## **Electronic Supporting Information**

## Constructing layer-by-layer self-assembly MoS<sub>2</sub>/C nanomaterials by one-step hydrothermal method for catalytic hydrogenation of phenanthrene

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## **Experimental Section**

**Chemicals.** Ammonium paramolybdate  $(NH_4)_6Mo_7O_{24}.4H_2O)$ , thiourea  $(CH_4N_2S)$ , and sucrose  $(C_{12}H_{22}O_{11})$  were purchased from Tianjin Kermel Chemical Reagent Company. Tridecane and phenanthrene were purchased from Aladdin Industrial Corporation. Chemicals were utilized without further purification.

Synthesis of MoS<sub>2</sub> and MoS<sub>2</sub>/C samples. 0.45 mmol of  $(NH_4)_6Mo_7O_{24}.4H_2O$ , 32.84 mmol of CH<sub>4</sub>N<sub>2</sub>S, and 1.30 mmol of sucrose  $(C_{12}H_{22}O_{11})$  were dissolved in 60 ml of deionized water. The resulting solution was transferred into a 100 ml Teflonlined autoclave, and kept at 210 °C for 24 h. The products were filtered, washed with distilled water several times, and dried in a vacuum oven at 60 °C over night. The obtained sample with C/Mo molar ratio of 5 in the precursor was denoted as MoS<sub>2</sub>/C, that is, MoS<sub>2</sub>/C-5. MoS<sub>2</sub>/C catalysts with C/Mo molar ratios from 0.7 to 27 in the precursor were also synthesized and denoted as MoS<sub>2</sub>/C-X. For comparison, the MoS<sub>2</sub> sample was prepared by a similar procedure in the absence of sucrose. The detailed synthesized conditions are summarized and listed in Table S1.

Samplas	Мо	S	С	
Samples	sources/mmol	sources/mmol	sources/mmol	
$MoS_2$	0.45	32.84	\	
$MoS_2/C(MoS_2/C-5)$	0.45	32.84	1.30	
$MoS_2/C-0.7$	0.45	32.84	0.182	
$MoS_2/C-1$	0.45	32.84	0.260	
$MoS_2/C-7$	0.45	32.84	1.82	
MoS <sub>2</sub> /C-10	0.45	32.84	2.60	
MoS <sub>2</sub> /C-15	0.45	32.84	3.90	
MoS <sub>2</sub> /C-27	0.45	32.84	7.02	

**Table S1**. The preparation conditions for  $MoS_2$  and  $MoS_2/C$  samples in this work.

Characterizations of  $MoS_2$  and  $MoS_2/C$  samples. The X-ray diffraction (XRD) patterns were acquired on a PANalytical X'Pert Pro X-ray diffractometer equipped with nickel-filtered Cu Ka radiation ( $\lambda$ =0.15418 nm) with 40 kV and 40 mA. Raman spectra were measured on a Renishaw inVia Raman spectrometer with 532 nm excitation line. The amounts of C, H, N, S in samples were analyzed using a Flash 2000 organic elemental analyzer from Thermo Scientific, and the amounts of Mo in samples were analyzed on a Optima 7300DV ICP-OES. The scanning electron

microscopy (SEM) and high-resolution transmission electron microscopy (HRTEM) images of samples were respectively taken from a JSM 7800F microscope and a JEM 2100 microscope. The scanning transmission electron microscopy (STEM) images and line-scan elemental distributions were obtained on a JEM F200 microscope with X-ray energy-dispersive spectroscopy. X-ray photoelectron spectroscopy (XPS) measurements were carried out on a Thermo Fisher Scientific ESCALAB 250Xi spectrometer with monochromatized Al K $\alpha$  excitation, and the C 1s peak (284.8 eV) was used as reference.

Samples	C <sup>a</sup> wt.%	H <sup>a</sup> wt.%	N <sup>a</sup> wt.%	S <sup>a</sup> wt.%	Mo <sup>b</sup> wt.%	C/Mo mol/mol	S/Mo mol/mol
$MoS_2$	0	0.93	2.14	35.49	51.62	0	2.06
MoS <sub>2</sub> /C	7.71	1.43	3.01	29.04	41.41	1.49	2.10

**Table S2**. The elemental analysis for  $MoS_2$  and  $MoS_2/C$  samples.

a-analyzed by CHNS; b-analyzed by ICP-OES.

