

Supporting Information

**Modulation of supported Ni catalysts with phosphorus for the hydrogenation of diethyl oxalate to ethyl glycolate**

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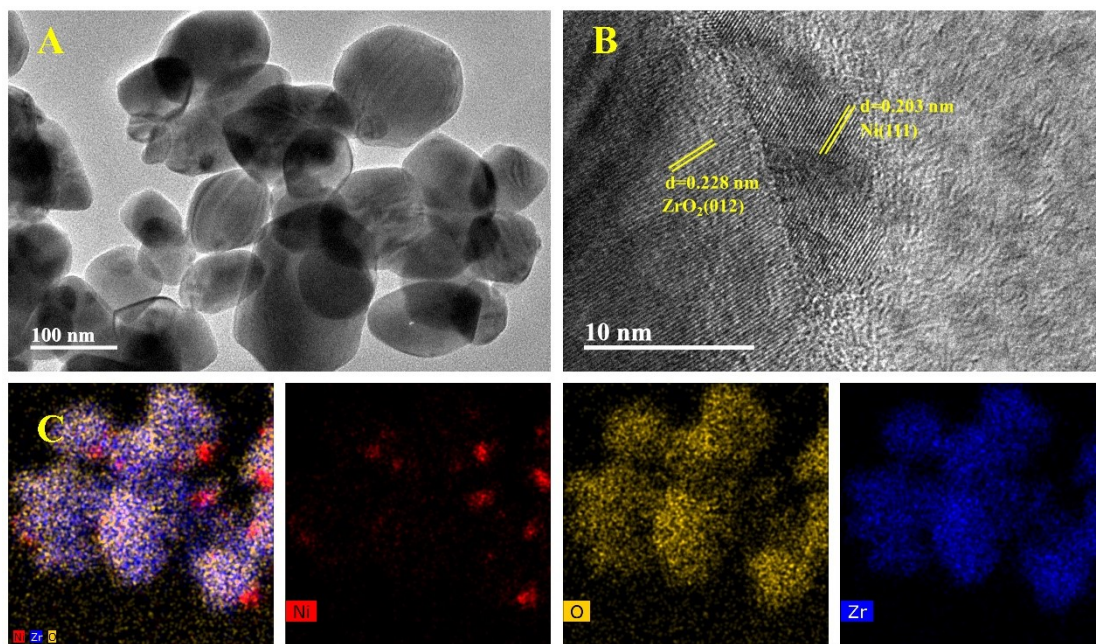


Fig.S1. TEM image and EDS mapping of 13-Ni/ZrO<sub>2</sub>.

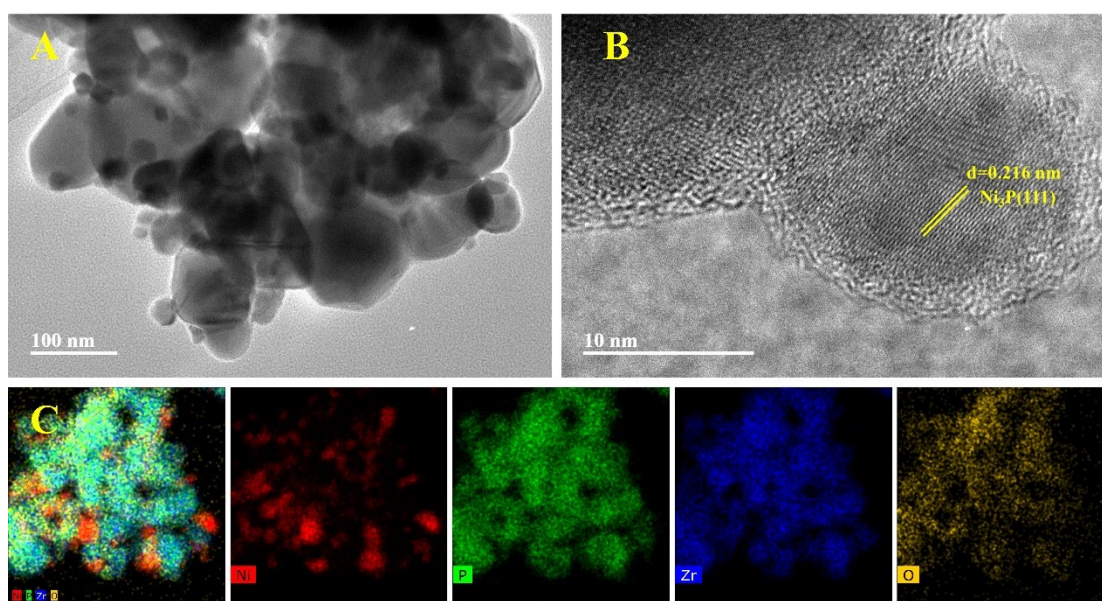


Fig.S2. TEM image and EDS mapping of 13-Ni<sub>3</sub>P/ZrO<sub>2</sub>.

