

Supporting information

Oxidative coupling of methane under microwave: Core-shell catalysts for selective C₂ production and homogeneous temperature control

Reina Kaneda,^a José Palomo,^a Lingjun Hu^{a,b} and Atsushi Urakawa,^{*a}

^a Catalysis Engineering, Department of Chemical Engineering, Delft University of Technology, Van der Maasweg 9, 2629 HZ Delft, The Netherlands

^b Institute of Chemical Research of Catalonia (ICIQ), The Barcelona Institute of Science and Technology, Av. Països Catalans 16, 43007 Tarragona, Spain

*corresponding author: Atsushi Urakawa (A.Urakawa@tudelft.nl)

Table S1. Microwave power supplied to reach the set-point reaction temperature.

Temperature (°C)	500	600	700	800	900
	Power (W)				
MgO@SiC	65	60	51	49	50
MgO-SiC	43	34	38	42	73
MgO@FeO ₄	16	17	20	30	31
MgO-Fe ₃ O ₄	11	12	17	23	31

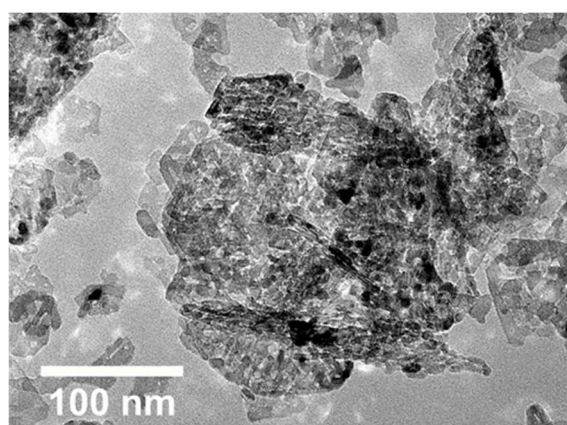


Figure S1. TEM image of Fe₃O₄@MgO catalyst.

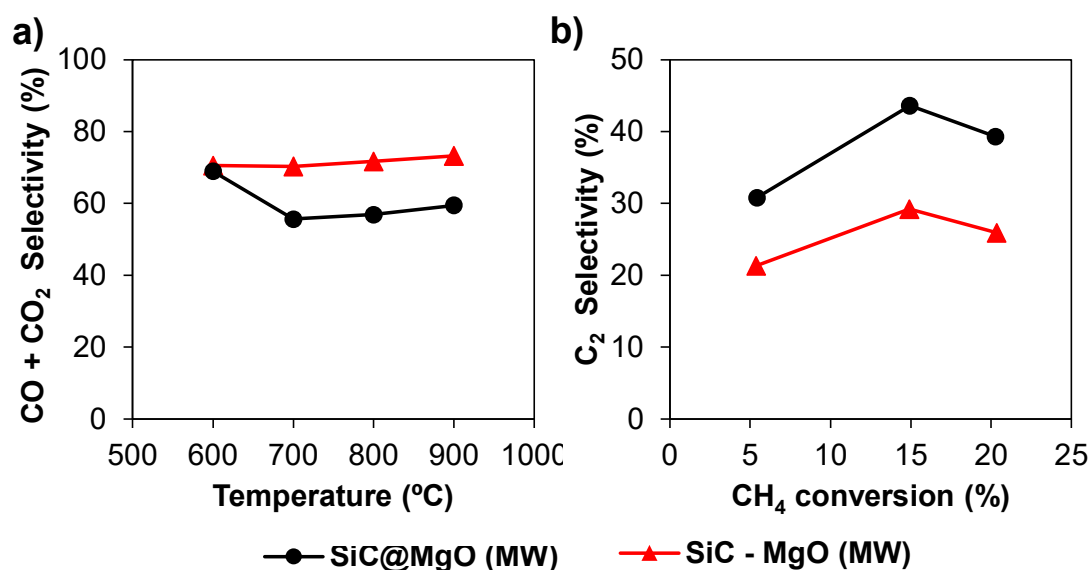


Figure S2. a) Total selectivity towards partial/deep oxidation products (CO+CO₂) as a function of the temperature; b) C₂ selectivity at different iso-conversion values for SiC@MgO and SiC-MgO, under microwave radiation conditions.

