

Supporting Information

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3 **OER-Highly-Active Encapsulant to Improve the**
4 **Electrochemical Anticorrosion of Fe-N-C for Ultralong-**
5 **Lifespan and High-Rate Rechargeable Zinc-Air Batteries**

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18 **Experimental Section**

19 ✧ **Materials**

20 Ferrous citrate ($C_6H_8FeO_7$), nickel chloride hexahydrate ($NiCl_2 \cdot 6H_2O$), urea,
21 dopamine hydrochloride (DA), dicyandiamide (DCA), hexadecyl trimethyl ammonium
22 bromide (CTAB), terephthalic acid (PTA), 20% Pt/C (Sigma-Aldrich No. 738549) and
23 Nafion[®]117 solution (5%, Sigma-Aldrich) are analytically pure. Hydrogen peroxide
24 (H_2O_2 , 35 wt.%) was purchased from Thermo Fisher Scientific. Horseradish peroxidase
25 (HRP) was purchased from Shanghai Aladdin Bio-Chem Technology Co., Ltd. HRP
26 was a lyophilized powder, with a purity of RZ: >2.5 and activity: >200 units/mg.
27 Carbon cloth (CC, HCP330N) was produced in Shanghai Hesen Electric Co., Ltd. The
28 carbon cloths were treated with piranha water for 24 h to enhance their hydrophilization.
29 Piranha water was made of concentrated sulfuric acid and hydrogen peroxide with a
30 volume ratio of 7:3. Deionized water (DI, 18.25 M Ω) was obtained from a Millipore
31 Milli-Q water purification system.

32

33 ✧ **Catalyst Syntheses**

34 **1. Syntheses of Fe-NCNT**

35 Fe-NCNT@NiFe-LDH was prepared by a chemical bath deposition (CBD) method
36 and a chemical vapor deposition (CVD) method. First, $C_6H_8FeO_7$ of 0.7378 g and urea
37 of 2.667 g were dissolved in 40 mL DI water. Then, the mixed liquid was placed in
38 cuvette with a piece of CC immersed into, which was kept at 95°C for 3 h. After that,
39 the CC piece with Fe-precursor grown on was clipped out, washed by DI water for

40 several times, and dried for use. Second, DA of 0.4 mg/mL was dissolved in Tris
41 solution (pH = 8.5). Then, the above CC piece was soaked in the homogeneous solution
42 at room temperature for 24 h. After that, polydopamine (PDA) was coated on the Fe-
43 precursor. Third, the Fe-NCNT catalyst was prepared by a CVD method. That is, the
44 above CC/Fe-precursor@PDA as a catalyst for catalyzing the growth of NCNTs was
45 put in the middle of a quartz tube, DCA of 1 g served as solid source was put near the
46 inlet port, and the reaction was processed at 350°C for 1 h and then heated up to 900°C
47 for 2 h with Ar as the carrier gas.

48 **2. Synthesis of NiFe-LDH**

49 NiCl₂·6H₂O of 0.71307 g, C₆H₈FeO₇ of 0.2459 g, urea of 2.667 g, and CTAB of
50 0.7289 g were dissolved in 40 mL DI water. Then, the mixed liquid was placed in
51 cuvette with a piece of CC immersed into, which was kept at 95°C for 3 h. After that,
52 NiFe-LDH was grown on the CC substrate.

53 **3. Syntheses of Fe-NCNT@NiFe-LDH**

54 NiCl₂·6H₂O of 0.71307 g, C₆H₈FeO₇ of 0.2459 g, urea of 2.667 g, and CTAB of
55 0.7289 g were dissolved in 40 mL DI water. Then, the mixed liquid was placed in
56 cuvette with Fe-NCNT immersed into, which was kept at 95°C for 3 h. After that, NiFe-
57 LDH was grown on the NCNTs of the Fe-NCNT, integrated as Fe-NCNT@NiFe-LDH.

58

59 **✧ Material Characterization**

60 X-ray powder diffraction (XRD) was performed on a Rigaku Ultima IV
61 diffractometer with an X-ray generator power of 3 KW (Cu-K_α radiation). The

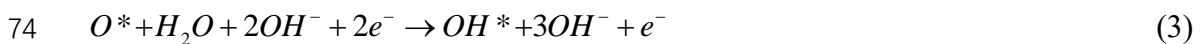
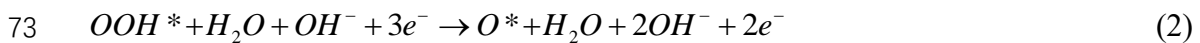
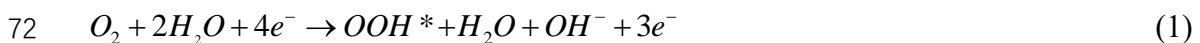
62 microstructures and morphologies of catalysts were characterized by field-emission
 63 scanning electron microscope (FESEM, JEOL, JSM-7500F) and transmission electron
 64 microscopy (TEM, FEI JEOL-2100F). The compositions and element states of catalysts
 65 were measured by X-ray photoelectron spectroscopy (XPS, Escalab 250Xi X-ray,
 66 Thermo Scientific).

67

68 ✧ **Reaction Mechanism**

69 **1. 4-electron oxygen reduction reaction (ORR)**

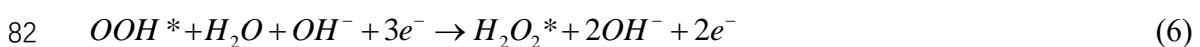
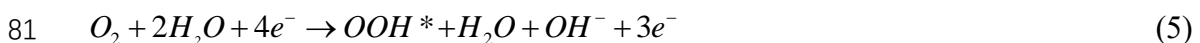
70 It is widely acknowledged that ORR could be carried out via a 4-electron transfer
 71 pathway in alkaline solution. The detailed steps are as follows:



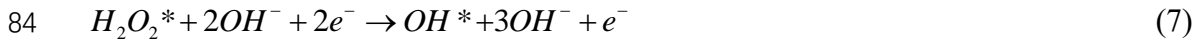
76 where * represents on surface active sites.

77 Alternatively, ORR could be carried out via another 4-electron transfer pathway in
 78 alkaline solution via 2-electron transfer process from O_2 to H_2O_2 plus 2-electron
 79 transfer process from H_2O_2 to OH^- . The detailed steps are as follows:

80 **2-electron transfer process from O_2 to H_2O_2**



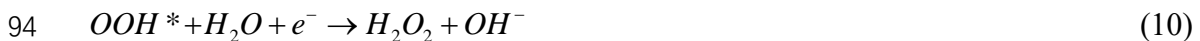
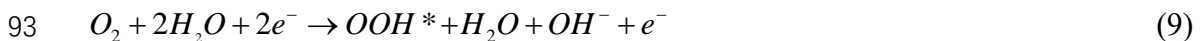
83 **2-electron transfer process from H_2O_2 to OH^-**



86 Notably, $H_2O_2^*$ represents the hydrogen peroxide molecule is adsorbed on catalyst
 87 surface. Here H_2O_2 acts as an ORR mediator. Intermediate H_2O_2 may pose threats
 88 to Fe-N-C catalyst structure via corrosion through Fenton and Fenton-like reactions.

89 **2. Generation of hydrogen peroxide**

90 The ORR reaction also could be carried out via a 2-electron transfer process, which
 91 is accompanied by the production of H_2O_2 in alkaline solution. The reaction steps are
 92 suggested below:



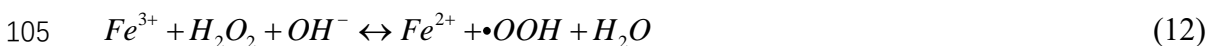
95 Notably, H_2O_2 represents the hydrogen peroxide molecule is dissolved into aqueous
 96 electrolyte. Here H_2O_2 acts as the ORR byproduct. Generation of byproduct H_2O_2
 97 means lower current density, which will in turn cut down the output power density of
 98 the Zn-air battery in discharging process. Besides, H_2O_2 is detrimental to Fe-N-C
 99 catalyst stability.

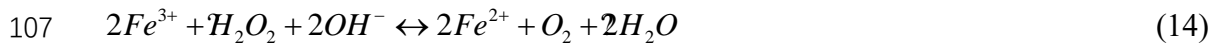
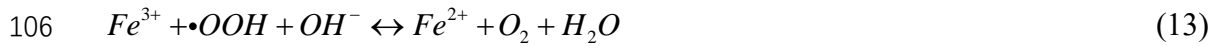
100 **3. Decomposition of byproduct H_2O_2 involving $\bullet OH$ radicals^{1,2}**

101 H_2O_2 could be decomposed to $\bullet OH$ radicals under some surroundings through Fenton
 102 or Fenton-like reactions. The Fenton reactions occur as follows:



104 The reduction of Fe^{3+} is achieved as follows:

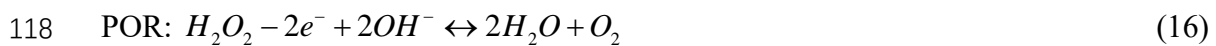
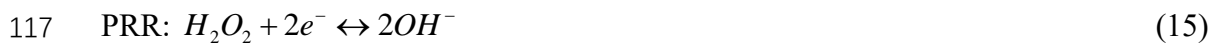




108 •OH radicals as a highly reactive oxygen group can damage durability via two pathways,
109 one involves the conversion of the carbon substrate to CO₂, resulting in the stripping of
110 the metal active center, another is the establishment of oxygen functional groups within
111 the catalyst, which will critically reduce the catalytic performance of the catalyst.

112 **4. Consumption of byproduct H₂O₂ without radicals³**

113 To eliminate the effect of •OH radicals on the stability of the catalyst, H₂O₂ could be
114 consumed via electrochemical pathways. There are two types of electrochemical
115 reaction pathways that are peroxide reduction reaction (PRR) and peroxide oxidation
116 reaction (POR) with the following equations:



119 In addition, H₂O₂ could be consumed via an important non-electrochemical pathway,
120 that is disproportionation with the following equation:⁴



122

123 ✧ **Measurements**

124 **1. Electrochemical tests on electrodes**

125 Electrochemical measurements were performed via electrochemical workstations
126 (CHI760E, Chenhua shanghai). Except specifically stated, all linear voltammetry
127 curves (LSV) were corrected via a scan rate of 5 mV s⁻¹ and with 95%-iR compensation

128 in a three-electrode system, which comprises of a counter electrode (carbon rod), a
129 reference electrode (Hg/HgO electrode), and a working electrode. Electrochemical
130 impedance spectroscopy (EIS) was carried out between 0.01 Hz and 100 kHz (AC
131 voltage with 5 mV). The electrochemical active surface area (ECSA) of the catalysts
132 were determined by calculating its bilayer capacitance (C_{dl}). The C_{dl} value was obtained
133 via CV curves measured in non-Faradic potential ranges with different scan rates. The
134 calculation formula was as $C_{dl} = \Delta j / 2\nu$, where Δj is defined as the difference between
135 the current densities at the middle potential of each curves and ν corresponds to scan
136 rates.