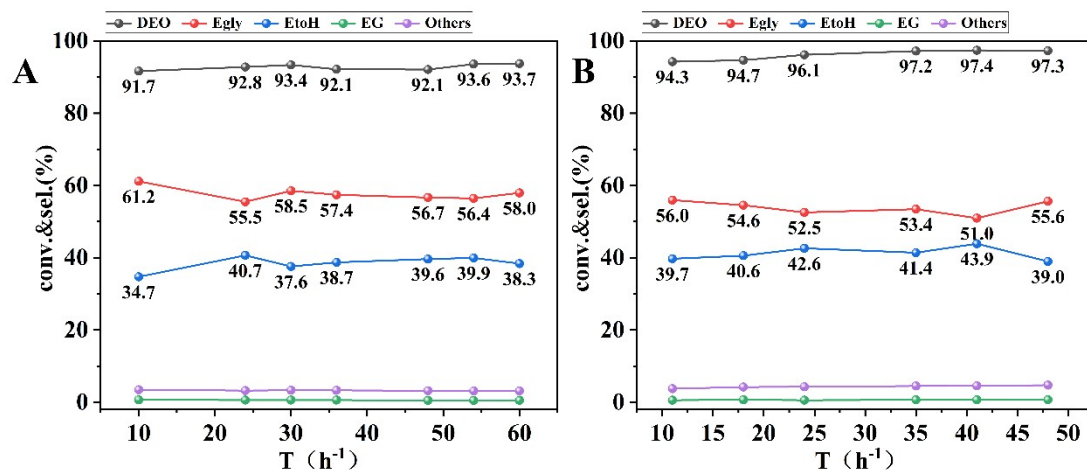


Fig.S3. DEO conversion and Egly selectivity versus time on stream over the 13-Ni<sub>3</sub>P/ZrO<sub>2</sub> catalyst. (A) reaction temperature 210°C, (B) reaction temperature 230°C (P=2.5MPa, H<sub>2</sub>/DEO molar ratio=120, WHSV= 1 h<sup>-1</sup>)

