

## Supplementary Information

### Improved methane dehydroaromatization reaction over Mo and Cr co-doped ZSM-5 catalyst

Koji Miyake,<sup>\*a,b</sup> Tomoka Sumi,<sup>a</sup> Shinya Kokuryo,<sup>a</sup> Haruna Kitamura,<sup>a</sup> Jose A. Hernandez  
Gaitan,<sup>a</sup> Yoshiaki Uchida<sup>a</sup> and Norikazu Nishiyama<sup>a,b</sup>

*<sup>a</sup>Division of Chemical Engineering, Graduate School of Engineering Science, Osaka University, 1-3  
Machikaneyama, Toyonaka, Osaka 560-8531, Japan*

*<sup>b</sup>Innovative Catalysis Science Division, Institute for Open and Transdisciplinary Research Initiatives (ICS-OTRI),  
Osaka University, Suita, Osaka 565-0871, Japan  
E-mail: [kojimiya@cheng.es.osaka-u.ac.jp](mailto:kojimiya@cheng.es.osaka-u.ac.jp)*

### Contents

<b>1. Experimental part</b> .....	<b>2-3</b>
<b>2. Supplementary tables and figures</b> .....	<b>4-10</b>

# 1. Experimental Part

## 1.1 Catalyst preparation

Ammonium Molybdate Tetrahydrate (Wako FUJIFILM), Chromium(III) Acetate (Wako FUJIFILM) and H<sup>+</sup> type ZSM-5 zeolite (822HOA, TOSOH Co.) were used without further purification. An incipient wetness impregnation was applied to load Mo or Cr on ZSM-5. First, ZSM-5 was mixed with an aqueous solution containing Mo or Cr. Afterward, the sample was dried at 363 K and calcined under air at 823 K for 5 h. The samples were denoted as “Mo/ZSM-5” and “Cr(x)/ZSM-5”, where x means the weight ratio of Cr [wt%]. Second, Mo was introduced to “Cr(x)/ZSM-5” by an incipient wetness impregnation similarly. Those samples were named “Mo/Cr(x)/ZSM-5”. As a comparison, we loaded 1 wt % of Cr on Mo/ZSM-5. The sample was denoted “Cr/Mo/ZSM-5”

## 1.2 Characterization

The crystal structures of all products were determined by X-ray diffraction (XRD) patterns recorded on a PANalytical X'Pert-MPD diffractometer using Cu-K $\alpha$  radiation. The morphology of samples was observed by transmission electron microscopy (TEM) observation. The energy dispersive X-ray spectroscopy (EDX) for the determination of Cr contents was performed on JEOL JCM-7000. To obtain physical information of samples, N<sub>2</sub> adsorption measurements at 77 K were conducted using BELSORP-Max (MicrotracBel). Diffuse reflectance ultraviolet-visible (UV-vis) spectra of the samples were analyzed on a JASCO V-770 spectrophotometer. NH<sub>3</sub> temperature programmed deposition (NH<sub>3</sub>-TPD) measurements were carried out to evaluate the acidity

## 1.3 Methane dehydroaromatization (MDA) reaction tests

MDA reactions over zeolite catalysts were carried out in a fixed bed reactor at atmospheric pressure referring to our previous work. The catalyst (0.05 g) was loaded into a quartz tube (i.d. 4 mm) and then the temperature was raised to 973 K under He flow. The feed gas of 66.5 vol% ethane and balanced He was fed at a total flow rate of 7.5 cm<sup>3</sup>/min. The product stream was analyzed online with Shimadzu GC-2025 gas chromatographs equipped with a flame ionization detector. GS ALUMINA was used as a GC column. Methane conversion [%] and product yields [%] were calculated as follows:

$$\text{Methane conversion [\%]} = 100 \times \frac{(C - \text{mol of methane at the inlet}) - (C - \text{mol of methane at the outlet})}{(C - \text{mol of methane at the inlet})}$$

$$(\text{Product yields [\%]}) = 100 \times \frac{(C - \text{mol of product at the outlet})}{(C - \text{mol of methane at the inlet})}$$

The amount of coke deposition on the spent catalysts was measured by Thermo Gravimetry Analyzer (TGA). The weight losses from 573 to 1073 K were assigned to the combustion of the deposited coke.