137 **2. Gas diffusion electrode (GDE) test**

138 The ORR activities of Fe-NCNT@NiFe-LDH, Fe-NCNT, NiFe-LDH, and Pt/C were
139 tested via a gas diffusion electrode (GDE), which supports an advanced three-phase
140 (gas-liquid-solid) interface on the catalyst surface.⁵⁻⁷ Because of the low saturated O₂
141 concentration in aqueous electrolyte, the mass transport limitation widely exists in LSV,
142 rotating disk electrode (RDE), and rotating ring disk electrode (RRDE) tests. However,
143 through the design on gas flow, the mass transport limitation could be well avoided to
144 achieve larger ORR current density.

145 The GDE test as well employed the three-electrode test system, with the catalyst as
146 working electrode, the carbon rod as counter electrode, and Hg/HgO electrode as
147 reference electrode, with the 1M KOH aqueous electrolyte saturated by O₂. The
148 structure of GDE is schematically shown in Figure S10.

149 The method to make the catalyst-loaded working electrode was as follows. Fe-

150 NCNT@NiFe-LDH, Fe-NCNT, and NiFe-LDH of 1 cm² geometric area (They are in-
151 situ grown on CC) were respectively ground to fine powder in an agate mortar and to
152 prepare slurry by adding drops of anhydrous ethanol and 30 μL of Nafion (for each
153 catalyst). The slurry was then uniformly dropped on a piece of hydrophobic carbon
154 cloth with the catalyst centered at an area of 1 cm², and then dried at 60°C in air. For
155 Pt/C, commercial 20% Pt/C of 5 mg and carbon cloth of 1 cm² (~ 10 mg) were used to
156 prepare slurry, and otherwise synthetic conditions were identical.

157 **3. Rotating ring disc electrode (RRDE) and rotating disc electrode (RDE) tests**

158 **ORR performance**

159 To evaluate the ORR performances of catalysts in O₂-saturated 0.1 M KOH, RRDE
160 (ALS, RRDE-3A) was carried out using the rotation speed of 1600 rpm. Fe-
161 NCNT@NiFe-LDH, Fe-NCNT, NiFe-LDH, and Pt/C based slurries were respectively
162 prepared via the same operations as used in GDE measurement. Each kind of slurry was
163 carefully transformed onto the glassy carbon disc electrode of the RRDE. After drying
164 at room temperature and in air, a uniform and dense film should be guaranteed on the
165 surface of the disc electrode.

166 Electron transfer number (*n*) and hydrogen peroxide yield (H₂O₂%) were calculated
167 according to the following two formulas:

$$168 \quad n = 4 \times \frac{I_D}{I_D + \frac{I_R}{N}} \quad (18)$$

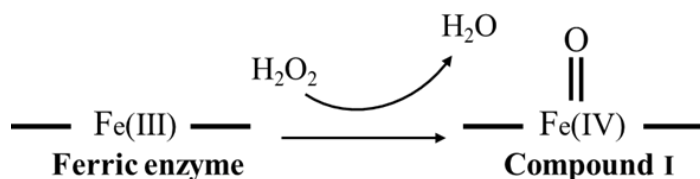
$$169 \quad H_2O_2\% = 200 \times \frac{\frac{I_R}{N}}{\frac{I_R}{N} + I_D} \quad (19)$$

170 where *I_R* and *I_D* were the ring and disk currents, *N* was the ring electrode collection

171 efficiency and was 0.4 here.

172 Peroxidase-coupled RRDE

173 To investigate the specific pathway of electron transfer, horseradish peroxidase was
174 introduced to (partially) terminate the “2+2”-electron transfer pathway of ORR by
175 capturing H₂O₂. The test conditions and electrode preparation were the same as for the
176 RRDE test, except with 0.02 mg/mL horseradish peroxidase added into the O₂-saturated
177 0.1 M KOH aqueous electrolyte. HRP is a natural metalloenzyme extracted from the
178 roots of the horseradish plant. HRP reacts with H₂O₂ to form compound I with a reaction
179 rate coefficient of 1*10⁷ M⁻¹s⁻¹.⁸ The capture mechanism of horseradish peroxidase on
180 H₂O₂ is as follows.⁹



(20)

183 PRR and POR by RDE

184 The test conditions and electrode preparations were the same as for the RRDE test,
185 except that 10 mM H₂O₂ was introduced and the electrolyte solution was saturated by
186 N₂ in the tests. LSV curves for PRR performances were collected in the range from 1.0
187 V to 0.3 V vs RHE (in the negative potential direction), and LSV curves for POR
188 performances were collected in the range from 0.9 V to 1.7 V vs RHE (in the positive
189 potential direction).

190

191 **4. Fluorescence test**

192 Detection on $\bullet\text{OH}$ radical¹⁰⁻¹² was performed by using a fluorescence
193 spectrophotometer (SHIMADZU, RF-6000A) with the excitation wavelength of 315
194 nm, the excitation bandwidth of 1.5 nm, and the wavelength range of 300 nm to 500
195 nm.

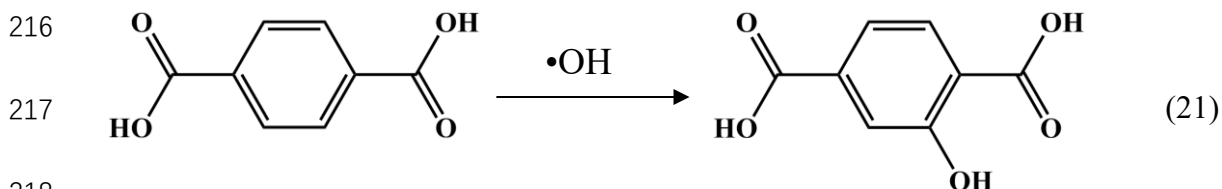
196 To probe if $\bullet\text{OH}$ radical could be generated without H_2O_2 , the catalyst samples (Fe-
197 NCNT@NiFe-LDH, Fe-NCNT, and NiFe-LDH) with 1 cm^2 geometric area were
198 immersed into a solution of 20 mL consisting of 0.1 M KOH and 0.08 mg/mL PTA,
199 respectively. After holding at 30 °C for 24 h, 3 mL solution was extracted out for
200 fluorescence test. The corresponding result is shown in Figure 5g in the main body,
201 where the sample marked “blank sample” represents no catalyst is introduced into the
202 solution while other conditions are identical.

203 To probe if $\bullet\text{OH}$ radical was generated through Fenton reactions in ZABs, the catalyst
204 samples with 1 cm^2 geometric area were immersed into a solution of 20 mL consisting
205 of 0.1 M KOH and 0.08 mg/mL PTA, respectively. After ORR reaction at a constant
206 potential of 0.5 V vs RHE for 3 h, 3 mL solution was extracted out for fluorescence test.
207 The corresponding result is shown in Figure 5h in the main body.

208 Furthermore, to resemble byproduct H_2O_2 in high concentration, the catalyst samples
209 with 1 cm^2 geometric area were immersed into a solution of 20 mL consisting of 0.1 M
210 KOH, 0.08 mg/mL PTA and 10 mM H_2O_2 , respectively. After holding at 30 °C for 24
211 h, 3 mL solution was extracted out for fluorescence test. The corresponding result is
212 shown in Figure 5i in the main body, where the sample marked “blank sample”

213 represents no catalyst is introduced into the solution while other conditions are identical.

214 If there are $\bullet\text{OH}$ radicals, they will capture fast by PTA through the reaction as
215 follows:



219 The generated 2-Hydroxy terephthalic acid has a fluorescent effect with the emission
220 wavelength of ~ 425 nm.

221 5. H_2O_2 detection methods.

222 A phosphate buffer was prepared by dissolving 2.8756 g $\text{K}_2\text{HPO}_4 \cdot 3\text{H}_2\text{O}$ and 11.935 g
223 KH_2PO_4 in 200 ml deionized water. Then prepared N, N-diethyl-1,4-phenylenediamine
224 sulfate (DPD, 97%, Aldrich) and peroxidase (POD, horseradish, Aldrich) stock
225 solutions. (Dissolve 0.1 g DPD in 10 ml 0.05 M H_2SO_4 solution and 10 mg POD in 10
226 ml deionized water.) During the experiment, take 2.5ml sample solution into a quartz
227 tube each time, added 0.4 ml phosphate buffer and 50 μL POD solution in sequence.
228 Liter and 50 microliters of DPD solution, mix well. Useing UV-2600 (Shanghai
229 Tianmei Scientific Instrument Co., Ltd.) to measure absorbance at 552 nm. Calibrate
230 the H_2O_2 concentration by diluting a 30% H_2O_2 stock solution.¹³

231 6. Off-line gas chromatography test

232 DI water of 4 mL were added to the bottom of a quartz reactor with the volume of
233 250 mL (PQ256, purchased from Beijing Perfect light Technology Co., Ltd., China).
234 Fe-NCNT@NiFe-LDH and Fe-NCNT were then respectively immersed into the DI

235 water. And then, the reactor is sealed, and Ar gas was continuously introduced into the
236 reactor for half an hour to remove the original oxygen from the system. After that, 50
237 μL H_2O_2 (35 wt.%) was added into the DI water, and simultaneously timing was begun.
238 At 5, 9, 13, 17, 21, 25, and 29 min, 1 mL gas was extracted from the system at each
239 time and used for analysis via gas chromatographs (GC9790II, FULI INSTRUMENTS).

240 **7. Aqueous Zn-air battery (ZAB) assembly and performance measurements**

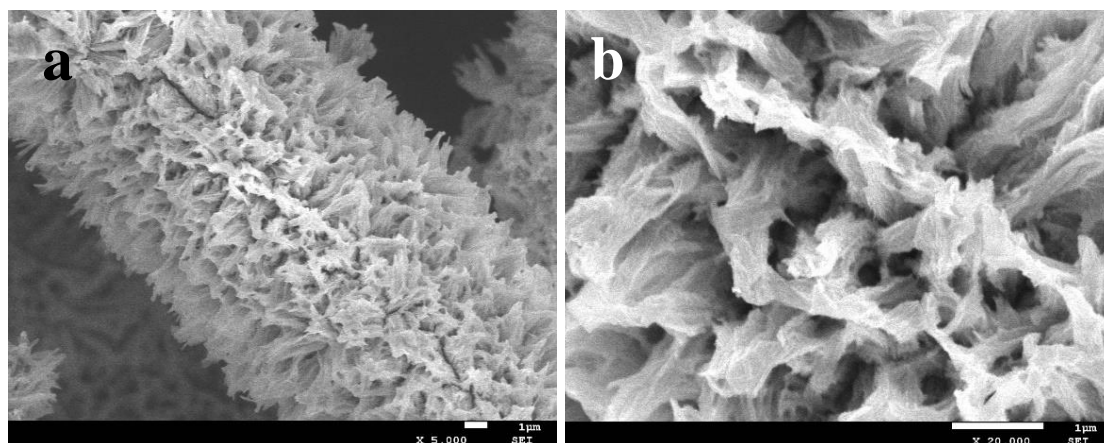
241 CC/catalysts of 1 cm^2 geometric area were sandwiched by two pieces of nickel foam.
242 And to enhance air diffusion, an air diffusion layer was made on the outward side of
243 the air cathodes. The detail is as follows. A viscous slurry was prepared by adequately
244 mixing 0.9 g carbon black, 3 mL isopropanol and 0.1 mL PTFE (10 wt% in DI water).
245 Then, the slurry was applied evenly to one side of the sandwich (that is the outside of
246 one piece of nickel foam) until every cavity was filled. And then the above sandwich
247 was compressed tightly by using an even pressure of 3 MPa for 2 min. Finally, the
248 excess slurry on the surface was scraped off by using a plastic or stainless-steel blade.
249 The above electrodes were used as the air cathode, polished zinc foil was used as the
250 anode, and a mixture of 6.0 M KOH + 0.2 M $\text{Zn}(\text{CH}_3\text{COO})_2$ was used as the electrolyte.
251 The structure of the assembled ZABs is schematically shown in Figure 6a in the main
252 body.

