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# **Supplementary Information**

Carbonylation of dimethoxymethane: A study on reactivity of different solid acid catalysts

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		GC Method:		
Agilent 8890				
 GC				
GC Summary				
Run Time	7.6 min			
Post Run Time	0 min			
Oven				
Equilibration Time	0 min			
Max Temperature	240 °C			
(Initial)	40 °C			
Hold Time	2 min			
Post Run	110 °C			
#1 Rate	25 °C/min			
#1 Value	180 °C			
#1 Hold Time	0 min			
ALS				
Front Injector				
Syringe Size	10 µL			
Injection Volume	1 μL			
Solvent A Washes (PreInj)	5			
Solvent A Washes (PostInj)	5			
Solvent A Volume	8 μL			
Sample Washes	1			
Sample Wash Volume	8 μL			

Sample Pumps	3
Solvent Wash Draw Speed	150 μL/min
Solvent Wash Dispense Speed	6000 μL/min
Sample Wash Draw Speed	150 μL/min
Sample Wash Dispense Speed	6000 μL/min
Injection Dispense Speed	6000 μL/min
Viscosity Delay	0 sec
L1 Airgap (	).2 μL

## Front SS Inlet He

Mode	Split
Heater	On 180 °C
Pressure	On 0
Total Flow	On 133.4 mL/min
Septum Purge Flow	On 3 mL/min
Pre-Run Flow Test	Off
Gas Saver	On 20 After 2 min mL/min
Split Ratio	50 :1
Split Flow	127.84 mL/min
Liner	Agilent 5190-3165: 870 μL (Split, taper, wool, low pressure drop)

## PolyArc

Temperature	
Setpoint	On
(Initial)	450 °C

## Column #1

Column Information	Agilent 123-7033UI DB-WAX Ultra I
Temperature Range	20 °C—240 °C (240 °C)
Dimensions	30 m x 320 μm x 0.5 μm

In	Front SS Inlet He
Out	Aux EPC 1
(Initial)	40 °C
Pressure	0
Flow	2.5568 mL/min
Average Velocity	33.826 cm/sec
Holdup Time	1.4781 min
Control Mode	Constant Flow
(Initial)	2.5568 mL/min
Post Run	1 mL/min

### Column #2

Column Information	Agilent FS, Deactivate
Temperature Range	20 °C—240 °C (240 °C)
Dimensions	2.5 m x 250 μm x 0 μm
Out	Front Detector FID
(Initial)	40 °C
Pressure	0
Flow	4 mL/min
Average Velocity	122.56 cm/sec
Holdup Time	0.033996 min
Control Mode	Constant Flow
Setpoint	On
(Initial)	4 mL/min
Post Run	9.5407 mL/min

# Front Detector FID

Makeup	Не
Heater	On 250 °C
H2 Flow	On 1.5 mL/min
Air Flow	On 350 mL/min

Makeup Flow	On 25 mL/min
Carrier Gas Flow Correction	Constant Makeup and Fuel FlowFlame
Initial Baseline Minimum	2 pA
Initial Baseline Maximum	20 pA
Initial Baseline Noise	0.3 pA
Final Baseline Minimum	2 pA
Final Baseline Maximum	40 pA
Final Baseline Noise	0.6 pA
Total Peak Area	100 pA*sec
Maximum Peak Height	3 pA
Time Window Start	0 min
Time Window End	0.5333333333 min

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Column(s)

\_\_\_\_\_\_

Column Description : DB-WAX Ultra I

Inventory# : autoID-2

Model# : 123-7033UI

Manufacturer : Agilent

Diameter : 320.0 µm

Length : 30.0 m

Film thickness :  $0.50 \ \mu m$ 

Void time : 1.478 min

Maximum Temperature: 240.0 °C

Comment :

Column Description: FS, Deactivate Inventory# : autoID-3

Model# :

Manufacturer	:	Agilent
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- Diameter : 250.0 µm
- Length : 2.5 m
- Film thickness :  $0.00 \ \mu m$
- Void time : 0.034 min

Maximum Temperature: 240.0 °C

GC-MS:



Figure S1: GC-MS Measurements of the liquid phase after the DMM Carbonylation reaction. 1 g of A36, 60 bar of CO, 110 °C and 43.0293 g of DMM.

