

## Supporting Information for:

# Insights into Size Effects of Pt/Al<sub>2</sub>O<sub>3</sub> Catalysts on Hydrogen Production from Methylcyclohexane Dehydrogenation

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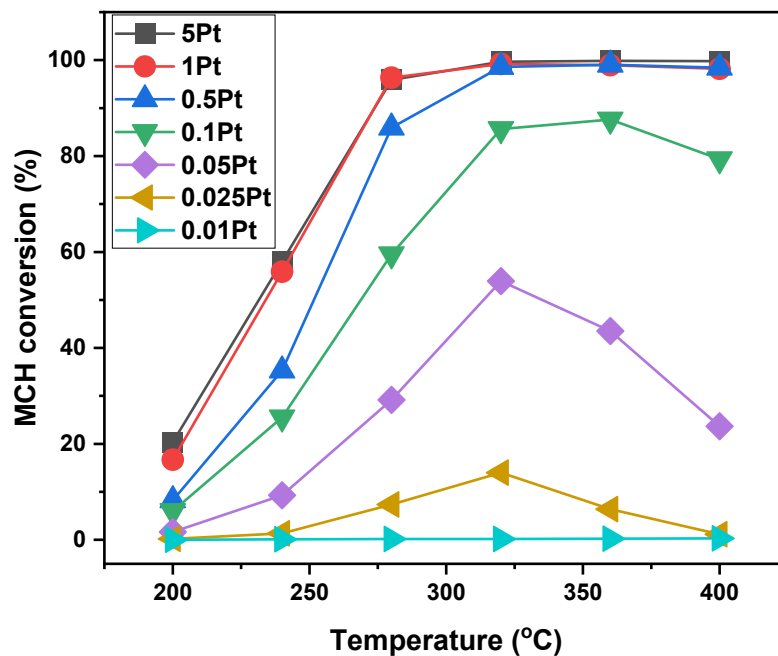
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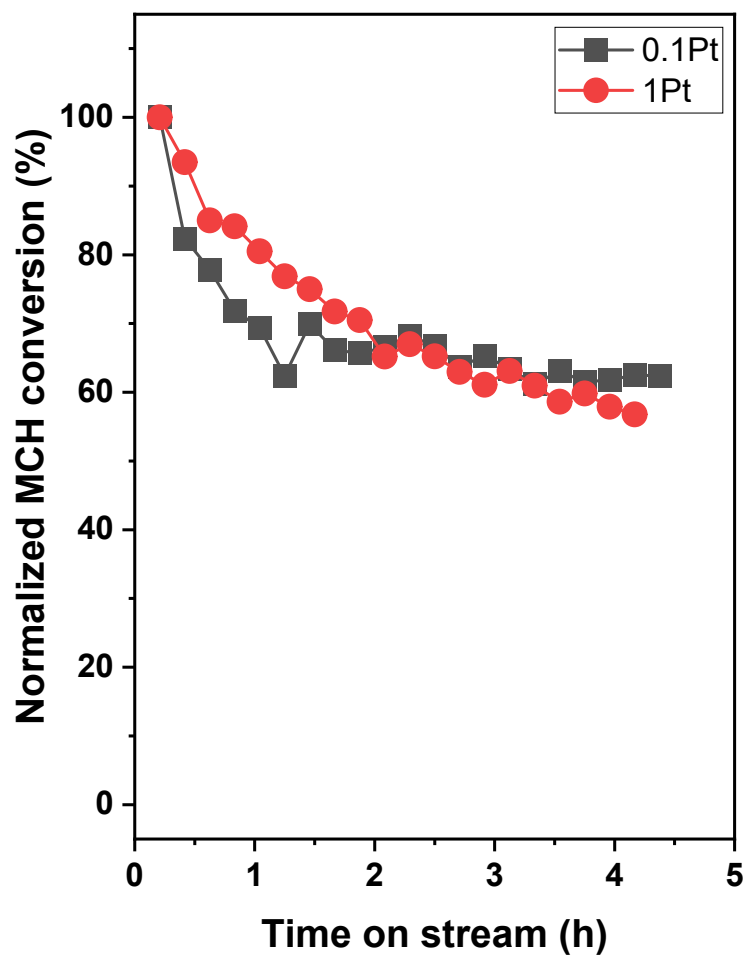
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Dr. Zili Wu