253 All ZABs were measured in air conditions without pumping oxygen.

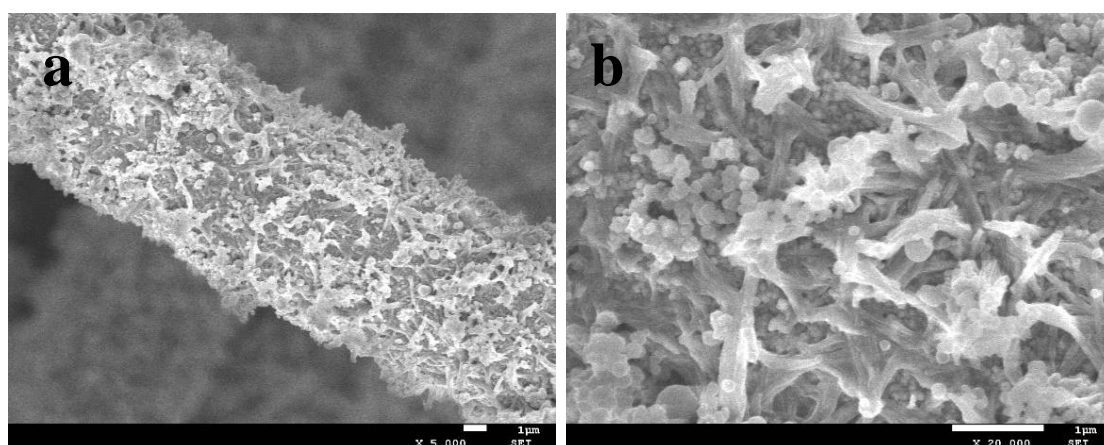
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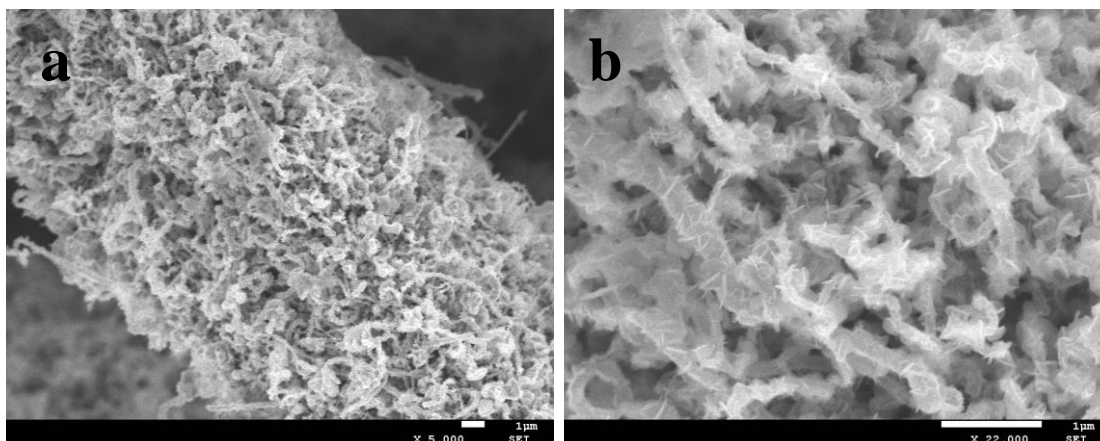
256 **Figures and Discussion**



258 **Figure S1.** SEM images of FeOx(OH)_y grown on the carbon fibers of CC.



261 **Figure S2.** SEM images of FeOx(OH)_y@PDA grown on the carbon fibers of CC.

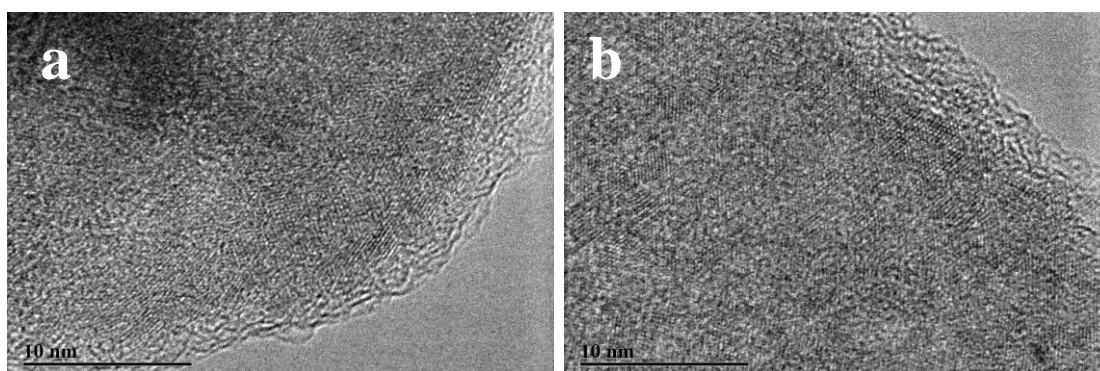


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264 **Figure S3.** SEM images of Fe-NCNT@NiFe-LDH grown on the carbon fibers of CC,
265 where NiFe-LDH is synthesized without CTAB addition.

266

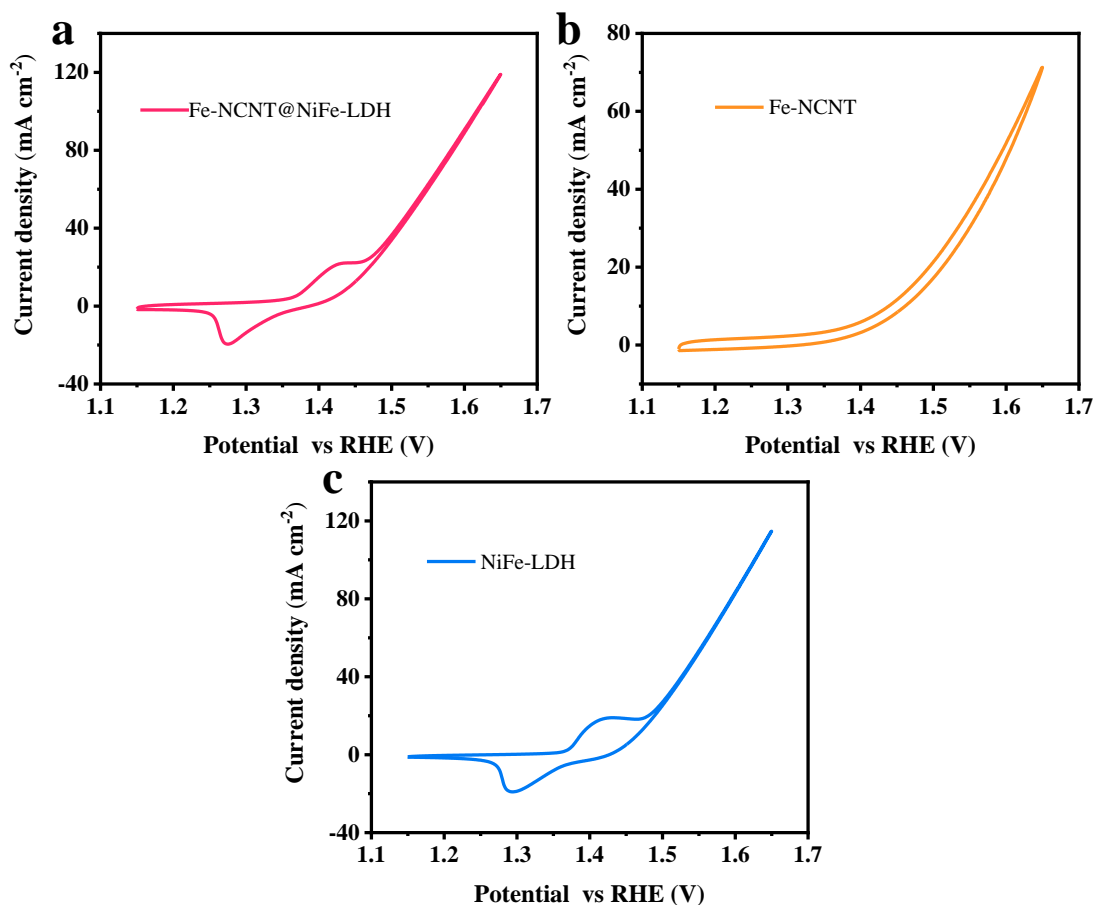
267 As revealed in Figure S3, when CTAB was not added, the NiFe-LDH nanosheets on
268 the surface of Fe-NCNT nanotubes were not uniformly distributed and had low
269 coverage.



270

271 **Figure S4.** HRTEM images of NiFe-LDH of Fe-NCNT@NiFe-LDH.

272

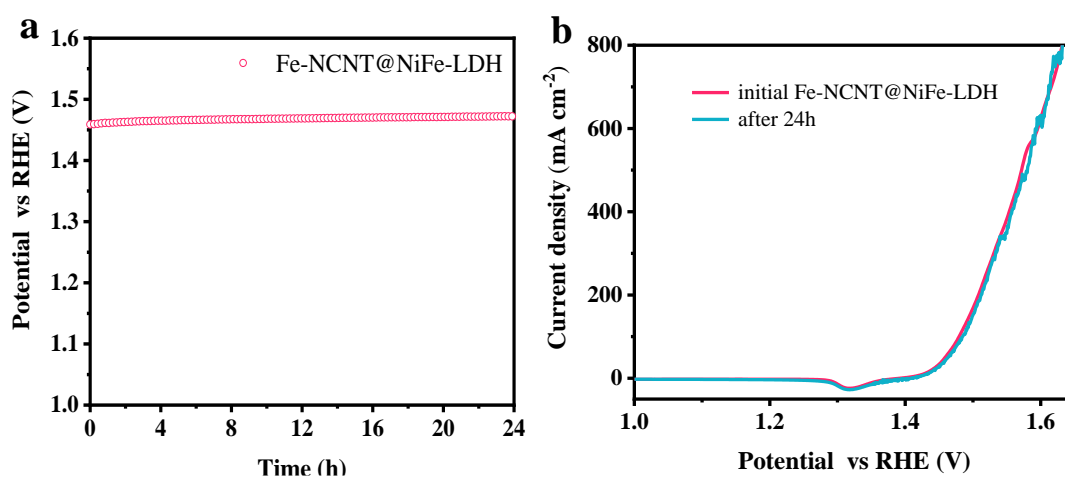


273

274 **Figure S5.** CV curves of (a) Fe-NCNT@NiFe-LDH, (b) Fe-NCNT, and (c) NiFe-LDH,

275 measured in O₂-saturated 1 M KOH without *iR* compensation.

