

# Sequencing batch photocatalytic H<sub>2</sub>O<sub>2</sub> production over magnetic resorcinol-formaldehyde polymer for on-site water purification by UV light irradiation

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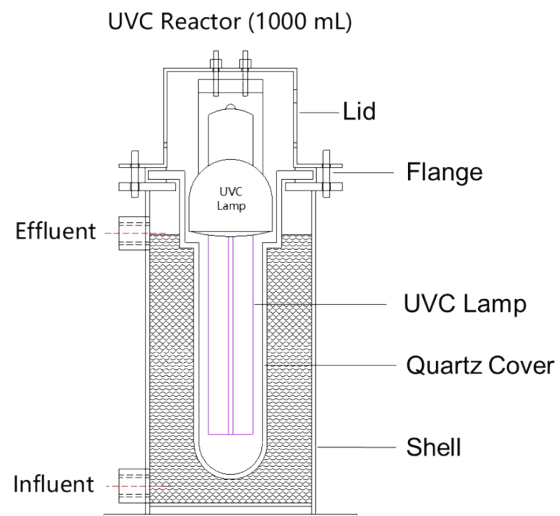
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**Table S1** Comparison of photocatalytic H<sub>2</sub>O<sub>2</sub> production over different photocatalysts in pure water

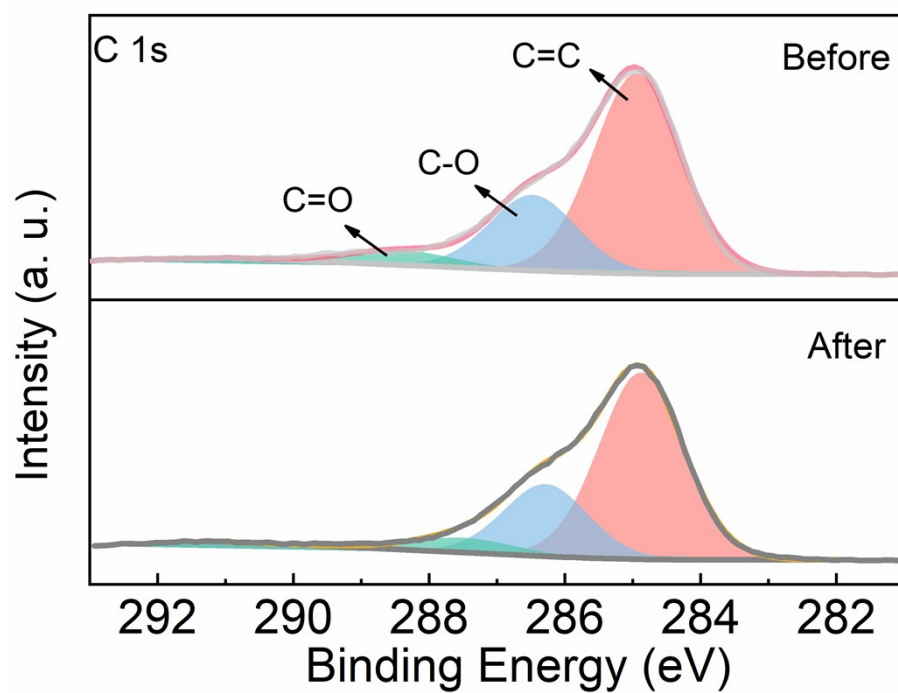
| Cat. (g/L)                            | $\lambda$ (nm) | Time (h)  | H <sub>2</sub> O <sub>2</sub> ( $\mu$ mol/L) | Ref.             |
|---------------------------------------|----------------|-----------|----------------------------------------------|------------------|
| Au/WO <sub>3</sub> (1.67)             | >420           | 10        | 13.9                                         | 1                |
| Au/BiVO <sub>4</sub> (1.67)           | >420           | 10        | 40.2                                         | 1                |
| Co-GCN/AQ (0.5)                       | >300           | 1         | 60                                           | 2                |
| Znnppc-BCN (0.4)                      | 400-800        | 1         | 45.6                                         | 3                |
| CdS/rGO (1.0)                         | >420           | 12        | 130                                          | 4                |
| SbPCN (2.0)                           | >420           | 2         | 365                                          | 5                |
| ORP/GCN (1.0)                         | >420           | 10        | 400                                          | 6                |
| GCN/MTI (1.67)                        | 420-500        | 24        | 917                                          | 7                |
| GCN/PDI/rGO (1.67)                    | 420-500        | 24        | 970                                          | 8                |
| <b>MRF (1 g/L)</b>                    | <b>&gt;420</b> | <b>12</b> | <b>1200</b>                                  | <b>This work</b> |
| CoO : MoBiVO <sub>4</sub> : Pd (0.17) | AM 1.5         | 1         | 1425                                         | 9                |
| RF523 (1.67)                          | 420-700        | 24        | 3300                                         | 10               |

