

Supplementary Materials for

The Lattice oxygen determines the methanol selectivity in CO<sub>2</sub> hydrogenation over  
ZnZrO<sub>x</sub> catalysts

This PDF file includes:

**Table. S1.** Catalytic performance of the ZnZrO<sub>x</sub> catalyst. Reaction conditions: 5.0 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3:1, GHSV = 24,000 mL/(g·h), 325 °C.

**Table. S2.** Catalytic performance of the ZnZrO<sub>x</sub> catalysts in literature for CO<sub>2</sub> hydrogenation to methanol.

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**Fig. S1.** The CO<sub>2</sub> conversion and the CH<sub>3</sub>OH Selectivity of catalysts prepared with various grinding speeds. Reaction conditions: 325 °C, 5.0 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3:1, GHSV = 24,000 mL/(g·h).

**Fig. S2. Catalytic performance of the catalyst.** (a) CO<sub>2</sub> conversion (b) CH<sub>3</sub>OH Selectivity and (c) CH<sub>3</sub>OH Yield of catalysts prepared at various Zr/Zn metal ratios. Reaction conditions: 5.0 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3:1, GHSV = 24,000 mL/(g·h).

**Fig. S3.** The EDS element energy spectrum of ZZ-320 catalyst.

**Fig. S4.** XRD patterns of catalysts with different Zr/Zn ratios.

**Fig. S5.** Nitrogen adsorption-desorption isotherms of catalysts prepared with various grinding speeds.

**Fig. S6.** Aperture distribution diagram catalysts prepared with various grinding speeds.

**Fig. S7.** O 1s XPS of catalysts with different Zr/Zn ratios.

**Fig. S8.** Zn 2p and Zr 3d XPS of catalysts with different Zr/Zn ratios.

**Fig. S9.** Zn LM XPS of catalysts with different Zr/Zn ratios.

**Fig. S10.** Zr/Zn metal ratio in the surface region of ZnO-ZrO<sub>2</sub> measured by XPS.

**Fig. S11.** H<sub>2</sub>-TPR profiles of ZnO/ZrO<sub>2</sub> and ZnZrO<sub>x</sub> catalysts.

**Fig. S12.** Temperature-dependent in-situ DRIFTS spectra in H<sub>2</sub> over ZZ-320 and ZZ-500. (Conditions: 100–400 °C, 0.1 MPa, H<sub>2</sub>, 40 mL/min, after reaction gas pretreatment).

**Table. S1.** Catalytic performance of the ZnZrO<sub>x</sub> catalyst. Reaction conditions: 5.0 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3:1, GHSV = 24,000 mL/(g·h), 325 °C.

Catalyst	CO <sub>2</sub> Conversion (%)	Production Selectivity (%)			Yield	
		CH <sub>3</sub> OH	CH <sub>4</sub>	CO	(mg/(g <sub>cat</sub> ·h))	(mg/(m <sup>2</sup> ·h))
ZZ-200	3.59	45.18	0.35	54.21	137.9	4.4
ZZ-300	5.06	52.90	0.66	46.21	170.8	4.4
ZZ-320	5.18	72.17	0.2	27.48	273.4	5.9
ZZ-350	4.19	55.17	1.75	42.88	170.0	3.9
ZZ-400	4.08	41.42	4.83	53.53	126.2	4.5
ZZ-500	3.98	37.13	2.45	59.91	86.52	3.2
Zr/Zn=19	4.95	32.59	7.08	60.23	114.0	3.9
Zr/Zn=3	3.36	54.9	1.44	43.23	135.2	3.7
ZnO-ZrO <sub>2</sub>	1.14	35.17	3.21	60.46	30.35	-

**Table. S2.** Catalytic performance of the ZnZrO<sub>x</sub> catalysts in literature for CO<sub>2</sub> hydrogenation to methanol.