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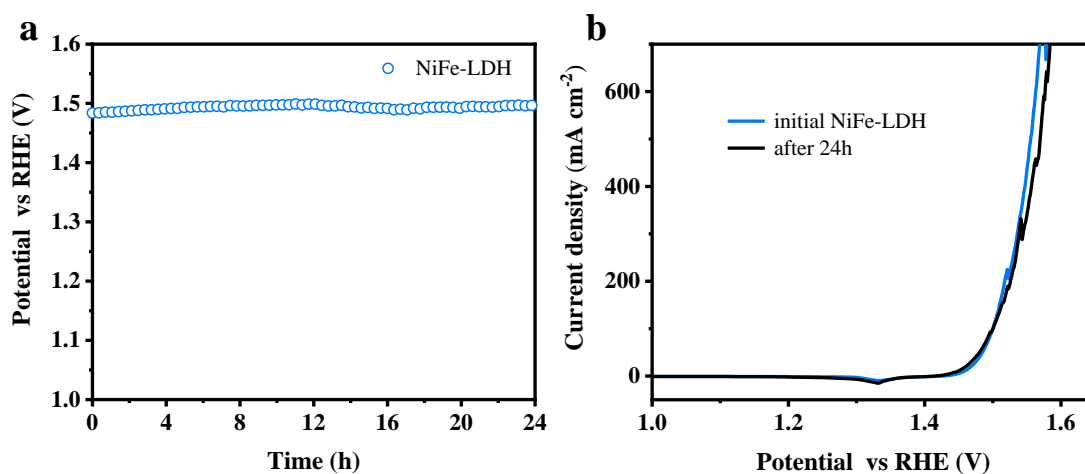
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278 **Figure S6.** (a) Chronopotentiometric curve of Fe-NCNT@NiFe-LDH measured at a

279 constant current density of 10 mA cm⁻² for 24 h in O₂-saturated 1 M KOH electrolyte,

280 (b) LSV curves before and after the stability test.

281



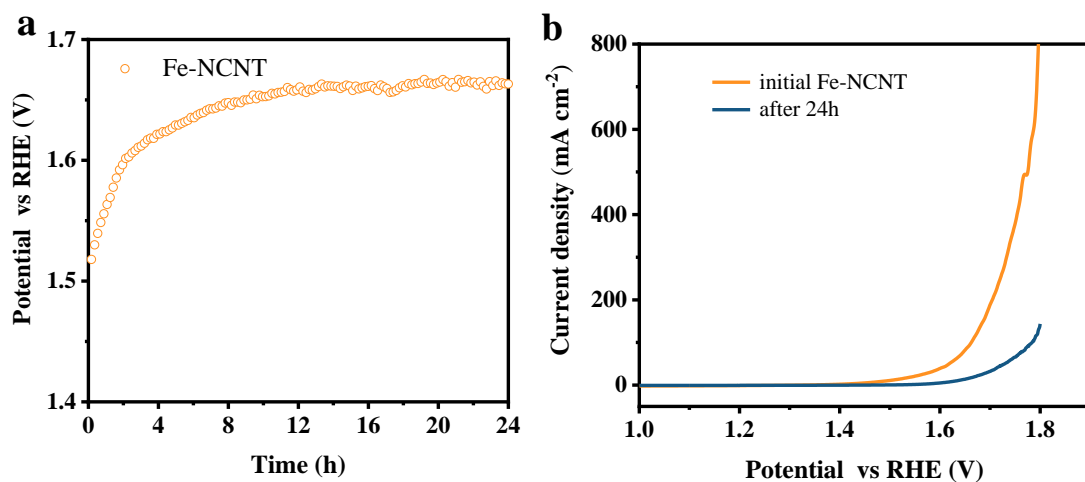
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283 **Figure S7.** (a) Chronopotentiometric curve of NiFe-LDH measured at a constant

284 current density of 10 mA cm⁻² for 24 h in O₂-saturated 1 M KOH electrolyte, (b) LSV

285 curves before and after the stability test.

286



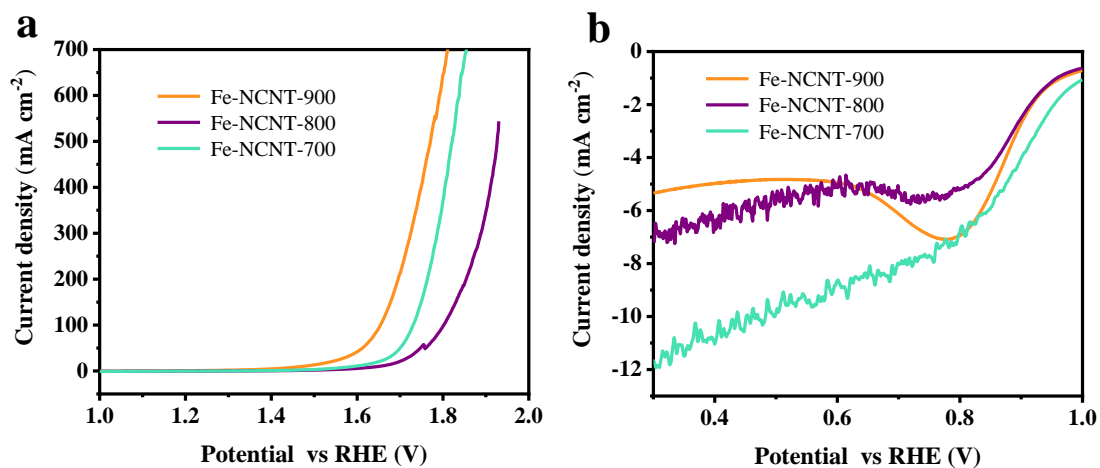
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288 **Figure S8.** (a) Chronopotentiometric curve of Fe-NCNT measured at a constant current

289 density of 10 mA cm⁻² for 24 h in O₂-saturated 1 M KOH electrolyte, (b) LSV curves

290 before and after the stability test.

291

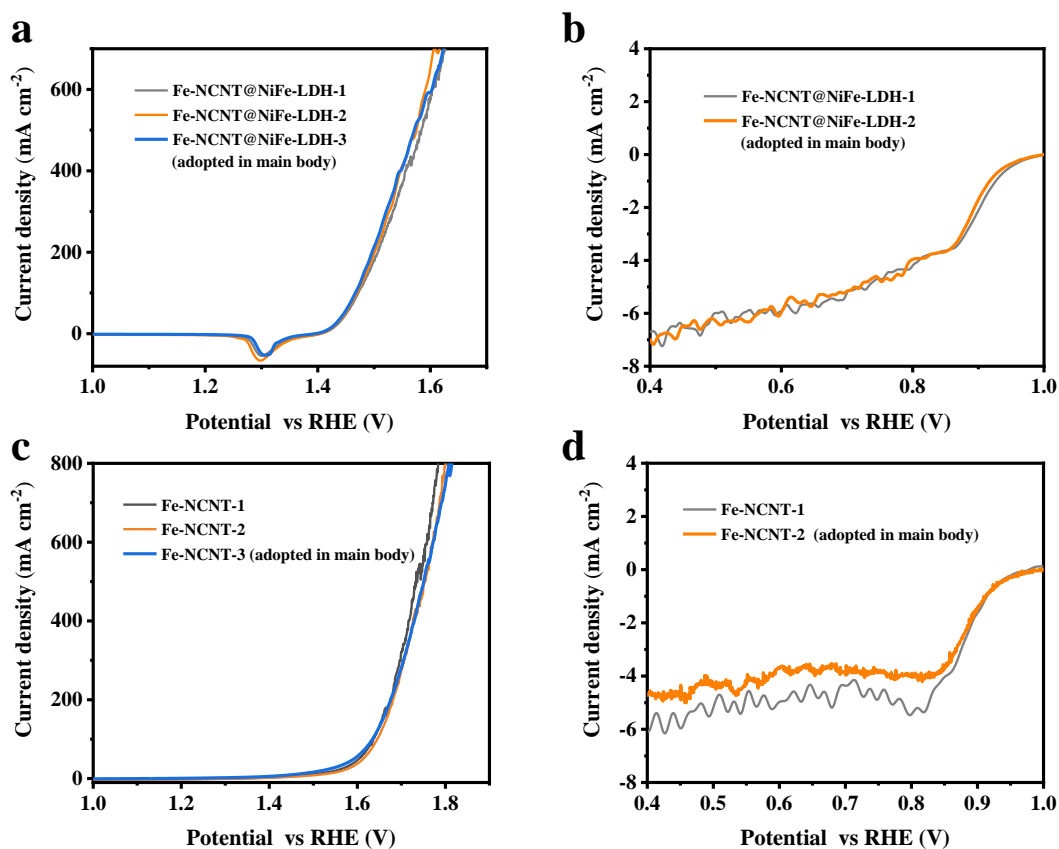


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293 **Figure S9.** (a) OER-LSV curves and (b) ORR-LSV curves of Fe-NCNT-700, Fe-

294 NCNT-800 and Fe-NCNT-900, measured in O₂-saturated 1 M KOH.

295



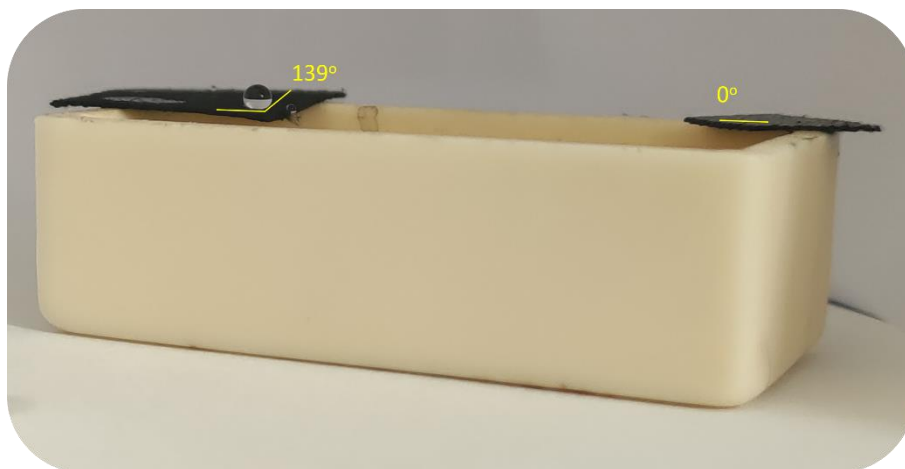
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297 **Figure S10.** Reproducibility of Fe-NCNT@NiFe-LDH from different Batches: (a)

298 OER at 1 M KOH and (b) ORR at 0.1 M KOH; Reproducibility of Fe-NCNT from

299 different Batches: (a) OER at 1 M KOH and (b) ORR at 0.1 M KOH.

