

Influence of Mo modification on coaromatization of methanol and n-hexane over [ZnMo]/HZSM-5 catalyst

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Table S1 XRD lattice constants for synthesized [Zn_xMo]/HZ-5

Sample	Cell parameters					
	a	b	c	α	β	γ
HZ-5	20.10	19.92	13.39	90	90	90
Zn/HZ-5	20.14	19.95	13.43	90	90	90
Zn-1Mo/HZ-5	20.15	19.94	13.43	90	90	90
Zn-3Mo/HZ-5	20.12	19.93	13.41	90	90	90
Zn-5Mo/HZ-5	20.13	19.92	13.40	90	90	90

Table S2. Acidity determined by NH₃-TPD

Catalyst	WAS		SAS		Total
	T(°C)	amount	T(°C)	amount	amount
		(mmol/g)		(mmol/g)	
HZ-5	198	0.452	423	0.280	0.732
Zn/HZ-5	197	0.436	413	0.078	0.514
Zn-1Mo/HZ-5	208	0.474	410	0.048	0.522
Zn-3Mo/HZ-5	196	0.495	402	0.037	0.532
Zn-5Mo/HZ-5	195	0.545	415	0.010	0.555

Table S3 Textural properties of the spent HZ-5, spent Zn/HZ-5 and spent Zn-3Mo/HZ-5.

Sample	S _{BET} ^[a] (m ² /g)	S _{mic} (m ² /g)	S _{ext} ^[b] (m ² /g)	V _{total} (cm ³ /g)	V _{mic} (cm ³ /g)	V _{meso} ^[c] (cm ³ /g)
spent HZ-5	296.1	255.5	40.6	0.19	0.11	0.08
spent Zn/HZ-5	247.7	220.9	26.8	0.14	0.10	0.04
spent Zn-3Mo/HZ-5 (10h)	218.2	187.3	30.9	0.16	0.08	0.08
spent Zn-3Mo /HZ-5 (24h)	138.4	116.4	21.7	0.12	0.05	0.07

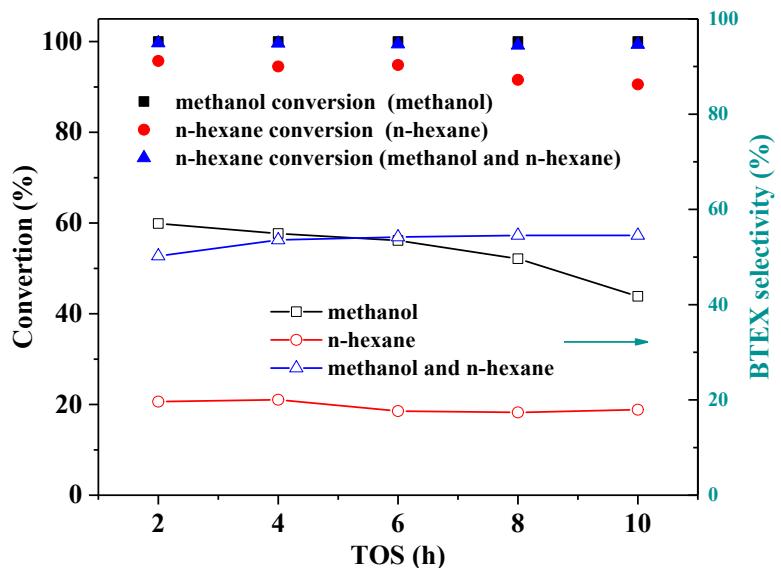


Fig. S1 Conversion and BTEX selectivity for different feedstocks. Reaction conditions: $T=470\text{ }^{\circ}\text{C}$, $\text{WHSV}=1.0\text{ h}^{-1}$, $\text{TOF}=2\text{ h}$)

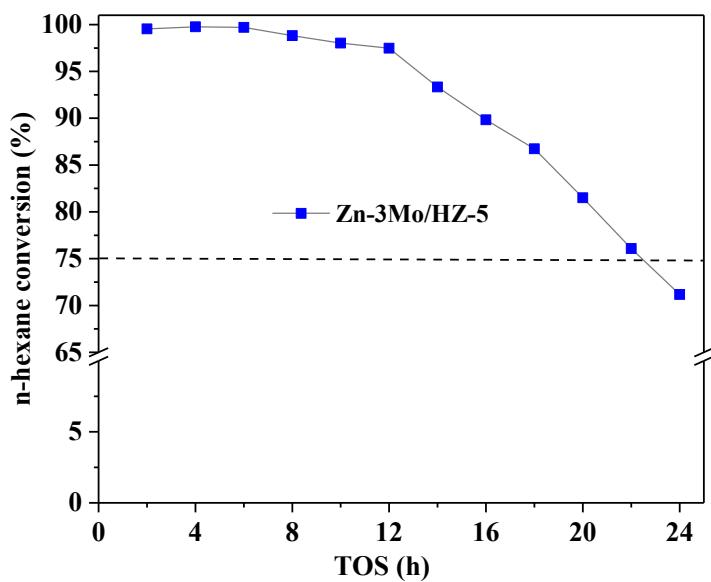


Fig. S2. n-hexane conversion over Zn-3Mo/HZ-5 catalyst.

Reaction conditions: methanol/n-hexane = 7:3, $T = 470\text{ }^{\circ}\text{C}$, and $\text{WHSV} = 1.0\text{ h}^{-1}$.