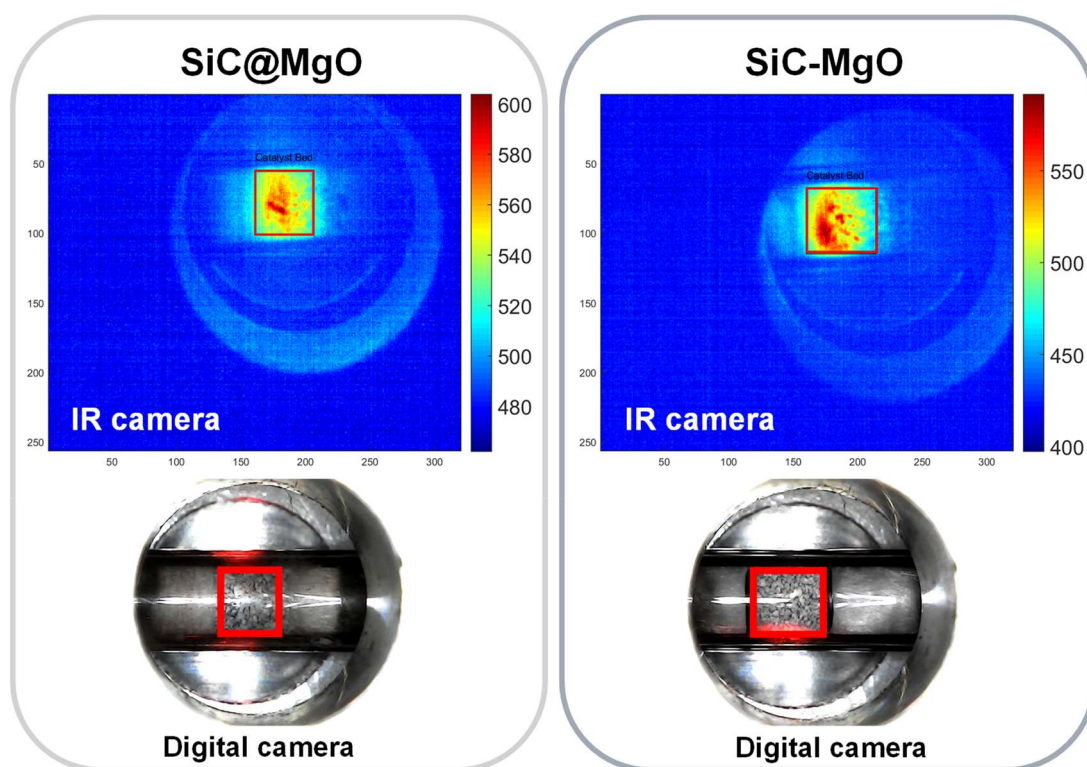


Figure S3. Catalyst bed digital microscopy and infrared thermography images of SiC@MgO and SiC-MgO during OCM reaction, under microwave radiation, at 500 °C. Red square shows catalyst bed in the reactor tube. The red light reflected on the reactor wall is the focusing light from the infrared temperature sensor. The gas flow is from the right to the left of the reactor tube.

