## **Electronic Supporting Information**

## SO<sub>x</sub>-modified porous carbon as highly active electrocatalyst for efficient H<sub>2</sub>O<sub>2</sub> generation

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## **Experimental Section**

**Materials:** 2-Hydroxyethyl methacrylate (HEMA), tetraethyl orthosilicate (TEOS), phenylbis(2,4,6-trimethylbenzoyl)phosphine oxide (819), carbon disulfide, and hydrofluoric acid (40%) were purchased from Aladdin (analytically pure grade). All chemicals and reagents were used directly without the further purification process.

**Preparation of SO<sub>x</sub>-Porous C:** 3.0 g of HEMA and 0.084 g of 819 were added into a beaker, and then stirred until completely dissolved. Subsequently, 150 mg of TEOS and different amounts of CS<sub>2</sub> were added to the above solution. After being stirred, the precursor was transferred into the porcelain combustion boat under a UV-curing reaction. The UV-curing process was straightforward; that, the required precursors were exposed under UV light. Then the liquid precursor was transformed into solid very quickly, and all the components in the precursor were uniformly mixed at a molecular level. The SO<sub>x</sub>-porous C was obtained after calcining the above solid precursor in a tubular furnace under a nitrogen atmosphere for 400 °C for 1 h and 700 °C for 1 h with a heating rate of 5 °C min<sup>-1</sup>, respectively. The achieved black powder was treated with HF (40%) for 24 h. The preparation process of porous carbon sample is the same as porous SO<sub>x</sub>-C catalyst, just without the addition of CS<sub>2</sub>. The procedure for synthesizing the catalysts and ORR reaction pathways is illustrated in Figure S1.



Figure S1 Schematic illustration of the catalysts and ORR reaction pathways.

**Characterizations:** Powder X-Ray diffraction (XRD) patterns were collected on a Bruker D8 Advance diffractometer using Cu K $\alpha$  irradiation ( $\lambda$ =1.5406 Å). Raman spectra were measured by the LabRAM HR Evolution Raman spectrometer. N<sub>2</sub> adsorption-desorption curves (BET) were obtained by automatic mesoporous microporous analyzer BK100C. The composition and morphology of the nanocomposite were characterized by transmission electron microscope (TEM, TECNAI-F20). X-ray photoelectron spectra (XPS) was collected on a THS-103X Xray photoelectron spectrometer. Fourier transform infrared spectroscopy (FTIR) was performed with a Nicolet Nexue 670 spectrometer. H<sub>2</sub>O<sub>2</sub> concentration was tested on Perkin Elmer Lambda 750 UV spectrophotometer. The static contact angle results were obtained by a Drop Shape Analysis System DSA100.

**Electrochemical Measurements:** The catalytic performance of the as-prepared  $SO_{x^{-}}$  porous C and porous C catalysts were tested at the CHI 760E electrochemical workstation and the rotary disk facility of Pine Company. A three-electrode system was constructed with an Ag/AgCl electrode as the reference electrode, platinum wire as the counter electrode, and a glassy carbon electrode (GC, diameter 5mm, effective area of 0.196 cm<sup>2</sup>) coated with catalyst as the working electrode. The 5 mg catalyst was dispersed and treated by ultrasonication in a mixture of 20 µL Nafion (5 wt%), 0.2 mL ethanol, and 0.78 mL deionized water for 40 min to form homogeneous catalyst ink. Subsequently, 27.5 µL of the above ink was transferred to the carbon electrode to prepare the working electrode. The cyclic voltammetry (CV) of the catalyst was tested in 0.1 M N<sub>2</sub>-saturated KOH solution at room temperature with the potential range of -

0.8 to 0.3 V (vs. Ag/AgCl), and the scanning rate was 50 mV s<sup>-1</sup>. The H<sub>2</sub>O<sub>2</sub> selectivity was obtained by linear sweep voltammetry in 0.1 M KOH solution saturated with O<sub>2</sub> at a rotating speed of 1600 rpm. The stability was determined by CV at a scanning rate of 100 mV s<sup>-1</sup> in an O<sub>2</sub> saturated solution of 0.1 M KOH at room temperature. The selectivity of hydrogen peroxide measured at the ring disk electrode is determined using the following relation:

$$H_2O_2(\%) = 200 * I_r / (N * I_d) + I_r$$

The number of transferred electrons measured at the ring disk electrode is based on the equation as follows:

$$n = 4 * I_d / (I_d + I_r / N)$$

in which  $I_r$  is the ring current,  $I_d$  is the ring current, and N is the collection efficiency of hydrogen peroxide at the ring electrode (N=0.37).