Catalyst	Temperature (°C)	Pressure (MPa)	GHSV (mL/g <sup>1</sup> ·h <sup>-1</sup> )	H <sub>2</sub> /CO <sub>2</sub>	CO <sub>2</sub> Conversion (%)	CH <sub>3</sub> OH Selectivity (%)
ZZ-320	325	5	24000	3	5.2	72.2
ZnO-ZrO <sub>2</sub> (Zn/Zr = 1:1) <sup>1</sup>	320	3	24000	3	5.7	70.0
Co <sub>3</sub> O <sub>4</sub> –ZrO <sub>2</sub> (Co/Zr = 3:1) <sup>1</sup>	320	3	24000	3	1.9	1.0
CuO–ZrO <sub>2</sub> (Cu/Zr = 3:1) <sup>1</sup>	320	3	24000	3	14.0	20.3
ZnInO <sub>x</sub> <sup>2</sup>	300	2	24000	3	4.7	47.0
11.5%GaZrO <sub>x</sub> <sup>2</sup>	300	2	24000	3	2.4	75.0
15ZnZr-600 <sup>3</sup>	340	3	24000	3	7.4	55.8
GaZnZrO <sub>x</sub> <sup>4</sup>	320	5	24000	3	8.8	85.0
ZrZn-15 <sup>5</sup>	350	3	12000	3	7.0	50.0
20% ZnO-ZrO <sub>2</sub> (CP) <sup>6</sup>	320	5.5	24000	3	7.0	87.0
0.8%PdZnZrO <sub>x</sub> <sup>7</sup>	280	5	24000	4	7.8	56.0
ZnZrO <sub>x</sub> -RA <sup>8</sup>	320	5	24000		4.4	94.0
13ZnZrO <sub>x</sub> ,FSP <sup>9</sup>	320	5	24000	4	7.0	80.0
5.0% Zn-CdZrO <sub>x</sub> <sup>10</sup>	320	5	24000	4	8.5	80.8
13%ZnO-ZrO <sub>2</sub> <sup>11</sup>	320	5	24000	4	10.0	86.0

**Table. S3.** Arrhenius plots of CO<sub>2</sub> hydrogenation over ZZ-320 and ZZ-500.

Catalyst	Ea (KJ/mol)	Correlation factor
Z-200	24.45	0.97
ZZ-320	22.86	0.97
ZZ-500	35.64	0.99

**Table. S4.** Elemental content of ZZ-320 catalyst from EDS results

Element	Atomic (%)	Error ( % )
O	47.07	0.30
Zn	9.41	0.26
Zr	43.52	0.08

**Table. S5.** d-spacings of catalysts calculated using the Bragg equation from XRD.

Catalyst	The average diameter of grains by XRD (nm)
ZZ-200	6.5
ZZ-300	7.2
ZZ-320	8.3
ZZ-350	7.4
ZZ-400	7.6
ZZ-500	6.3

**Table. S6.** The BET results from catalysts with various grinding speeds.

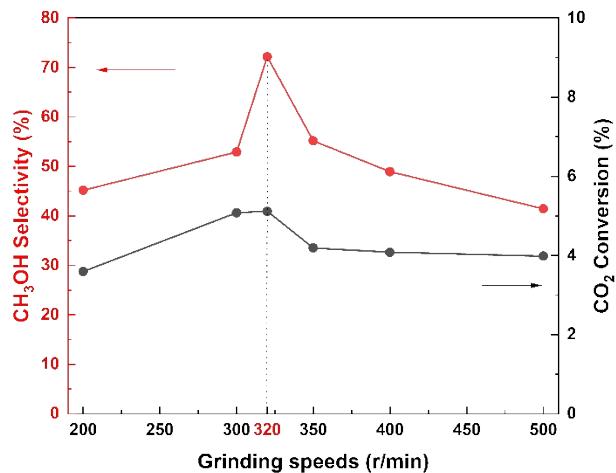
Catalyst	BET Surface Area(m <sup>2</sup> /g)	Pore Volume (cm <sup>3</sup> /g)	Pore Size (nm)
ZZ-200	31.2	0.054	5.8
ZZ-300	38.5	0.0632	5.6
ZZ-320	46.5	0.0638	3.9
ZZ-350	43.3	0.0625	5.4
ZZ-400	28.1	0.0460	6.6
ZZ-500	27.1	0.0265	8.2

