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Supplementary information

Hierarchical submicrosized Y zeolites prepared by sequential desilicationdealumination post-synthesis modification and their catalytic performance in vacuum gas oil hydrocracking

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Scheme 1S. post-synthesis modifications of nanozeolite NaY.





Figure 1S. SEM imagens of parent and modified zeolites





















Figure 2S. TEM imagens of parent and modified zeolites



Figure 3S. FT-IR spectra of NaY and modified zeolites.



Figure 4S. Position of absorption band of zeolites at ~1000 cm⁻¹ as a function of the Si/A1 ratio framework



Figure 5S. Ammonia (NH₃-TPD) profiles of Y zeolites



Figure 68. Conversion of the catalysts in vacuum gas oil hydrocracking



Figure 7S. Selectivity to middle distillate of the catalysts in vacuum gas oil hydrocracking

Catalysts	Hydrocracking conversion (%)	Selectivity (%)	Yield (%)
		Middle distillate	
HY	12	81	10
HY0.5	10	69	7
HY1.0	9	74	7
HY0.5S	82	5	4
HY0.5(2S)	76	4	3
HY1.0S	77	3	2
HY1.0(2S)	76	6	5
HYS	74	8	5
HYS0.5	73	9	5
HYS1.0	63	6	3

Table 1S: Average produced conversion, selectivity and yields in VGO hydrocracking after $$370^\circ \rm C$$

Middle distillates: B.P. in the range 180–370°C.



Figure 8S. Correlation between Brønsted acid site concentration - H⁺ and conversion (%) (taken from Table 4 and Table 5). 1. HY0.5S; 2. HY0.5(2S); 3. HY1.0S; 4. HY1.0(2S); 5. HYS; 6. HYS0.5; 7. HYS1.0