**Table S2** Removal efficiency and EEO value of different treatment processes

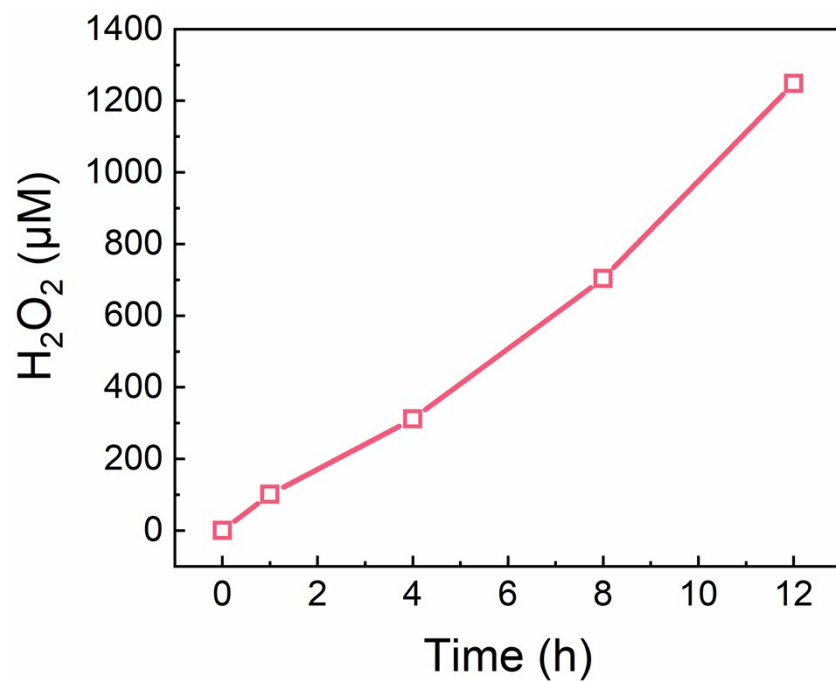
| Treatment process                | Contaminants                   | Removal efficiency (%) | EEO value (kWh/m <sup>3</sup> /order) | Ref.      |
|----------------------------------|--------------------------------|------------------------|---------------------------------------|-----------|
| Photo-Fenton                     | Reactive Orange 4              | 100%                   | 357.1                                 | 11        |
| UV-H <sub>2</sub> O <sub>2</sub> | Reactive Orange 4              | 80%                    | 1666.7                                | 11        |
| UV-TiO <sub>2</sub>              | Reactive Black 5               | 70%                    | 220.0                                 | 12        |
| UV-TiO <sub>2</sub>              | Sodium dodecylbenzenesulfonate | 100%                   | 595.0                                 | 13        |
| UV/Peroxydisulfate               | Basic Red 46                   | 80%                    | 155.4                                 | 14        |
| Flow-through                     | Rhodamine B                    | 99%                    | 10.4                                  | This Work |
| UV-H <sub>2</sub> O <sub>2</sub> | Humic acid                     | 65%                    | 54.8                                  |           |
|                                  | Tetracycline                   | 80%                    | 35.8                                  |           |



