Supporting Information

## Suppression of H<sub>2</sub> bubble formation on an electrified Pt electrode interface in an acidic "water-in-salt" electrolyte solution

Cheolmin Park<sup>1</sup>, Jinho Chang<sup>1,2\*</sup>

<sup>1</sup>Department of Chemistry and Research Institute for Convergence of Basic Science, Hanyang University, Seoul 04763, Republic of Korea

<sup>2</sup>Department of HY-KIST Bio-convergence, Hanyang University, Seoul 04763, Republic of Korea

Table of Contents						
Figure S1. S-1						
The linearity of $i_{pc}$ and $i_{pa}$ as a function of $v^{1/2}$ .						
Figure S2. S-2						
(a) The CV at 50 mV/s on a Pt MDE in a 6 m LiTFSI solution containing 50 mM HClO <sub>4</sub> (black line) and the best-fit simulation result (red circle), and (b) the surface concentration profiles of chemical species from the simulated CV in a. For the simulation, the e <sup>-</sup> -transfer rate constant, $k^{0}$ , and the transfer coefficient, $\alpha$ , were set to be 0.1 cm/s and 0.5, respectively.						
Figure S3. S-3						
The CV in an aqueous 6 m LiTFSI solution without $HClO_4$ on a Pt UME at 20mV/s.						
Figure S4. S-4						
The $i_{pa}/i_{pc}$ vs. v plots in aqueous solutions containing the four different types electrolytes with 25 mM HClO <sub>4</sub> .						
Figure S5. S-5						
The CVs (black line) at various $v$ (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiTFSI solutions containing either (a-d) 50 or (e-h) 100 mM HClO <sub>4</sub> , and the corresponding best-fit simulation results (dotted red circle).						
simulation results (dotted red circle).						

Figure S6. S-6

The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiOTf solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted blue circle).

Figure S7. S-7

The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiNO<sub>3</sub> solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted pink circle).

Figure S8. S-8

The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiCl solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted green circle). For the CV in e, the experimentally obtained CV was too distorted to be fitted by the digital simulation due to the adsorption of H<sub>2</sub> bubbles on an electrode surface.

Figure S9. S-9

(a) The electrode potential profile vs. t for (b) the resulting voltammograms at 20 mV/s, which were measured from acidic solutions with the four different types of 6 m electrolytes.

Figure S10. S-10

The sequential snapshots of  $H_2$  bubble formation on a Pt MDE during cyclic voltammetry for  $H^+/H_2$  redox reaction in 50 mM HClO<sub>4</sub> solutions containing either (a) 6 m LiCl or (b) the same molal concentration of LiTFSI.

Note S1. S-11

Estimation of the thickness of a modulation layer

Figure S11. S-12

The  $\zeta$ -histograms obtained from  $\Delta f$  vs. t curves in solutions containing various molal concentrations of LiOTf.

Figure S12. S-13

The  $\Delta f$  vs. *t* curves during HER on Pt electrodes in 50 mM HClO<sub>4</sub> solutions containing 6 m LiTFSI (black) and 9 m LiTFSI (red) through the EQCM measurements.

Note S2. S-14

The EQCM measurements for retention of electrogenerated  $H_2$  bubbles on a Pt electrode as a function of applied potentials.

Figure S13. S-15

The  $\Delta f$  vs. *t* curves measured in acidic 3 m LiTFSI solutions on a Pt electrode as the electrode potential was applied to -0.6 V for 40 minutes and stepped to (a) 0, (b) 0.5, (c) 1, and (d) 1.5 V vs. Ag/AgCl, respectively.

Figure S14. S-16 The  $C_d$  as a function of the electrode potentials (vs. Ag/AgCl) on Pt MDEs in 6 m (a) LiTFSI

Figure S15. S-17

and (b) LiOTf solutions.

The  $C_d$  as a function of the electrode potentials (vs. Ag/AgCl) on an Au MDE in a 6 m LiTFSI solution.

```
Table S1. S-18
```

The reaction parameters for the simulation results in Figure S5-S8. The transfer coefficients of all the charge transfer reactions were assumed to be 0.5.