The synthesis of  $H_2O_2$  was carried out in a three-electrode system with an H-type electrolytic cell separated by a Nafion115 (Dupont) membrane. The platinum wire is used as the counter electrode, and Ag/AgCl as the reference electrode. 5 mg of catalyst is dispersed in 10 µL Nafion (5 wt %), 0.25 mL isopropanol, and 0.74 mL deionized water. The ink was dispersed uniformly by ultrasonication for more than 40 minutes, and then the working electrode can be obtained through evenly coating the carbon paper with a catalyst loading of 0.5 mg cm<sup>-2</sup>. In a 10 mL O<sub>2</sub>-saturated 0.1 M KOH, 1 mL reaction solution was taken at different intervals to identify the concentration of  $H_2O_2$  after the I-t test at 0.5 V vs. RHE.

TiO(SO<sub>4</sub>) was used as a chromogenic agent, and UV-visible spectrum was used for the quantitative determination of  $H_2O_2$ . The principle of quantitative reaction is based on the chemical equation  $Ti^{4+} + H_2O_2 + 2H_2O = H_2TiO_4 + 4H^+$ . 0.37g of TiOSO<sub>4</sub> was dissolved in 50 mL water.  $H_2O_2$  of known concentration was added to the TiOSO<sub>4</sub> solution and measured using UV- visible spectrum, then the calibration curve was obtained. And the concentration of  $H_2O_2$  could be calculated according to the standard curve (Figure S1).



Figure S2 The standard curves of  $H_2O_2$  with varying concentrations ranging from 0.1 to 1 mM.

The Faraday efficiency is calculated according to the following formula:

$$FE(\%) = 2n_{H_2O_2} * \frac{100}{ne^-} = 2Fc_{H_2O_2}V * 100/It$$

Where  ${}^{n_{H_2O_2}}$  is the produced H<sub>2</sub>O<sub>2</sub> (mol),  $ne^-$  is the electron consumption (mol), *F* is the Faraday constant (96,485 C mol<sup>-1</sup>),  ${}^{c_{H_2O_2}}$  is the produced H<sub>2</sub>O<sub>2</sub> concentration (mol L<sup>-1</sup>), V is the volume of catholyte (10.0 mL), I is the current (A), and t is the time (s).

**Computational methods:** First-principles calculations were carried out on the basis of periodic DFT using a generalized gradient approximation within the Perdew-Burke-Ernzerhof exchange correction functional. We used the projector-augmented wave method for describing ionic cores as implemented in the Vienna ab initio simulation package (VASP). DFT calculations were performed using the Vienna Ab initio Simulation Package (VASP). The wave functions were constructed from the expansion of plane waves with an energy cutoff of 450 eV. Gamma centered k-piont of  $3\times3\times1$  have been used for geometry optimization. The consistence tolerances for the geometry optimization are set as  $1.0 \times 10^{-5}$  eV/atom for total energy and 0.05 eV/Å for force, respectively. In order to avoid the interaction between the two surfaces, a large vacuum gap of 15 Å has been selected in the periodically repeated slabs.



Initiators produce free radicals:  $I \xrightarrow{hv} R$ .

Free radicals initiate polymerization of monomers:

 $R \cdot + CH_2 = CHR \longrightarrow RCH_2C \cdot HR$   $RCH_2C \cdot HR + n CH_2 = CHR \longrightarrow R(CH_2CHR)_n - CH_2 - C \cdot HR$  $m R(CH_2CHR)_n - CH_2 - C \cdot HR \longrightarrow Unreactive species$ 

Figure S3 UV-curing polymerization mechanism.



Figure S4 SEM images of (a) porous C and (b) SO<sub>x</sub>-porous C.



Figure S5 (a-c) TEM image, and (d) HRTEM images of porous C.







Figure S7 XRD patterns of SO<sub>x</sub>-porous C and porous C.



Figure S8 Raman spectra of  $SO_x$ -porous C and porous C.



Figure S9 (a)  $N_2$  adsorption/desorption isotherms, (b) the corresponding pore size

distribution.

Sample	Surface area	Pore volume
	(m <sup>2</sup> /g)	$(cm^{3}/g)$
Porous C	244.55	0.31
SO <sub>x</sub> -Porous C	311.96	6.36

**Table S1** Physical properties of porous C and SO<sub>x</sub>-porous C.

	C/%	O/%	S/%
porous C	67.67	32.33	0
SO <sub>x</sub> -porous C	70.69	27.68	1.63

Table S2 The mass ratio of C, O, and S element for porous C and  $SO_x$ -porous C



Figure S10 (a) RRDE voltammograms of  $SO_x$ -porous C catalysts with different mass ratios of HEMA and  $CS_2$  in  $O_2$ -saturated 0.1 M KOH. (b)  $H_2O_2$  selectivity of  $SO_x$ -porous C catalysts.



