

Supplementary Information

Fabrication of Highly Efficient Encapsulated SnO₂@Alginate Beads as Regenerative Nanosorbents for Anionic Dye Pollutants Removal from Aqueous Solution

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Video S1: Video demonstrating the adsorption of CR by SnO₂ NPs. Within 1 min of contact time rapid adsorption results in change in color from light red to nearly grayish white color.

Video S2: Video demonstrating the adsorption of CR by 0.5% SnO₂@SA beads. Within the first min of contact, rapid adsorption results in change in color from light red to nearly transparent solution.

S1: Adsorption Efficiency

The removal efficiency (η) has been calculated using Equation (S1), where C_0 and C_t are concentrations at $t=0$ and at time t , respectively^{1,2}.

$$\eta = \frac{C_0 - C_t}{C_0} \times 100 \quad \text{Equation S1}$$

S2: Adsorption Kinetics

The PFO³ kinetic model is expressed as:

$$\ln(q_e - q_t) = \ln(q_e) - k_1 t, \quad \text{Equation S2}$$

where k_1 (min^{-1}) refers to the equilibrium rate constant; q_e (mg/g) and q_t (mg/g) indicate the amount of dye adsorbed at equilibrium and time t , respectively. The slope and intercept obtained from the plot of $\ln(q_e - q_t)$ versus t were used to determine the values of k_1 and q_e , respectively.

Contrastingly, the pseudo-second-order (PSO)⁴ kinetic model follows the equation:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \left(\frac{1}{q_e}\right)t, \quad \text{Equation S3}$$

where k_2 ($\text{g mg}^{-1} \text{min}^{-1}$) refers to the PSO rate constant. The plot of $\frac{t}{q_t}$ versus t is used to determine the values of k_2 and q_e .

Additional investigations to determine the probabilities of IPD resistance affecting the adsorption of CR on SnO_2 were carried out by using IPD^{5,6} model, which follows:

$$q_t = k_p t^{1/2} + C, \quad \text{Equation S4}$$

where k_p ($\text{mg g}^{-1} \text{min}^{-1/2}$) is the IPD rate constant and C (mg/g) is the intercept. The slope from the linear plot of q_t versus $t^{1/2}$, is used to determine the values of k_p and q_e .

S3. Adsorption Isotherms

The Langmuir isotherm predicts that monolayer adsorption originates at binding sites with homogeneous energy levels, independent of interactions between adsorbed molecules and the transfer of adsorbed molecule onto the adsorption surface⁷. The Langmuir equation can be expressed as:

$$\frac{C_e}{q_e} = \frac{1}{k_1 q_m} + \frac{1}{q_m} C_e, \quad \text{Equation S5}$$

where q_e , C_e , k_1 , q_m are adsorption capacity at equilibrium (mg/g), equilibrium concentration (mg/L), constant related to free energy of adsorption (L/mg) and maximum adsorption capacity at monolayer coverage (mg/g), respectively.

The favorability of the adsorption isotherm was further determined by evaluating the dimensionless separation factor (R_L), using the equation^{7,8}

$$R_L = \frac{1}{1 + k_1 C_0}, \quad \text{Equation S6}$$

The Freundlich isotherm holds true for non-ideal sorption on heterogeneous surfaces as well as multilayer sorption⁹. It is represented as:

$$\ln q_e = \ln k_f - \frac{1}{n} \ln C_e, \quad \text{Equation S7}$$

where k_f and n are the Freundlich constants of the system. The reaction is favorable when $0 < 1/n < 1$, but reaction is unfavorable if $n > 1$.

Temkin isotherm is generally used for heterogeneous systems or non-uniform distribution of sorption heat¹⁰. It is represented as

$$q_e = \frac{RT}{b} \ln K_t + \frac{RT}{b} \ln C_e, \quad \text{Equation S7}$$

where K_t is the equilibrium binding constant, b is related to the adsorption heat, R is universal gas constant and T is temperature.

S4: Calculation for Sn concentration in treated water

Molecular weight of $\text{SnO}_2 = 151$ g and atomic weight of $\text{Sn} = 118$ g

151 g of SnO_2 has 118 g of Sn, then 0.5 g of SnO_2 contains, $\frac{0.5 \times 118}{151} = 0.3940 \text{ g} = 394 \text{ mg}$

394 mg of Sn is used to prepare $\text{SnO}_2@SA$ beads, which are added to 100 mL of CR dye aqueous solution. So, 394mg/100 mL or 3940 mg/L of Sn (encapsulated within beads) is used to treat CR dye aqueous solution.