Figure S2: Fragmentation pattern for all considered compounds (1-12) measured by GC-MS. Since compounds 1, 3, 4, 9 are all acetals with the same oxymethylene repetition unit  $-CH_2O$ , their fragmentation pattern is quite similar and often the ion peak is not detected due to fragmentation of long-chained compounds (e.g. 9). For each new oligomer with a higher chain length, there is typically a new peak with an increase of 30 g/mol due to the oxymethylene repetition unit.









#### Catalytic results for catalyst screening

Table S1: Table of catalytic results for figures 4 and 6 in the main text (catalyst screening); performed at 90 °C, with 10 g of DMM, 0.5 g of catalyst powder, 55 bar of CO and 6 h of runtime.

Cataluct	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
Catalyst	$g_{cat}^{-1}$	$g_{cat}^{-1}$	$g_{cat}^{-1}$	$g_{cat}^{-1}$	$g_{cat}^{-1}$
B-25	306.87	508.57	229.57	13.47	6.00
H-Y-30	206.22	352.76	98.86	27.47	0.23
F-20	248.98	327.22	84.59	441.51	9.82
M-20	260.38	402.46	190.24	82.71	0.26
Z-30	611.88	756.32	845.52	160.27	1.29
Z-80	2264.59	446.11	217.86	52.74	0.12
Z-280	443.56	218.47	215.87	75.46	0.25
DX2	295.04	574.76	15965.40	198.05	2.27
DX4	524.09	627.79	22791.37	191.51	3.54
DX8	410.40	797.39	27408.61	224.87	6.28
A15	534.83	600.32	24651.50	209.95	6.00
A16	354.91	558.82	21326.16	212.17	5.71
A36	534.90	880.82	40012.18	193.23	14.46
A46	238.54	216.34	706.05	191.40	1.49

Catalyst	S(FA) [%]	S(MeFo) [%]	S(MMA) [%]	S(OME-2) [%]	S(OME-3) [%]	X(DMM) [%]	X(CO) [%]
B-25	28.83	47.78	21.57	1.27	0.56	4.44	0.91
H-Y-30	30.08	51.46	14.42	4.01	0.03	1.22	0.52
F-20	22.39	29.42	7.61	39.70	0.88	4.48	6.54
M-20	27.82	43.00	20.32	8.84	0.03	4.85	0.39
Z-30	25.76	31.84	35.60	6.75	0.05	12.97	10.14
Z-80	75.96	14.96	7.31	1.77	0.00	8.61	27.89
Z-280	46.51	22.91	22.64	7.91	0.03	4.40	31.69
DX2	1.73	3.37	93.72	1.16	0.01	25.38	9.45
DX4	2.17	2.60	94.42	0.79	0.01	34.26	16.21
DX8	1.42	2.76	95.01	0.78	0.02	39.06	21.58
A15	2.06	2.31	94.80	0.81	0.02	27.43	16.34
A16	1.58	2.49	94.96	0.94	0.03	23.36	14.32
A36	1.28	2.12	96.10	0.46	0.03	54.84	26.61
A46	17.62	15.98	52.15	14.14	0.11	5.95	2.00

#### Effect of catalyst amount

Table S2: Table of catalytic results for figures 7 and 8 in the main text (variation of catalyst amount); performed at 110 °C, with 43 g of DMM, 60 bar of CO and 6 h of runtime for 0.5 g A36.

Time	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
[h]	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l⁻¹·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·
	g <sub>cat</sub> -1]	$g_{cat}^{-1}$ ]	g <sub>cat</sub> -1]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]
1	281.22	337.55	2756.55	45.15	0.14

2	222.90	681.68	10370.82	125.03	0.68
3	286.93	892.54	15749.45	187.70	2.08
4	279.78	975.15	20343.01	230.38	5.39
6	322.00	1165.35	27505.04	264.48	3.18

Time	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X (CO)
[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	8.22	9.87	80.59	1.32	0.00	6.71	13.84
2	1.96	5.98	90.96	1.10	0.01	18.71	27.33
3	1.68	5.21	92.00	1.10	0.01	27.98	32.13
4	1.28	4.47	93.17	1.06	0.02	37.74	32.13
6	1.10	3.98	94.00	0.90	0.01	55.66	38.59

Table S3: Table of catalytic results for figures 7 and 8 in the main text (variation of catalyst amount); performed at 110 °C, with 43 g of DMM, 60 bar of CO and 6 h of runtime for 1.0 g A36.