**Table. S7.** Deconvolution results of O 1s XPS peaks.

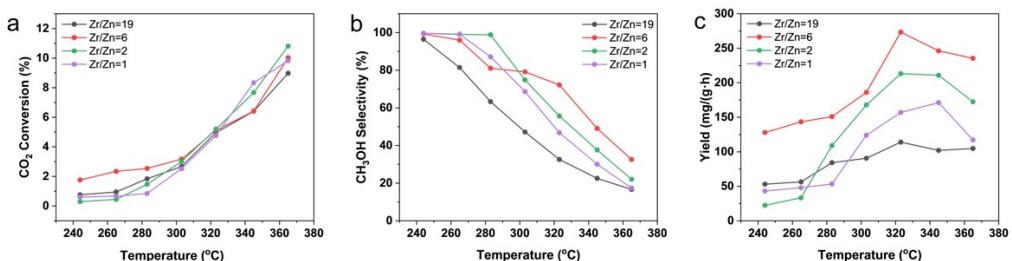
Catalyst	O species (%)		
	O <sub>I</sub>	O <sub>II</sub>	O <sub>III</sub>
Zr/Zn=19	55.12	34.02	10.86
Zr/Zn=6	71.10	22.10	6.80
Zr/Zn=3	53.83	30.88	15.29

**Table. S8.** Quantitative results of the H<sub>2</sub>-TPR, O<sub>2</sub>-TPD, CO<sub>2</sub>-TPD.

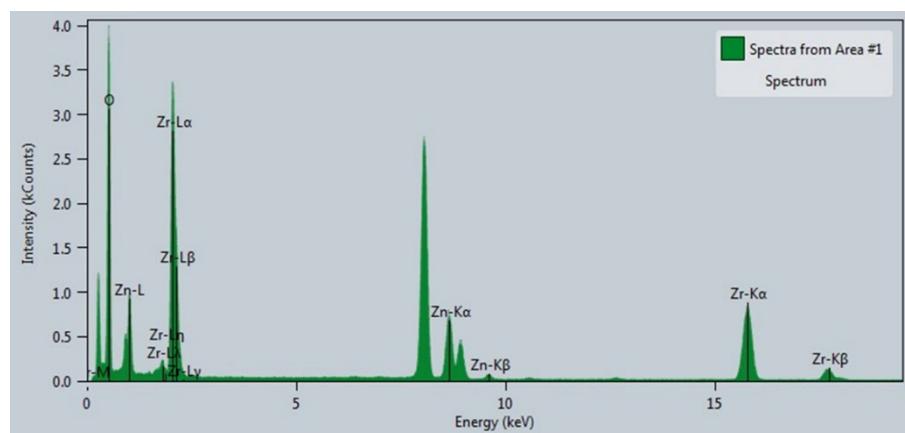
Catalyst	H <sub>2</sub> uptake in H <sub>2</sub> -TPR (mmol/g)		CO <sub>2</sub> uptake in CO <sub>2</sub> -TPD (mmol/g)		O <sub>2</sub> uptake in O <sub>2</sub> -TPD (mmol/g)		
	332 °C 0.0041	617 °C 0.54	100 °C 0.66	408 °C 0.35	82 °C 44.42	461 °C 72.60	658 °C 51.65
ZZ-320	332 °C 0.0041	617 °C 0.54	100 °C 0.66	408 °C 0.35	82 °C 44.42	461 °C 72.60	658 °C 51.65
ZZ-500	337 °C 0.0017	617 °C 0.49	108 °C 0.46	414 °C 0.12	76 °C 37.67	444 °C 0.079	642 °C 0.087