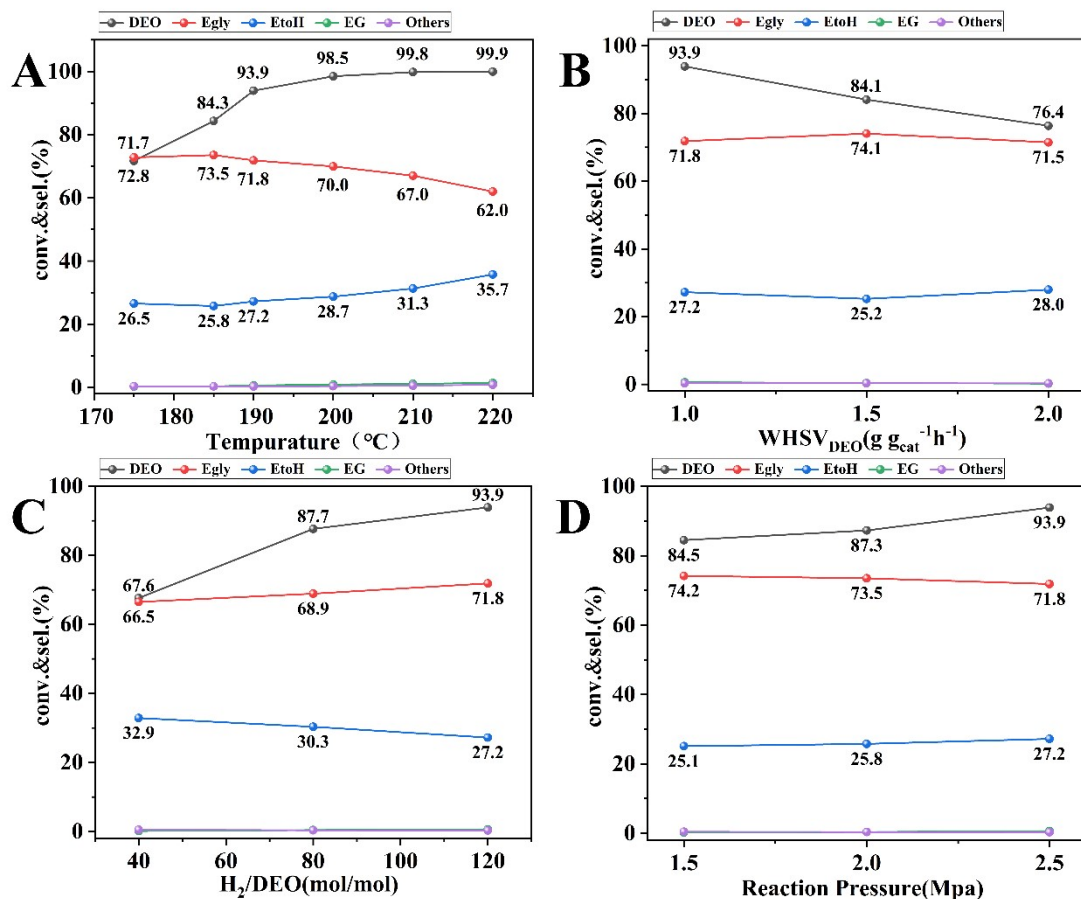


Fig. S4. Conversion and selectivity of the 13-Ni<sub>3</sub>P/SiO<sub>2</sub> catalyst under different reaction conditions. (A) reaction temperature (P=2.5MPa, H<sub>2</sub>/DEO molar ratio=120, WHSV= 1 h<sup>-1</sup>), (B) WHSV (T=190°C, P=2.5MPa, H<sub>2</sub>/DEO molar ratio=120), (C) H<sub>2</sub>/DEO molar ratio (T=190°C, P=2.5MPa, WHSV= 1 h<sup>-1</sup>), (D) reaction pressure (T=190°C, WHSV= 1 h<sup>-1</sup>, H<sub>2</sub>/DEO molar ratio=120).