**Catalytic activities of MoS<sub>2</sub> and MoS<sub>2</sub>/C samples.** The catalytic activities of catalysts were evaluated by hydrogenation of phenanthrene (PH) in slurry bed reactor as our previous work. Catalytic activity for PH hydrogenation was evaluated in a 100 ml Parr high pressure micro-reactor. 30.0 g of tridecane solvent, 3.0 g of PH, and a certain amount of catalyst with 0.075g of catalytic active MoS<sub>2</sub> were put into the micro-reactor. The dosage of catalyst was calculated according to the results of elemental analysis, in which molybdenum was 45 mg. Hydrogen was purged into the micro-reactor three times to exchange the air in the reaction system, and subsequently, the micro-reactor was charged with H<sub>2</sub> to an initial pressure of 8.0 MPa at room temperature. Hydrogenation reaction was performed at 350 °C with a stirring rate of 300 r.p.m.. After the reaction was maintained for 4 h, the micro-reactor was naturally cooled down. The liquid products were obtained by filtering the catalyst with filter membrane. The liquid products were identified with Agilent 7890B-5977A GC-MS, and quantitatively analyzed with a gas chromatograph (Agilent 7890A with a FID detector and a HP-5 column).

With polycondensed ring aromatic hydrocarbons, the first-ring hydrogenation into preliminary hydrogenation product has been observed to be most favored kinetically.

The rates of hydrogenation of subsequent rings tend to become lower and more difficult, and hydrogenation of the last ring into deep hydrogenation product proceeds with considerable difficulty compared with the initial hydrogenation steps.<sup>1</sup> The products of PH hydrogenation are mainly PH derivatives including PH2, PH4, PH8, and PH14. The reaction pathway of PH hydrogenation was given in Scheme S1.



Scheme S1. Reaction pathways for phenanthrene hydrogenation using MoS<sub>2</sub> catalysts.

The PH conversion (Conv.), PH hydrogenation percent (HP), and product selectivity (*Sel*) were calculated as follows.

The hydrogenation product selectivity (Sel.) to PHx is calculated with Eq. (1).

 $AT(PHx) \times 100\%$  $Sel._{(PHx)}(mol\%) = \frac{1}{AT(PH2) + AT(PH4) + AT(PH8) + AT(PH14)}$ (1)AT(PHx) means the molar of PHx.

The conversion (Conv.) is calculated with Eq. (2).  $Conv.(\%) = \frac{[PH]_0 - [PH]}{[PH]_0} \times 100\%$ (2)  $[PH]_0$  means the initial concentration of PH, and [PH] represents the final concentration of PH after catalytic hydrogenation reaction.

The HP is calculated with Eq. (3).  $HP(\%) = \frac{\left(Sel_{(PH2)} \times 2 + Sel_{(PH4)} \times 4 + Sel_{(PH8)} \times 8 + Sel_{(PH14)} \times 14\right)}{14} \times Conv.$ 

(3)  $Sel._{(PHx)}$  is the selectivity to the PH hydrogenation products, and *Conv.* is the PH hydrogenation conversion. Hence, HP represents of hydrogenation degree of PH, which is the percent between the real reaction and the theoretic reaction " $PH+7H_2$  to PH14".



Fig. S1 The C 1s XPS spectrum of MoS<sub>2</sub>/C sample.

Three peaks can be observed from the C1s XPS spectrum of  $MoS_2/C$  sample in Fig. S1. The binding energy of 284.7 eV can be ascribed to the C-C/C=C bonds in sp2hybridized carbon.<sup>2-5</sup> The binding energy of 285.8 eV is the C1s peak of typical C-S bond,<sup>4</sup> and the peak at 288.5 eV may be assigned to the C1s peak of C=O bonds.<sup>2</sup> The result of C1s XPS spectrum indicates the successful introduction of C with oxygen functional groups and the interaction between C and MoS<sub>2</sub> in MoS<sub>2</sub>/C sample.



Fig. S2 XPS spectra of (a) Mo 3d, and (b) S 2p for MoS<sub>2</sub> and MoS<sub>2</sub>/C samples.