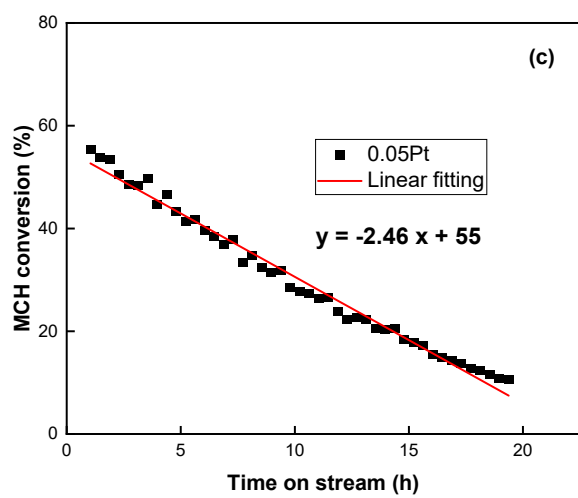
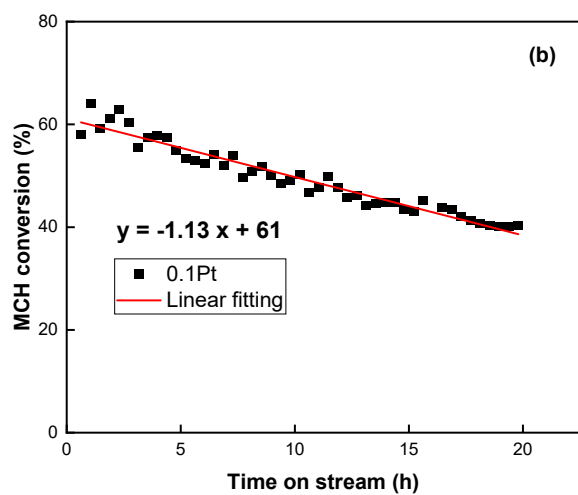
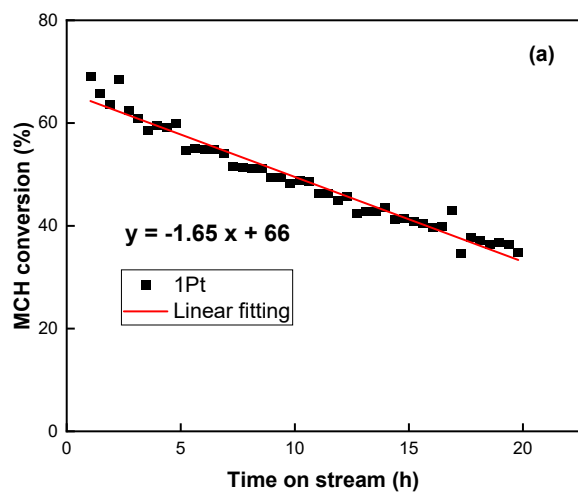
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**Figure S1.** MCH conversion over Pt/Al<sub>2</sub>O<sub>3</sub> catalysts with different Pt loadings. Reaction conditions: 6.5 mL/min Ar and 0.006 mL/min MCH (14kPa MCH) injected using a syringe pump; 30 mg catalyst was used in each experiment.



**Figure S2.** MCH dehydrogenation over 0.1Pt and 1Pt samples at 200 °C with both MCH and toluene in the feed at ratio of 6:1. Experiment conditions: 0.006 mL/min MCH injected using a syringe pump with Ar carrier gas flow rate at 6.5 mL/min.



**Figure S3.** Linear fitting of the MCH conversion over 1Pt (a), 0.1P (b) and 0.05Pt (c) samples during a 20h MCH dehydrogenation test at 320 °C (Figure 6 in the manuscript). The amount of catalysts used for the reaction: 30 mg 0.1Pt sample, 60 mg 0.05Pt sample, and 3mg 1Pt sample mixed with 27 mg quartz sand. Reaction conditions: 6.5 mL/min Ar and 0.006 mL/min MCH injected using a syringe pump.

### **Estimation of mass and heat transfer limitation**

To accurately evaluate the catalytic performance of Pt/Al<sub>2</sub>O<sub>3</sub> catalysts, it is essential to ensure that the catalyst is free of heat transfer limitation and mass transfer limitation. MCH dehydrogenation is a highly endothermic reaction, and given the small amount of catalyst in this study and the long time wait at each temperature (at least 1 hour), the heat transfer limitation should be minimal.

