(\%) = \frac{CO_0 - CO_t}{CO_0} \times 100\%$$
 (S1)

Where CO_0 and CO_t represent the moles of CO at the beginning and at moment *t*, respectively. Total organic carbon (TOC) products represent total hydrocarbons at moment *t* was obtained according to formula (S2), *m* represents the mass of the catalyst:

$$TOC = \frac{1}{m} \times \sum_{i=1}^{n} moles \ of \ C_i \ hydrocarbon \ \times i$$
(S2)

The selectivity of C_i hydrocarbon at moment *t* was given as formula (S3):

$$C_i hydrocarbon_{sel}(\%) = \frac{moles of Ci hydrocarbon \times i}{m \times TOC} \times 100\%$$
(S3)

 CO_2 selectivity (CO_{2sel}) was calculated by formula (S4):

$$CO_{2sel}(\%) = \frac{CO_{2t}}{CO_0 - CO_t} \times 100\%$$
 (54)

Where CO_{2t} denotes the moles of CO_2 at moment *t*.



Fig. S1. The photograph and illustrated scheme of the enclosed-circuit system for catalyst performance test.

Table S1.	Catalytic	performance	comparison.

Commission of the second se	CO _{con}	selectivity (%) ^[a]			0/10	Р	-	D-f
Samples	(%)	CH_4	C ₂₌ -C ₄₌	C ₂₋ -C ₄₋	· 0/P	(MPa)	I	Ket.
Thermal Catalys	is							
Fe-Zn-0.36Na	82.7	11.7	22.9	3.6	6.3	2.0	340 °C	1
Fe-Zn	34.1	27.1	13.3	16.6	0.8	2.0	340 °C	1
Fe-1.2Na	48.7	7.5	20.3	2.45	8.3	2.0	340 °C	1
Fe	32.7	21.0	17.5	10.9	1.6	2.0	340 °C	1
ZnCrO _x /MSAPO	17	2	80	14	5.7	2.5	400 °C	2
Photo+Thermal	Catalysi	5						
30% Co/TNT	17.1	31.5	31.8	0.7	0.02	2.0	220 °C + UV light	3
Photothermal Ca	atalysis							
Ni-500	14.9	30.6	33.0	32.1	1.0	0.18	300 W Xe lamp	4
3Co/STO	15.2	21.7	19.7	12.4	1.6	0.05	300 W Xe lamp	5
Co-450	15.4	48.0	36.0	5.9	6.1	0.18	300 W Xe lamp	6
CoMn alloys	13.9	28.4	27.0	8.4	3.22	0.18	300 W Xe lamp	7
α/γ -Fe ₂ O ₃	28.8	24.8	71.9	4.06	16.7	0.05	300 W Xe lamp	This study

[a] C₂₌-C₄₌: olefins; C₂₋-C₄₋: paraffins;



Fig. S2. The XRD pattern of Fe-based catalyst precursor $\alpha\text{-Fe}_2\text{O}_3$ and $\gamma\text{-Fe}_2\text{O}_3.$



Fig. S3. a, SEM image, b, TEM image, c, HRTEM image of α -Fe₂O₃.



Fig. S4. The XRD pattern of $\alpha\mbox{-}\mbox{Fe}_2\mbox{O}_3$ and $\gamma\mbox{-}\mbox{Fe}_2\mbox{O}_3$ before and after reaction.



Fig. S5. UV-Vis spectra of α -Fe₂O₃ and γ -Fe₂O₃, and Fe₃O₄.



Fig. S6. Temperature variation curves of the catalysts during the reaction.



Fig. S7. The XRD pattern of photothermal synthesized composite catalyst precursor with α -Fe₂O₃ as the precursor.



Fig. S8. The XRD pattern of photothermal synthesized composite catalyst precursor with γ -Fe₂O₃ as the precursor.

Table S2. Mössbauer parameters of α -C30A30.

Phase	Spectral Contribution(%)	IS (mms)	QS (mms)	Hhf (kOe)
α -Fe ₂ O ₃	18.3	0.39	-0.21	514
γ -Fe ₂ O ₃ (A)	50.7	0.35		483
γ -Fe ₂ O ₃ (B)	31.0	0.30	0.06	500



Fig. S9. The components of gas products of (a) α -Fe₂O₃ and (b) γ -Fe₂O₃, and Mass Spectrometry of (c) C₂H₄, (d) C₂H₆, (e) C₃H₆, and (f) C₃H₈.



Fig. S10. The catalytic (a) activity and (b) selectivity of repeat experiments.

 Table S3.
 The catalytic activity and selectivity.