Time	c(FA) [mol·l <sup>-1</sup> ·	c(MeFo) [mol·l <sup>-1</sup> ·	c(MMA) [mol·l <sup>-1</sup> ·	c(OME-2) [mol·l <sup>-1</sup> ·	c(OME-3) [mol·l <sup>-1</sup> ·
[h]	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]
1	81.09	276.99	2922.99	51.67	0.42
2	182.63	459.39	8457.78	114.75	2.05
3	155.50	510.24	11849.68	137.38	4.39
4	181.51	481.62	16043.93	150.16	6.91
6	167.59	609.88	19420.01	105.61	7.62

Time	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X (CO)
[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	2.43	8.31	87.69	1.55	0.01	12.80	18.13
2	1.98	4.98	91.77	1.24	0.02	31.94	34.21
3	1.23	4.03	93.62	1.09	0.03	43.11	39.83
4	1.08	2.86	95.14	0.89	0.04	60.26	39.83
6	0.83	3.00	95.61	0.52	0.04	75.97	47.39

Table S4: Table of catalytic results for figures 7 and 8 in the main text (variation of catalyst amount); performed at 110 °C
with 43 g of DMM, 60 bar of CO and 6 h of runtime for 1.5 g A36.

Time	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
[h]	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·
['']	g <sub>cat</sub> <sup>-1</sup> ]	$g_{cat}^{-1}$ ]	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]	$g_{cat}^{-1}$ ]
1	72.91	167.37	1951.48	35.47	0.61
2	118.21	316.20	6739.98	90.61	2.10
3	141.25	365.57	9828.64	98.81	4.75
4	116.14	361.30	12186.25	88.50	5.69
6	104.50	345.26	12183.45	28.66	2.91

|--|

[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	3.27	7.51	87.60	1.59	0.03	12.19	16.95
2	1.63	4.35	92.75	1.25	0.03	37.45	33.47
3	1.35	3.50	94.15	0.95	0.05	54.47	39.57
4	0.91	2.83	95.52	0.69	0.04	69.97	39.57
6	0.83	2.73	96.20	0.23	0.02	91.72	46.89

#### Effect of temperature

Table S5: Table of catalytic results for figure 9 in the main text (temperature variation); performed with 43 g of DMM, 60 bar of CO and 3 h of runtime.

Temperature	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
[]01]	[mol·l <sup>-1</sup> ·	[mol·l⁻¹·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l⁻¹·
[ 0]	$g_{cat}^{-1}$ ]	g <sub>cat</sub> -1]	$g_{cat}^{-1}$	$g_{cat}^{-1}$ ]	g <sub>cat</sub> -1]
40	113.79	0.00	255.69	30.74	0.08
50	88.43	66.04	685.05	29.37	0.08
60	131.59	67.78	2231.17	23.89	0.16
110	165.90	599.20	16005.82	159.74	7.31
120	218.74	650.22	18467.46	115.57	8.29
130	155.68	794.09	19186.47	61.80	12.62
140	126.04	778.54	15735.91	34.71	1.71

Т [°С]	S(FA) [%]	S(MeFo) [%]	S(MMA) [%]	S(OME-2) [%]	S(OME-3) [%]	X(DMM) [%]	X(CO) [%]
40	28.43	0.00	63.87	7.68	0.02	1.85	5.01
50	10.18	7.60	78.83	3.38	0.01	7.61	5.24
60	5.36	2.76	90.90	0.97	0.01	7.50	11.62
110	0.98	3.54	94.50	0.94	0.04	51.62	36.68
120	1.12	3.34	94.90	0.59	0.04	79.95	37.94
130	0.77	3.93	94.93	0.31	0.06	89.86	36.37
140	0.76	4.67	94.36	0.21	0.01	93.43	29.49

Table S6: Table of catalytic results for figure 9 in the main text (temperature variation); performed with 43 g of DMM, 60 bar of CO and 6 h of runtime.