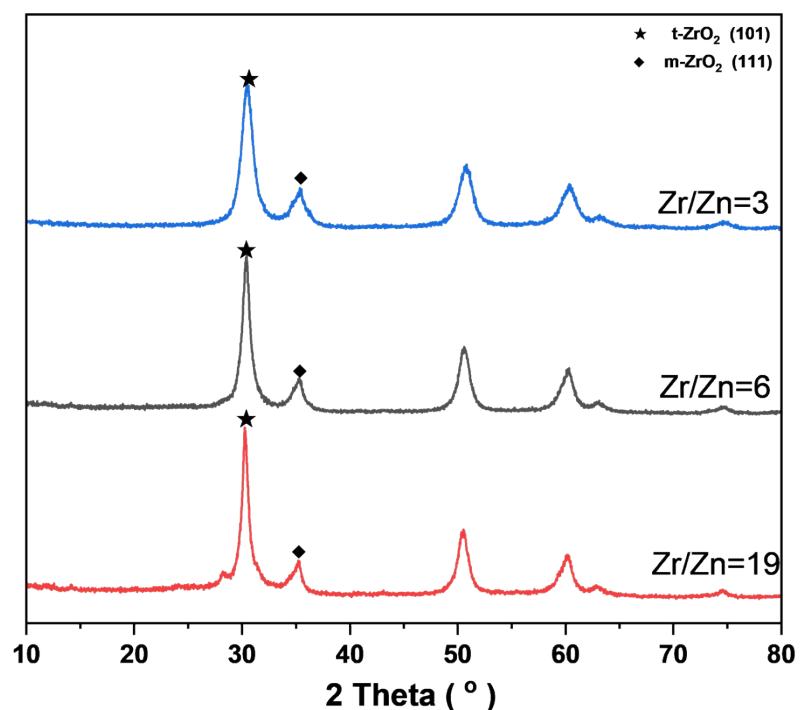
**Fig. S1.** The CO<sub>2</sub> conversion and the CH<sub>3</sub>OH Selectivity of catalysts prepared with various grinding speeds. Reaction conditions: 325 °C, 5.0 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3:1, GHSV = 24,000 mL/(g·h).



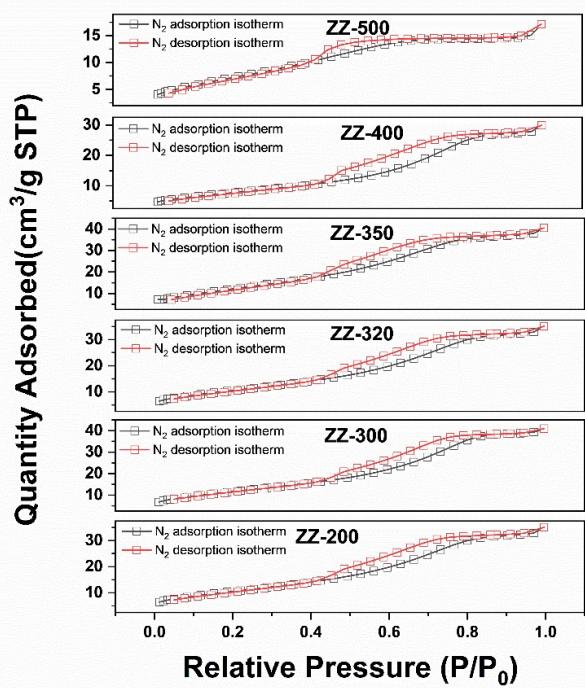
**Fig. S2. Catalytic performance of the catalyst.** (a) CO<sub>2</sub> conversion (b) CH<sub>3</sub>OH selectivity and (c) CH<sub>3</sub>OH yield of catalysts prepared at various Zr/Zn metal ratios. Reaction conditions: 5.0 MPa, H<sub>2</sub>/CO<sub>2</sub> = 3:1, GHSV = 24,000 mL/(g·h).



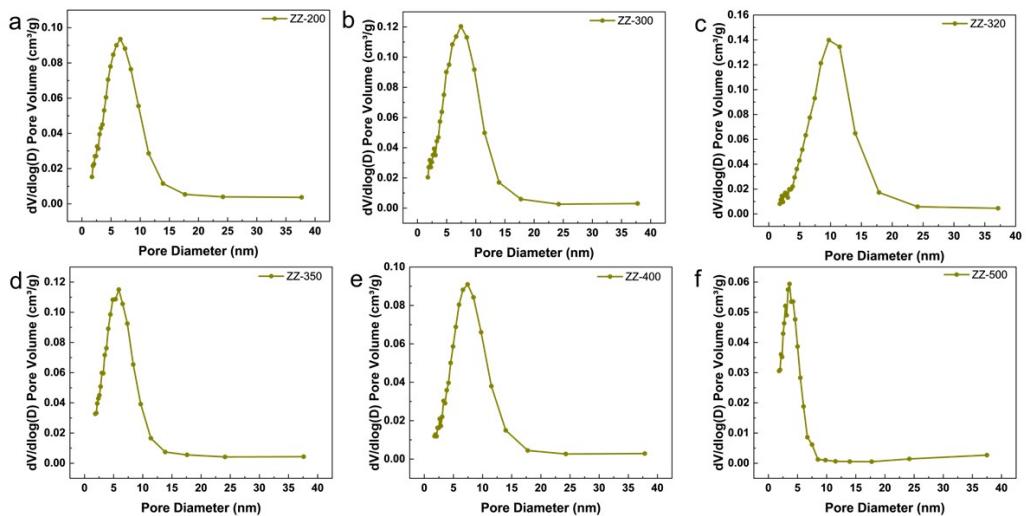
**Fig. S3.** The EDS element energy spectrum of ZZ-320 catalyst.