Detected Sn levels in treated water = 7.729 ppb or 0.007729 mg/L.

Thus, percentage of Sn present in CR after treatment = $\frac{0.007729}{3940} \times 100 = 0.0002 \%$

Table S1 Adsorption isotherm parameters obtained using Langmuir, Freundlich and Temkin model

Langmuir Model

q_m (mg/g)	961.54
R²	0.9998
k_L	8.8135
R_L	0.000113

Freundlich Model

R²	0.9177
1/n	0.0083
k_f	20.025

Temkin Model

R²	0.9178
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Fig. S1. Moving anti-clockwise, 1,2,3 and 4 depicts synthesized SnO_2 NPs, 0.1 g SnO_2 NPs after adsorption of CR dye, completely dried 0.5% $\text{SnO}_2@SA$ beads and completely dried 0.5 % $\text{SnO}_2@SA$ beads after adsorption, respectively.

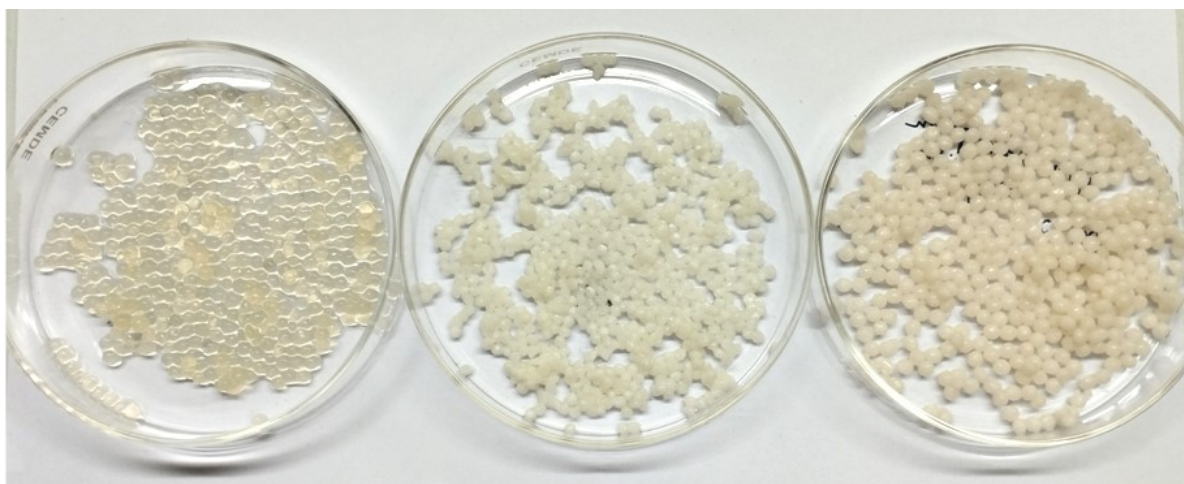


Fig. S2. From L to R, pure SA beads, 0.2% $\text{SnO}_2@SA$ beads and 0.2% $\text{SnO}_2@SA$ beads after adsorption of CR dye