Table S2. S-19

The measured parameters in acidic solutions containing different types of 6 m electrolytes for the calculation of the thickness of the modulation layers,  $\lambda$ .

```
References S-20
```



**Figure S1.** The linearity of  $i_{pc}$  and  $i_{pa}$  as a function of  $v^{1/2}$ .



**Figure S2.** (a) The CV at 50 mV/s on a Pt MDE in a 6 m LiTFSI solution containing 50 mM HClO<sub>4</sub> (black line) and the best-fit simulation result (red circle), and (b) the surface concentration profiles of chemical species from the simulated CV in a. For the simulation, the e<sup>-</sup>-transfer rate constant,  $k^{\circ}$ , and the transfer coefficient,  $\alpha$ , were set to be 0.1 cm/s and 0.5, respectively.



Figure S3. The CV in an aqueous 6 m LiTFSI solution without  $HClO_4$  on a Pt UME at 20mV/s.



**Figure S4.** The  $i_{pa}/i_{pc}$  vs. v plots in aqueous solutions containing the four different types electrolytes with 25 mM HClO<sub>4</sub>.



**Figure S5.** The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiTFSI solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted red circle).



**Figure S6.** The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiOTf solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted blue circle).



**Figure S7.** The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiNO<sub>3</sub> solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted pink circle).



**Figure S8.** The CVs (black line) at various v (20, 50, 100, and 200 mV/s) on a Pt MDE in 6 m LiCl solutions containing either (a-d) 50 or (e-h) 100 mM HClO<sub>4</sub>, and the corresponding best-fit simulation results (dotted green circle). For the CV in e, the experimentally obtained CV was too distorted to be fitted by the digital simulation due to the adsorption of H<sub>2</sub> bubbles on an electrode surface.



Figure S9. (a) The electrode potential profile vs. t for (b) the resulting voltammograms at 20 mV/s, which were measured from acidic solutions with the four different types of 6 m electrolytes.



**Figure S10.** The sequential snapshots of  $H_2$  bubble formation on a Pt MDE during cyclic voltammetry for  $H^+/H_2$  redox reaction in 50 mM HClO<sub>4</sub> solutions containing either (a) 6 m LiCl or (b) the same molal concentration of LiTFSI.

## Note S1. Estimation for thickness of a modulation layer

The thickness of the modulation layer  $(\lambda)$  in solutions with different types of 6 m electrolytes were estimated by the following equation.<sup>1</sup>

$$\lambda = \frac{1}{2} \left( \sqrt{\frac{\rho\omega}{2\eta}} \right)^{-1} \tag{1}$$

Here,  $\omega$  is the resonant frequency of the fundamental mode,  $\rho$  is the liquid density, and  $\eta$  is the liquid viscosity. Each of the corresponding parameters and the estimated  $\lambda$  in the different electrolytes solutions are listed in Table S2.



**Figure S11.** The  $\zeta$ -histograms obtained from  $\Delta f$  vs. *t* curves in acidic solutions containing various molal concentrations of LiOTf.



**Figure S12.** The  $\Delta f$  vs. *t* curves during HER on Pt electrodes in 50 mM HClO<sub>4</sub> solutions containing 6 m LiTFSI (black) and 9 m LiTFSI (red) through the EQCM measurements.

## Note S2. The EQCM measurements for retention of electrogenerated H<sub>2</sub> bubbles on a Pt electrode as a function of applied potentials

We chose an aqueous acidic solution containing 3 m LiTFSI as a model electrolyte condition. For the EQCM measurements, -0.6 V was constantly applied for 40 minutes to drive HER, and the potential was stepped to various positive values for another 20 minutes. After  $\Delta f$  increased and reached at the equilibrium under at constantly applied -0.6 V for 40 min., the potential was stepped to either 0 or 0.5 V, and  $\Delta f$  barely decreased (see Figure S9a-b). As the electrode potential was positively stepped to 1 and 1.5 V (Figure S9c-d),  $\Delta f$  instantaneously reduced, and in the case of 1.5 V,  $\Delta f$  was even reduced to ~0.