## 2. Supplementary tables and figures

Table S1 Si/Al, Si/Mo and Si/Cr ratios determined by EDX analysis

	Si/Al	Si/Mo	Si/Cr
ZSM-5	9.94	-	-
Cr0.5/ZSM-5	10.37	-	164.44
Cr1.0/ZSM-5	11.19	-	89.83
Cr3.0/ZSM-5	10.53	-	38.84
Mo/ZSM-5	9.94	5.34	-
Mo/Cr0.5/ZSM-5	10.18	6.54	199.62
Mo/Cr1.0/ZSM-5	9.87	7.17	127.34
Mo/Cr3.0/ZSM-5	9.43	6.53	47.20

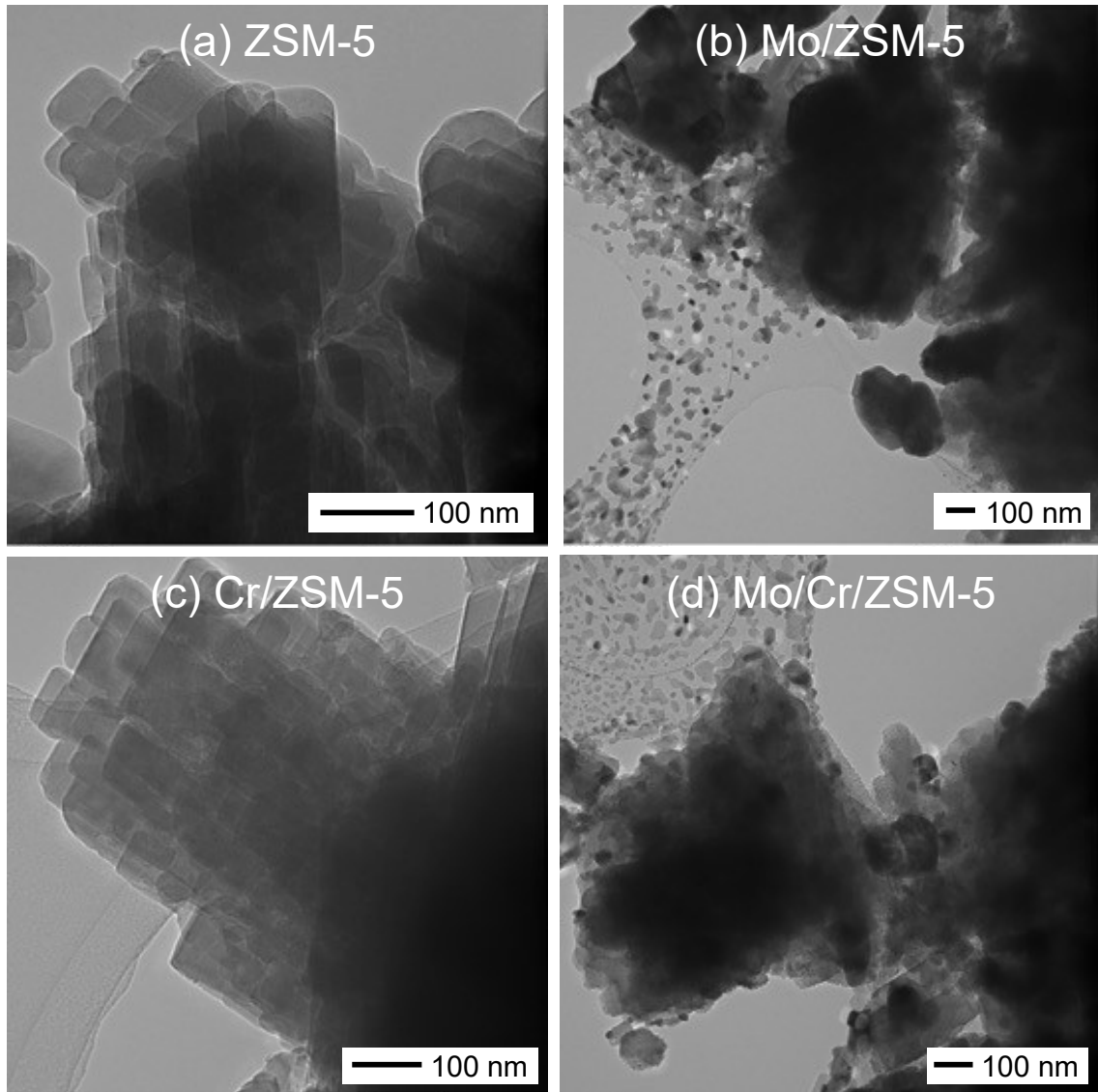


Fig. S1 (a) ZSM-5, (b) Mo/ZSM-5, (c) Cr/ZSM-5 and (d) Mo/Cr/ZSM-5.

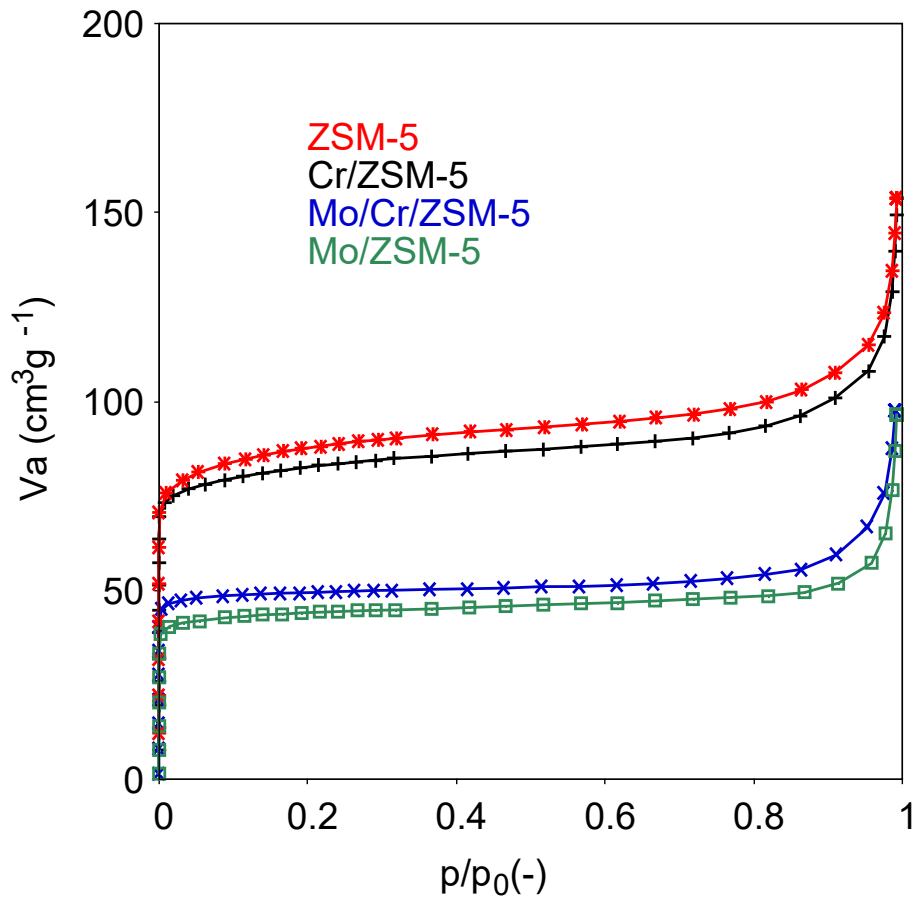


Fig. S2 N<sub>2</sub> adsorption isotherms of ZSM-5, Cr/ZSM-5, Mo/Cr/ZSM-5 and Mo/ZSM-5.