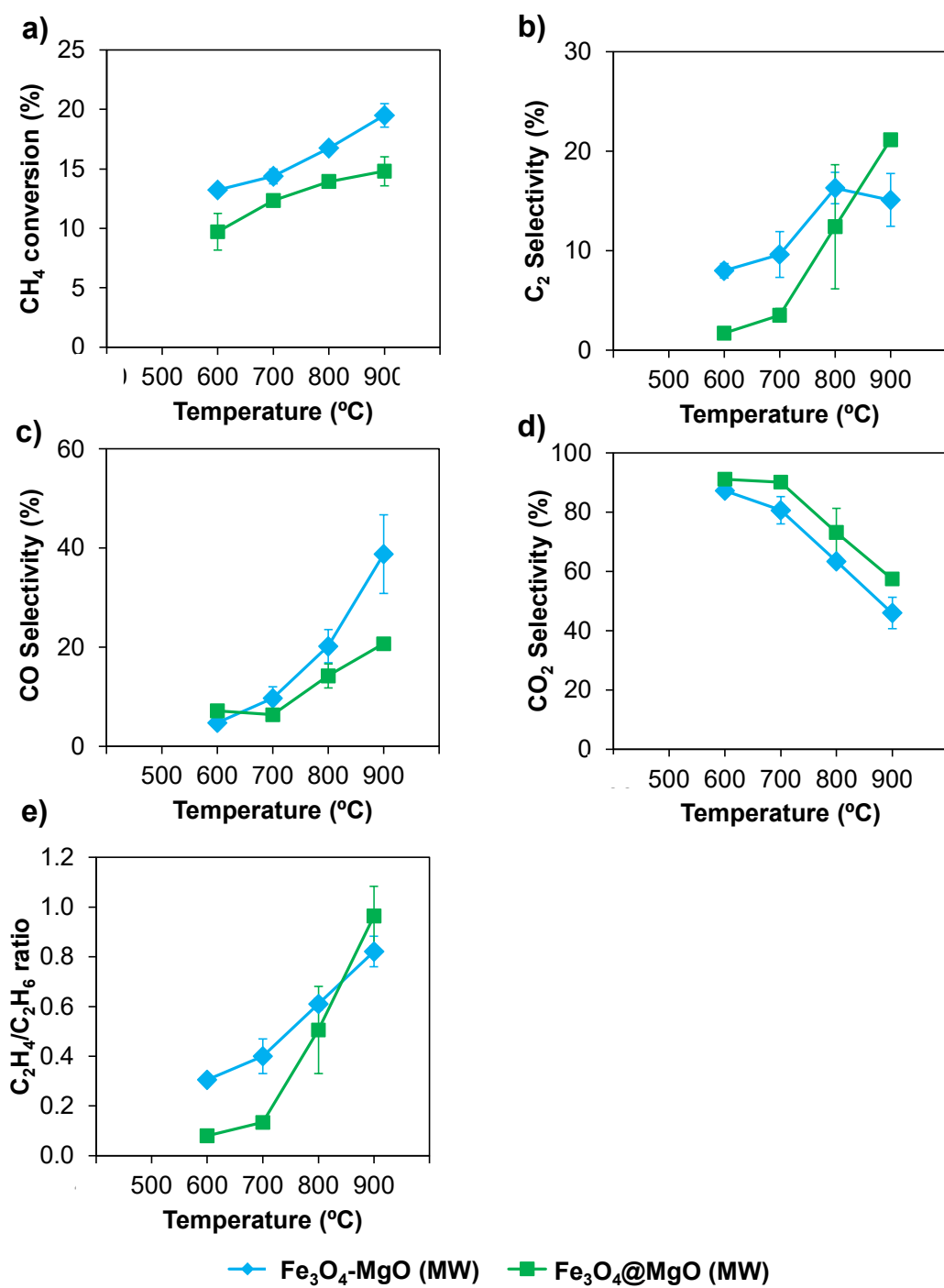


Figure S4. a) CH₄ conversion, b) C₂ selectivity, c) CO selectivity, d) CO₂ selectivity and e) C₂H₄/C₂H₆ ratio for Fe₃O₄@MgO and Fe₃O₄-MgO catalysts under microwave radiation (MW) conditions.