300



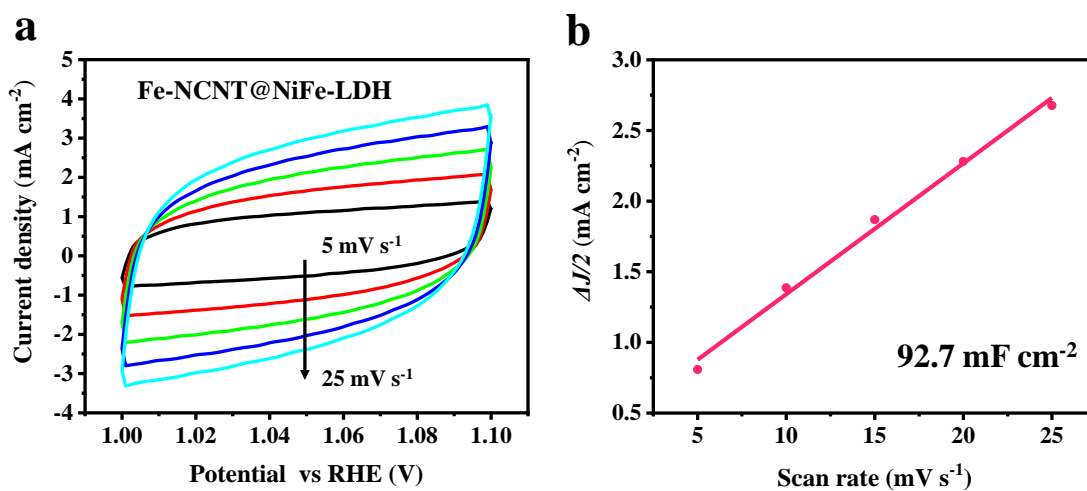
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302 **Figure S11.** Contact angles of DI water on Fe-NCNT (in the left) and Fe-NCNT@NiFe-
303 LDH (in the right).

304

305 **Notes: Movies S1** (Hydrophilicity/hydrophobicity evaluation of Fe-NCNT) **and S2**
306 (Hydrophilicity/hydrophobicity evaluation of Fe-NCNT@NiFe-LDH) are separately
307 uploaded as MP4 files.

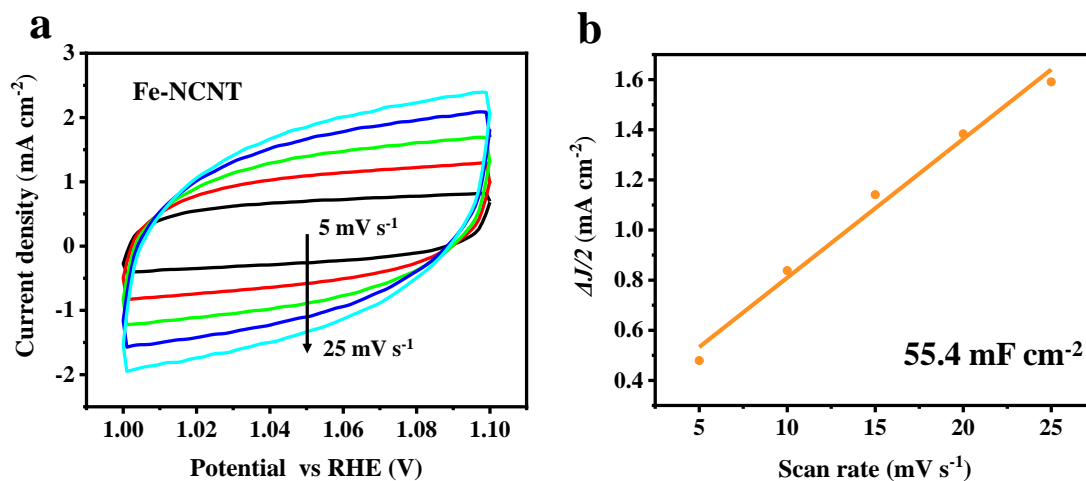
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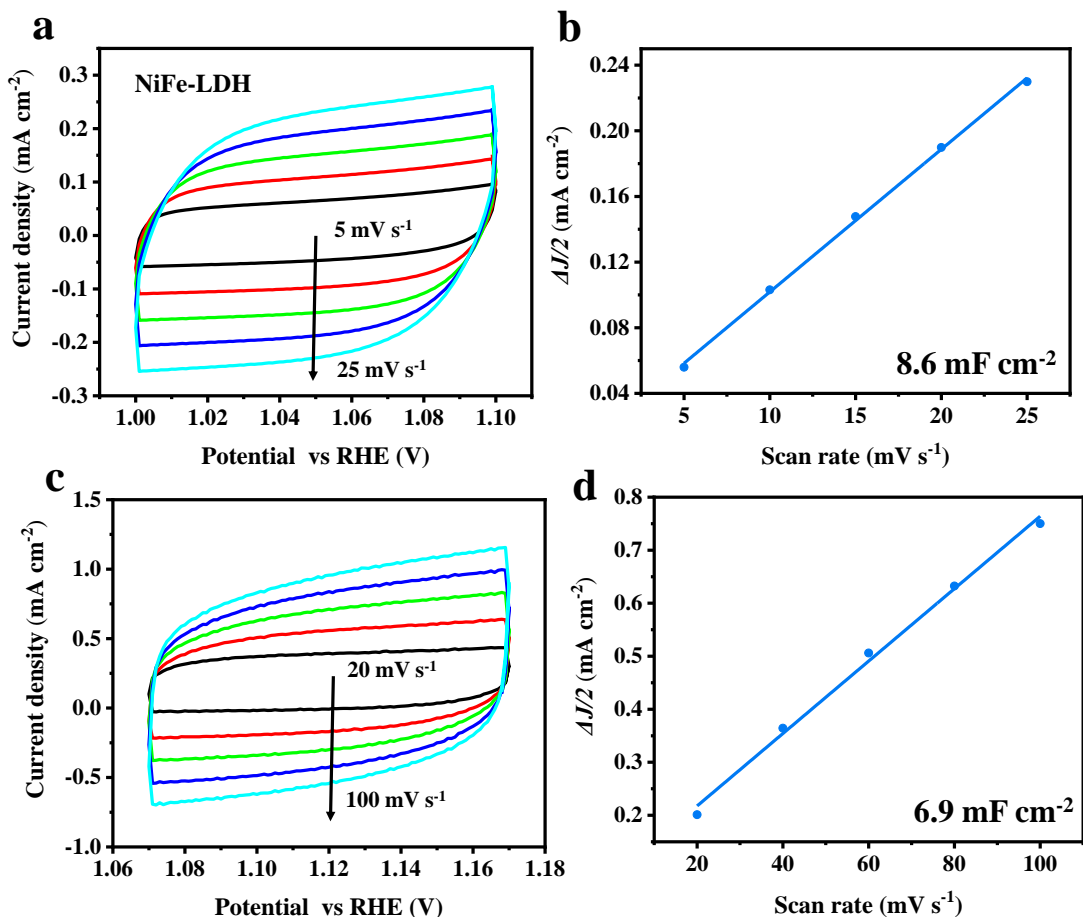
309

310 **Figure S12.** (a) CV curves of Fe-NCNT@NiFe-LDH at 5, 10, 15, 20, and 25 mV/s

311 scanning rates. (b) Correspondingly plot of the capacitive current as a function of the
312 scan rate of the Fe-NCNT@NiFe-LDH.
313



314
315 **Figure S13.** (a) CV curves of Fe-NCNT at 5, 10, 15, 20, and 25 mV/s scanning rates.
316 (b) Correspondingly plot of the capacitive current as a function of the scan rate of the
317 Fe-NCNT.
318



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320 **Figure S14.** (a) CV curves of NiFe-LDH measured at 5, 10, 15, 20, and 25 mV/s

321 scanning rates in potential range from 1.0 to 1.1 V vs. RHE. (b) Correspondingly plot

322 of the capacitive current as a function of the scan rate of the Fe-NCNT@NiFe-LDH. (c)

323 CV curves of NiFe-LDH measured at 20, 40, 60, 80, and 100 mV/s scanning rates in

324 potential range from 1.07 to 1.17 V vs. RHE. (d) Correspondingly plot of the capacitive

325 current as a function of the scan rate of the Fe-NCNT@NiFe-LDH.

326

327 Figures S11-13 show CV curves of Fe-NCNT@NiFe-LDH, Fe-NCNT, and NiFe-

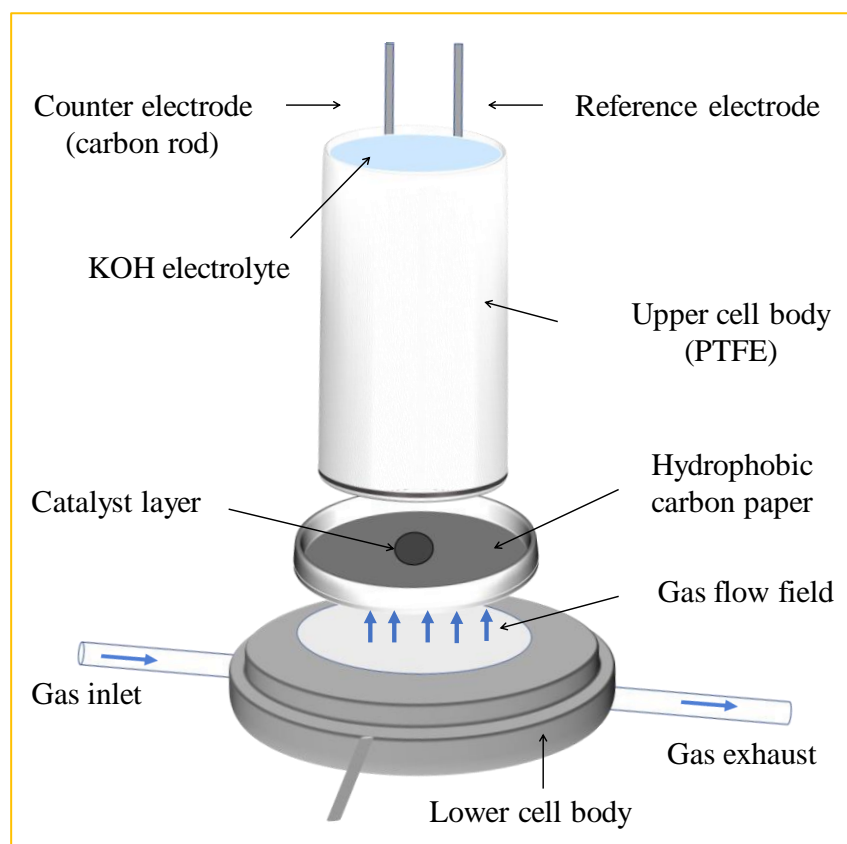
328 LDH measured at non-Faradic potential ranges. The electrochemical double-layer

329 capacitance (C_{dl}) is calculated from the CV curves via different sweep speeds. As shown

330 in Figures S10b, S11b, and S12b, the C_{dl} value of the Fe-NCNT@NiFe-LDH is 92.7

331 mF cm^{-2} , which is higher than the Fe-NCNT (55.4 mF cm^{-2}), and much larger than that
332 of NiFe-LDH ($6.9\sim 8.6 \text{ mF cm}^{-2}$). The electrochemical active surface area (ECSA) of
333 the catalysts are positively correlated with the value of C_{dl} . The C_{dl} trend clearly
334 demonstrates that Fe-NCNT@NiFe-LDH has larger electrochemical active surface area
335 per geometric area, superior to Fe-NCNT and NiFe-LDH. And the C_{dl} values of Fe-
336 NCNT@NiFe-LDH and Fe-NCNT are almost 10 times of that of NiFe-LDH. The
337 enhancement of ECSA of Fe-NCNT@NiFe-LDH probably originates from its uniform
338 wrapping structure with thinner vertically grown NiFe-LDH nanosheets, facilitating to
339 achieve high surface area and better mass accessibility.