	CO _{Con}	Selectivity (%)								тос
Sample (%)	(%)	CH4	C	C ₂	С ₃₌	C ₃	C ₄₌	C ₂ =-C ₄ =	CO ₂	(mmol.g⁻¹)
α -Fe ₂ O ₃	11.8	31.3	33.3	36.5	24.5	25.6	6.6	64.4	75.8	1.4
γ -Fe ₂ O ₃	24.0	28.4	22.7	34.3	28.0	32.4	4.9	55.6	66.8	3.9
α-C30A10	26.0	33.4	23.9	32.6	26.0	28.7	5.4	55.3	58.7	5.3
α-C30A30	28.8	24.8	32.1	34.7	27.9	29.1	11.9	71.9	75.2	3.5
α-C30A50	24.7	25.6	34.1	35.9	25.9	27.0	11.5	71.5	79.1	2.5



Fig. S11. The catalytic (a) activity and (b) selectivity of photothermal synthesized composite catalyst precursor with γ -Fe₂O₃ as the precursor.



Fig. S12. The XRD pattern of catalysts after reaction.



Fig. S13. The XRD pattern of catalysts after reaction.



Fig. S14. The XRD pattern of catalysts after reaction.



Fig. S15. Mössbauer spectra of α -C30A30 after reaction.

Table S4. Mössbauer	parameters of α -C30A30 after reaction.
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Phase	Spectral Contribution(%)	IS (mms)	QS (mms)	Hhf (kOe)
Fe_3O_4 (A)	7.0	0.28	-0.01	496
Fe ₃ O ₄ (B)	15.2	0.68	-0.01	465
Fe ₅ C ₂ (1)	32.9	0.18	0.04	182
Fe ₅ C ₂ (2)	26.7	0.27	0.09	217
Fe_5C_2 (3)	18.1	0.20	0.07	111



Fig. S16. Mössbauer spectra of γ -Fe₂O₃ after reaction.

Table S5. Mössbauer	[•] parameters of ^{<i>·</i>}	γ -Fe ₂ O ₃ after reaction.
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Phase	Spectral Contribution(%)	IS (mms)	QS (mms)	Hhf (kOe)
Fe ₃ O ₄ (A)	9.0	0.29	-0.02	484
Fe ₃ O ₄ (B)	28.5	0.59	-0.01	450
Fe₅C ₂ (1)	22.1	0.17	0.06	184
Fe₅C ₂ (2)	23.8	0.25	0.10	216
Fe₅C ₂ (3)	13.0	0.20	0.07	109
Fe(II)Fe(III)	3.6	0.23	1.11	



Fig. S17. Mössbauer spectra of α -Fe₂O₃ after reaction.

Table S6. Mössbauer	parameters of α -Fe ₂ O ₃	after reaction.
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Phase	Spectral Contribution(%)	IS (mms)	QS (mms)	Hhf (kOe)
Fe ₃ O ₄ (A)	22.8	0.30	0.03	500
Fe ₃ O ₄ (B)	17.5	0.67	0.02	465
Fe ₅ C ₂ (1)	24.7	0.18	0.03	185
Fe_5C_2 (2)	20.3	0.26	0.08	220
Fe_5C_2 (3)	10.9	0.21	0.04	111
Fe(II)Fe(III)	3.8	0.21	1.00	



Fig. S18. The catalytic (a) activity and (b) selectivity of α -Fe₂O₃ and α -C3OA30.



Fig. S19. Raman spectra of α -C30A0.

Theoretical Calculation

The DFT calculations were carried out by using the Vienna ab initio simulation package (VASP)^{8, 9}. The exchange-correlation interaction is described by generalized gradient approximation (GGA) with the Perdew–Burke–Ernzerhof (PBE) functional¹⁰. The Van der Waals interaction was described by using the empirical correction in Grimme's scheme, i.e. DFT+D₃¹¹. The energy cutoff was set to 500 eV. To model (021) surface, a 3-atom-layer slab, including two buffer layers and one fixed layer, were used. For (510) surface's case, a slab with two buffer layers and two fixed layers were constructed. In addition, a vacuum region of 15 Å was used to avoid the interactions among the periodic slabs. The CO₂ reduction was processed on the top of (510) and (021) surfaces (vacuum region). The Brillouin zone was sampled by a Monkhorst-Pack $2 \times 3 \times 1$ and $3 \times 2 \times 1$ K-point grid in reciprocal space for (510) and (021) slabs, respectively. The CI-NEB method was used to find saddle points and minimum energy paths¹². In all of our calculations, atoms in fixed region are held fixed at the bulk positions, while the atoms in the buffer and vacuum regions are fully relaxed until all force components acting on the atoms are below 0.005 eV/Å.