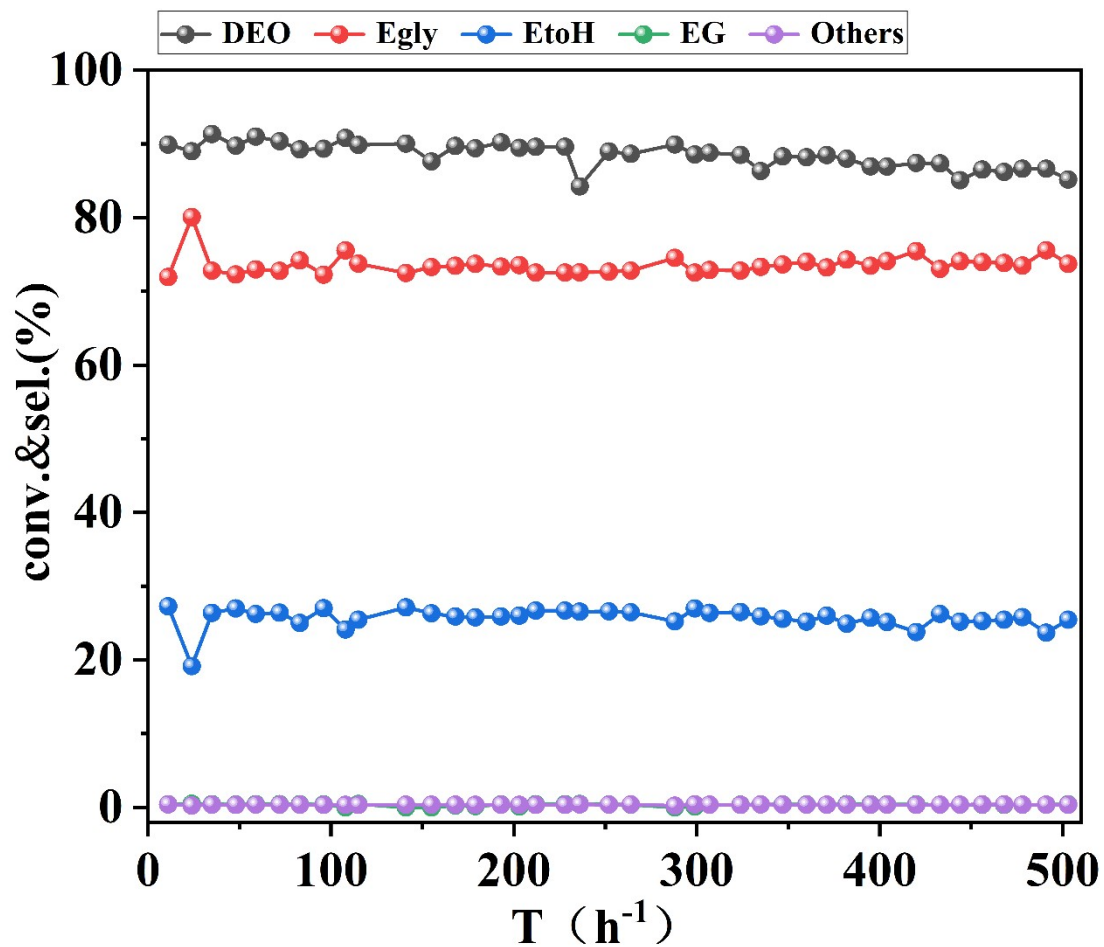


Fig. S5. Long-term performance of DEO hydrogenation over 13-Ni<sub>3</sub>P/SiO<sub>2</sub> catalyst. Reaction conditions: P=2.5MPa, T=190°C, H<sub>2</sub>/DEO molar ratio=120, WHSV= 1 h<sup>-1</sup>

The stability of the catalyst was also tested. As shown in Fig. S5, no significant loss of activity and selectivity was observed during the 500 h continuous test.

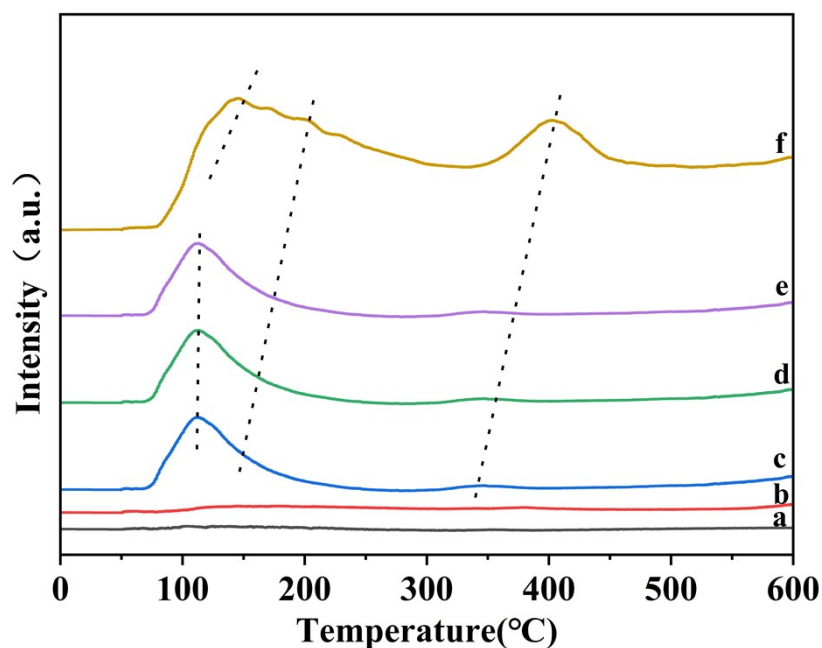


Fig. S6. NH<sub>3</sub>-TPD profiles of the (a) 13-Ni/ZrO<sub>2</sub>, (b) 13-Ni<sub>3</sub>P/ZrO<sub>2</sub>, (c) 6-Ni<sub>3</sub>P/SiO<sub>2</sub>, (d) 13-Ni/SiO<sub>2</sub>, (e) 13-Ni<sub>3</sub>P/SiO<sub>2</sub>, (f) 25-Ni<sub>3</sub>P/SiO<sub>2</sub>.

Fig. S6. shows the NH<sub>3</sub>-TPD profiles of the nickel-based catalyst. The low-temperature peak centered at 120°C observed in the spectra is attributed to the adsorption peak of the SiO<sub>2</sub> carrier itself<sup>[1]</sup>. The NH<sub>3</sub> desorption peak appearing as a shoulder at about 170°C is attributed to the adsorption at the weak acid sites. In addition, the weak adsorption peak at about 390°C is attributed to the adsorption of NH<sub>3</sub> on the medium-strength acid sites on the surface (Fig. S6.c-f)<sup>[2]</sup>. The ZrO<sub>2</sub>-loaded nickel-based catalysts did not show NH<sub>3</sub> desorption peaks (Fig. S6. a, b).