The XPS spectra of Mo 3d and S 2p are given in Fig. S2. As shown in Fig. S2a, the peaks at about 229.5 eV and 232.6 eV can be respectively ascribed to Mo  $3d_{5/2}$  and Mo  $3d_{3/2}$  of Mo<sup>4+</sup> in S-Mo-S bonds of MoS<sub>2</sub> sample. For MoS<sub>2</sub>/C sample, the peaks at about 229.1 eV (Mo  $3d_{5/2}$ ) and 232.2 eV (Mo  $3d_{3/2}$ ) can be assigned to Mo<sup>4+</sup> in S-Mo-S bonds in MoS<sub>2</sub>/C sample. The binding energies of Mo 3d for MoS<sub>2</sub>/C sample shift negatively for 0.4 eV compared with those of MoS<sub>2</sub> sample. Besides, Mo<sup>5+</sup> and Mo<sup>6+</sup> can be determined from the Mo 3d XPS spectrum of MoS<sub>2</sub>/C sample. The high-valent Mo may be generated by the intercalated species such as H<sub>2</sub>O or C with oxygen functional groups in MoS<sub>2</sub> and MoS<sub>2</sub>/C samples.

XPS spectra of S 2p of MoS<sub>2</sub> and MoS<sub>2</sub>/C samples in Fig S2b exhibit two binding energies of 162.4 eV and 163.6 eV, which are correspondingly ascribed to S  $2p_{3/2}$  and S  $2p_{1/2}$  of S<sup>2-</sup> for MoS<sub>2</sub> sample. The S  $2p_{3/2}$  and S  $2p_{1/2}$  of S<sup>2-</sup> can be observed at 161.9 eV and 163.1 eV for MoS<sub>2</sub>/C sample in Fig. S2b. The binding energies of S 2p for MoS<sub>2</sub>/C sample shift negatively for 0.5 eV in comparison with those of MoS<sub>2</sub> sample. In addition to S<sup>2-</sup>, the binding energies at 163.4 eV and 164.6 eV can be ascribed to the S  $2p_{3/2}$  and S  $2p_{1/2}$  of C-S bonds, which proves the self-assembly interaction between C and MoS<sub>2</sub>. We measured the lateral sizes of 177  $MoS_2$  slabs in 67  $MoS_2/C$  nanosheets for scientific analysis of the layer structure.

The average lateral size  $\bar{L}$  of MoS<sub>2</sub> slab was calculated as follows:

$$\mathcal{L} = \frac{\sum_{i=1...n} l_i}{n} \tag{4}$$

where  $l_i$  is the lateral size of MoS<sub>2</sub> slab i, and n is the total number of slabs.

The average stacking layer number  $\overline{N}$  of MoS<sub>2</sub> slab was calculated as follows:

$$\overline{N} = \frac{\sum_{i=1\dots t}^{n_i \cdot N_i} n_i}{\sum_{i=1\dots t}^{n_i} n_i}$$
(5)

where  $n_i$  is the number of stacking layers in  $N_i$  layers.

MoS<sub>2</sub> dispersion ( $^{D}$ ) was statistically evaluated by dividing the total number of Mo atoms at the edge surface ( $^{M_{e}}$ ) and corner sites ( $^{M_{c}}$ ) by the total number of Mo atoms ( $^{M_{T}}$ ), <sup>6-8</sup> using the lateral sizes measured in the TEM images:

$$D = \frac{Mo_e + Mo_c}{Mo_T} = \frac{\sum_{i=1...t} 6n_i - 6}{\sum_{i=1...t} 3n_i^2 - 3n_i + 1}$$
(6)

where  $n_i$  is the number of Mo atoms along one side of the MoS<sub>2</sub> slab, as determined by its lateral size  $(L = 3.2(2n_i - 1)[\text{Å}])$ , and t is the total number of slabs in the TEM images.

According to Eq. (6), the  $MoS_2$  dispersion ( $^D$ ) is correlated with the average lateral size, and is independent of the average stacking layer number. Rim sites are the active sites of catalytic hydrogenation.<sup>9</sup> The Rim-dispersion (R) for  $MoS_2$  sheets can be deduced according to equation 7. So the R is dependent of both the average lateral size and average stacking layer number.