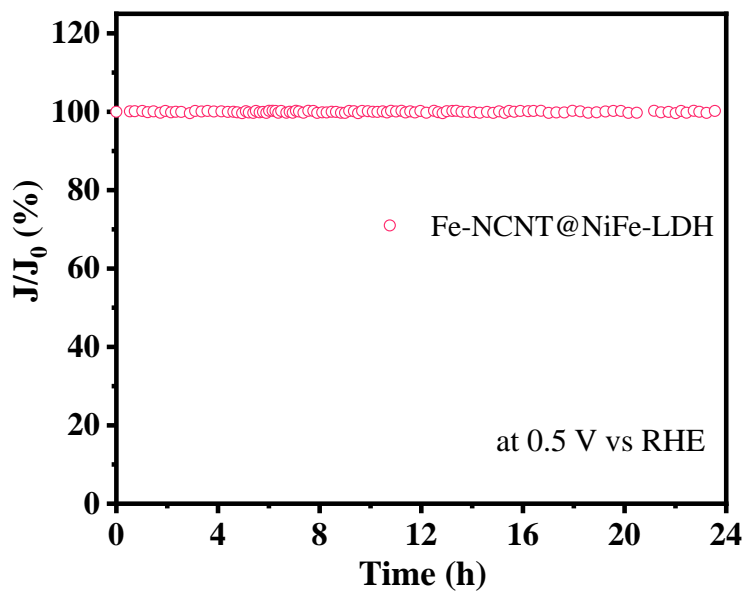
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342 **Figure S15.** Schematic structure of GDE equipment.

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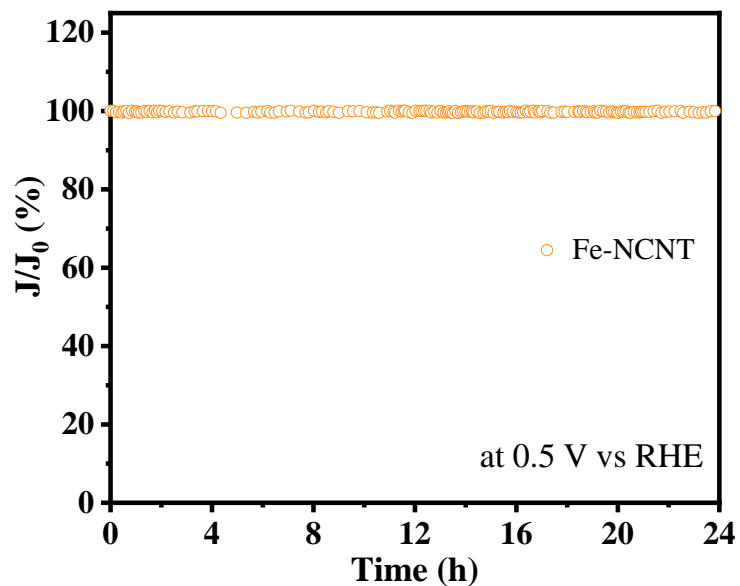


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345 **Figure S16.** Durability test of Fe-NCNT@NiFe-LDH measured at constant potential

346 of 0.5 V vs RHE.

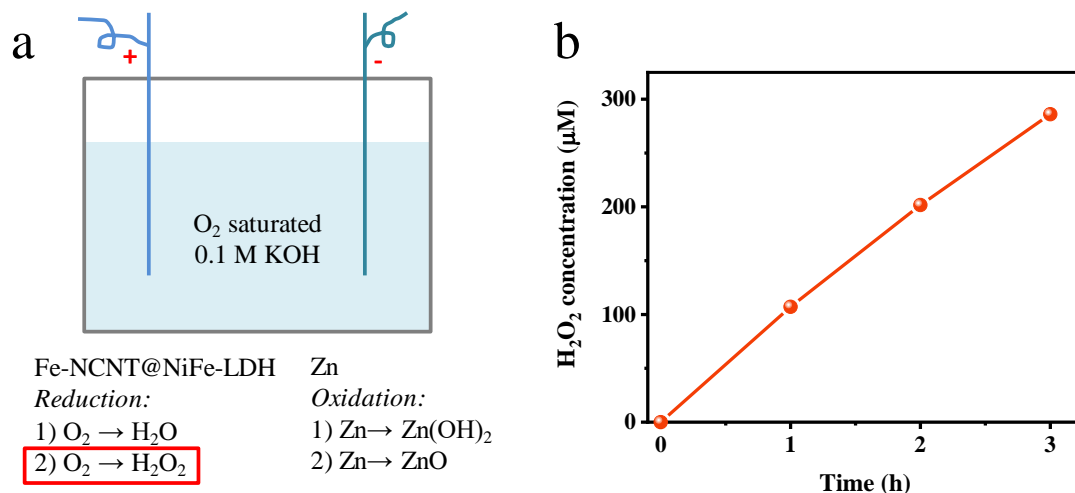
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349 **Figure S17.** Durability test of Fe-NCNT measured at constant potential of 0.5 V vs

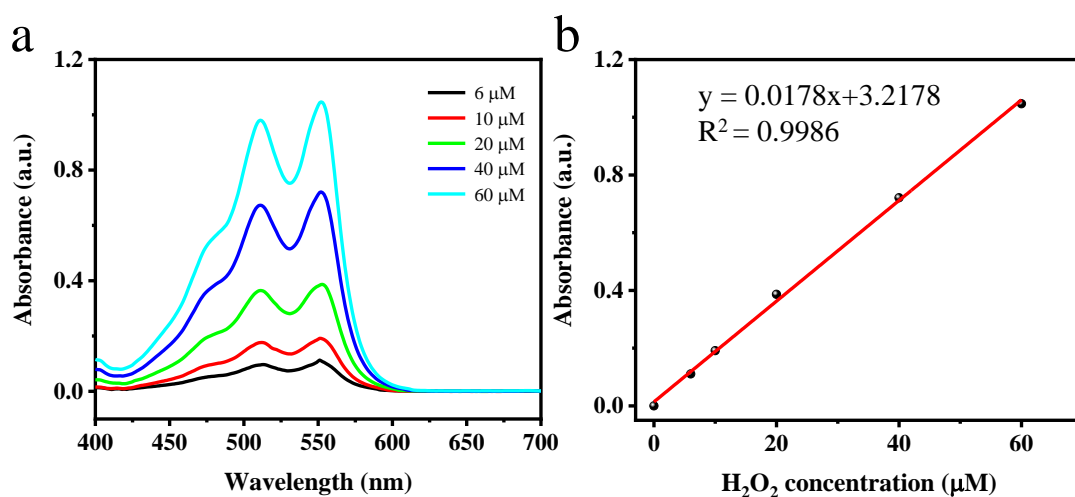
350 RHE.



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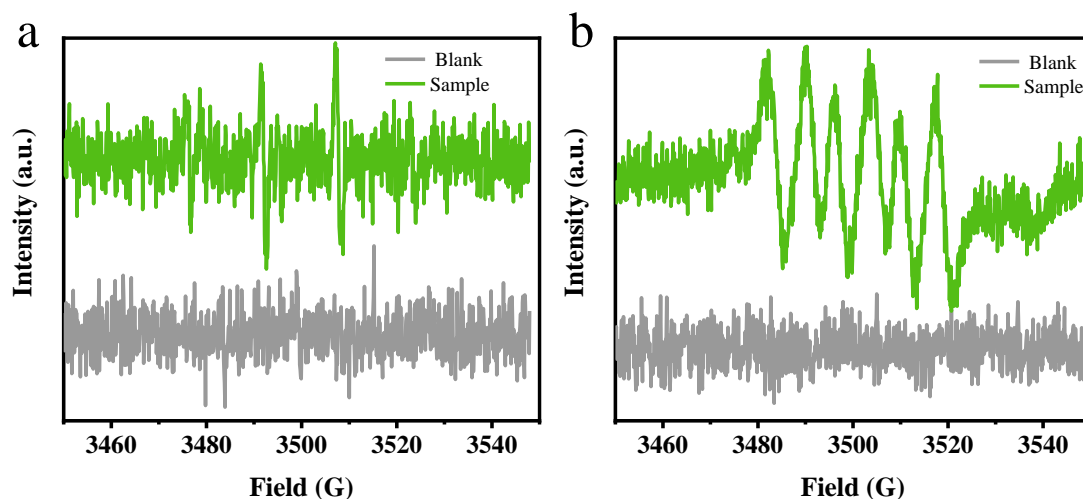
352 **Figure S18.** (a) A simulated Zn-air discharging battery and (b) The H₂O₂ accumulation
 353 along with discharging time. Conditions: The area of CFP/Fe-NCNT@NiFe-LDH is of
 354 2 cm², the area of Zn plate is of 6 cm², the volume of the electrolyte is of 130 mL, and
 355 the discharging current is 10 mA.

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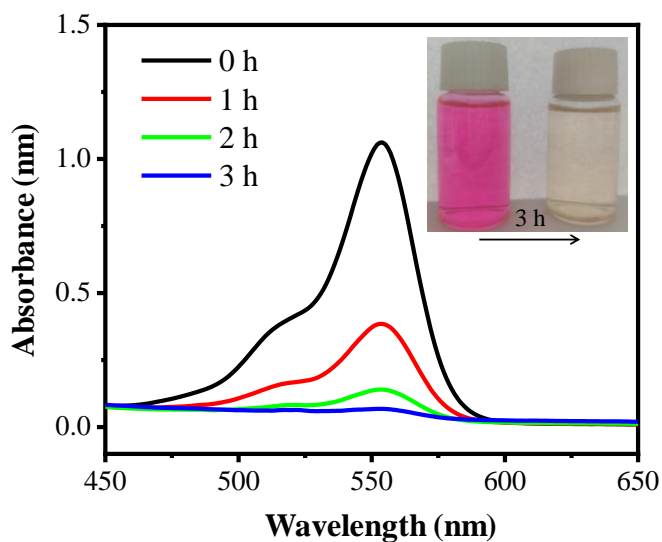
358 **Figure S19 (a)** The absorption spectra of H₂O₂ at different concentrations (6 μM, 10
 359 μM, 20 μM, 40 μM, 60 μM) at wavelengths of 400-700 nm; (b) and a standard curve
 360 of H₂O₂ concentration-absorbance was drawn.



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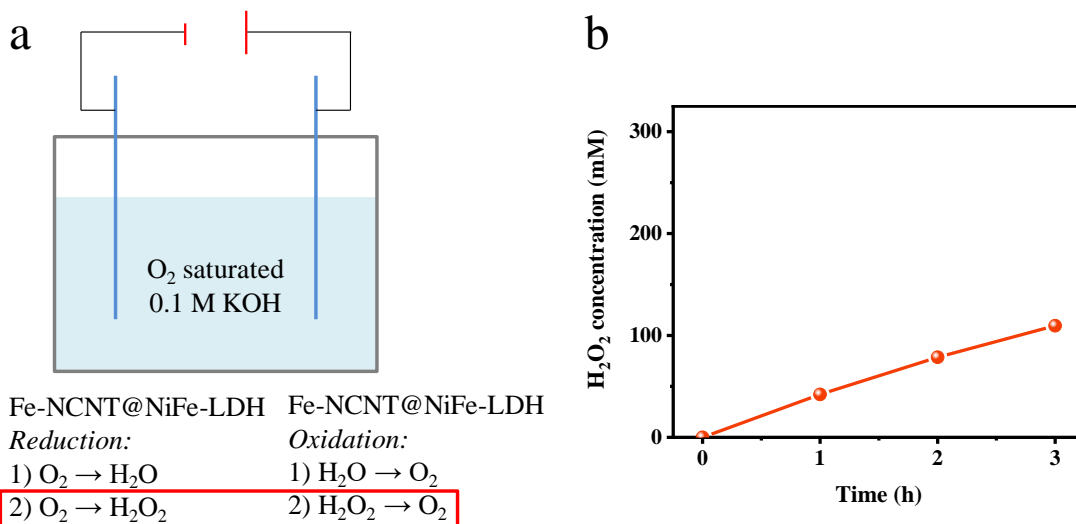
362 **Figure S20.** (a) ESR spectrum of DMPO-•OH and (b) DMPO-•OOH of the sample
 363 solution composed of 0.1 M KOH aqueous solution with 0.03 mM FeSO₄ and 10 mM
 364 H₂O₂, and blank contrast composed of 0.1 M KOH aqueous solution with 10 mM H₂O₂
 365 (non Fe species added). The signals were collected after the radical trap (5,5-dimethyl-
 366 1-pyrroline-N-oxide, DMPO) added for 30 min.