**Figure S13.** The  $\Delta f$  vs. *t* curves measured in acidic 3 m LiTFSI solutions on a Pt electrode as the electrode potential was applied to -0.6 V for 40 minutes and stepped to (a) 0, (b) 0.5, (c) 1, and (d) 1.5 V vs. Ag/AgCl, respectively.



**Figure S14.** The  $C_d$  as a function of the electrode potentials (vs. Ag/AgCl) on Pt MDEs in 6 m (a) LiTFSI and (b) LiOTf solutions.



**Figure S15.** The  $C_d$  as a function of the electrode potentials (vs. Ag/AgCl) on an Au MDE in a 6 m LiTFSI solution.

**Table S1.** The reaction parameters for the simulation results in Figure S5-S8. The transfer coefficients of all the charge transfer reactions were assumed to be 0.5.

	6 m LiTFSI	6 m LiOTf	6 m LiNO <sub>3</sub>	6 m LiCl
Diffusion coefficient	$D_{H^+} = 9 \times 10^{-6} \mathrm{cm}^2/\mathrm{s}$	$D_{H^+} = 1.4 \times 10^{-5} \mathrm{cm}^2/\mathrm{s}$	$D_{H^+} = 3 \times 10^{-5} \mathrm{cm^2/s}$	$D_{H^+} = 3 \times 10^{-5} \mathrm{cm^{2/s}}$
Charge transfer reaction	$E^0 = -0.4 \text{ V}$	$E^0 = -0.4 \text{ V}$	$E^0 = -0.4 \text{ V}$	$E^0 = -0.4 \text{ V}$
$H^+ + e^- \rightleftharpoons H$	$k_{\text{et}} = 0.03 \text{ cm/s}$	$k_{\text{et}} = 0.03 \text{ cm/s}$	$k_{\text{et}} = 0.03 \text{ cm/s}$	$k_{\text{et}} = 0.03 \text{ cm/s}$
Chemical reaction	$K_{\rm eq} = 2 \times 10^4 { m M}^{-1}$	$K_{\rm eq} = 2 \times 10^4 {\rm M}^{-1}$	$K_{\rm eq} = 2 \times 10^4 {\rm M}^{-1}$	$K_{\rm eq} = 2 \times 10^4 {\rm M}^{-1}$
$H + H \rightleftharpoons H_2$	$k_{\rm f} = 2 \times 10^7 { m M}^{-1}{ m s}^{-1}$	$k_{\rm f} = 2 \times 10^7 {\rm M}^{-1}{\rm s}^{-1}$	$k_{\rm f} = 2 \times 10^7 {\rm M}^{-1}{\rm s}^{-1}$	$k_{\rm f} = 2 \times 10^7 {\rm M}^{-1} {\rm s}^{-1}$
$H_2 + H_2 \rightleftharpoons (H_2)_2$	$K_{\rm eq} = 3.5 \times 10^8 { m M}^{-1}$	$K_{\rm eq} = 3.5 \times 10^8 {\rm M}^{-1}$	$K_{\rm eq} = 3.5 \times 10^8 {\rm M}^{-1}$	$K_{eq} = 3.5 \times 10^8 \mathrm{M}^{-1}$
	$k_{\rm f} = 0.01 { m M}^{-1} { m s}^{-1}$	$k_{\rm f} = 0.6 {\rm M}^{-1}{\rm s}^{-1}$	$k_{\rm f} = 4 {\rm M}^{-1}{\rm s}^{-1}$	$k_f = 56 \mathrm{M}^{-1} \mathrm{s}^{-1}$

	No Li electrolytes	6 m LiTFSI	6 m LiOTf	6 m LiNO <sub>3</sub>	6 m LiCl
η (cp)	0.91	4.51	3.4	2.2	1.9
ho (g/cm <sup>3</sup> )	1.03	1.44	1.33	1.2	1.12
$\lambda$ (nm)	220	420	380	320	308

**Table S2.** The measured parameters in acidic solutions containing different types of 6 m electrolytes for the calculation of the thickness of the modulation layers,  $\lambda$ .

## References

1. S. Na Songkhla and T. Nakamoto, Chemosensors, 2021, 9, 350.