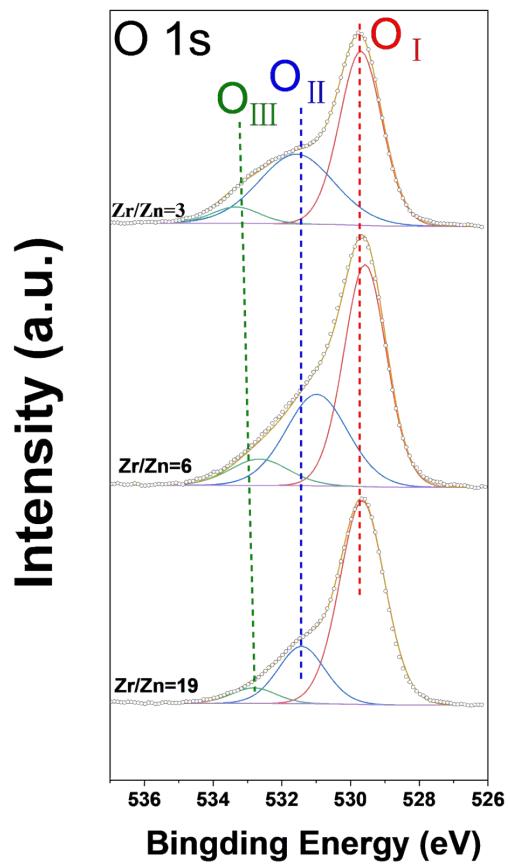
**Fig. S4.** XRD patterns of catalysts with different Zr/Zn ratios.



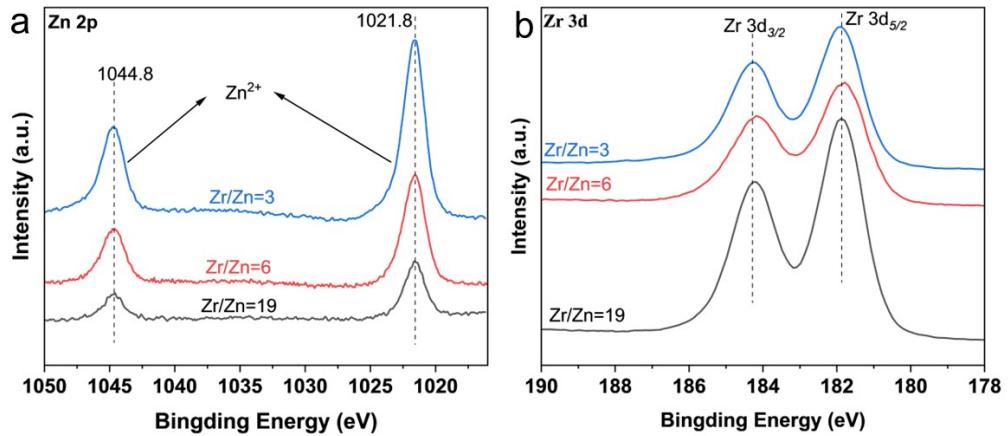
**Fig. S5.** Nitrogen adsorption-desorption isotherms of catalysts prepared with various grinding speeds.