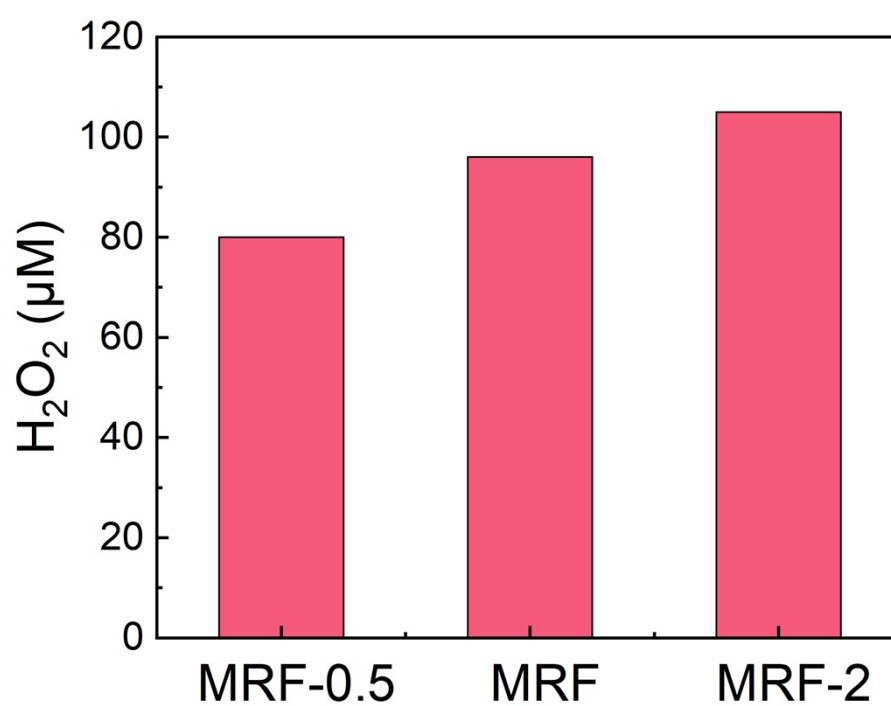
**Figure S1** The section view of UVC reactor for a flow through process.



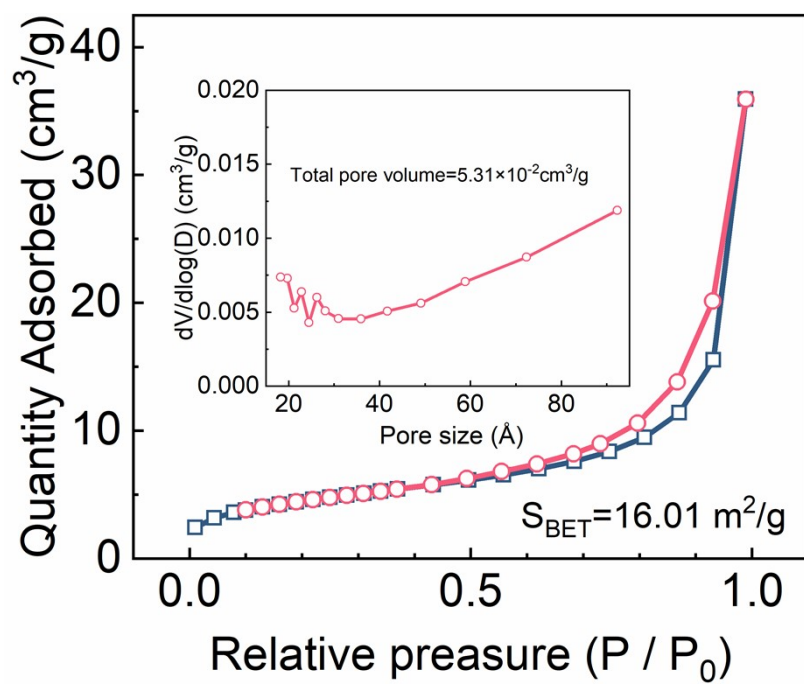
**Figure S2** The C 1s high-resolution XPS spectra of MRF before and after usage.