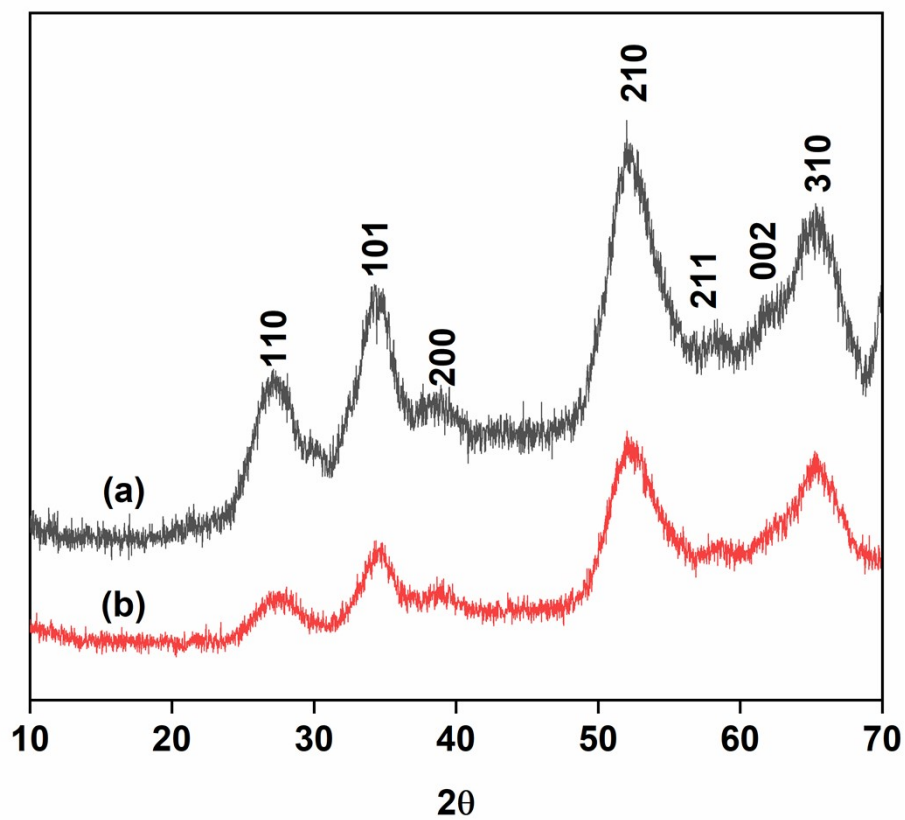


Fig. S3. XRD obtained for SnO₂@SA beads (a) before and (b) after adsorption of 5 μ M CR from its aqueous solution.