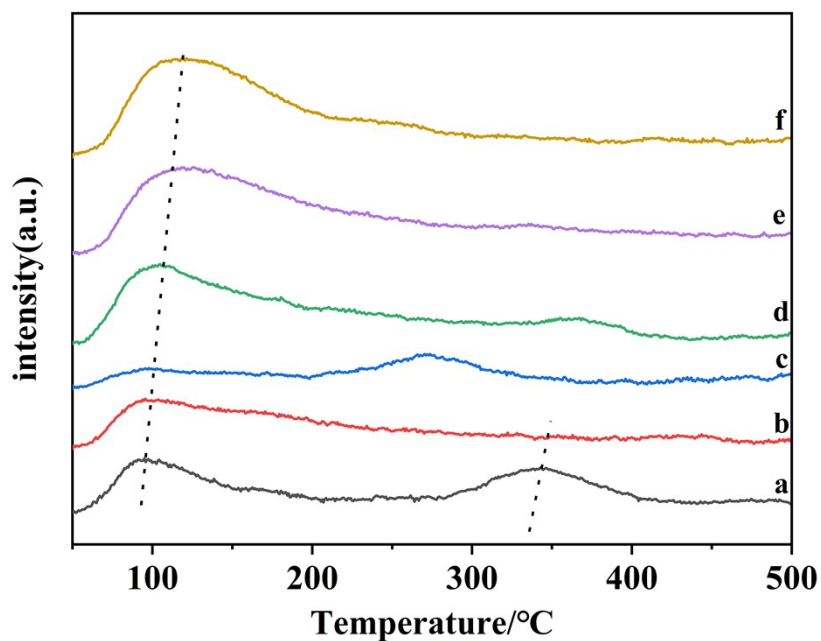


Fig. S7. CO<sub>2</sub>-TPD profiles of the (a)13-Ni/ZrO<sub>2</sub>, (b) 13-Ni<sub>3</sub>P/ZrO<sub>2</sub>, (c) 6-Ni<sub>3</sub>P/SiO<sub>2</sub>, (d) 13-Ni/SiO<sub>2</sub>, (e) 13-Ni<sub>3</sub>P/SiO<sub>2</sub>, (f) 25-Ni<sub>3</sub>P/SiO<sub>2</sub>.

CO<sub>2</sub>-TPD profiles (Fig. S7.) showed that the desorption peaks located at low temperatures (~100°C) were weakly basic sites, and the desorption peaks around 300°C were attributed to moderately strong basic sites<sup>[3]</sup>. As shown in Fig.S7.a,b and c-f, the moderate intensity basicity peak site is weakened after phosphorylation. Taking into account that the actual reaction temperature is around 200 °C, the medium-strength basicity plays a major role in DEO hydrogenation. However, the medium-strength basicity almost disappeared after phosphatization, indicating that the surface basicity has a relatively small effect on the catalyst reaction performance.

Table S1. Comparison of the 13-Ni<sub>3</sub>P/SiO<sub>2</sub> catalyst with the reported ones for the DMO/DEO-to-MG/Egly reaction.

Catalyst	T (°C)	P (Mpa)	H <sub>2</sub> /DMO (mol/mol)	WHSV (gg <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup> )	DMO/DEO Conv.(%)	MG/Egly Sel.%	Lifetime (h)	Ref
Ni <sub>2</sub> P/TiO <sub>2</sub>	230	3.0	300	0.1	100	76	3600	[4]
Ni <sub>3</sub> P/Ni-Foam	230	2.5	180	0.44	99.5	97	1000	[5]
Ni <sub>3</sub> P/RB-MSN	190	2.5	90	0.44	100	86	500	[1]
13-Ni <sub>3</sub> P/SiO <sub>2</sub>	210	2.5	120	1.0	100	67	No data	This
13-Ni <sub>3</sub> P/SiO <sub>2</sub>	190	2.5	120	1.0	94	72	500	work

## References

- [1] G. Zhao, *ACS Sustainable Chemistry & Engineering* **2021**, *9*, 16719-16729.
- [2] a)Y. Zhu, X. Kong, X. Li, G. Ding, Y. Zhu, Y.-W. Li, *Acs Catalysis* **2014**, *4*, 3612-3620; b)P. Wu, J. Zhang, Z. J. Huang, J. A. Chen, *Fuel* **2022**, 324.
- [3] F. Han, H. Liu, W. Cheng, Q. Xu, *Rsc Advances* **2020**, *10*, 33620-33627.
- [4] H. Chen, J. Tan, Y. Zhu, Y. Li, *Catalysis Communications* **2016**, *73*, 46-49.
- [5] J. Zhu, L. Cao, C. Li, G. Zhao, T. Zhu, W. Hu, W. Sun, Y. Lu, *ACS Appl Mater Interfaces* **2019**, *11*, 37635-37643.