**Figure S3** Photocatalytic  $\text{H}_2\text{O}_2$  production over MRF upon prolonged irradiation  
(catalysts: 1 g/L, pH = 7,  $\lambda > 420$  nm, Air: 0.5 L/min).

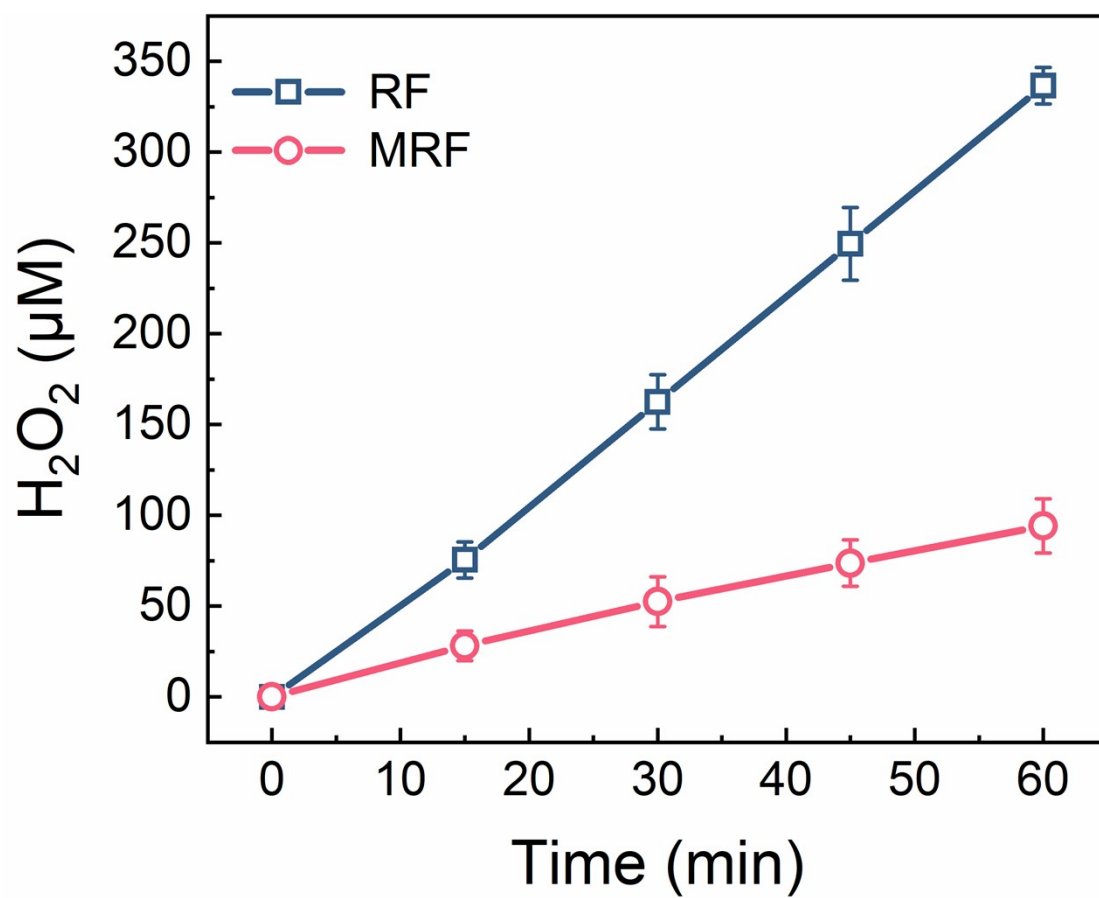


**Figure S4** Photocatalytic  $\text{H}_2\text{O}_2$  production within 60 min over MRFs with different RF contents (catalysts: 1 g/L, pH = 7.5,  $\lambda > 420$  nm, Air: 0.5 L/min).

