Supplementary information for

MoO_x decorated-Ru/TiO₂ with monomeric structure boosts the selective one-pot conversion of levulinic acid to 1,4pentanediol

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- 6) Pyridine-adsorption profiles of (a) Ru–(5 wt%)/TiO₂, (b) Ru–(0.47) MoO_x/TiO₂ (Mo = 0.47 wt%; Mo/Ru = 1:10.5), and (c) Ru–(0.91) MoO_x/TiO₂ (Mo = 0.90 wt%; Mo/Ru = 1:5.3) catalysts (Fig. S5).
- 7) XRD patterns of (a) fresh and (b) recovered Ru-(0.47)MoOx/TiO₂ after the second reaction run (Fig. S6).



Fig. S1 XRD patterns of $Ru-MoO_x/TiO_2$ (Mo = 0.47 wt%; Mo/Ru = 1:10.5) after reduction with H₂ at (a) 400 °C and (b) 500 °C and (c) 600 °C for 1.5 h.



Fig. S2 (a) Kinetics profiles and (b) Arrhenius plot of LA hydroconversion to 1,4-PeD over Ru- $(0.47)MoO_x/TiO_2$ catalyst.



Fig. S3 (a) Kinetics profiles and (b) Arrhenius plot of LA hydroconversion to 1,4-PeD over Ru (5 wt%)/TiO₂ catalyst.



Fig. S4 NH₃-TPD profiles of Ru-(y)MoO_x/TiO₂ and deconvoluted NH3-TPD spectra of Ru-(0.24) MoO_x/TiO₂ (Mo = 0.24 wt%; Mo/Ru = 1:19.5), Ru-(0.47) MoO_x/TiO₂ (Mo = 0.47 wt%; Mo/Ru = 1:10.5), and Ru-(0.91) MoO_x/TiO₂ (Mo = 0.90 wt%; Mo/Ru = 1:5.3) catalysts.



Fig. S5 Pyridine-adsorption profiles of (a) $Ru-(5 \text{ wt\%})/TiO_2$, (b) $Ru-(0.47) \text{ MoO}_x/TiO_2$ (Mo = 0.47 wt%; Mo/Ru = 1:10.5), and (c) $Ru-(0.91) \text{ MoO}_x/TiO_2$ (Mo = 0.90 wt%; Mo/Ru = 1:5.3) catalysts.

Entry	Catalyst	Total surface acidity	
		NH ₃ -TPD ^a	Pyridine-adsorption ^b
		(µmol NH₃ g⁻¹)	(µmol Pyridine g⁻¹)
1	Ru (5 wt%)/TiO ₂	Nd	0.49
2	Ru-(0.47)MoO _x /TiO ₂	201	2.53
3	Ru-(0.91)MoO _x /TiO ₂	321	24.21

Table S1. Total	acidity of typical	Ru and Ru-MoOx/	TiO ₂ catalysts
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^{*a*} The acidity was measured by using NH₃-TPD. ^{*b*} The acidity of the catalysts was tested by the gravimetric method using pyridine gas as a basic adsorbate.



Fig. S6 XRD patterns of (a) fresh and (b) recovered Ru-(0.47)MoOx/TiO₂ after the second reaction run.