Tomporaturo	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
[°C]	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·
	g <sub>cat</sub> <sup>-1</sup> ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]
110	43.63	677.39	21165.78	61.82	2.26
120	55.97	639.20	21896.49	32.38	5.15
130	76.89	745.58	20214.32	9.99	3.00
140	30.85	906.54	18470.50	3.97	3.03

Т	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X(CO)
[°C]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
110	0.20	3.09	96.42	0.28	0.01	84.28	47.47

120	0.25	2.82	96.76	0.14	0.02	94.25	48.56
130	0.37	3.54	96.03	0.05	0.01	94.66	42.19
140	0.16	4.67	95.14	0.02	0.02	97.50	33.04

Table S7: Table of catalytic results for figure 9 in the main text (temperature variation); performed with 43 g of DMM, 60 bar of CO and 24 h of runtime.

Temperature [°C]	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
	[mol·l <sup>-1</sup> ·				
	g <sub>cat</sub> -1]	$g_{cat}^{-1}$ ]	g <sub>cat</sub> -1]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]
40	173.62	46.81	1520.79	29.95	0.17
50	165.77	86.96	3789.92	32.99	0.25
60	280.88	104.48	9039.88	59.86	1.07

Т	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X(CO)
[°C]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
40	9.80	2.64	85.86	1.69	0.01	4.22	23.90
50	4.07	2.13	92.98	0.81	0.01	11.89	29.94
60	2.96	1.10	95.30	0.63	0.01	19.82	39.09

#### Effect of pressure

Table S8: Table of catalytic results for figures 10 and 11 in the main text (pressure variation); performed at CO pressure of 20 bar, 110 °C, with 43 g of DMM, 1.0 g of A36 and 6 h of runtime.

Time [h]	c(FA) [mol·l <sup>-1</sup> ·	c(MeFo) [mol·l <sup>-1</sup> ·	c(MMA) [mol·l <sup>-1</sup> ·	c(OME-2) [mol·l <sup>-1.</sup>	c(OME-3) [mol·l <sup>-1</sup> ·
	$g_{cat}^{-1}$	g <sub>cat</sub> -1]	$g_{cat}^{-1}$ ]	g <sub>cat</sub> -1]	$g_{cat}^{-1}$ ]
1	102.47	171.14	524.09	27.08	0.41
2	76.55	452.29	2173.42	81.35	0.49
3	156.70	628.14	3451.51	138.85	1.33
4	142.96	769.23	4618.84	190.54	4.11
6	56.91	825.93	5998.88	225.88	9.34

Time	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X(CO)
[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	12.42	20.74	63.51	3.28	0.05	2.72	16.88
2	2.75	16.25	78.07	2.92	0.02	16.86	29.80
3	3.58	14.35	78.86	3.17	0.03	21.25	38.75
4	2.50	13.43	80.67	3.33	0.07	27.34	45.31
6	0.80	11.61	84.29	3.17	0.13	49.44	53.63

Table S9: Table of catalytic results for figures 10 and 11 in the main text (pressure variation); performed at CO pressure of 40 bar, 110 °C, with 43 g of DMM, 1.0 g of A36 and 6 h of runtime.

Time [h]	c(FA)	c(MeFo)	c(MMA)	c(OME-2)	c(OME-3)
	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l <sup>-1</sup> ·	[mol·l⁻¹·
	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]	g <sub>cat</sub> <sup>-1</sup> ]

1	95.02	186.09	1309.11	40.16	0.25
2	131.68	388.77	4361.35	82.47	0.97
3	135.73	465.54	7426.11	131.75	2.68
4	109.87	512.09	9810.08	147.22	4.97
6	44.67	513.91	10099.69	130.01	2.77

Time	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X(CO)
[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	5.83	11.41	80.28	2.46	0.02	4.00	17.85
2	2.65	7.83	87.84	1.66	0.02	22.73	30.52
3	1.66	5.70	90.99	1.61	0.03	32.39	38.49
4	1.04	4.84	92.69	1.39	0.05	46.27	45.02
6	0.41	4.76	93.59	1.20	0.03	69.43	52.83

Table S10: Table of catalytic results for figures 10 and 11 in the main text (pressure variation); performed at CO pressure of 60 bar, 110 °C, with 43 g of DMM, 1.0 g of A36 and 6 h of runtime.