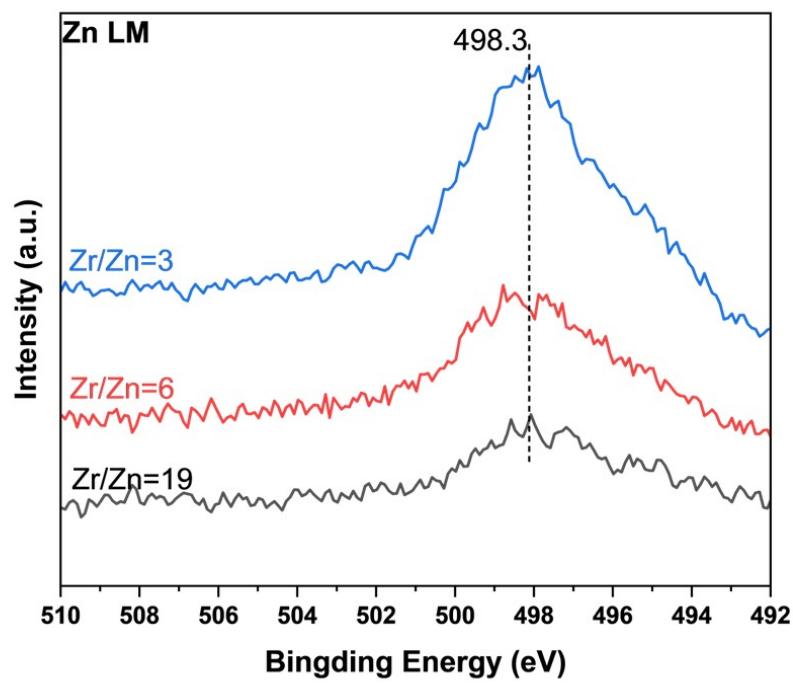
**Fig. 6.** Aperture distribution diagram catalysts prepared with various grinding speeds. (a)ZZ-200, (b)ZZ-300, (c)ZZ-320, (d)ZZ-350, (e)ZZ-400, (f)ZZ-500.



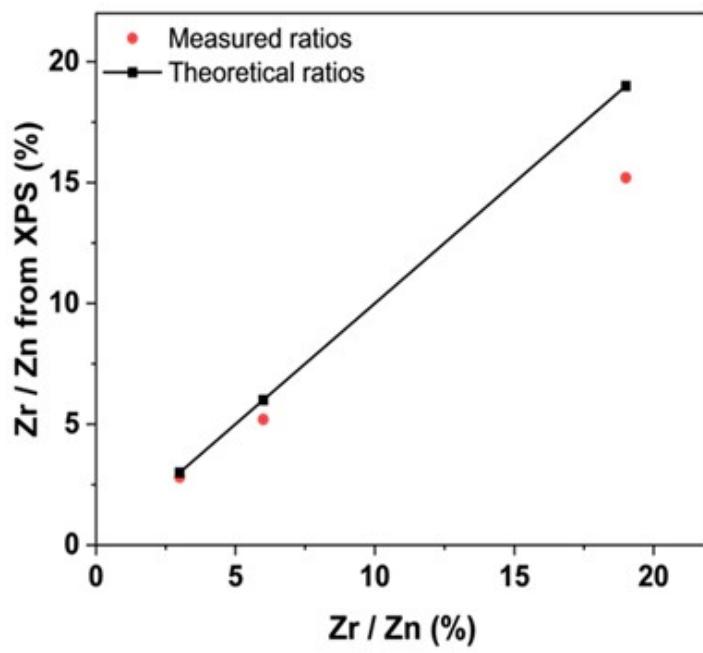
**Fig. S7.** O 1s XPS of catalysts with different Zr/Zn ratios.