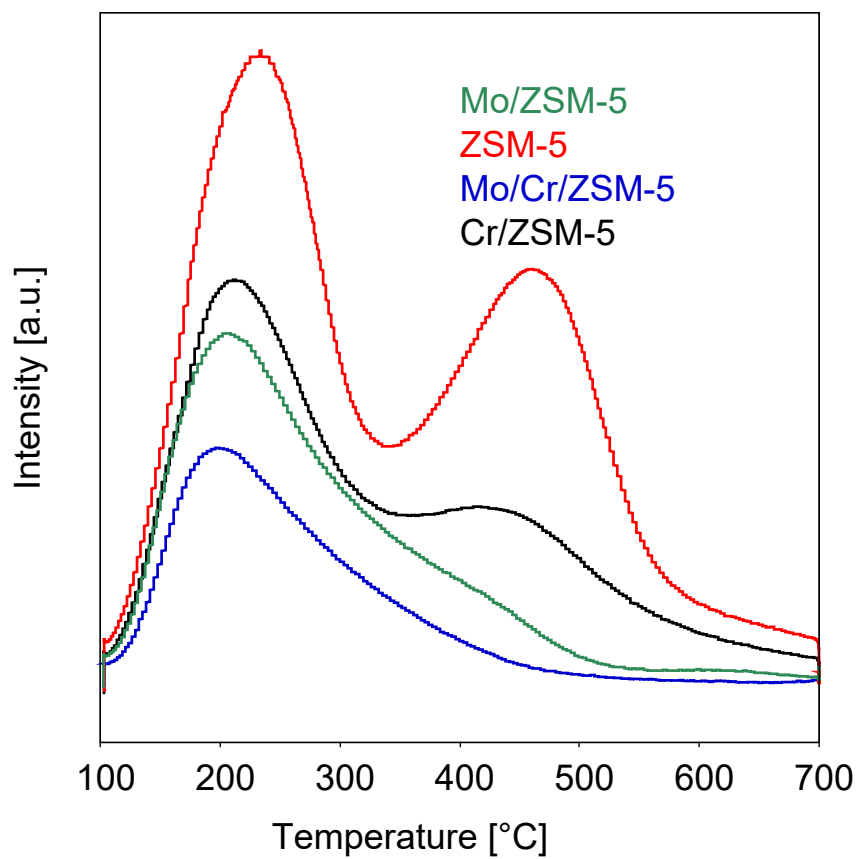


Fig. S3 NH<sub>3</sub>-TPD profiles of ZSM-5, Cr/ZSM-5, Mo/Cr/ZSM-5 and Mo/ZSM-5.

Table S2 Conversion and yields during MDA reaction over Mo/ZSM-5.

Time on stream [min]	Methane Conversion [C-mol%]	Yield [C-mol%]			
		Ethane	Ethylene	Benzene	Toluene
60	1.19	0.02	0.38	0.81	0
120	1.51	0	0.34	0.52	0
180	1.40	0	0.32	0.37	0
240	1.01	0	0.27	0.27	0
300	0.71	0	0.25	0.25	0

Table S3 Conversion and yields during MDA over Mo/Cr1.0/ZSM-5.

Time on stream [min]	Methane Conversion [C-mol%]	Yield [C-mol%]			
		Ethane	Ethylene	Benzene	Toluene
60	2.43	0.20	0.35	2.66	0.15
120	1.80	0.12	0.46	1.81	0
180	3.47	0.07	0.49	1.31	0
240	2.35	0.06	0.53	1.17	0
300	2.46	0.05	0.54	1.01	0