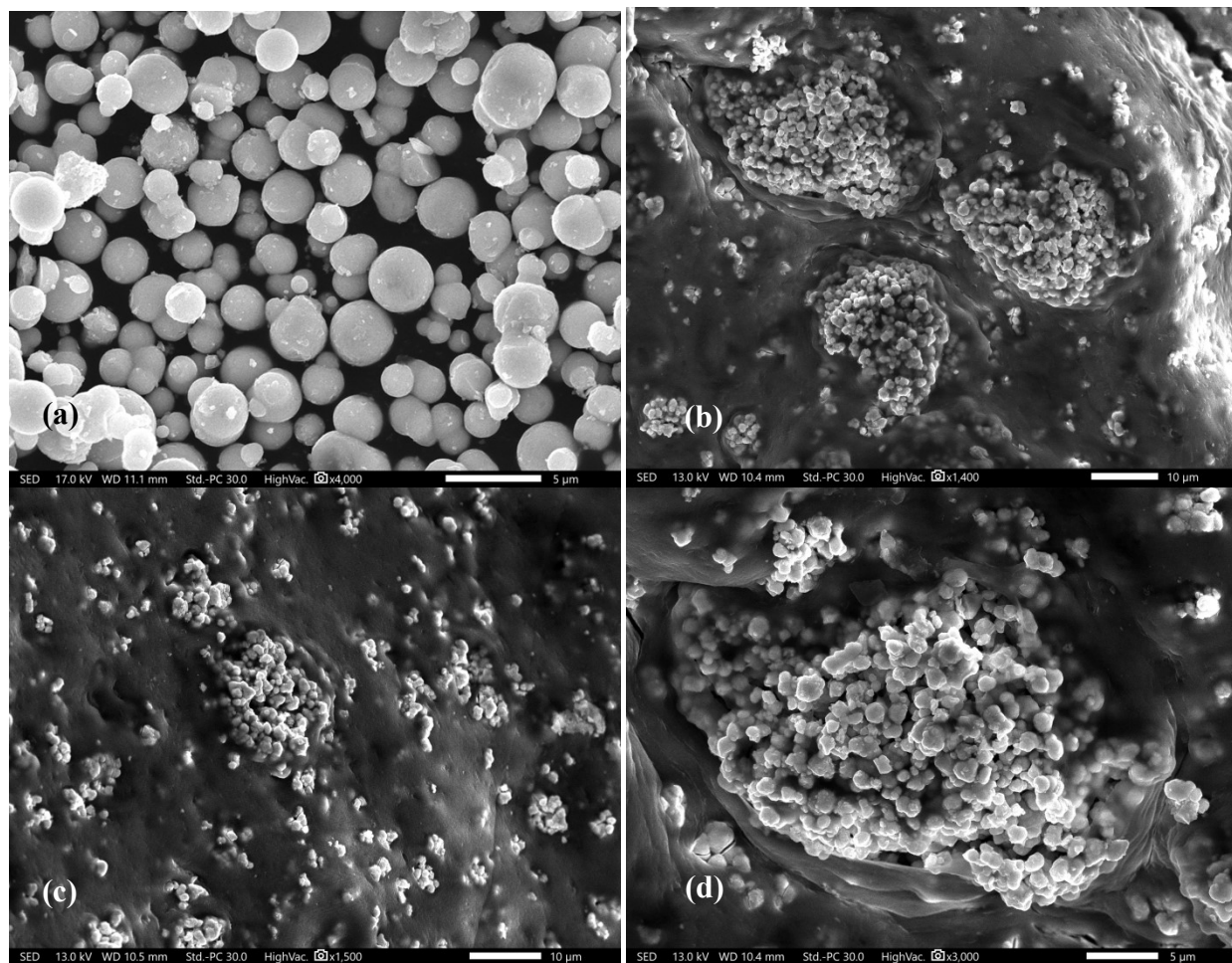
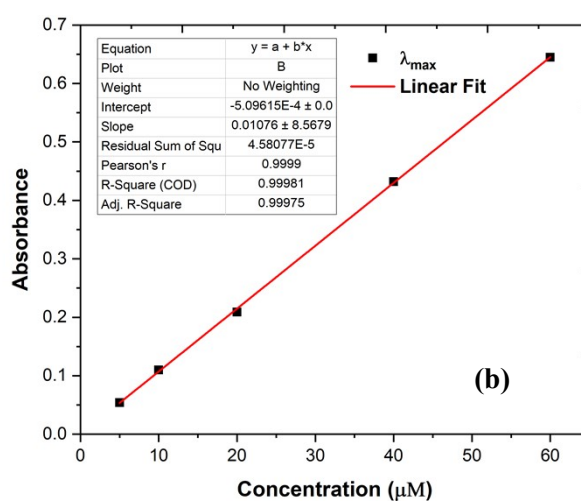
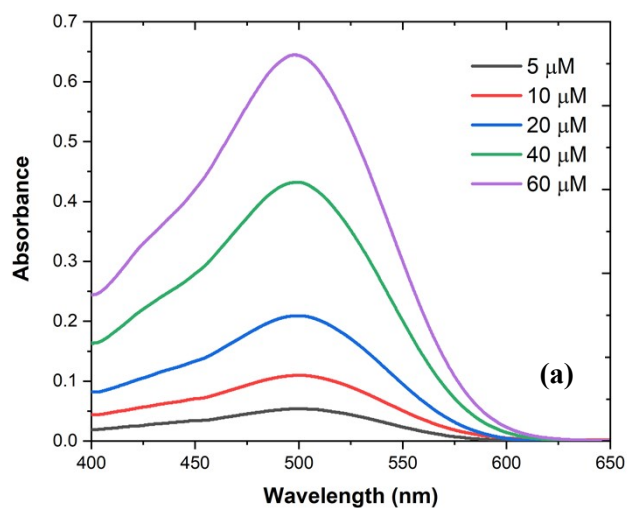


Fig. S4. SEM images of (a) various sizes of spherically shaped SnO₂ NPs; (b), (c) and (d) 0.2% SnO₂@SA beads at various magnifications



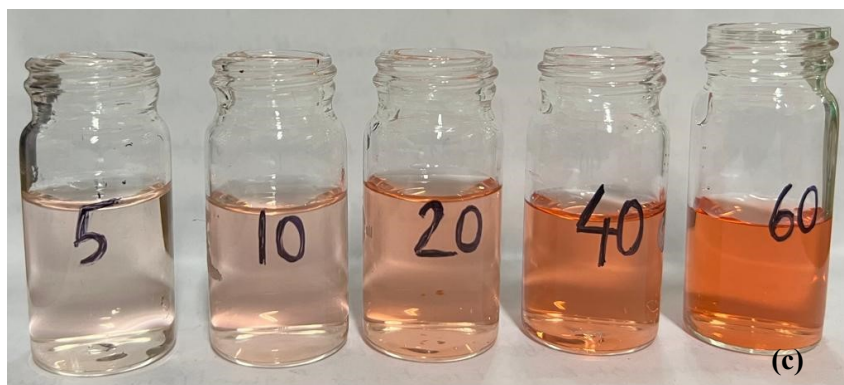


Fig. S5. (a) UV-Vis plot for different concentrations of CR dye (5- 60 μM); (b) Linear fit analysis and (c) Image of the various CR concentrations used in this study