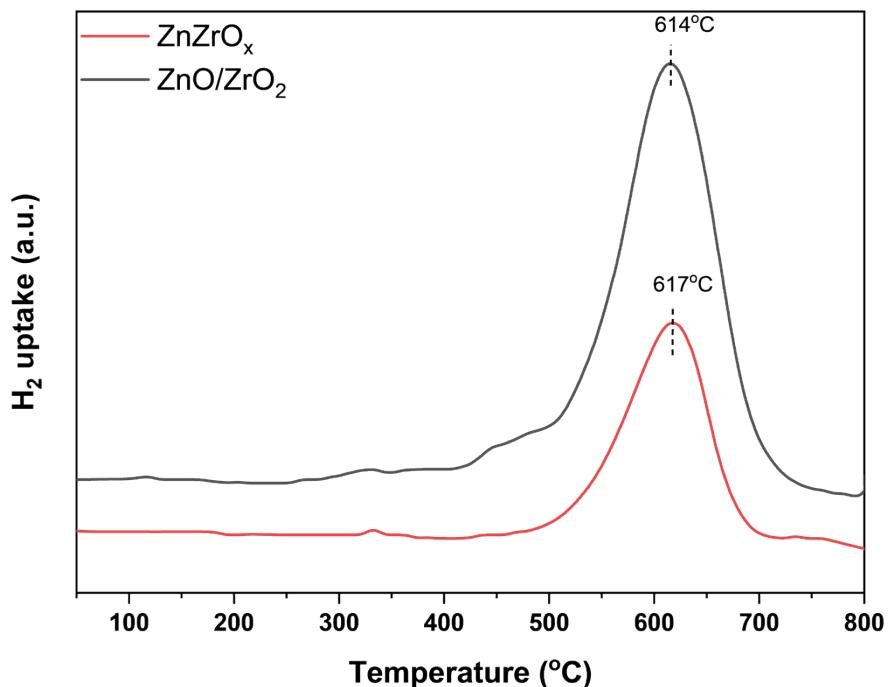
**Fig. S8.** Zn 2p (a) and Zr 3d (b) XPS of catalysts with different Zr/Zn ratios.



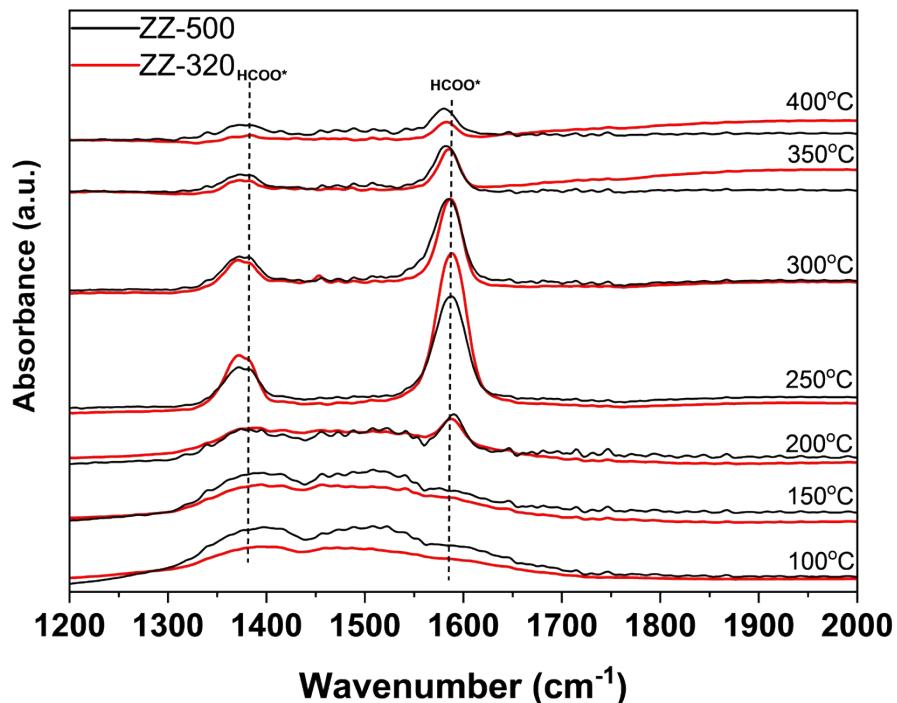
**Fig. S9.** Zn LM XPS of catalysts with different Zr/Zn ratios.



**Fig. S10.** Zr/Zn metal ratio in the surface region of ZnO-ZrO<sub>2</sub> measured by XPS.



**Fig. S11.** H<sub>2</sub>-TPR profiles of ZnO/ZrO<sub>2</sub> and ZnZrO<sub>x</sub> catalysts.



**Fig. S12.** Temperature-dependent in-situ DRIFTS spectra in H<sub>2</sub> over ZZ-320 and ZZ-500. (Conditions: 100–400 °C, 0.1 MPa, H<sub>2</sub>, 40 mL/min, after reaction gas pretreatment).

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