Electronic property-dependent activity and durability in Pd/C

catalyzed hydrogenation of benzoic acid

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Experimental detail

Synthesis of Pd/C-H₂O₂, Pd/C-50 and Pd/C-150 catalysts

The commercial Pd/C catalysts (Batch number: D5H2B) were obtained from Shannxi Rock New Materials Co., Ltd. and washed three times alternately by ethanol and water. The loading of Pd in Pd/C was 5.0 wt.%.

The Pd/C-H₂O₂ catalysts were treated by 30 *wt*.% H₂O₂ solution. Typically, 100 mg of the commercial Pd/C catalysts were dispersed in a 25 mL of deionized water and 2.5 mL H₂O₂ solution (30 *wt*.%), and then stirred at room temperature for 1 h. After the oxidation process, the Pd/C-H₂O₂ catalysts were washed with H₂O for three times and dried at 60 °C.

The commercial Pd/C catalysts were treated in 5% H_2/Ar at 50°C and 150°C for 2 h, respectively, to yield the Pd/C-50 and Pd/C-150 catalysts.

Catalyst Characterization

High-resolution TEM (HRTEM) images and element dispersive spectroscopy (EDS) images were recorded by a JEOL JEM-2100F with electron acceleration energy of 200 kV. High-angle annular dark field scanning TEM (HAADF-STEM) images were taken by JEOL 200F TEM operated at 200 keV, which was equipped with a probe spherical aberration corrector. All measured binding energies were calibrated with the C 1s peak (284.6 eV). The d-band electron structures of various catalysts were characterized by high-resolution valence-band (VB) XPS analysis.

Catalytic Reaction

For a typical hydrogenation of benzoic acid (BA), 20 mg of catalyst and 2 mmol of BA were added to 3 mL of isopropanol in 8 mL glass tube. Then, the glass tube was transferred into the autoclave equipped with a pressure system. After purging with 1 MPa H_2 for three times, the hydrogenation was performed at 100°C for a given time. The products were analyzed by gas chromatography (GC, Agilent 7890B).

The BA (A) conversion is defined by:

$$Conv.A\% = \frac{n_A - n_A}{n_A} \times 100$$

The reaction rate was calculated as:

$$r = \frac{n_A \times (1 - Conv.A)/V}{t}$$

(2)

(1)

Where n_A is the molar amount of BA added in the reaction system; $n_{A'}$ the molar amount of BA in the reaction system after the reaction; *Conv.A* is the conversion of substrates at the reaction of *t*; *V* is the volume of reaction solution; *t* is reaction time, h.

Stability test

Typically, 20 mg of catalysts and 2 mmol of BA were added into 3 mL of isopropanol in 10 mL glass bottle. The glass bottle with mixture was transferred to 500 mL of autoclave, which was purged with 1 MPa H_2 for three times. Subsequently, the reactions were carried out at 100°C for 6 h and 1 MPa H_2 . After the reaction, the liquid phase was analyzed using gas chromatograph (Agilent 7890B).

The Pd/C catalyst was centrifuged from the reaction solution and washed three times with isopropanol. Then, 0.5 mL H_2O_2 solution (30 *wt*.%) were added and stirred at room temperature for 1 h. Finally, the separated H_2O_2 treated Pd/C catalysts was used for the next cycles under the same reaction conditions.

XPS analysis

X-ray photoelectron spectroscopy (XPS) spectra were carried out by Thermo Fisher Scientific K-Alpha. The signals of Pd⁰, Pd²⁺ and Pd⁴⁺ of various catalysts were assigned by the NIST XPS Database (<u>https://srdata.nist.gov/xps/selEnergyType.aspx</u>). The XPS peak of Pd *3d* peaks were corrected by the C 1s peaks (binding energy of 284.6 eV). During the fitting process, the peak shape is fitted by Gaussian-Lorentzian with ratio GL of 30%. The FWHM of Pd *3d*_{5/2} and *3d*_{3/2} is consistent. The binding energy difference between Pd *3d*_{5/2} and *3d*_{3/2} is 5.3eV, and the area ratio of Pd *3d*_{5/2} and *3d*_{3/2} is 3:2. The respective peak shifts of Pd⁰, Pd²⁺ and Pd⁴⁺ were listed in the Table S1.

Table S1. Summary of the assigned binding energy of Pd⁰, Pd²⁺ and Pd⁴⁺.

	3d_ _{5/2}			3d _{3/2}		
	Pd ^o	Pd ²⁺	Pd ⁴⁺	Pd ⁰	Pd ²⁺	Pd ⁴⁺
Binding energy (eV)	335.3 ± 0.1	337.3 ± 0.1	338.1 ± 0.1	340.8 ± 0.1	342.6 ± 0.1	343.4 ± 0.1

DFT

The first principle calculations are performed by Vienna Ab initio Simulation Package(VASP)¹ with the projector augmented wave (PAW) method². The exchange-functional is treated using the Perdew-Burke-Ernzerhof (PBE)³ functional, in combination with the DFT-D3 correction⁴. The cut-off energy of the plane-wave basis is set at 400 eV. For the optimization of both geometry and lattice size, the Brillouin zone integration is performed with 2*2*1 Monkhorts-Pack⁵ kpoint sampling. The self-consistent calculations apply a convergence energy threshold of 10⁻⁵ eV. The equilibrium geometries and lattice constances are optimized with maximum stress on each atom within 0.02 eV/Å.

Reference:

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Figure S1. Size distribution of Pd nanoparticles for the Pd/C catalysts.



Figure S2. (a) HRTEM image of the Pd/C catalysts. (b) Fast Fourier transform pattern of the selected yellow area.



Figure S3. (a) TEM image and (b) size distribution of Pd nanoparticles for the Pd/C-50 catalysts.



Figure S4. (a) TEM image and (b) size distribution of Pd nanoparticles for the Pd/C-100 catalysts.



Figure S5. (a) TEM image and (b) size distribution of Pd nanoparticles for the Pd/C-H₂O₂ catalysts.



Figure S6. C 1s peaks of various catalysts.



Figure S7. (a) TEM image and (b) size distribution of Pd nanoparticles for the used Pd/C catalysts without treatment.



Figure S8. (a) TEM image and (b) size distribution of Pd nanoparticles for the used Pd/C catalysts after H_2O_2 treatment.



Figure S9. (a) TEM and (b) HRTEM images of the PdO/C catalysts. (c) XPS analysis of Pd 3d peak of the PdO/C catalysts. (d) Catalytic performance of BA hydrogenation catalyzed the PdO/C catalysts. **Reaction conditions:** BA (2 mmol), PdO/C (20 mg), isopropanol (3 mL), 100 °C and 1 MPa H₂.



Figure S10. Adsorption configuration of benzoic acid molecule on (a) Pd(111) and (b) PdO(111) surface.