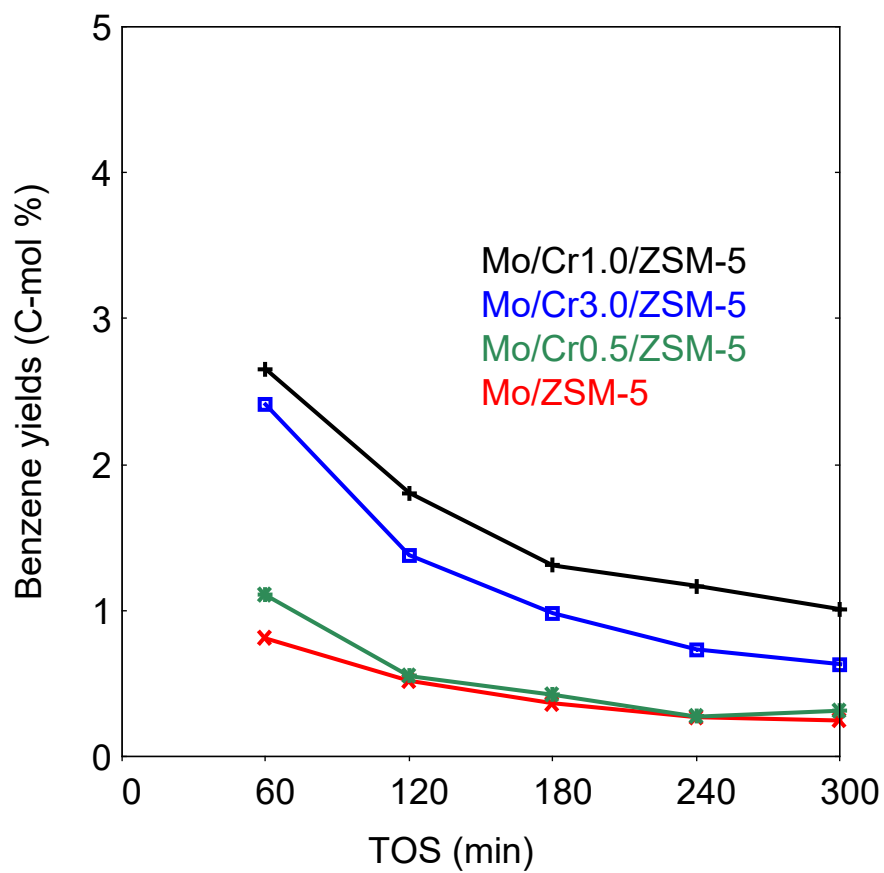


Fig. S4 Time courses of benzene yield over Mo/Cr(x)/ZSM-5 and Mo/ZSM-5.

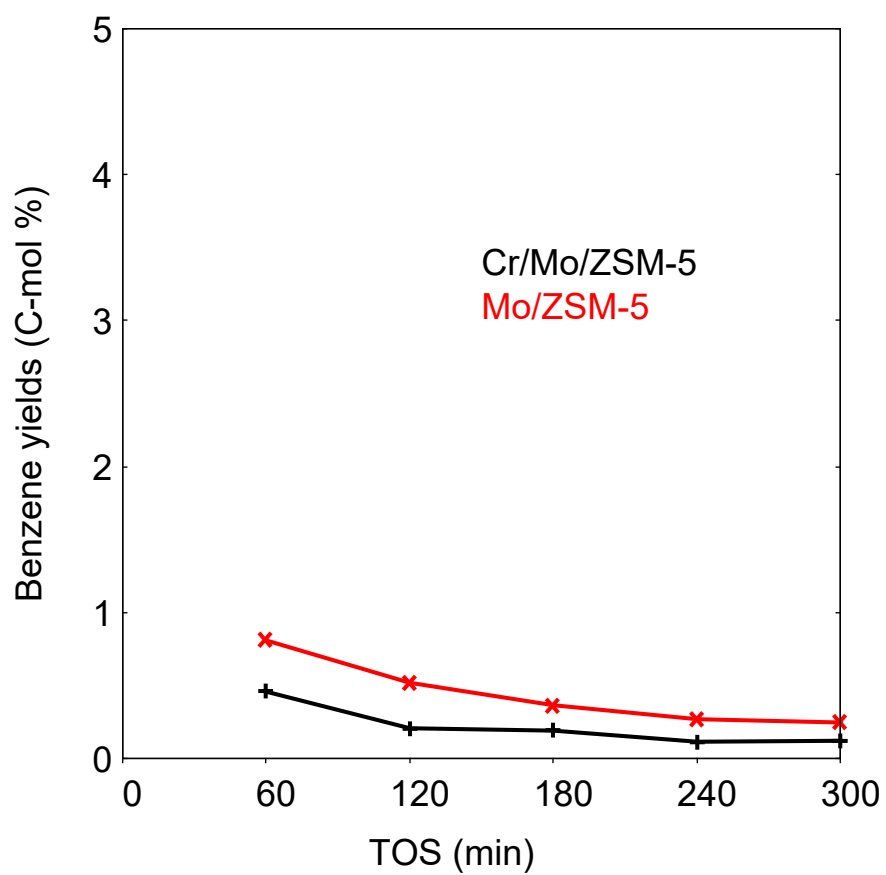


Fig. S5 Time courses of benzene yield over Cr/Mo/ZSM-5 and Mo/ZSM-5.