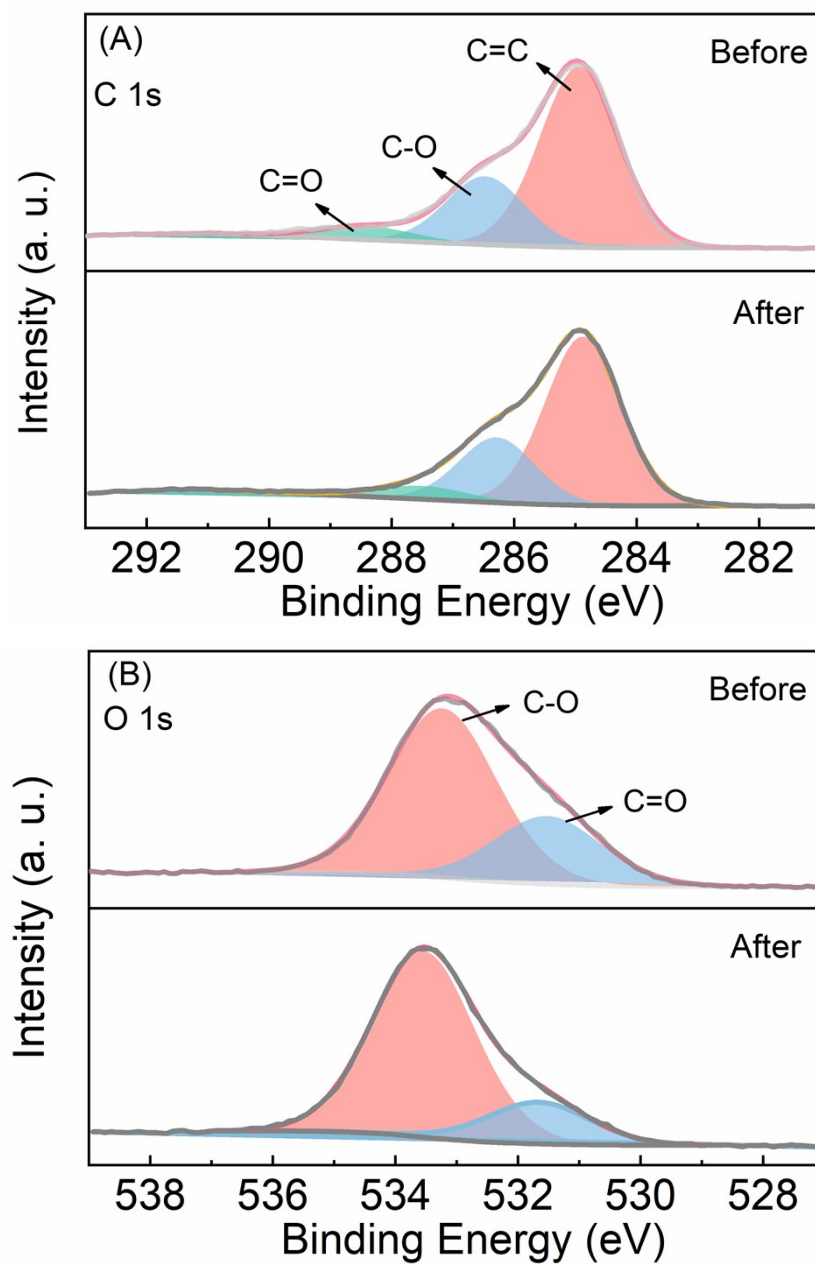


**Figure S5** N<sub>2</sub> adsorption/desorption analysis for MRF (inset is the pore-size distribution curve).

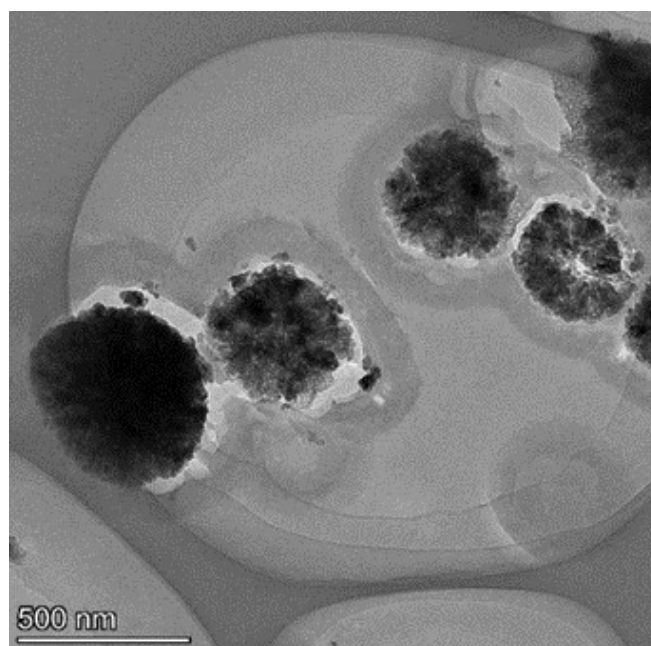




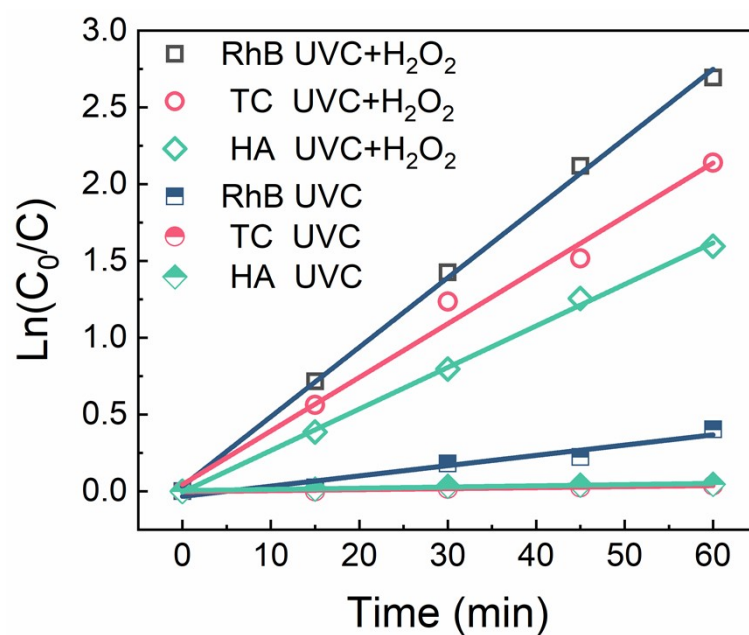
**Figure S6** Photocatalytic  $\text{H}_2\text{O}_2$  production over RF and MRF powders (Catalysts: 1 g/L, pH=7,  $\lambda > 420$  nm, Air: 0.5 L/min).



**Figure S7** (A) C 1s and (B) O 1s high-resolution XPS spectra of MRF before and after photocatalytic reaction.



**Figure S8** TEM image of MRF after photocatalytic reaction.



**Figure S9** Kinetic model of RhB, TC and HA decomposition in the batch UVC/H<sub>2</sub>O<sub>2</sub> process (RhB, TC or HA: 1 mg/L; H<sub>2</sub>O<sub>2</sub>: 10 μM).

| The Slope and R <sup>2</sup> of kinetic model in <b>Figure S9</b> |                            |                |
|-------------------------------------------------------------------|----------------------------|----------------|
|                                                                   | Slope (min <sup>-1</sup> ) | R <sup>2</sup> |
| RhB UVC+H <sub>2</sub> O <sub>2</sub>                             | 0.045                      | 0.997          |
| TC UVC+H <sub>2</sub> O <sub>2</sub>                              | 0.032                      | 0.984          |
| HA UVC+H <sub>2</sub> O <sub>2</sub>                              | 0.027                      | 0.998          |
| RhB UVC                                                           | 0.0067                     | 0.923          |
| TC UVC                                                            | 0.00066                    | 0.930          |
| HA UVC                                                            | 0.00078                    | 0.932          |

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