Figure S11 (a) Electron transfer number of of porous C and  $SO_x$ -porous C catalysts.



Figure S12 CV curves of SO<sub>x</sub>-porous C and porous C at different scan rates.



Figure S13 Electrochemically active surface area measurements of SO<sub>x</sub>-porous C and porous C.



Figure S14 LSV (a) and CV (b) curves of  $SO_x$ -porous C after cycles.



Figure S15 TEM (a), HRTEM (b), STEM (c), and TEM-EDX elemental mapping (df) of O, C and S in SO<sub>x</sub>-porous C after stability test.



Figure S16 S 2p XPS spectra of SO<sub>x</sub>-porous C after 10000 CV cycles of ORR.

Sample	nple S% O%		S%	O%	
	(EDS)	(EDS)	(XPS)	(XPS)	
Initial	1.83	29.90	1.63	27.68	
After cycles	1.50	22.00	1.22	20.10	

**Table S3** The mass ratio of S and O element of S-porous C before and after the10.000 cvcles.



**Figure S17** The configurations of C-O and C=O examined in this study.



Figure S18 Calculated two-electron ORR-related volcano plot for  $H_2O_2$  formation for the studied configurations.

	electrolyte	Potential	Selectivity	productivity	Ref.
		(V <sub>RHE</sub> )	(%)		
S-porous C	0.1M KOH	0.3-0.6	~95	$604.2 \text{ mmol } g_{cat}^{-1} \text{ h}^{-1}$	This
				(0.5 V vs RHE)	work
_					
Porous C	0.1M KOH	0.4	~87		This
		0 4 0 6 7	0.0	2050 T 11 1	work
O-CN1s	0.1M KOH	0.4-0.65	~90	$\sim 3950 \text{ mg L}^{-1} \text{ h}^{-1}$	[1]
$CNT_{a}$		0 4 0 65	60	(30 mA)	[1]
CNTS	0.1M KOH	0.4-0.03	~60		[1]
Commercial	0.11M KOH	0.07	90		[Z]
5)					
Mesoporous	0 1M KOH	0.55	80		[3]
defective	0.1101 11011	0.00	00		[9]
carbon					
Nitrogen-doped	0.1M KOH	0.5	95		[4]
carbon					
BN-C1	0.1M KOH	0.65	90		[2]
F-mrGO	0.1M KOH	0.75	100	430.8 mmol $g_{cat}^{-1}$	[2]
				$h^{-1}$	
				(0.685 V vs RHE)	
GOMC	0.1M KOH	0.72	93		[5]
				$51.3 \pm 4 \text{ mg } \text{L}^{-1} \text{h}^{-1}$	
				(3 mA)	
HPCS-S	0.1M KOH	0.5	70	183.99 mmol $g_{cat}^{-1}$	[6]
				$h^{-1}$	
E. ONT		0.75	> 05	(0.3  V vs RHE)	[7]
Fe-CNI		0.75	>95		[/] [7]
CO-CN1	0.11M KOH	0.05	/4		[/]
Co-POC-O	0 1М КОН	0.6	82	478 mmol $\sigma -^{1} h^{-1}$	[8]
00-100-0	0.1101 KOII	0.0	02	(100  mA)	[0]
$Co_1$ -NG(O)	0.1M KOH	0.2	~82	$418 \pm 19 \text{ mmol } g_{\text{ext}}^{-1}$	[9]
		0.2	02	$h^{-1}$	[2]
				(50  mA)	
				()	
Mo <sub>1</sub> /OSG-H	0.1M KOH	0.3-0.75	95±1		[10]
Co-N/HPC	0.1M KOH	0.5	95	1.7 mol g <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup>	[11]
				(0.5 V vs RHE)	_

 Table S4 Comparison of 2e ORR performance for Carbon-based electrocatalysts.

(PAQS)/CNT	0.1M KOH	0.5	91	86.5 mmol g <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup> (0.5 V vs RHE)	[12]
B-C	0.1M KOH	0.6	90		[13]
NBO-GQDs	0.1M KOH	0.7	90	709 mmol g <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup> (0.7 V vs RHE)	[14]
P-Ni/MC	0.1M KOH	0.15	98	4.4 mol g <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup> (0.15 V vs RHE)	[15]

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