## **Electronic supporting Information**

## Spectroscopic Investigation on the Structural Transformation of Ru in

## the Ru/CeO<sub>2</sub> Catalyst

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**Fig. S1** *In situ* DRIFTS results of Ru/CeO<sub>2</sub> catalyst after pretreatment in O<sub>2</sub>: (a) CO adsorption results during heating process (-20 °C to 250 °C); (b) CO adsorption results during cooling process (250 °C to -20 °C)

The CO adsorption on Ru species was very complex, which included monocarbonyl, dicarbonyl, and tricarbonyl species adsorbed on Ru sites with different oxidation states. The positions of the bands were likely to have been red-shifted as the temperature increased because of the decrease in surface coverage that led to a weaker dipole-dipole coupling.



**Fig. S2** *In situ* DRIFTS results of Ru/CeO<sub>2</sub> catalyst after pretreatment in H<sub>2</sub>-N<sub>2</sub>: (a) CO adsorption results during heating process (-20 °C to 250 °C); (b) CO adsorption results during cooling process (250 °C to -20 °C)



**Fig. S3** *In situ* DRIFTS results of Ru/CeO<sub>2</sub> catalyst after pretreatment in H<sub>2</sub>-O<sub>2</sub>: (a) CO adsorption results during heating process (-20 °C to 250 °C); (b) CO adsorption results during cooling process (250 °C to -20 °C)



**Fig. S4** *In situ* DRIFTS results of Ru/CeO<sub>2</sub> catalyst after pretreatment in N<sub>2</sub>: (a) CO adsorption results during heating process (-20 °C to 250 °C); (b) CO adsorption results during cooling process (250 °C to -20 °C)



Fig. S5 The H<sub>2</sub>-TPR of the Ru/CeO<sub>2</sub> catalyst after pretreatment in O<sub>2</sub>-N<sub>2</sub> atmospheres

It showed an overall broad peak around 110 °C, which was considered as the reduction of  $RuO_x$  clusters. This phenomenon indicated that although N<sub>2</sub> was an inert gas, it could still cause state changes of Ru species at a high temperature. Besides, we also found that after treated with N<sub>2</sub> atmosphere at 300 °C, the well-dispersed Ru single atoms gradually agglomerated into Ru nanoclusters and the state of Ru species changed significantly.



Fig. S6 Three rounds CO oxidation activity results of  $Ru/CeO_2$  catalyst after pretreatment in  $H_2$ ,  $N_2$  and 20%  $O_2/N_2$ : (a) 5%  $H_2/Ar$ ; (b)  $N_2$ ; (c) 20%  $O_2/N_2$ 



**Fig S7.** Three rounds CO oxidation activity results of  $Ru/CeO_2$  catalyst after pretreatment in 5%  $H_2/Ar$ ,  $N_2$  and 20%  $O_2/N_2$ : (a) the result of the first-round of testing; (b) the result of the second-round of testing; (c) the result of the third-round of testing



**Fig. S8** In situ DRIFTS results of Ru/CeO<sub>2</sub> catalyst in CO oxidation reaction gas after pretreatment in 20%  $O_2/N_2$  during cooling process (250 °C to 20 °C)



**Fig. S9** *In situ* DRIFTS results of Ru/CeO<sub>2</sub> catalyst in CO oxidation reaction gas after pretreatment in H<sub>2</sub>: (a) the test results during heating process (20 °C to 250 °C); (b) the test results during cooling process (250 °C to 20 °C)



**Fig. S10** *In situ* DRIFTS study of CO adsorption on the Ru/CeO<sub>2</sub> catalysts after pretreatment ((a, b)  $H_2$ , (c, d)  $N_2$ , (e, f) air, 300 °C) at 20 °C: (a, c, e)  $N_2$  purging, (b, d, f) 1% O<sub>2</sub>/Ar purging

The *in situ* DRIFTS in a "CO-N<sub>2</sub>–CO-O<sub>2</sub>" mode was performed to explore the active Ru site for CO oxidation reaction. However, the CO adsorption on Ru site showed no obvious difference at 20 °C. The reason for the result might attribute to the low activity of the Ru/CeO<sub>2</sub> for CO oxidation under this condition.



**Fig. S11.** In situ DRIFTS study of CO adsorption on the Ru/CeO<sub>2</sub> catalysts after pretreatment (O<sub>2</sub>, 300 °C) at 100 °C: (a) N<sub>2</sub> purging, (b) O<sub>2</sub> purging



Fig. S12. In situ DRIFTS study of CO adsorption on the Ru/CeO<sub>2</sub> catalysts after pretreatment (N<sub>2</sub>, 300 °C) at 100 °C: (a) N<sub>2</sub> purging, (b) O<sub>2</sub> purging