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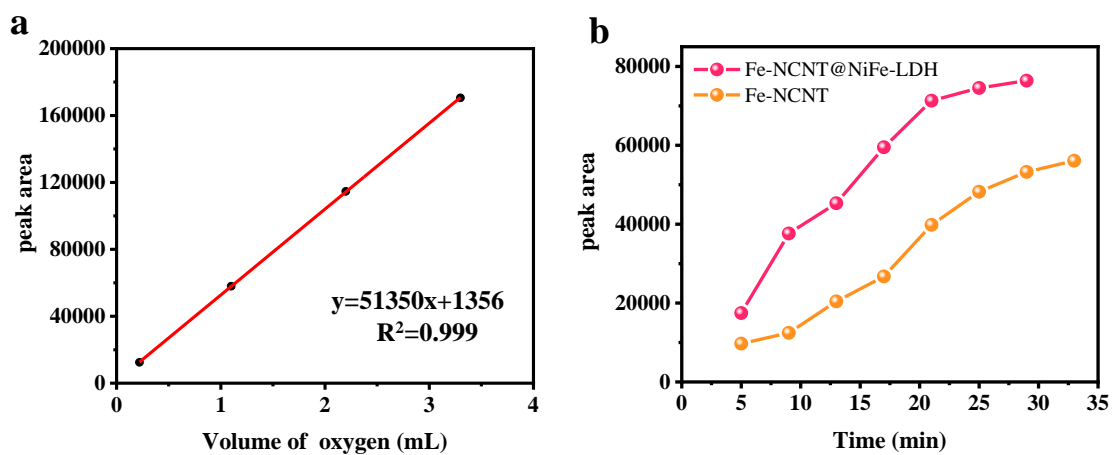
369 **Figure S21.** The degradation of Rhodamine B (RhB) via Fenton-like reactions. The
 370 primary solution is composed of 0.1 M KOH aqueous solution with 0.03 mM FeSO₄,
 371 10 mM H₂O₂ and 10 mg/L RhB.



372

373 **Figure S22.** (a) A designed cell for simulating H₂O₂ generation in ORR and
 374 electrochemical consumption in POR. (b) The H₂O₂ concentration varied along with
 375 time. Conditions: The area of two electrodes (CFP/Fe-NCNT@NiFe-LDH) are of 2 cm²,
 376 the volume of the electrolyte is of 130 mL, and the discharging current is 10 mA.

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379 **Figure S23.** (a) Gas phase standard curve of oxygen, measured by gas chromatograph.

380 (b) Oxygen peak area at different times of Fe-NCNT@NiFe-LDH and Fe-NCNT.

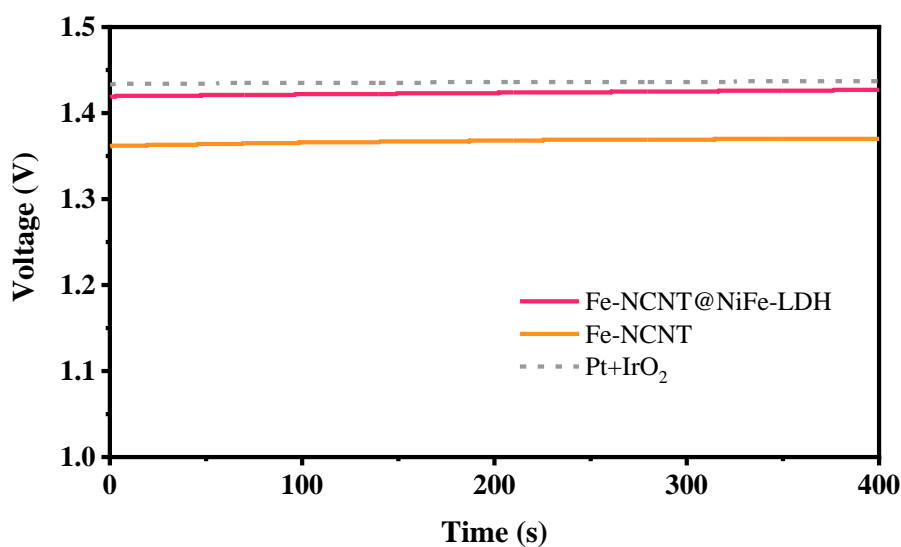
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384 **Notes: Movies S3** (The isproportionation of H_2O_2 in NiFe-LDH contained H_2O_2 -DI
385 water system), **S4** (The isproportionation of H_2O_2 in Fe-NCNT contained H_2O_2 -DI
386 water system), **S5** (The isproportionation of H_2O_2 in Fe-NCNT@NiFe-LDH contained
387 H_2O_2 -DI water system), and **S6** (The isproportionation of H_2O_2 in Fe-NCNT@NiFe-
388 LDH contained H_2O_2 -1 M KOH-DI water system) are separately uploaded as MP4 files.

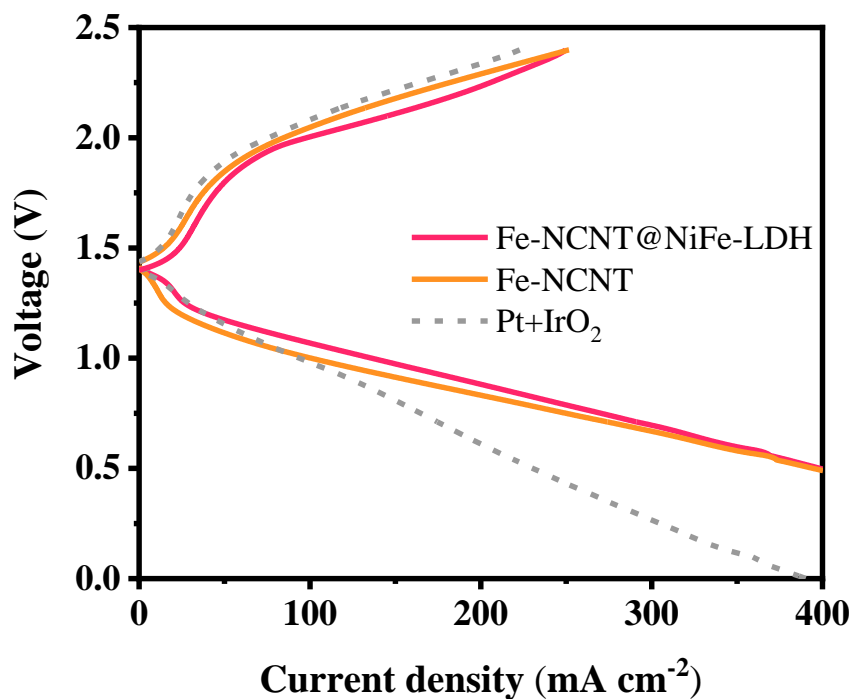
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391 **Figure S24.** Open circuit curves of Fe-NCNT@NiFe-LDH, Fe-NCNT, and Pt+IrO₂
392 respectively assembled ZABs.

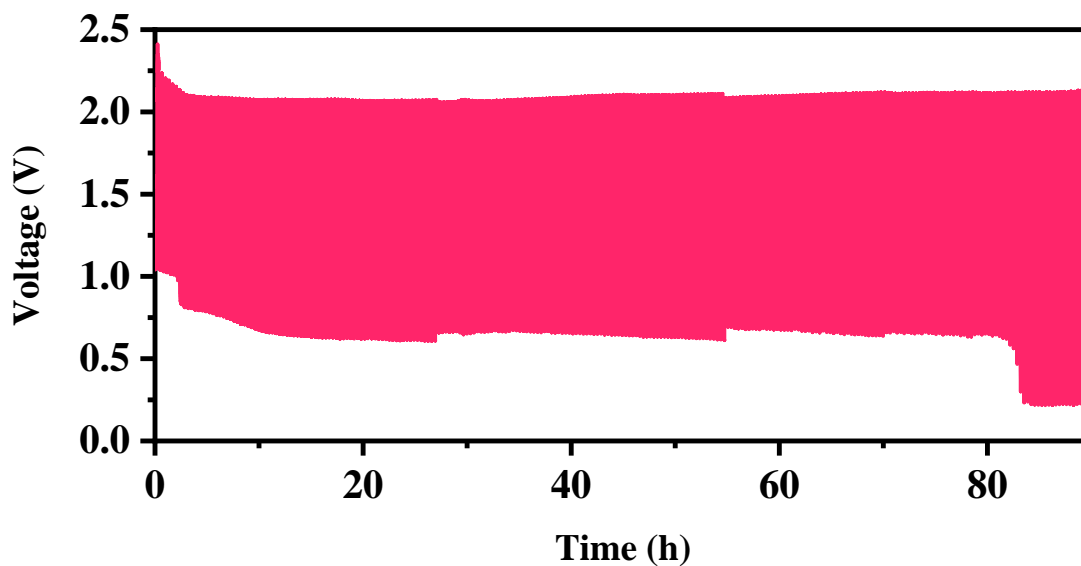
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395 **Figure S25.** Discharge-charge polarization curves of Fe-NCNT@NiFe-LDH, Fe-
 396 NCNT, and Pt+IrO₂ respectively assembled ZABs.

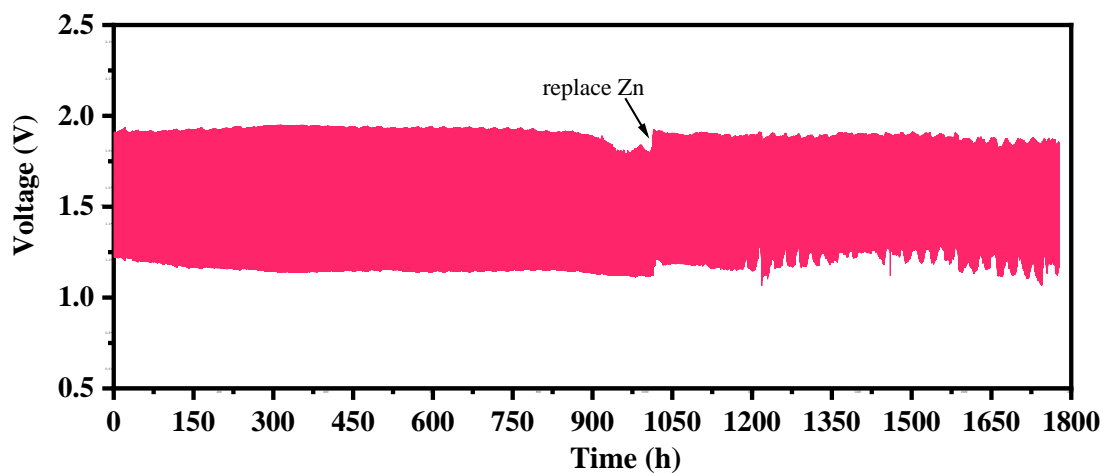
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399 **Figure S26.** Charge/discharge cycle test at 100 mA cm⁻² current density for Fe-
 400 NCNT@NiFe-LDH based ZAB.