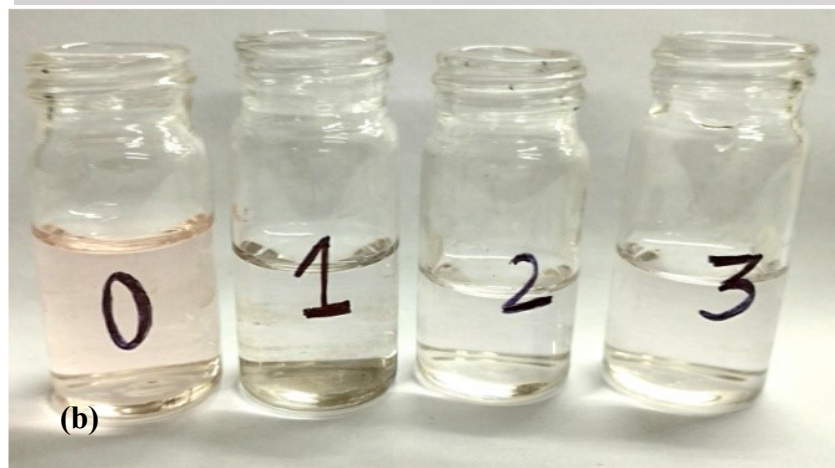
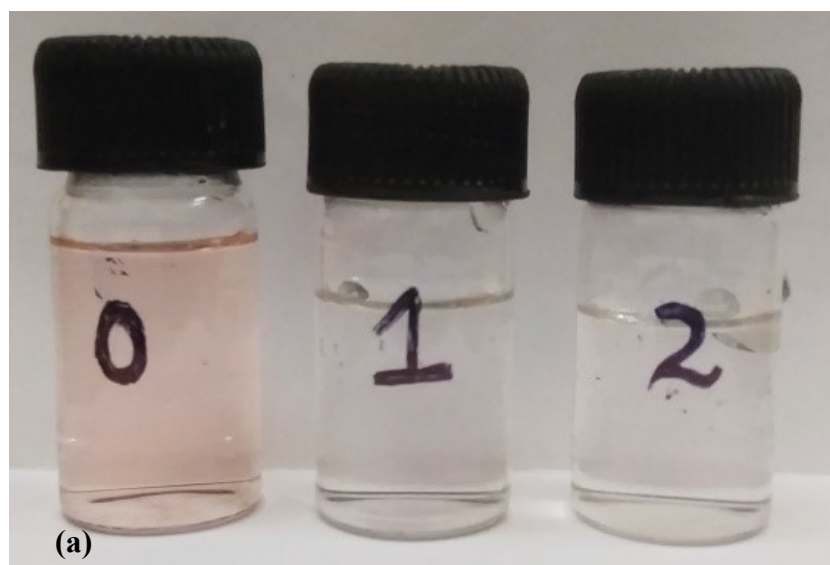


Fig. S6. Adsorption of 5 μM CR dye using (a) powdered 0.1 g SnO_2 NPs and (b) 0.5% $\text{SnO}_2@SA$ beads