Time [h]	c(FA) [mol·l <sup>-1</sup> ·	c(MeFo) [mol·l <sup>-1.</sup>	c(MMA) [mol·l <sup>-1</sup> ·	c(OME-2) [mol·l <sup>-1.</sup>	c(OME-3) [mol·l <sup>-1</sup> ·
	g <sub>cat</sub> <sup>-1</sup> ]	g <sub>cat</sub> <sup>-1</sup> ]			
1	81.09	276.99	2922.99	51.67	0.42
2	182.63	459.39	8457.78	114.75	2.05
3	155.50	510.24	11849.68	137.38	4.39
4	181.51	481.62	16043.93	150.16	6.91
6	167.59	609.88	19420.01	105.61	7.62

Time	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X(CO)
[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	2.43	8.31	87.69	1.55	0.01	12.80	11.87
2	1.98	4.98	91.77	1.24	0.02	31.94	24.29
3	1.23	4.03	93.62	1.09	0.03	43.11	32.78
4	1.08	2.86	95.14	0.89	0.04	60.26	38.99
6	0.83	3.00	95.61	0.52	0.04	75.97	46.27

Table S11: Table of catalytic results for figures 10 and 11 in the main text (pressure variation); performed at CO pressure of 80 bar, 110 °C, with 43 g of DMM, 1.0 g of A36 and 6 h of runtime.

Time	c(FA) [mol·l <sup>-1</sup> ·	c(MeFo) [mol·l <sup>-1</sup> ·	c(MMA) [mol·l <sup>-1</sup> ·	c(OME-2) [mol·l <sup>-1.</sup>	c(OME-3) [mol·l <sup>-1</sup> ·
[ [11]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]	$g_{cat}^{-1}$ ]
1	121.81	192.67	2542.05	43.22	0.23
2	94.83	322.36	8455.59	88.67	1.35
3	123.22	325.81	14411.98	117.87	4.61
4	148.85	337.86	18061.72	113.45	6.59
6	39.45	497.81	21612.66	55.92	6.31

Time	S(FA)	S(MeFo)	S(MMA)	S(OME-2)	S(OME-3)	X(DMM)	X(CO)
[h]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
1	4.20	6.64	87.66	1.49	0.01	5.59	8.08
2	1.06	3.60	94.34	0.99	0.02	29.97	18.63
3	0.82	2.17	96.19	0.79	0.03	56.75	25.45
4	0.80	1.81	96.75	0.61	0.04	69.47	30.57
6	0.18	2.24	97.30	0.25	0.03	84.91	36.27

Pictures of the catalysts used in this study



Figure S3: Picture of the zeolite catalysts used in this study. From Left to right: H-Y-30, H-BEA-25, H-FER-20, H-MOR-20, H-ZSM-5-30, H-ZSM-5-80 and H-ZSM-5-280.



Figure S4: Picture of the ion exchange resins used in this study. From left to right: Dowex50WX2, Dowex50WX4, Dowex50WX8, Amberlyst15, Amberlyst16, Amberlyst36, Amberlyst46.

#### **Calculation of the CO-Conversion**

Because of the high pressures used in this study all calculations were done using the Van-der-Waals equation to calculate molar amounts of CO. For this the volumes of the reactors with and without the dosing line were determined.

Volumes Reactors with dosing line:

Reactor 1: 132.27 ml

Reactor 2: 132.51 ml

Reactor 3: 130.51 ml

Volume dosing line:

Reactor 1 dosing line: 15.04 ml

Reactor 2 dosing line: 16.10 ml

Reactor 3 dosing line: 15.05 ml

From integrating the flow over time diagram of the MFCs the total amount of dosed CO could be calculated. To get the total amount of CO which is able to react inside the reactor the total amount of dosed CO was subtracted from the total amount of CO in the dosing line. Dividing the total amount of CO able to react from the used CO, which was calculated by the pressure drop in the reactor the CO-Conversion was calculated.

#### Calculation of the percentage contribution of the desorption peaks to the total NH<sub>3</sub> uptake:

For the evaluation of the percentage contribution of the desorption peaks to the total NH<sub>3</sub> uptake the baseline was subtracted using OriginPro. Further normalisation of the thermograms lead to the normed and baseline corrected thermograms shown in the main manuscript. The desorption peaks were deconvoluted and the area% of each peak was calculated (see Figure S5).



Figure S5: Exemplary evaluation step for the deconvolution of the two desorption peaks for the H-ZSM-5-80 catalyst.



#### Pressure curves of the screening runs:

Figure S6: The pressure over time diagram for all screening runs done with all SAC. a) shows the pressure curves of the screening runs with the zeolites and b) shows the pressure curves of the screening runs with ion exchange resins.