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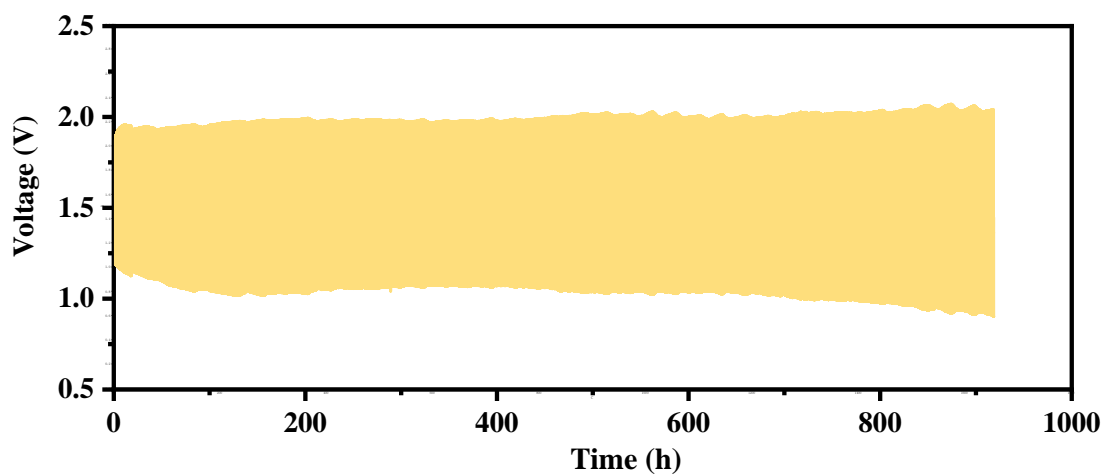


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403 **Figure S27.** Charge/discharge cycle test at 10 mA cm^{-2} current density for Fe-

404 NCNT@NiFe-LDH based ZAB.

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407 **Figure S28.** Charge/discharge cycle test at 10 mA cm^{-2} current density for Fe-NCNT

408 based ZAB.

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414 **Tables**

415 **Table S1.** Comparison of OER performance of Fe-NCNT@NiFe-LDH with recently
 416 reported electrocatalysts.¹⁴⁻²⁵

Sample	OER			References
	$E_{j=10}$ (V)	$E_{j=100}$ (V)	Tafel slope (mV dec ⁻¹)	
Fe-NCNT@NiFe-LDH	1.41	1.46	37	This work
FeCoSn(OH) ₆ -300	1.50	1.55	39	14
Ni ₈₃ Fe ₁₇ -ONCAs	1.42	1.46	48	15
(Fe,Co)OOH/MI	1.46	1.52	53	16
CF-FeSO	1.42	1.46	40	17
Br-Ni-MOF (A)	1.54	1.71	79	18
W-NiS _{0.5} Se _{0.5}	1.40	1.47	41	19
a-LNFBPO	1.44	1.52	37	20
OLC-Co-N-C	1.57	1.66	58	21
Ir/CoNiB	1.41	1.47	35	22
ENWs-FeNi-C ₂ O ₄	1.44	1.5	54	23
Co ₃ O ₄ -Mo ₂ N NFs	1.45	1.62	88	24
F-Ni ₂₇ Fe ₁₀ LDH	1.46	1.48	29.7	25

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422 **Table S2.** OER and ORR electrochemical performances of Fe-NCNT@NiFe-LDH,
 423 Fe-NCNT, and NiFe-LDH in 1 M KOH.

Sample	OER		Tafel slope (mV dec ⁻¹)	ORR	ΔE
	η_{10} (mV)	η_{100} (mV)		$E_{1/2}$ (V)	$E_{j=10}-E_{1/2}$ (V)
Fe-NCNT@NiFe-LDH	180	230	37	0.87	0.54
NiFe-LDH	250	300	39	0.78	0.70
Fe-NCNT	230	410	143	0.85	0.61

424

425 **Table S3.** OER and ORR electrochemical performances of Fe-NCNT@NiFe-LDH, Fe-
 426 NCNT, and NiFe-LDH in 0.1 M KOH.

Sample	OER		$E_{1/2}$ (V)	ΔE
	η_{10} (mV)	Tafel slope (mV dec ⁻¹)		$E_{j=10}-E_{1/2}$ (V)
Fe-NCNT@NiFe-LDH	210	49	0.89	0.55
NiFe-LDH	260	57	0.69	0.80
Fe-NCNT	250	185	0.88	0.60

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439 **Table S4** Comparison of overpotential difference ($\Delta E = E_{j=10} - E_{1/2}$) and ZAB (two-
 440 electrode cell) performance of (or based on) Fe-NCNT@NiFe-LDH with recently
 441 reported electrocatalysts.²⁵⁻⁶²

Sample	OER-ORR			ZABs		References
	ΔE (V)	$E_{j=10}$ (V)	$E_{1/2}$ (V)	Power density (mW cm ⁻²)	cycling ability X h / Y cycle @ Z mA cm ⁻²	
Fe-NCNT@NiFe-LDH	0.52	1.41	0.89	204	1743 h / 5229 cycle @ 50 1777 h / 5331 cycle @ 10 80 h / 240 cycle @ 100	This work
FeNC F-Ni ₂₇ Fe ₁₀ LDH Zn(0.2 mm)	0.53	1.43	0.90	259	258 h @ 10	25
CoNC@LDH	0.63	1.47	0.84	173	3600cycle@10 656 cycle@50 29 cycle@100	26
Co SA/NCFs	0.76	1.61	0.85	154	600 h @ 10	27
Fe ₂ Ni ₃ -NFCM	0.69	1.51	0.82	128	10 h @ 10	28
Co-NC@LDH	0.80	1.6	0.8	107	300 h @ 5	29
FeNi@NCSs	0.71	1.55	0.84	128	120 h @ 5	30
Mn-RuO ₂	0.64	1.5	0.86	181	2500 h @ 10 467 h @ 50 300 h @ 100	31
NiFe-LDH/FeSoy- CNSs-A	0.62	1.53	0.91	238	50 h @ 5	32
FeNi/N-LCN	0.72	1.57	0.85	162	1100 h @ 5 600 h @ 10	33
glu-NiFe	0.82	1.67	0.85	127	240 h @ 5	34
NiFe/N-CNT	0.77	1.52	0.75	300	300 cycle @ 5	35

NiFe-ND/FeCo-NC	0.81	1.66	0.85	141	160 h @ 20	36
Fe-Me-Ni	0.70	1.54	0.84	168	102 h @ 10	37
defected-NiFe LDH	0.72	1.47	0.75	35	100 cycle@ 10	38
NiCo ₂ S ₄ @NiFe LDH	0.67	1.50	0.83	--	--	39
DBD-NiFe/NiSe ₂ @NCNT	0.71	1.52	0.81	132	1000 cycle@10	40
NiFe@N-CFs	0.7	1.53	0.83	102	480 h @ 10 330 h @ 20	41
S-Ni ₃ FeN/NSG	0.61	1.49	0.88	207	1200 cycle@10	42
NiFe-Mi-C-Gr	0.68	1.54	0.85	111	100 h @ 10	43
NiFe@C@Co CNFs	0.70	1.57	0.87	130	200 h @ 5	44
NiFe-DG	0.73	1.59	0.86	148	12 h @ 10	45
NiFe@NCNT	0.77	1.56	0.79	360	200 h @ 10	46
NiFe LDH@Fe-N-CNFs	0.86	1.58	0.72	158	185 h @ 10	47
LDH@N-CoOx@C	0.66	1.50	0.84	156	150 h @ 5	48
ZGNiFe@NG	0.84	1.65	0.81	140	120 h @ 5	49
NiFe ₃ @NGHSNCNTs	0.79	1.61	0.82	126	1000 cycle@10	50
FeCo-NPCNs	0.6	1.47	0.87	161	400 cycle@10	51
Co ₉ S ₈ @Co/Mn-S,N-PC	0.7	1.55	0.85	80	210 h @ 10	52
FeN _x /NC-S	0.63	1.55	0.92	194	65 h @ 10	53
Co@NrC-0.3	0.76	1.61	0.85	168	40 h @ 2	54
Co@N-HPC-800	0.87	1.69	0.82	89	25 h @ 5	55
Co@CoFe _{0.01} -N-C	0.81	1.65	0.84	174	100 h @ 1	56
BN-PCN	0.87	1.71	0.84	194	1000 h @ 5	57

o-CoSe ₂ /AK	0.77	1.61	0.84	122	90 h @ 5	58
NG/Ni	0.63	1.49	0.86	165	2500 h @ 2	59
CoWCP-NPC-2:1	0.63	1.43	0.80	205	83.5 h / 501 cycle @ 10	60
CoS/Co/MoC-N,S- PCNFs	0.65	1.52	0.87	169	50 h @ 2	61
Ti ₃ C ₂ @SrTiO ₃	0.65	1.43	0.78	122	500 h@10	62

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443 The ΔE values of catalysts containing NiFe nanosheets are concentrated in the range
444 of 0.6–0.75 V, such as NiFe-LDH/FeSoy-CNSs-A³² with a ΔE of 0.62 V ($E_{1/2}$ of 0.91
445 V and $E_{j=10}$ of 1.53 V), CoNC@LDH²⁶ with a ΔE of 0.63 V ($E_{1/2}$ of 0.84 V and $E_{j=10}$ of
446 1.47 V), NiCo₂S₄@NiFe-LDH³⁹ with ΔE of 0.63 V ($E_{1/2}$ of 0.83 V and $E_{j=10}$ of 1.497
447 V), and LDH@N-CoOx@C⁴⁸ with ΔE of 0.665 V ($E_{1/2}$ of 0.83 V and $E_{j=10}$ of 1.503 V).
448 The ΔE of catalysts containing NiFe nanoparticles are principally concentrated in the
449 scope of 0.7–0.85 V, such as Fe–Me–Ni³⁷ with ΔE of 0.702 V ($E_{1/2}$ of 0.841 V and $E_{j=10}$
450 of 1.543 V), NiFe@C@Co-CNFs⁴⁴ with ΔE of 0.7 V ($E_{1/2}$ of 0.87 V and $E_{j=10}$ of 1.57
451 V), NiFe@NCNTs⁴⁶ with ΔE of 0.77 V ($E_{1/2}$ of 0.79 V and $E_{j=10}$ of 1.56 V), and
452 ZGNiFe@NG⁴⁹ with ΔE of 0.84 V ($E_{1/2}$ of 0.81 V and $E_{j=10}$ of 1.65 V).

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