The mass transfer limitation can be categorized into internal mass transfer limitation and external mass transfer limitation, which are evaluated using Weisz-Prater Modulus and effectiveness factor, respectively. These two coefficients are calculated using the open-source method developed by Purdue University (link: [https://engineering.purdue.edu/~catalyst/gradientcheck/grad\\_index.html](https://engineering.purdue.edu/~catalyst/gradientcheck/grad_index.html)). The parameters required in this method are listed as follows:

- (1) quartz reactor diameter is 4 mm.
- (2) 30 mg catalyst is used in each reaction with the catalyst bed length of 3 mm.
- (3) Particle size of Pt/Al<sub>2</sub>O<sub>3</sub> sample is estimated to be 0.1 mm (150 mesh) obtained from the vender. Surface area of catalyst is 120 m<sup>2</sup>/g with a pore volume of 0.5 cm<sup>3</sup>/g. The catalyst tortuosity

is estimated to be 3 according to the previous study on  $\gamma\text{-Al}_2\text{O}_3$  (ref: doi.org/10.1016/j.micromeso.2017.04.010).

(3) Catalyst bed density is estimated at  $750 \text{ kg/m}^3$  with a void fraction of 0.4.

(4) Enthalpy of MCH dehydrogenation is  $204.8 \text{ kJ/mol}$  (Ref: doi.org/10.3390/membranes11120955).

(5) Fluid viscosity.

The fluid viscosity of MCH and toluene at  $473 \text{ K}$  is estimated to be  $1.2 \times 10^{-5} \text{ (kg m}^{-1} \text{ s}^{-1})$  which is calculated via the open-source link (<http://ddbonline.ddbst.de/VogelCalculation/VogelCalculationCGI.exe>) on the basis of cyclohexane assuming that cyclohexane has similar viscosity as the MCH and toluene. Fluid viscosity of Ar gas is calculated based on the open-source link ([https://www.engineeringtoolbox.com/gases-absolute-dynamic-viscosity-d\\_1888.html](https://www.engineeringtoolbox.com/gases-absolute-dynamic-viscosity-d_1888.html)).

(6) Heat capacity

The heat capacity of MCH is  $2280 \text{ J kg}^{-1} \text{ K}^{-1}$  at  $473 \text{ K}$  according to the open-source NIST document (<https://webbook.nist.gov/cgi/cbook.cgi?ID=C108872&Mask=FFF>). The heat capacity of toluene is assumed to be same as MCH at  $2280 \text{ J kg}^{-1} \text{ K}^{-1}$  at  $473 \text{ K}$ , given their similar molecular weight and structure. The heat capacity of Ar is determined to be  $520 \text{ J kg}^{-1} \text{ K}^{-1}$  at  $473 \text{ K}$  based on open-source NIST document (<https://webbook.nist.gov/cgi/cbook.cgi?ID=C7440371&Mask=1&Type=JANAFG&Table=on>).

(7) Thermal conductivity:

The thermal conductivity of MCH is determined to be  $0.03 \text{ W m}^{-1} \text{ K}^{-1}$  at  $473 \text{ K}$  (based on the data at  $450 \text{ K}$  from ref (doi.org/10.1021/je800255r) and the thermal conductivity of toluene is assumed to be the same as MCH, given their similar molecular weight and structure. The thermal

conductivity of Ar is determined to be  $0.0268 \text{ W m}^{-1} \text{ K}^{-1}$  (based on the data at 500 K in the open source data profile [https://www.engineersedge.com/heat\\_transfer/thermal-conductivity-gases.htm](https://www.engineersedge.com/heat_transfer/thermal-conductivity-gases.htm)).

With these parameters and reaction rate at  $0.1 \text{ mol MCH (kg-cat} \cdot \text{s)}^{-1}$ , the WP number is calculated to be 0.12, which is lower than 0.3, indicating that internal mass transfer limitation can be excluded. The effectiveness factor is calculated to be 0.93 ( $>0.9$ ), indicating the external mass transfer can also be excluded. Note that the maximum reaction rate in our study is  $0.01 \text{ mol MCH (kg-cat} \cdot \text{s)}^{-1}$ , much less than  $0.1 \text{ mol MCH (kg-cat} \cdot \text{s)}^{-1}$  used in the calculation. Hence, the mass transfer limitation is anticipated to be smaller than that determined in this calculation, and can be ignored in this study.