Fig. S7. 0.1% $\text{SnO}_2@SA$ beads before and after 10 min adsorption

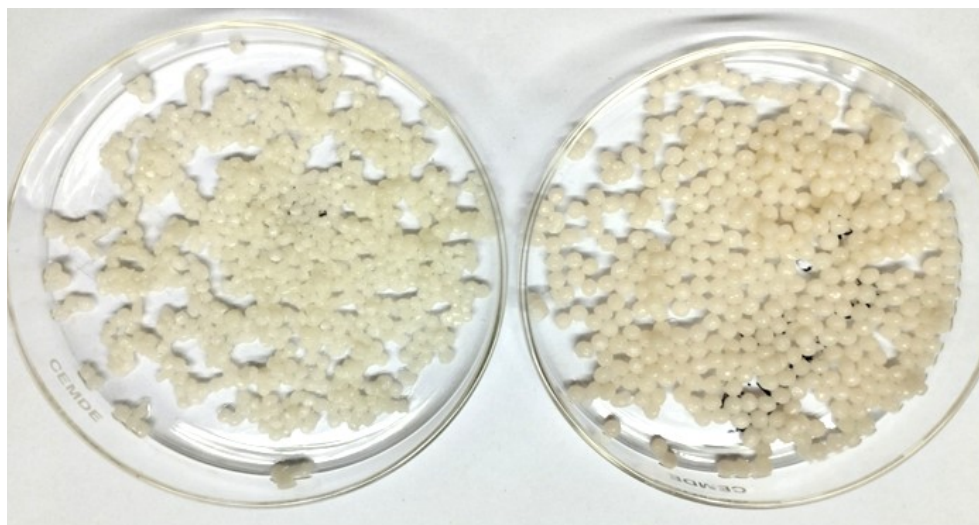


Fig. S8. 0.2% $\text{SnO}_2@SA$ beads before and after 10 min adsorption

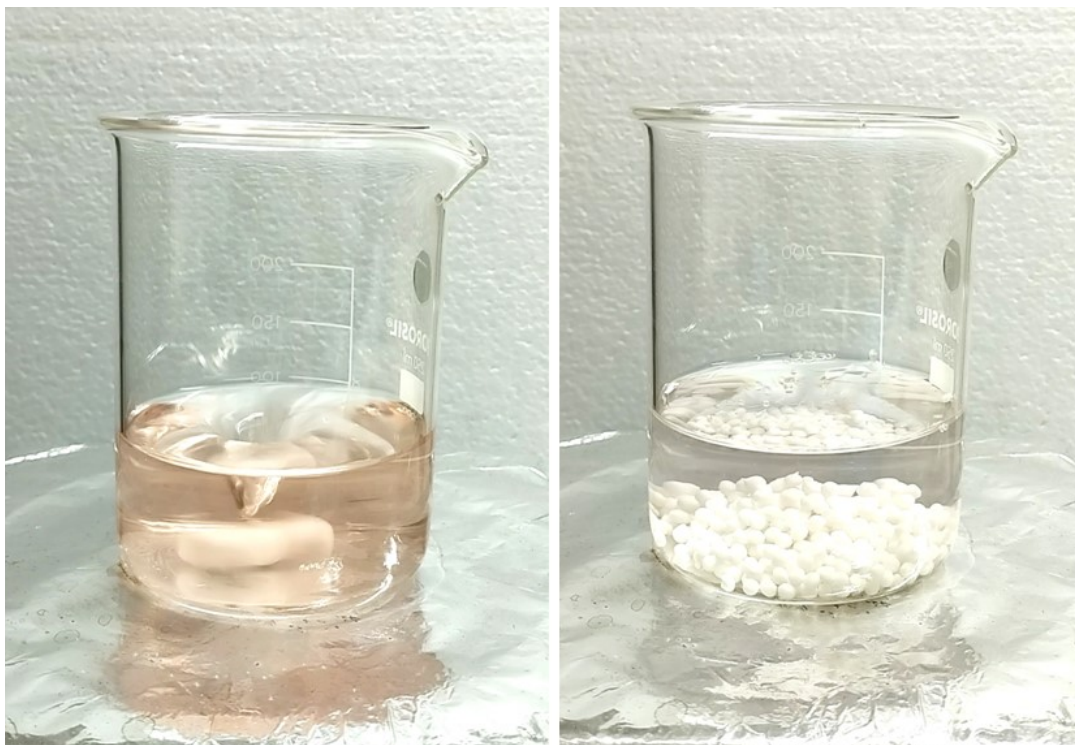


Fig. S9. Adsorption of 5 μM CR using 0.5% SnO_2/SA beads within 2 min



Fig. S10. MeOH used as an eluent for regenerative studies pale red color observed after being in contact with 0.2% SnO₂@SA beads for 2 min with continuous stirring

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