Fig. S3 (a) The lateral size and (b) stacking number distributions of  $MoS_2$  in  $MoS_2/C$  nanosheets.



Fig. S4 HRTEM images used to measure the layer structures of MoS<sub>2</sub>/C sample.

Fig. S4 shows partial TEM images used to measure the layer structures of  $MoS_2/C$  sample. In order to collect statistics data of average stacking layers and lateral sizes, we respectively counted 177  $MoS_2$  slabs in 67 batches of  $MoS_2/C$  nanosheets from

more than 10 images obtained by the HRTEM characterization.



Fig S5 The STEM/EDS mapping of MoS<sub>2</sub>/C catalyst. (a) Bright field STEM image and (b) Dark field STEM image of MoS<sub>2</sub>/C catalyst, (c) S element mapping, (d) Mo element mapping, (e) C element mapping and (f) The mapping overlay of Mo and C elements.

Fig. S5 shows the element mapping of  $MoS_2/C$  catalyst. Mo, S and C elements can be detected, and display the analogous distributions in  $MoS_2/C$  catalyst. The mapping overlay in Fig.S5f comfirms the uniform distribution of  $MoS_2$  and C in layer-by-layer self-assembly  $MoS_2/C$  catalyst.



Fig. S6 (a) Conversion (Conv) and hydrogenation percent (HP) of phenanthrene; (b) Selectivity to hydrogenated products (PH2, PH4, PH8 and PH14) of catalytic phenanthrene (PH) hydrogenation with MoS<sub>2</sub> catalyst and MoS<sub>2</sub>/C catalysts synthesized with different C/Mo molar ratios in the synthesis medium.

For the catalyst hydrogenation of PH over  $MoS_2$  catalyst, low active catalyst exhibits higher selectivity to preliminary hydrogenation product PH2, lower selectivity to deep hydrogenation product PH8, lower PH conversion and lower hydrogenation percentage. On the contrary, high active catalyst demonstrates lower selectivity to preliminary hydrogenation product PH2, higher selectivity to deep hydrogenation product PH8, higher PH conversion and higher hydrogenation percentage. In this work, the hydrogenation percentage represents the hydrogenation saturation degree of PH, and it is positively correlated with PH conversion and selectivity to deep hydrogenation product.

The catalytic hydrogenation activities of all the  $MoS_2/C$  catalysts were evaluated and given in Figure S6. As the C/Mo molar ratio increased in the raw materials from 0.7 to 5, the obtained  $MoS_2/C$  catalysts demonstrated enhanced catalytic activities of phenanthrene hydrogenation in comparison with  $MoS_2$  catalyst. When the C/Mo molar ratio is further increased in the raw materials from 5 to 27, the obtained  $MoS_2/C$  catalysts displayed decreased catalytic activities of phenanthrene hydrogenation. Figure S6 indicates that MoS<sub>2</sub>/C catalyst synthesized with C/Mo molar ratio of 5 exhibits the highest catalytic activity of phenanthrene hydrogenation.



Fig. S7 The surface areas and hydrogenation percentages of  $MoS_2$  and  $MoS_2/C$  catalysts.

The surface areas of  $MoS_2$  and  $MoS_2/C-5$  catalysts are respectively 4.7 m<sup>2</sup>/g and 3.9 m<sup>2</sup>/g, which are very close and smaller than 5.0 m<sup>2</sup>/g. Although MoS<sub>2</sub> catalyst has larger particle size than that of  $MoS_2/C$  catalyst, the  $MoS_2$  nanosheets in  $MoS_2$  catalyst assembled loosely. Hence the surface area of  $MoS_2$  catalyst is slightly larger than that of  $MoS_2/C$  catalyst. The surface area of  $MoS_2/C-27$  synthesized with high C/Mo molar ratio in the precursor is 17.5 m<sup>2</sup>/g, which is much higher than those of  $MoS_2$  and  $MoS_2/C-5$  catalysts. However, according to Fig. S7,  $MoS_2/C-27$  with larger surface area exhibits much lower catalytic activity of PH hydrogenation than that of  $MoS_2/C$ . Therefore, it can be speculated that catalytic activity for  $MoS_2$  catalyst has no direct correlation with its surface area. The results are consistent with previous reported works.<sup>9-14</sup>

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