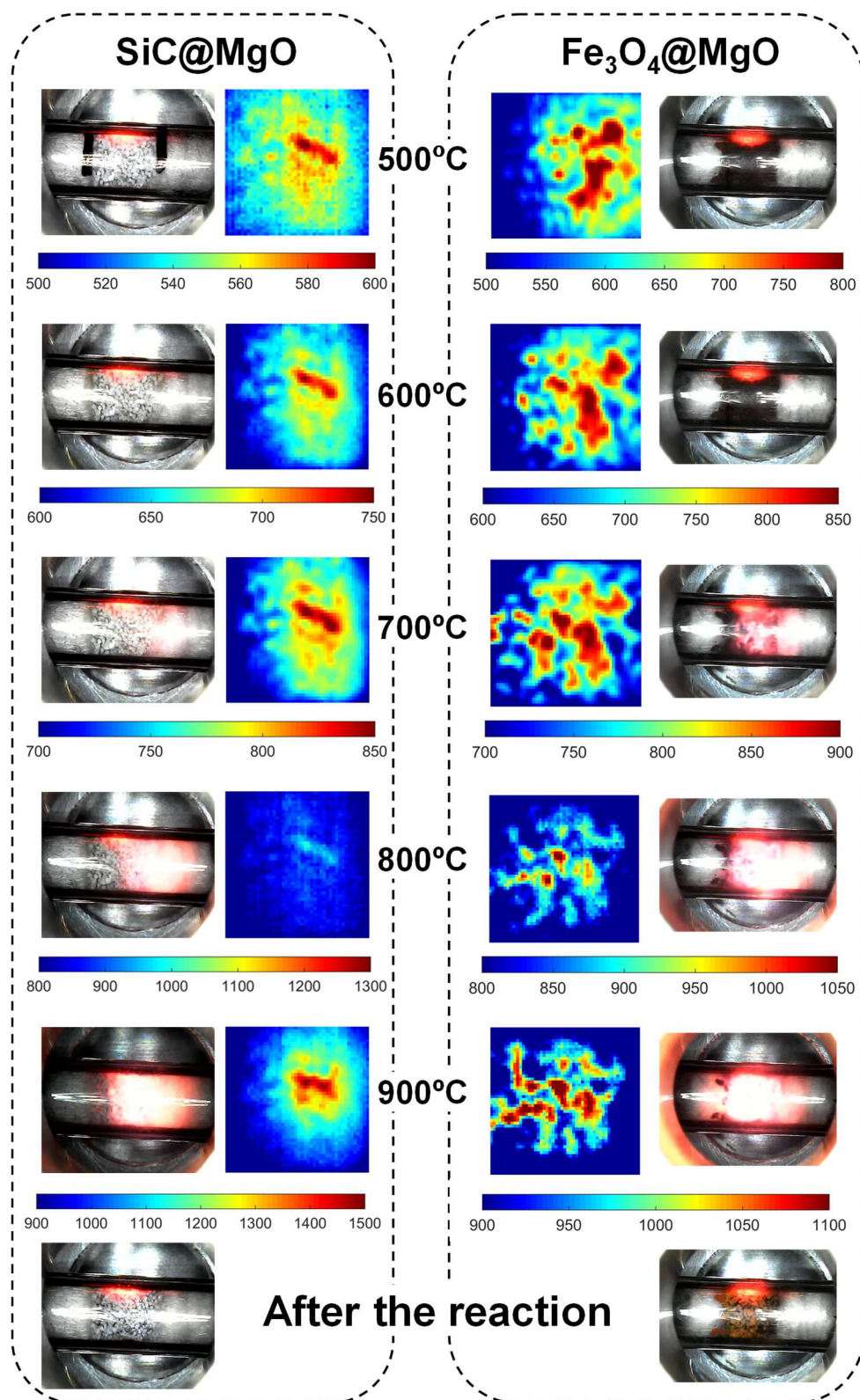


Figure S5. Digital microscopy images and temperature distributions during OCM, under MW, at different reaction temperatures for SiC@MgO and Fe₃O₄@MgO catalytic beds. The red light reflected on the reactor wall is the focusing light from the infrared temperature sensor. The gas flow is from the left to the right of the reactor tube.

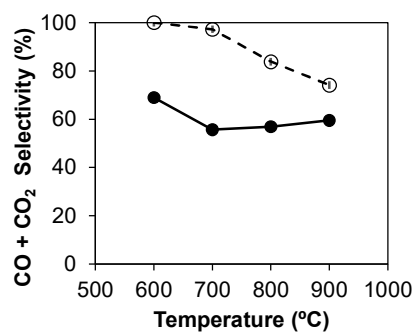


Figure S6. a) Total selectivity towards partial/deep oxidation products (CO+CO₂) as a function of the temperature for SiC@MgO under MW and RH conditions.

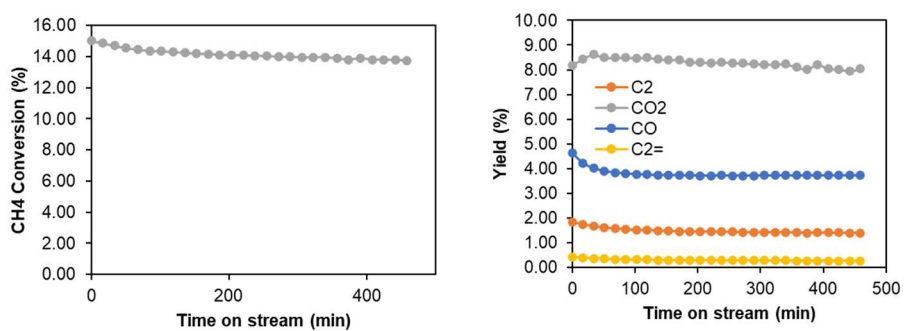


Figure S7. Reactants conversion and products selectivity as a function of time on stream at 750 °C (RH), total flow = 150 mL min⁻¹ (40% CH₄, 10% O₂), W_{cat}= 100 mg, W_{SiC} = 350 mg.

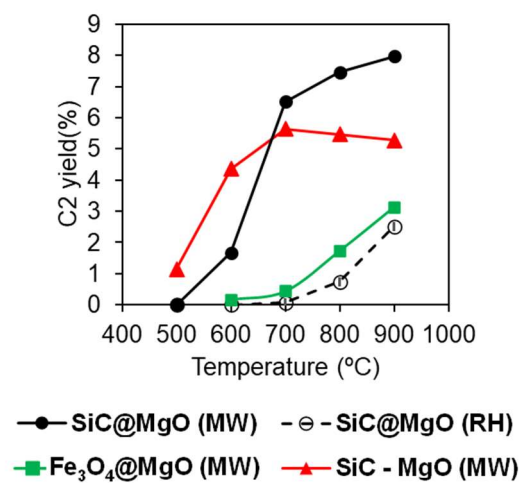


Figure S8. C₂ yield for Fe₃O₄@MgO, SiC@MgO and SiC-MgO catalysts under microwave radiation (MW) conditions, and SiC@MgO under resistive heating (RH) conditions.