	(021)					(510)				
Reactions	Total	energy (eV)	Ea	∆E	Tota	l energy (eV)	Ea	riangleE (eV)		
			(eV)	(eV)			(eV)			
C+H	R	-919.96			R	-682.43				
\downarrow	TS	-918.96	1.00	0.35	TS	-681.63	0.80	0.53		
СН	Р	-919.61			Р	-681.90				
CH+H	R	-923.69			R	-685.98				
↓ ↓	TS	-922.65	1.04	0.90	TS	-685.02	0.96	0.83		
CH ₂	Р	-922.79			Р	-685.15				
CH ₂ +H	R	-926.84			R	-689.20				
↓ ↓	TS	-925.87	0.97	0.18	TS	-688.52	0.67	0.37		
CH₃	Р	-926.66			Р	-688.82				
CH₃+H	R	-930.75			R	-692.91				
↓ ↓	TS	-929.60	1.15	0.24	TS	-691.46	1.45	0.46		
CH_4	Р	-930.51			Р	-692.46]			

 Table S7. Influence of crystal facet on CH₄ formation reaction barrier and reaction energy.

 Table S8. Influence of crystal facet on C-C coupling reaction barrier and reaction energy.

	(021)			(510)				
Reactions	Total	energy (eV)	Ea	ΔE	Tota	al energy (eV)	Ea	\triangle E (eV)
			(eV)	(eV)			(eV)	
CH ₂ +CH ₂	R	-930.41			R	-701.90		
↓ ↓	TS	-929.36	1.05	-0.17	TS	-700.83	1.07	0.17
CH ₂ CH ₂	Р	-930.57			Р	-701.73		
CH ₂ CH ₂ +H	R	-934.62			R	-705.89		
↓ ↓	TS	-934.24	0.39	0.26	TS	-704.89	1.00	0.66
CH ₂ CH ₃	Р	-934.37			Р	-705.24		
CH ₂ CH ₃ +H	R	-938.41			R	-709.38		
↓ ↓	TS	-937.08	1.32	0.43	TS	-708.38	1.00	0.36
CH ₃ CH ₃	Р	-937.98			Р	-709.03		
CH ₂ +CH ₂ CH ₂	R	-947.21			R	-718.91		
↓ ↓	TS	-946.37	0.84	-0.13	TS	-716.94	1.98	0.84
CH ₂ CH ₂ CH ₂	Р	-947.35			Р	-718.08		
CH ₂ CH ₂ CH ₂	R	-947.35			R	-718.08		
↓ ↓	TS	-946.33	1.02	-0.84	TS	-717.84	0.24	-0.75
CH ₂ CHCH ₂ +H	Р	-948.18			Р	-718.83		
CH ₂ CHCH ₂ +H	R	-948.18			R	-718.83		
↓ ↓	TS	-947.02	1.17	0.81	TS	-717.89	0.94	0.25
CH ₂ CHCH ₃	Р	-947.37			Р	-718.58		
CH ₂ CH ₂ CH ₂ +H	R	-951.22			R	-721.99		
↓ ↓	TS	-950.28	0.94	0.26	TS	-720.98	1.00	-0.18
CH ₂ CH ₂ CH ₃	Р	-950.95			Р	-722.16		
CH ₂ CH ₂ CH ₃ +H	R	-955.06			R	-726.41		
↓ ↓	TS	-953.69	1.37	0.46	TS	-724.59	1.83	0.65
CH ₃ CH ₂ CH ₃	Р	-954.60			Р	-725.76]	
CH ₃ CHCH ₂ +H	R	-951.39			R	-722.75		
↓ ↓	TS	-949.34	2.05	0.43	TS	-721.52	1.23	0.59
CH ₃ CH ₂ CH ₂	Р	-950.95			Р	-722.16		
CH ₂ CH ₂ CH ₃ +H	R	-955.06			R	-726.41		
↓ ↓	TS	-953.69	1.37	0.46	TS	-724.59	1.83	0.65
CH ₃ CH ₂ CH ₃	Р	-954.60			Р	-725.76		
CH ₂ +CH ₂ CH ₂ CH ₂	R	-963.90			R	-725.61		
↓ ↓	TS	-962.30	1.60	-0.06	TS	-722.73	2.88	1.21
CH ₂ CH ₂ CH ₂ CH ₂ CH ₂	Р	-963.96	1		Р	-724.41	1	

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